

OPPORTUNITIES AND CHALLENGES OF LIQUID HYDROGEN SUPPLY CHAIN



Amgad Elgowainy, PhD

Senior Scientist and Group Leader

Ed Frank, PhD

Principal Energy Systems Scientist

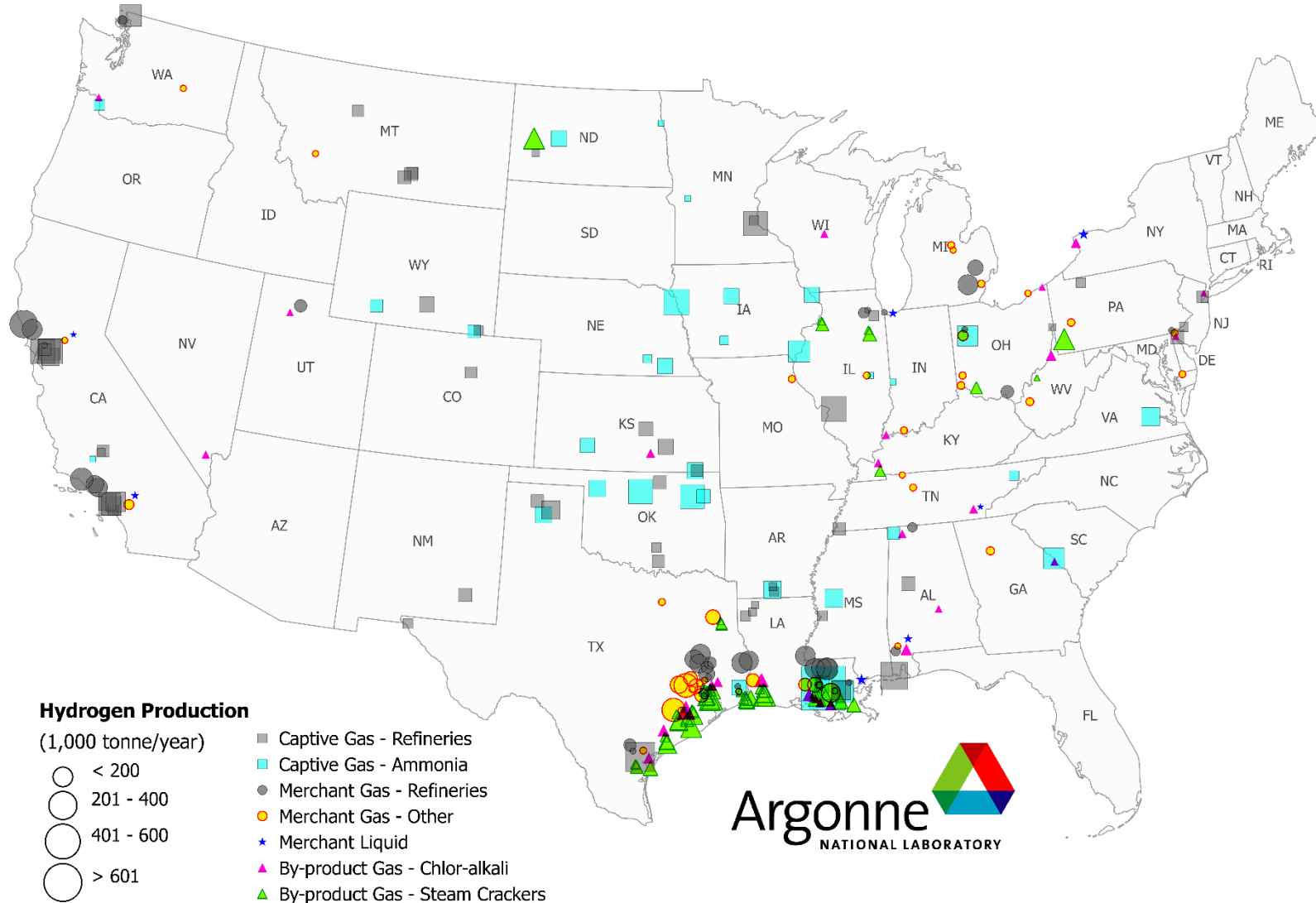
Argonne National Laboratory

Presentation at Liquid Hydrogen Technologies Workshop

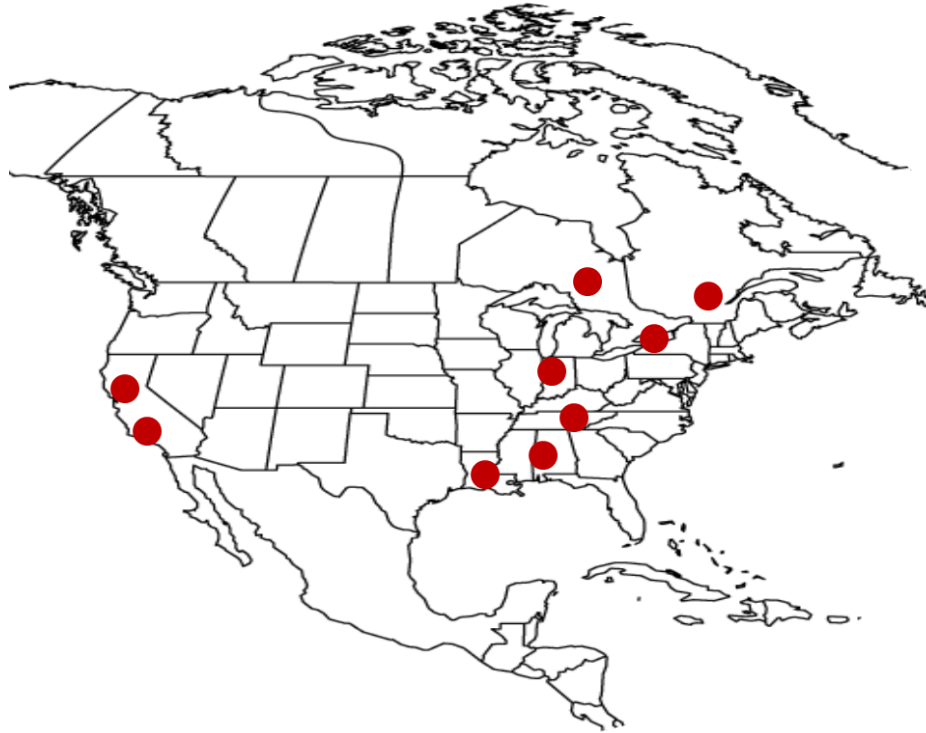
February 22, 2022

Today, more than 10M metric tons of hydrogen are produced in the U.S. annually near their end use

1600 mi. of H₂ pipeline; 10 Liquefaction plants in North America



~260 MT/day H₂ liquefaction capacity in North America

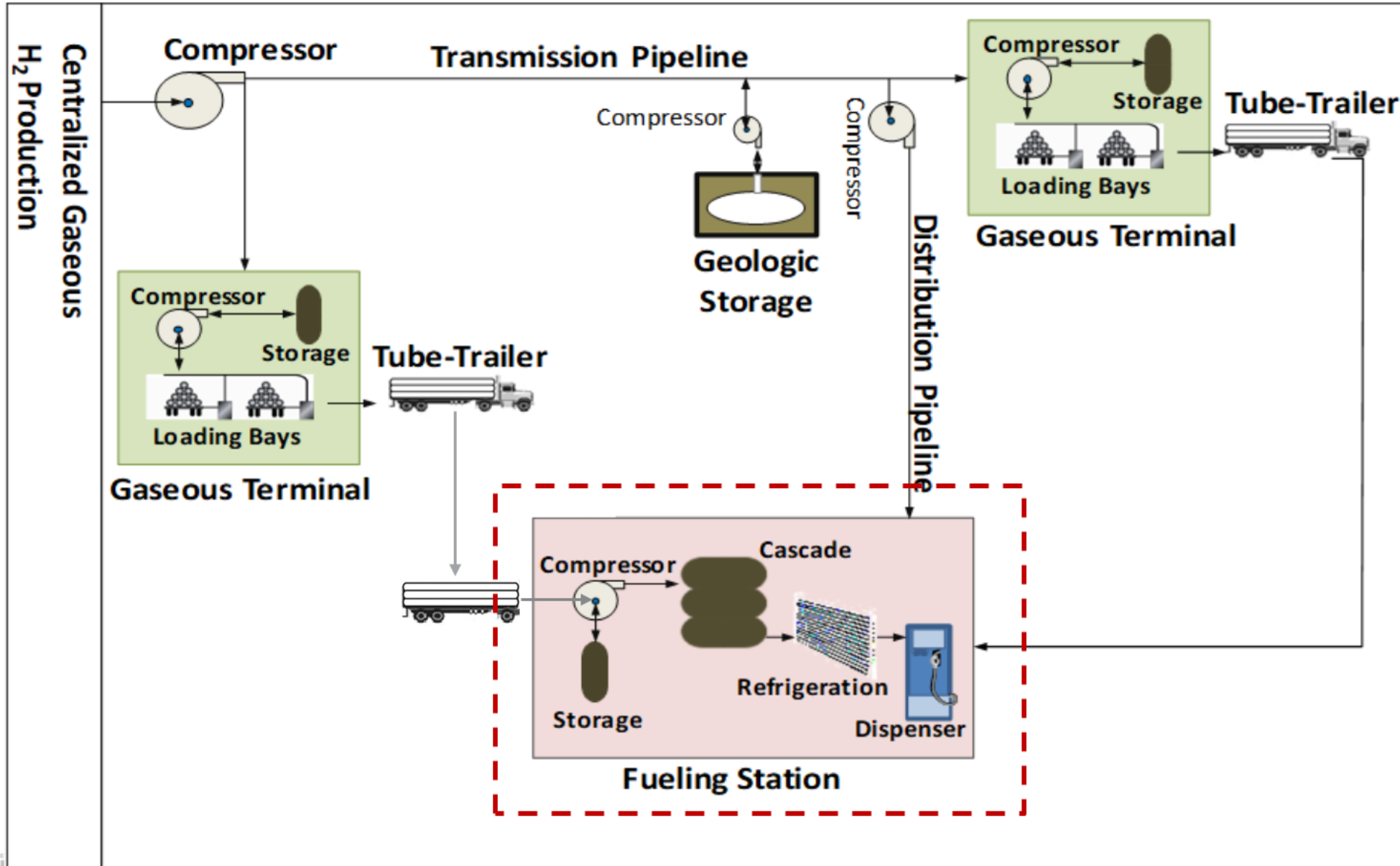


Region	Liquefaction Capacity (MT/day)
California	30
Louisiana	70
Indiana	30
New York	40
Alabama	30
Ontario	30
Quebec	27
Tennessee	6
Total	263

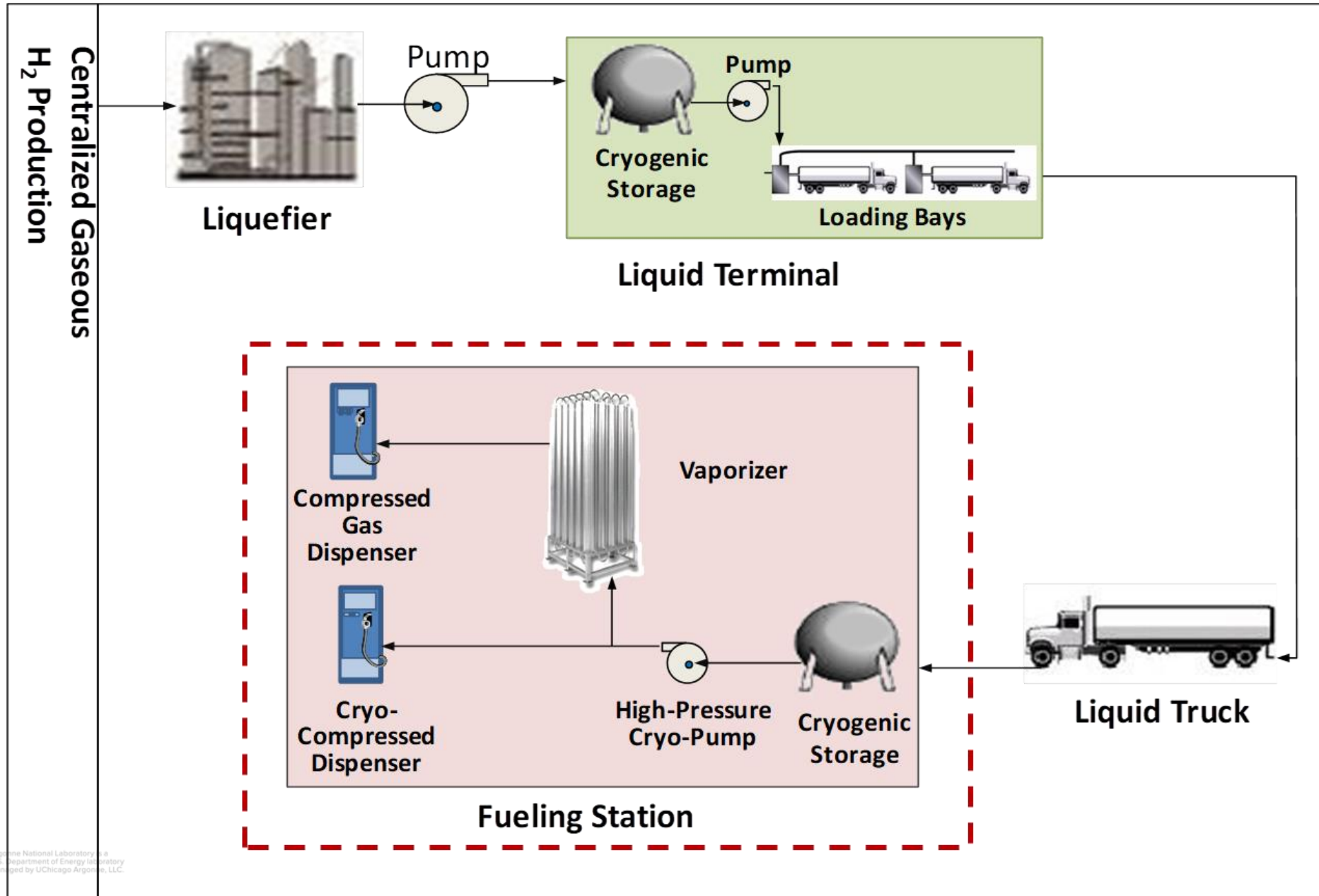
→ Liquefaction energy intensity = 10-15 kWhe/kg_{H₂}

Four additional H₂ liquefaction plants have been recently announced to serve the growing H₂ market

Infrastructure of gaseous hydrogen delivery



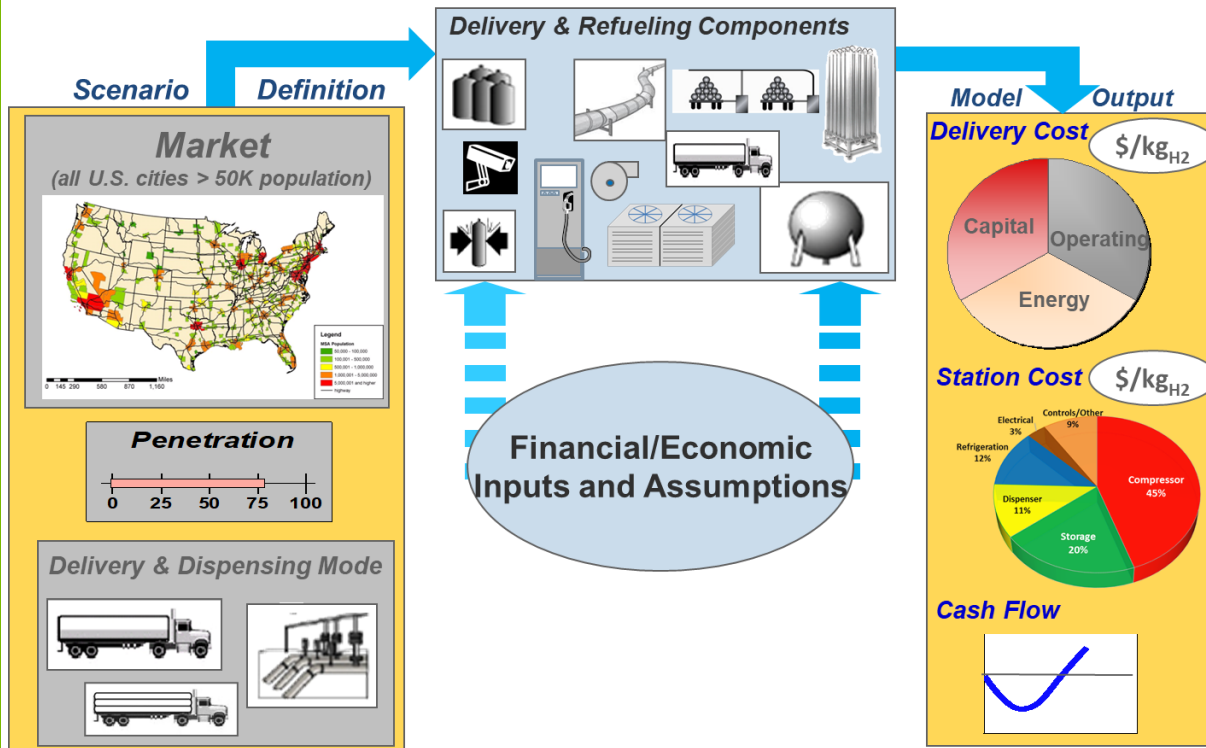
Infrastructure of liquid hydrogen delivery



Argonne models evaluate techno-economics and environmental implications of H₂ production and delivery

HDSAM

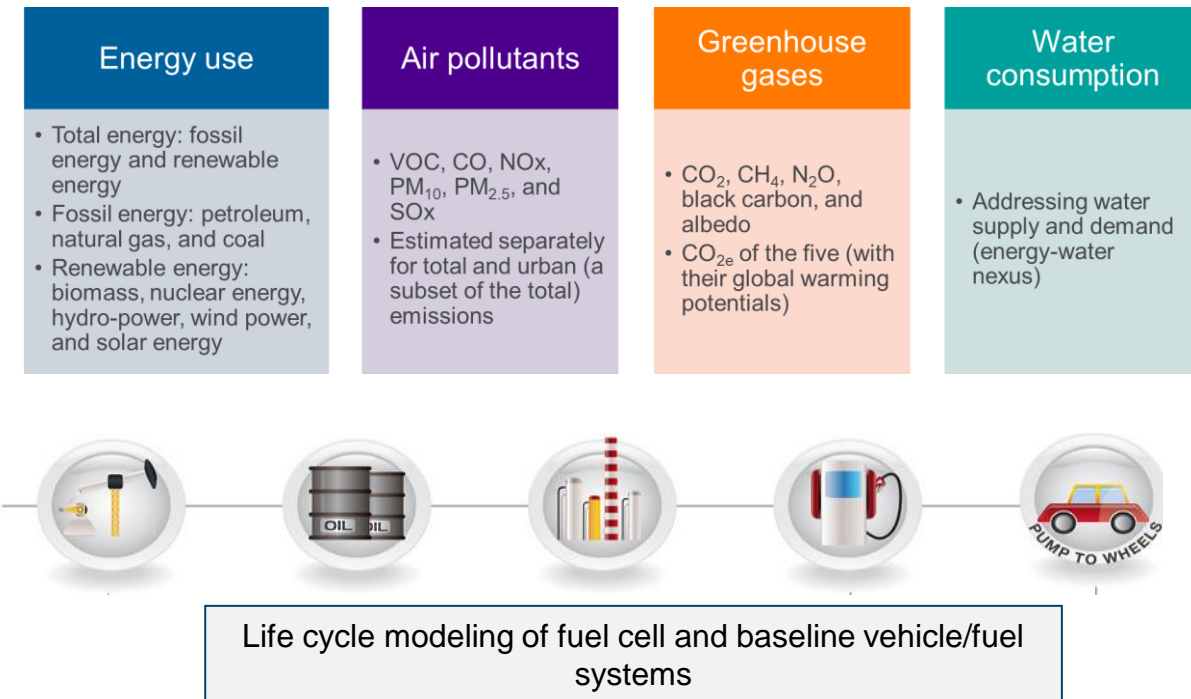
Techno-economic Evaluation



<https://hdsam.es.anl.gov/>

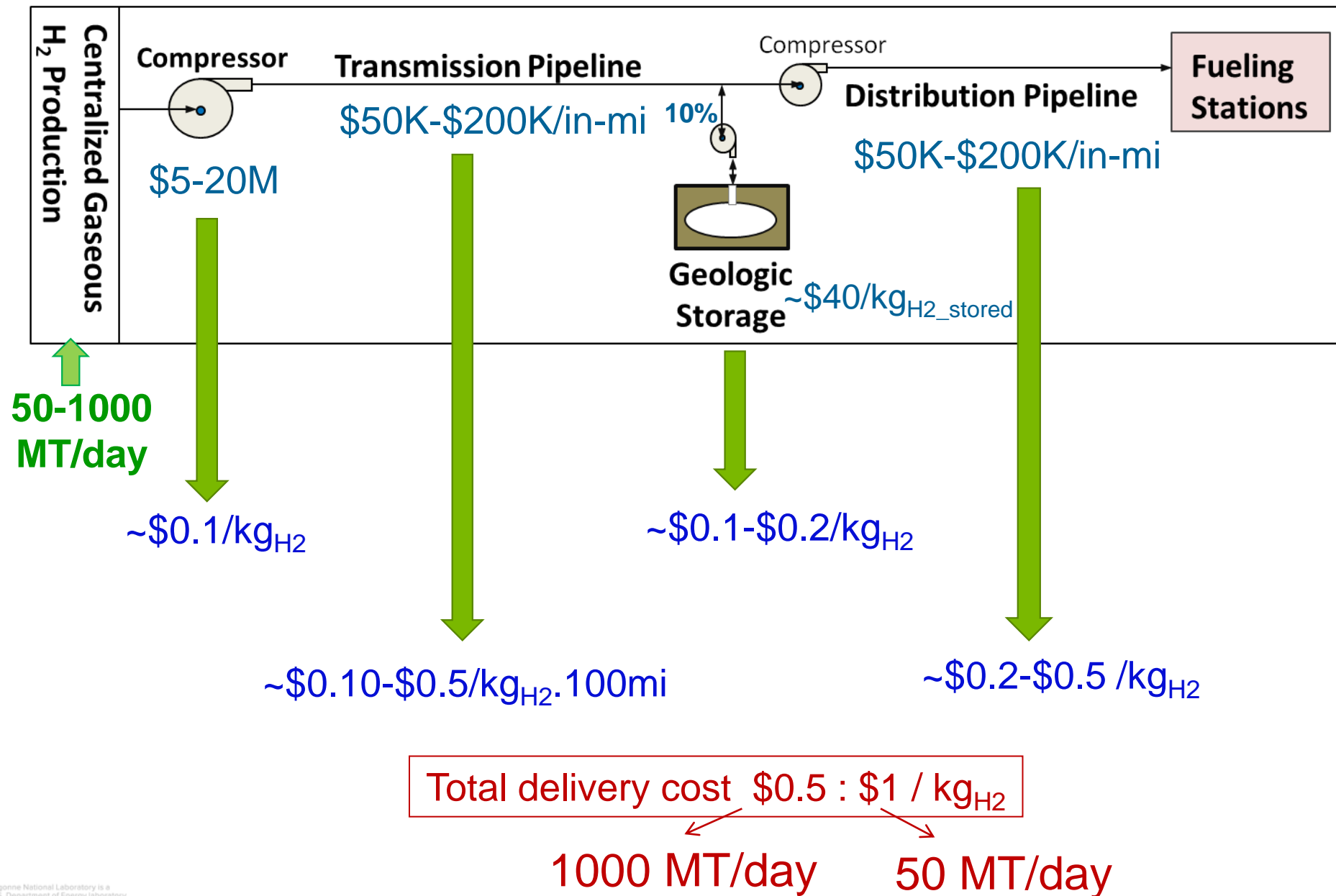
GREET

Environmental Life Cycle Evaluation

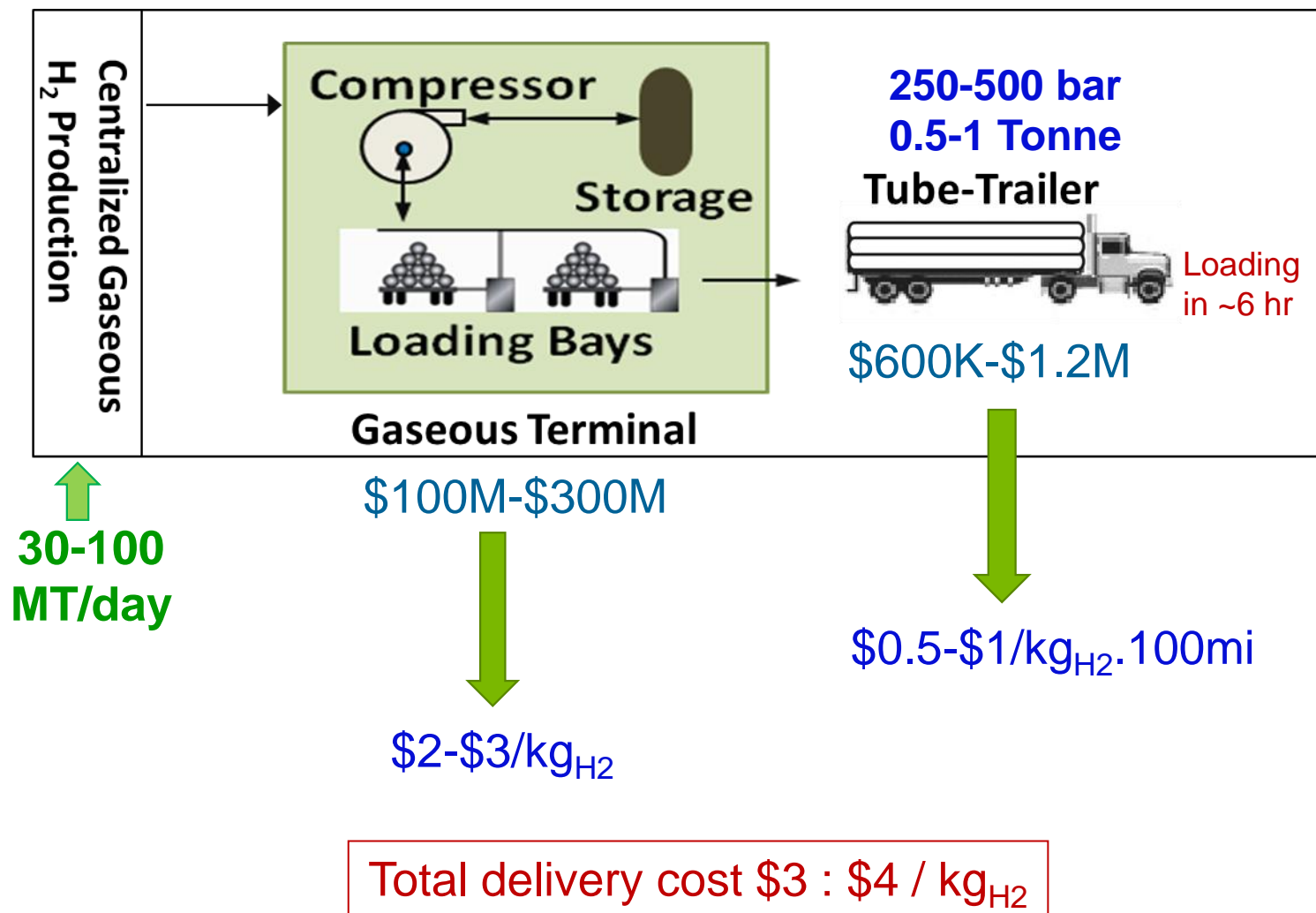


<https://greet.es.anl.gov/>

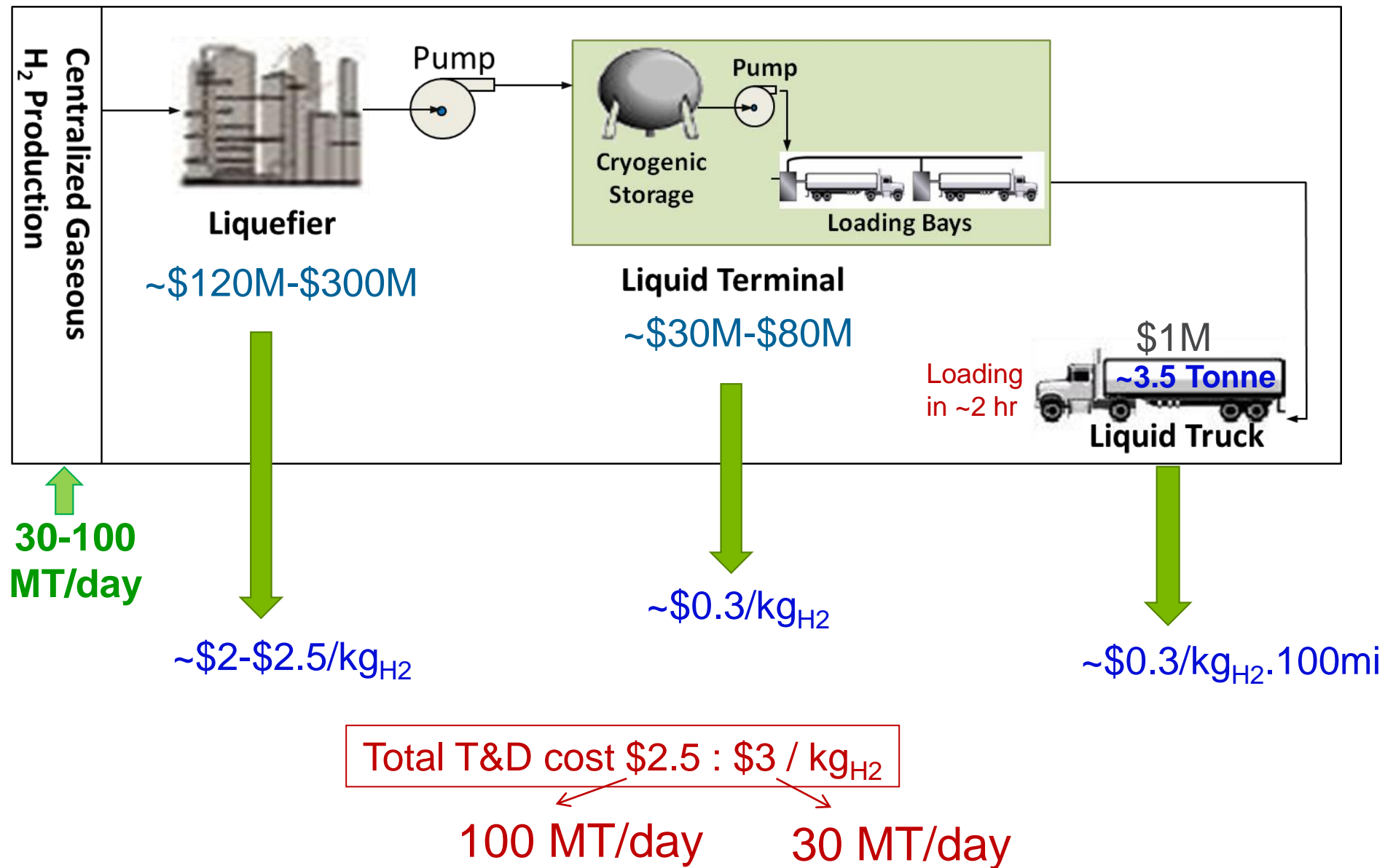
Cost contribution of pipeline delivery



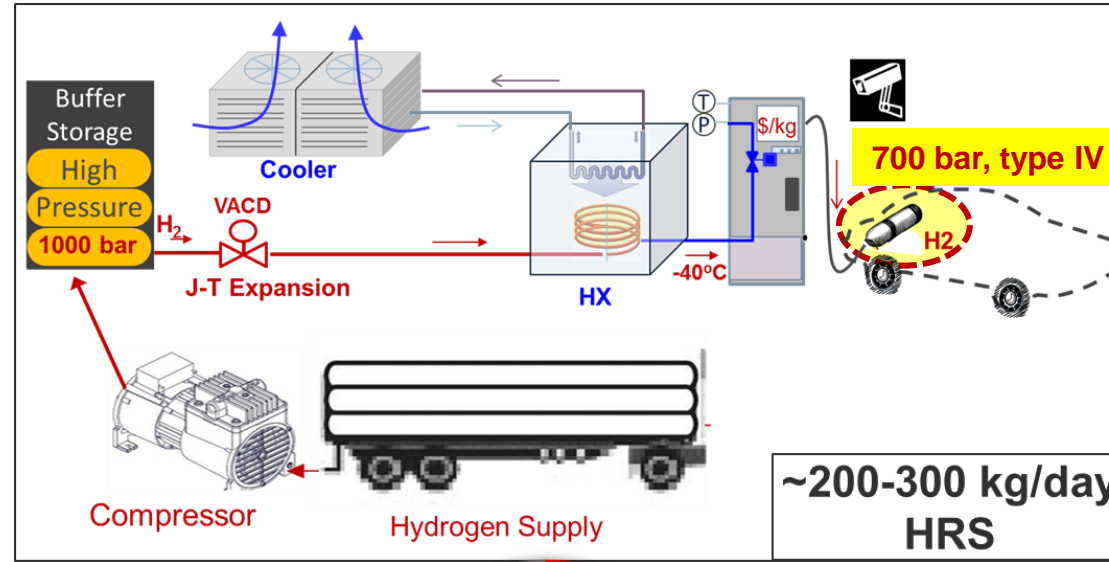
Cost contribution of tube-trailer delivery



Cost contribution of LH₂ delivery

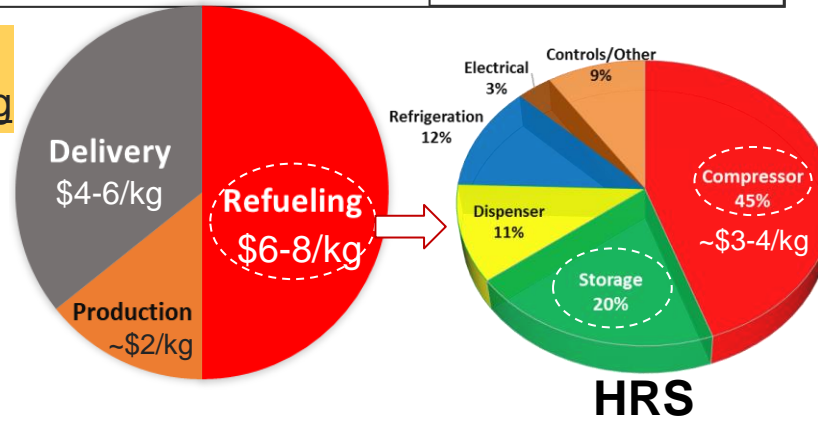


Cost of Hydrogen Delivery and Refueling for LD FCEVs is strongly driven by onboard storage requirement



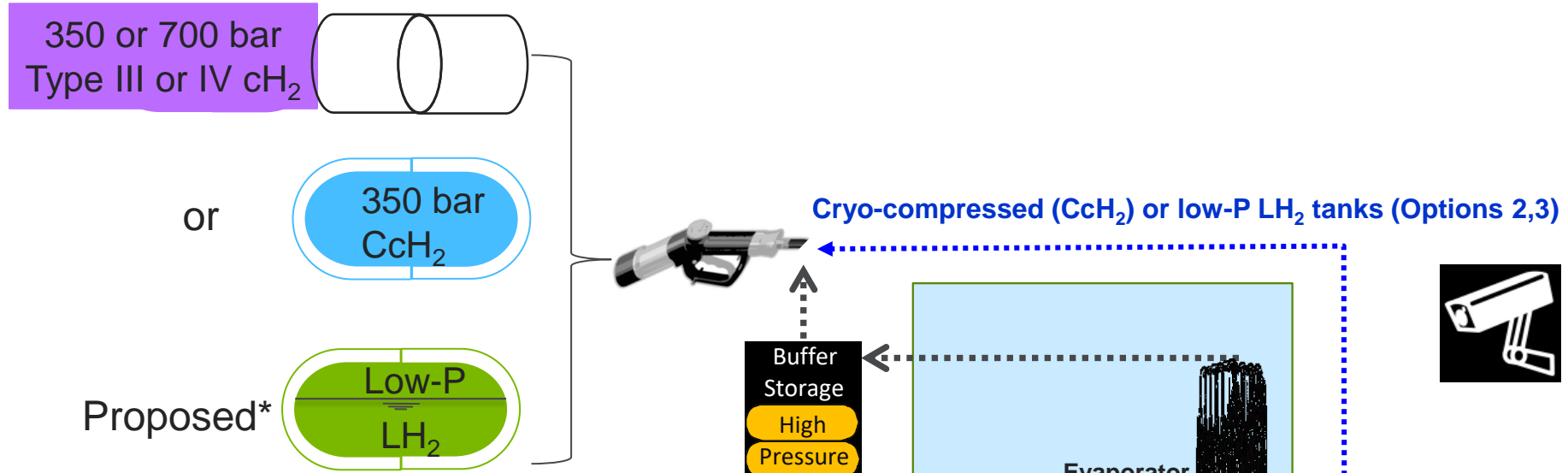
Today, hydrogen cost at the dispenser in CA is **\$15-\$16/kg**

Bulk of H₂ cost is in delivery and refueling

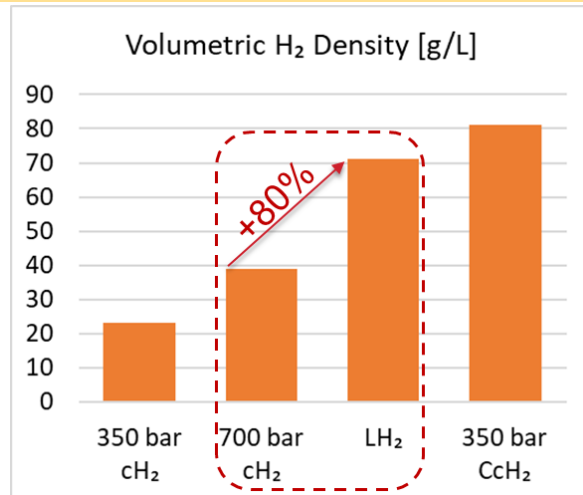


✓ HX: Heat Exchange	✓ VACD: Variable Area Control Device
✓ J-T: Joule-Thomson	✓ CA: California

Versatile refueling configuration options with LH₂ delivery



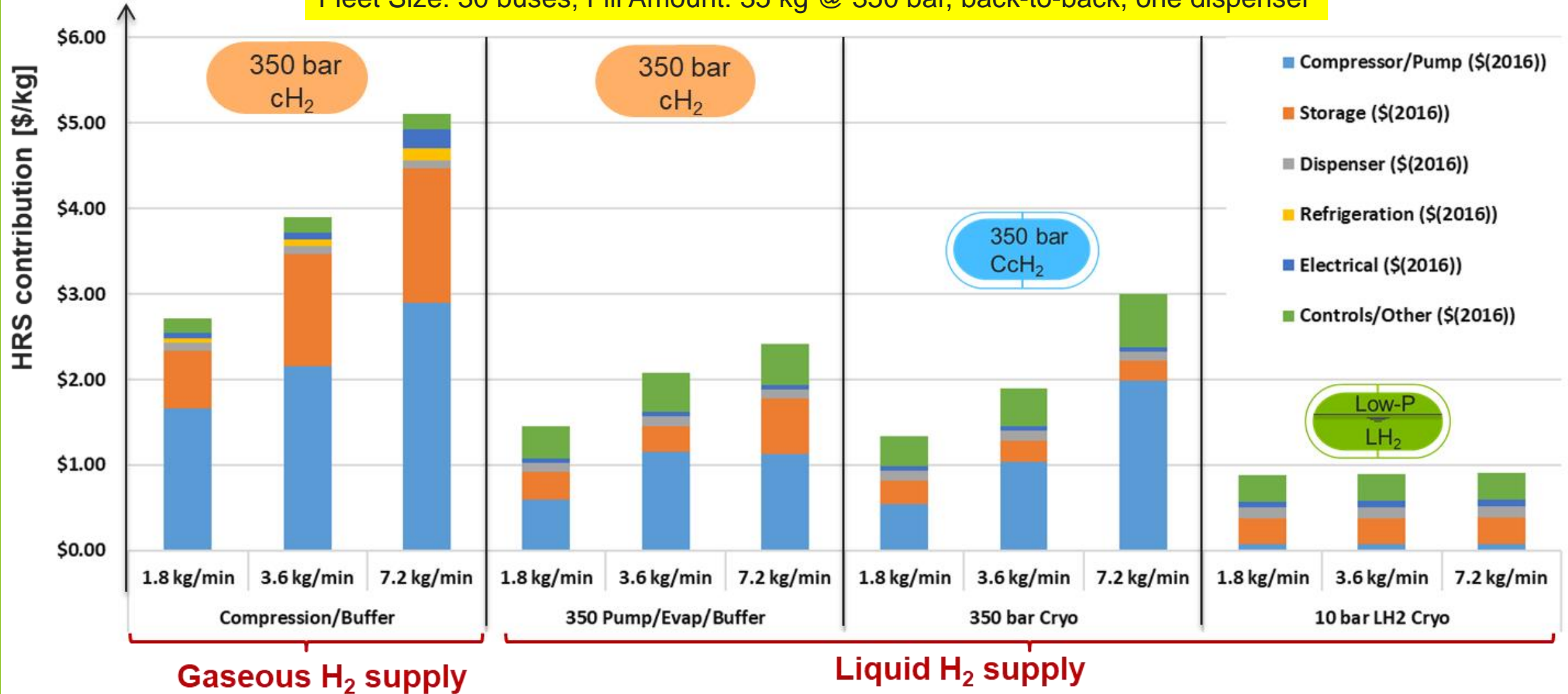
*Dormancy may be less of an issue with a predictable duty cycle of M/HDVs



- ✓ LH₂: Liquid Hydrogen
- ✓ CcH₂: Cryo-compressed hydrogen
- ✓ cH₂: compressed hydrogen
- ✓ Low-P: Low Pressure (<10 bar)

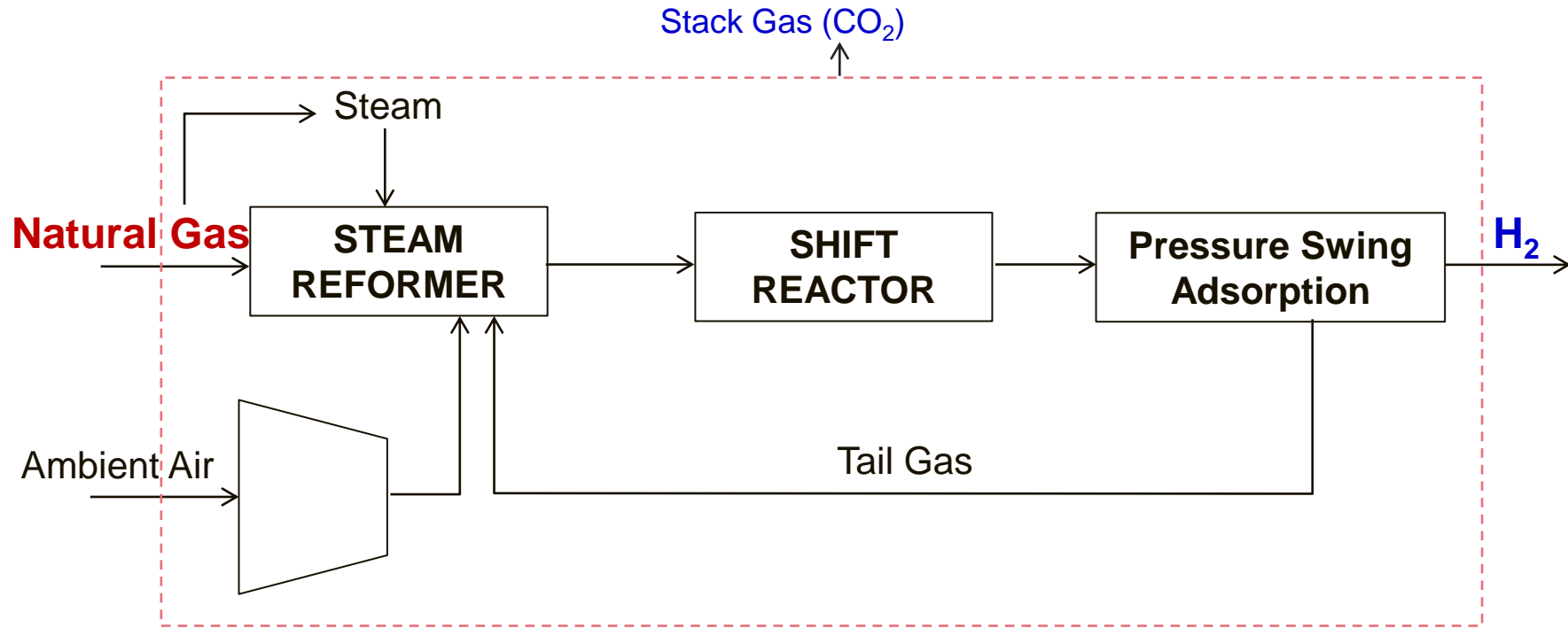
Compression and pumping dominate refueling cost for high-pressure tanks

Fleet Size: 30 buses; Fill Amount: 35 kg @ 350 bar, back-to-back, one dispenser



- Liquid supplied stations can handle faster fills with less cost increase compared to gaseous supply
- Cost of H₂ delivered to the station is additional

Hydrogen production today is mainly from NG SMR



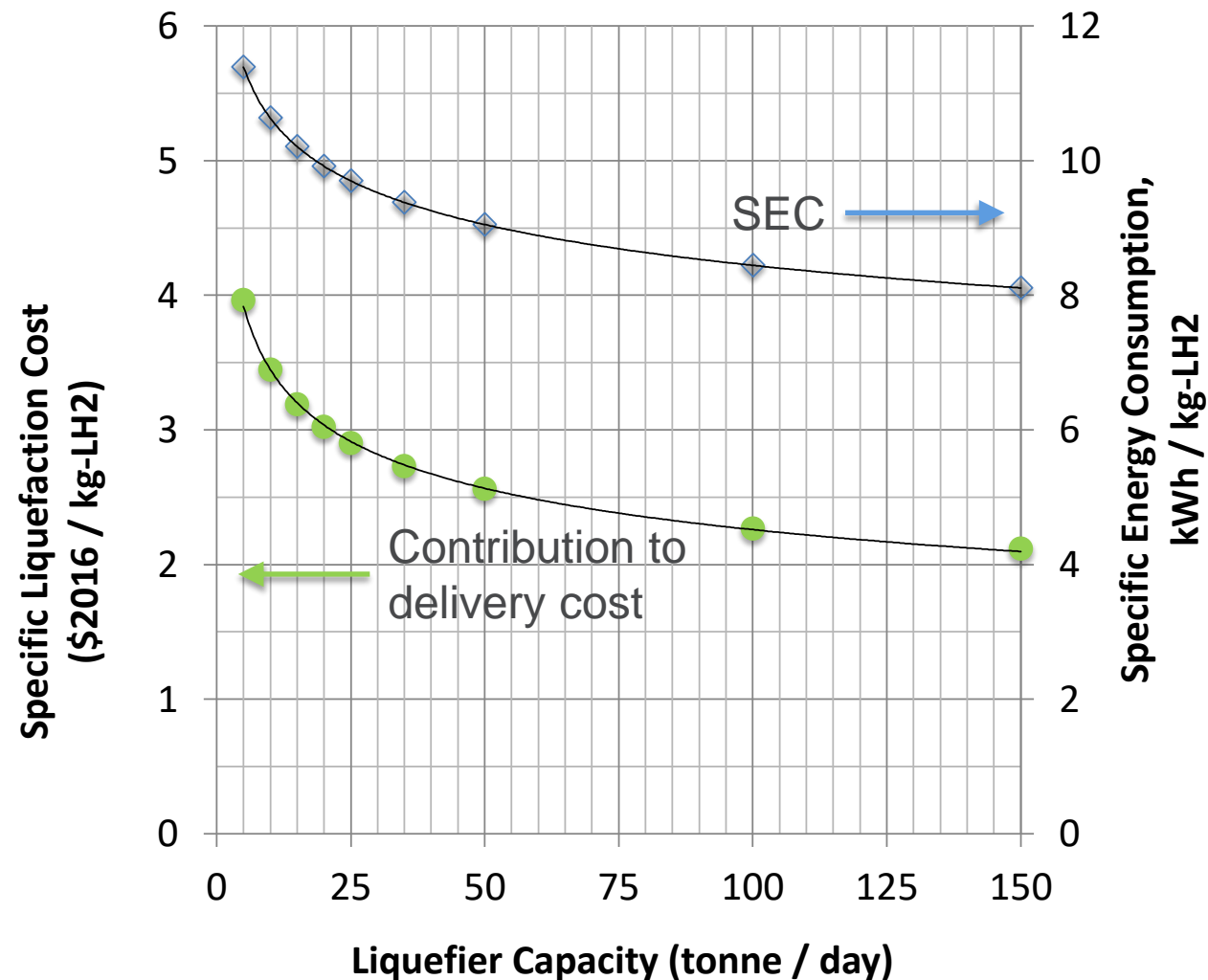
✓ SMR: Steam Methane Reforming
✓ NG: Natural gas
✓ LHV: Lower Heating Value
✓ WTW: Well-To-Wheels
✓ E10: 10% ethanol in gasoline (by vol.)
✓ GGE: Gallon Gasoline Equivalent
✓ ICEV: Internal Combustion Engine Vehicle

At 72% **NG** to **H₂** energy efficiency (LHV-basis)

→ Well-to-plant gate GHG emissions = 10 kg_{CO_{2e}}/kg_{H₂}

HDSAM liquefaction model

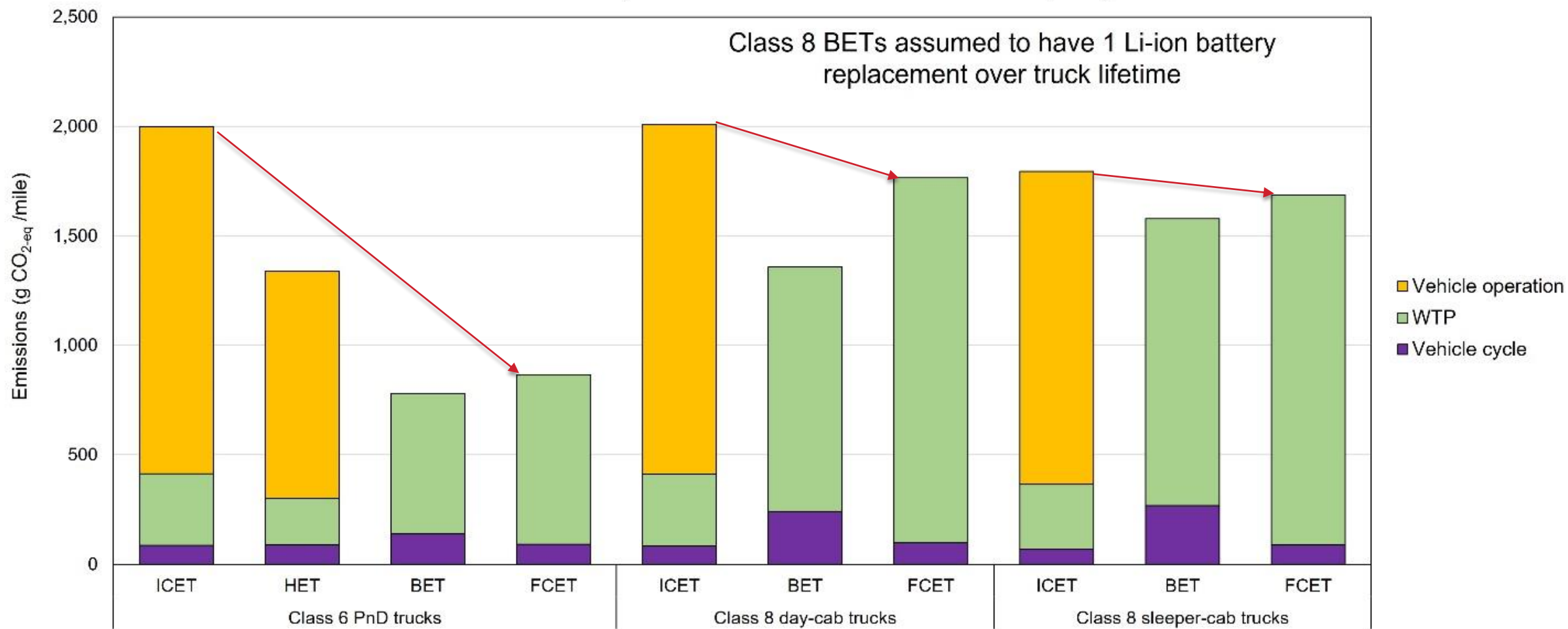
- Scaling laws based on aggregation of industry input
 - Liquefier CAPEX
 - Specific energy consumption (SEC)
- Modeling and analysis in the literature suggest SEC can potentially be as low as 6 kWh/kg
- SLC – Specific liquefaction cost



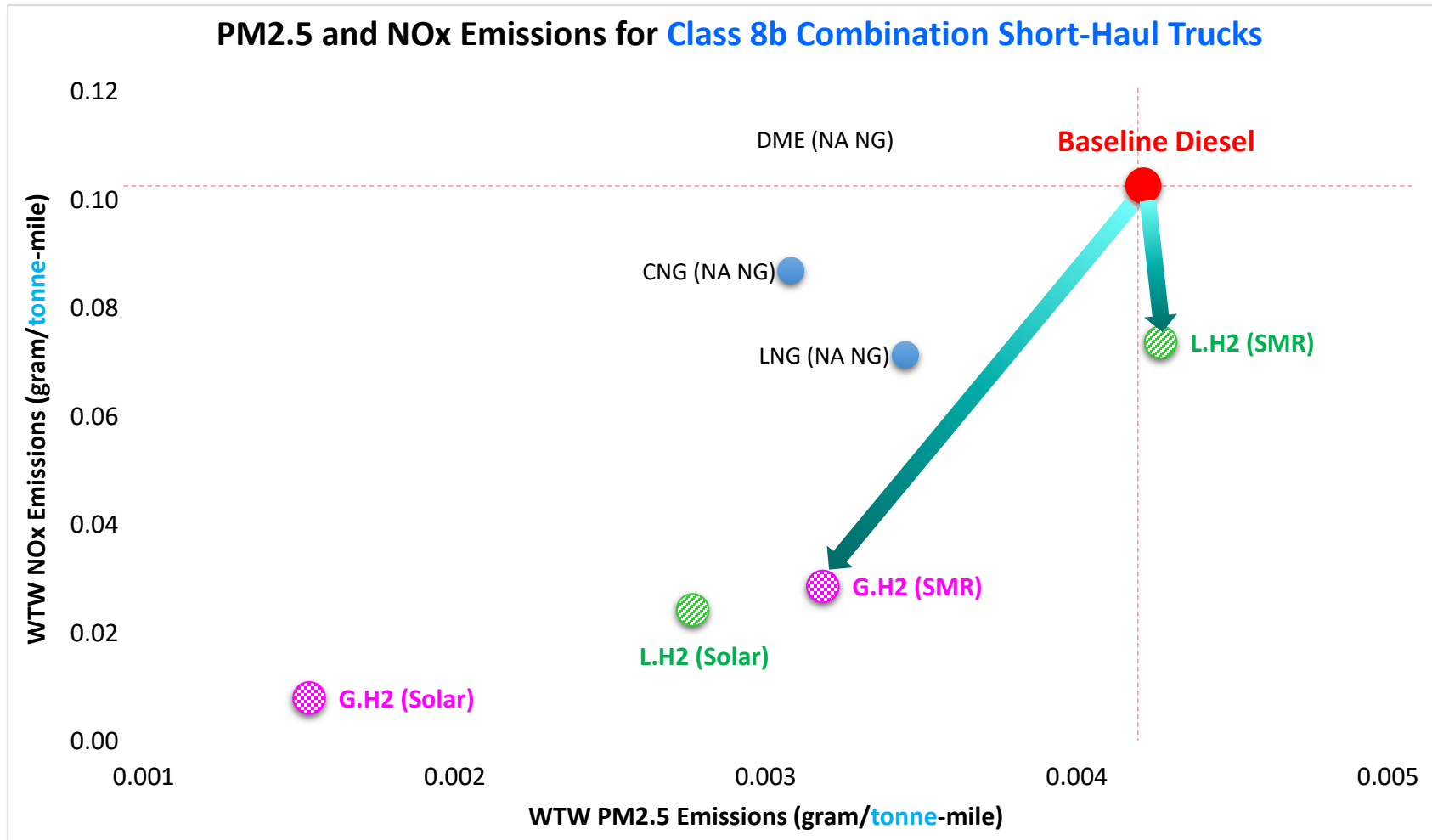
Delivered	Liquefier	SLC	SEC	GHG Emissions 2021 (US mix)
	5 tpd	\$4.0 / kg-LH2	11 kWh / kg	4.8 kgCO _{2e} / kgH ₂
30 tpd	33 tpd	\$2.8 / kg-LH2	9.4 kWh / kg	4.1 kgCO _{2e} / kgH ₂
120 tpd	130 tpd	\$2.1 / kg-LH2	8.2 kWh / kg	3.6 kgCO _{2e} / kgH ₂

Complete C2G GHG emissions: gaseous supply (i.e., not including liquefaction GHG emissions)

MHDVs: Life-cycle GHG emissions – Baseline scenario (2021)



Liquefaction: life-cycle criteria air pollutant emissions can also be significant



LH₂ impacts criteria air pollutant emissions depending on electricity grid mix used for liquefaction (US grid mix used for the above graph)

Thank You!
aelgowainy@anl.gov
efrank@anl.gov

***Our models and publications are
available at:***
<https://hdsam.es.anl.gov/>
<https://greet.es.anl.gov/publications>