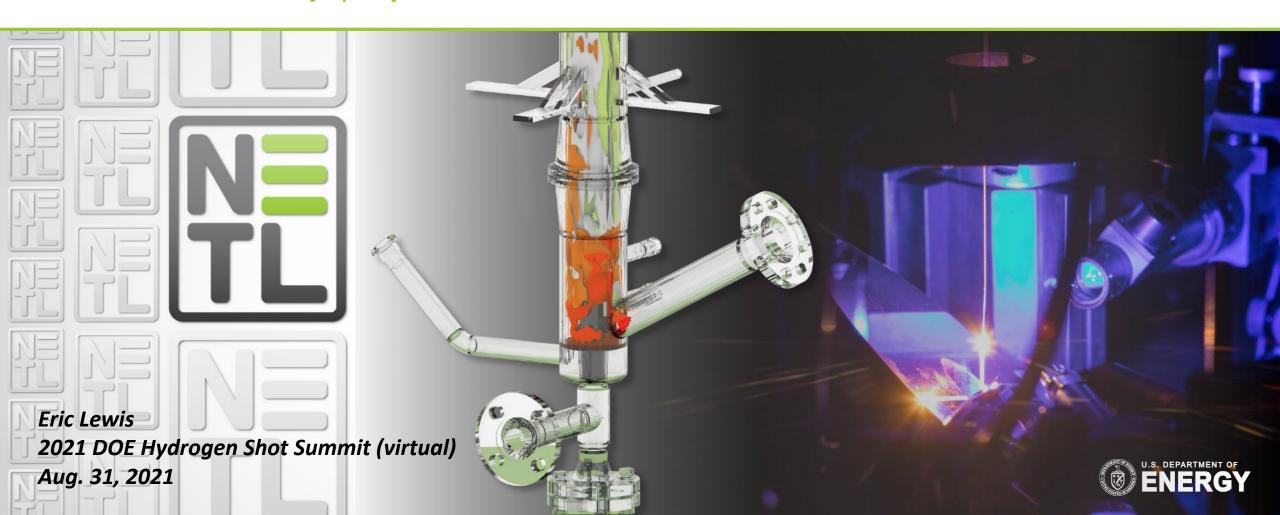
Overview of Integrated Pathway Analyses to Meet the Hydrogen Energy Earthshot Goal



Solutions for Today | Options for Tomorrow



NETL H₂ Production Systems Analyses

NATIONAL ENERGY TECHNOLOGY LABORATORY

Current Studies

- Comparison of Commercial, State-of-the-Art, Fossil-Based Hydrogen Production Technologies
 - NETL Internal Report <u>Complete</u>
 - Peer Reviewed Report Publication <u>In Progress</u>
- Hydrogen Energy Earthshot Initiative Screening Analysis <u>In Progress</u>





Project Summary

Objectives

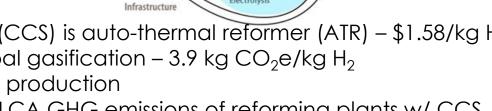
- Develop a reference study of H₂ production technologies using current, commercial technologies¹ with emphasis on coal gasification, co-gasification of coal with an alternative feedstock, and NG technologies using the levelized cost of hydrogen (LCOH) (2018 \$/kg) as the figure of merit
- Identify areas of R&D to further improve the performance and cost of fossil fuel-based H₂ production, including follow-on analyses

Justification

 Provide a baseline reference for DOE Office of Fossil Energy and Carbon Management (FECM) R&D program planning to reduce the LCOH and greenhouse gas (GHG) footprint of future fossil-to-H₂ plants

Highlights

- Lowest LCOH of cases examined w/ carbon capture and storage (CCS) is auto-thermal reformer (ATR) \$1.58/kg $\rm H_2$
- Lowest LCA GHG profile of fossil-only cases examined w/ CCS is coal gasification 3.9 kg CO₂e/kg H₂
- Co-gasifying 43.5 wt.% biomass with coal enables net-zero GHG H₂ production
- NG supply chain and grid electricity are significant contributors to LCA GHG emissions of reforming plants w/ CCS



Electric Grid

Natural Gas,

1 Commercial technologies are considered process systems that do not face fundamental R&D challenges within the plant flowsheets considered and at the scales studied



Source: NETL



Case Matrix

Case	Plant Type	Feedstock(s)	Reformer Type	Gasifier Type	CO ₂ Capture ^A	H ₂ Purification	Hydrogen Production Capacity	Lifecycle Emissions Target (kg CO ₂ e/kg H ₂)	
1	Reforming		SMR	-	0%	PSA	200 MMSCFD (Single Train SMR Max)		
2	Reforming	Natural Gas			96.2%				
3	Reforming		ATR		94.5%		274MMSCFD (Match H_2 output of Cases 4 and 5)	N/A	
4	Gasification		-	Shell	0%		274 MMSCFD (BBR Rev. 4 Case B1B Shell Gasifier Capacity)		
5	Gasification	Coal (Illinois No. 6)			92.5%				
6	Gasification	Illinois No. 6/Torrefied Woody Biomass			92.6%		55 MMSCFD (1,400 tpd gasifier feedstock) ^B	0	

 $^{^{}A}$ CO $_{2}$ capture targets the maximum amount of feedstock carbon captured from the syngas (ATR and gasification cases) and syngas + furnace flue gas steam methane reformer (SMR) case



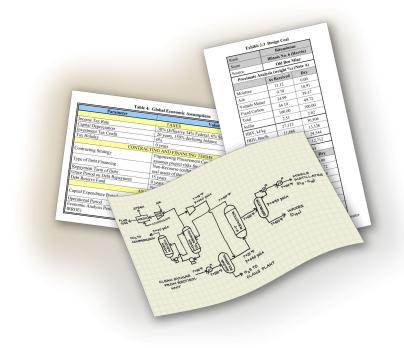
^B The smaller-scale co-gasification case reflects the feedstock capacity of the Buggenum IGCC facility

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General Evaluation Basis

- Performance and economic modeling conforms to the 2019 revision of NETL's QGESS reports:
 - CO₂ Transport and Storage
 - CO₂ Purity
 - Cost Estimation Methodology
 - Capital Cost Scaling Methodology
 - Energy Balance
 - Feedstock Specifications
 - Fuel Prices
 - Process Modeling Design Parameters
 - Techno-Economic Analysis
- Transparent, consistent, highly-detailed analysis methodology

Quality Guidelines for Energy System Studies (QGESS)





Feedstock/Byproduct Pricing



Site-delivered feedstock prices (2018\$)

- Natural Gas, levelized
 - -\$4.42/MMBtu (HHV basis)
- Coal (Illinois No. 6), levelized
 - -\$2.23/MMBtu (HHV basis)
- Woody Biomass (torrefied, non-pelletized), levelized
 - -\$5.43/MMBtu (HHV basis)
- Grid Electricity (Imports and Sales)
 - -\$71.7/MWh 2019 MISO average industrial consumer price
 - —Only coal + biomass gasification sells electricity, <1 MWh/day</p>

No revenue from the sale of export steam





H₂ Product Purity

Characteristics	Concentration
Hydrogen Purity (vol%)	99.90
Max. CO ₂ (ppm)	Α
Max. CO (ppm)	Α
Max. H ₂ S (ppb)	10
Max. H ₂ O (ppm)	Α
Max. O_2 (ppm)	А

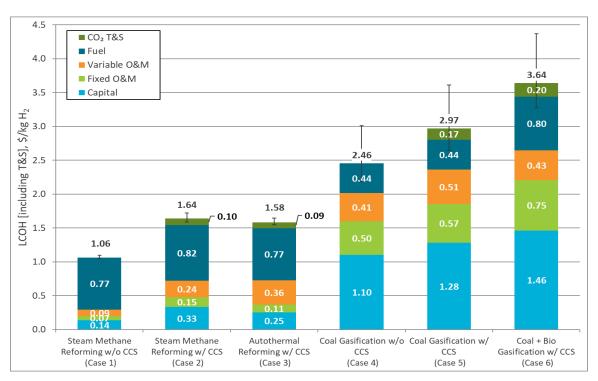
^AThe maximum total concentration of all oxygen containing species is 10ppm

- The hydrogen product meets the purity specification shown, which results in a product suitable for several potential applications
- Contaminant levels are for ammonia-grade H₂ to avoid catalyst poisoning
- Additionally, the specification results in a product exceeding specifications for the following ISO 14687:2019 gaseous H₂ grades:
 - Grade A combustion applications
 - Internal combustion engines, residential/commercial heating appliances
 - Grade B industrial power and heat applications
 - Excluding PEM fuel cells
- H₂ product is compressed to 925 psig for pipeline injection



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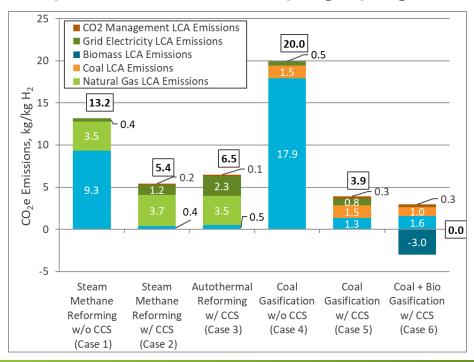
Results (Pending Peer Review)



- Lowest reforming cases SMR w/o CCS (\$1.06/kg H₂)
- Highest reforming case SMR w/ CCS (\$1.64/kg H₂)
- Lowest gasification case coal w/o CCS (\$2.46/kg H₂)
- Highest gasification case "net-zero" coal/biomass (\$3.64/kg H₂)

Global Warming Impact Factors (100-yr, with climate feedback)

- U.S. Electricity, 2016 National Average Profile¹: 590 kg CO₂e/MWh
- Production and Delivery, Cradle-to-city gate²: 0.99 kg CO₂e/kg NG
- Bituminous, Transport Distance (MRO Average)³: 0.19 kg CO₂e/kg of coal
- Torrefied, non-pelletized SRWC⁴: -0.72 kg CO₂e/kg AR biomass
- CO₂ Management, saline aquifer⁵: 0.02 kg CO₂e/kg CO₂ sequestered





S1 Announcement





Key Details:

- \$1/kg H₂
- One decade (i.e., 2030)
- "1, 1, 1"







1 Kilogram

https://www.energy.gov/eere/fuelcells/hydrogen-shot

https://www.energy.gov/articles/secretary-granholm-launches-hydrogen-energy-earthshot-accelerate-breakthroughs-toward-net



Project Goals and Benefits



Identify potential pathway scenarios to meet the Hydrogen Energy Earthshot 2030 production cost and (informal) emissions intensity goals via screening analyses

- Opportunities for holistic reductions in production cost and life cycle emissions will be critically reviewed
- Both natural gas and waste coal primary feedstocks will be evaluated
- Advancements to contemporary commercial technologies (e.g., SMR, ATR, gasification), advanced technologies (e.g., chemical looping, pyrolysis, etc.), unit siting choices, the application of biofuels, and finance assumptions at a minimum will be considered
- VRE-based H₂ production pathways will be examined for comparison purposes

Provide an informed framework for FECM H₂ R&D

- Screening-level analyses intended to be performed quickly
- Pathway scenarios to guide program R&D
- Facilitate office and programmatic communications with stakeholders



Project Approach

Five (5) Tasks:



- Ongoing H₂ baseline work and other contemporary estimates available
- Summarize key process information (including LCA data)

Task 2: Literature review/information gathering on advanced H₂ production

- Consider both current commercial and advanced (future) H₂-production technologies
- Summarize detailed descriptions, flow diagrams, performance/cost data, strengths/weaknesses, etc.

	Process	Markets	LCA	Sub- Surface
Task 1	#		•	
Task 2	#		•	
Task 3	•	#	•	•
Task 4	‡	•	•	•
Task 5	‡	•	•	•

‡ = Lead; • = Support



Task 3: Additional options for improvements (cost and emissions)

 Plant Siting, Process Intensification, Financing and Byproduct Sales, Biofuels, CO₂ Transport and Storage costs

Task 4: Exploratory analyses to identify candidate pathways

- From Tasks 2 and 3, identify/propose pathways, summarize design basis and assumptions, estimate H₂ production costs and emission intensities
- Down-select 4-6 scenarios for detailed analyses

Task 5: Final analyses, presentation, and whitepaper

- Refine analyses on 4-6 down-selected scenarios
- Conduct sensitivity analyses

Project Timeline:

• September 2021 – January 2022



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