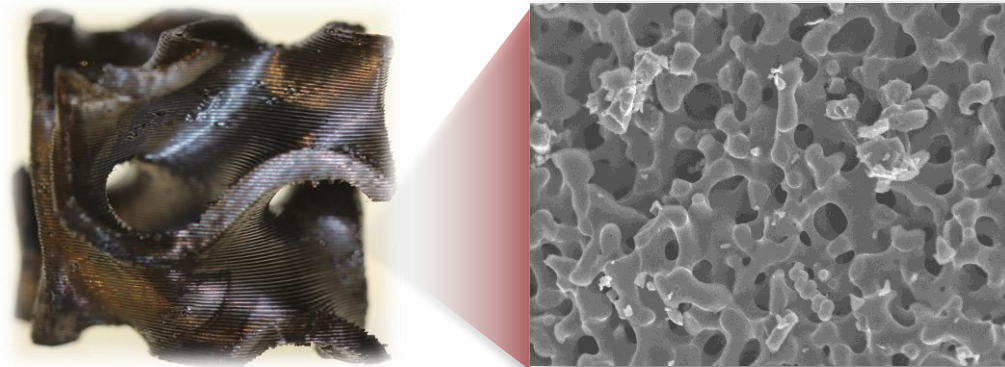


# Modular Microbial Electromethanogenesis Flow Reactors for Biogas Upgrading

March 4-8, 2019

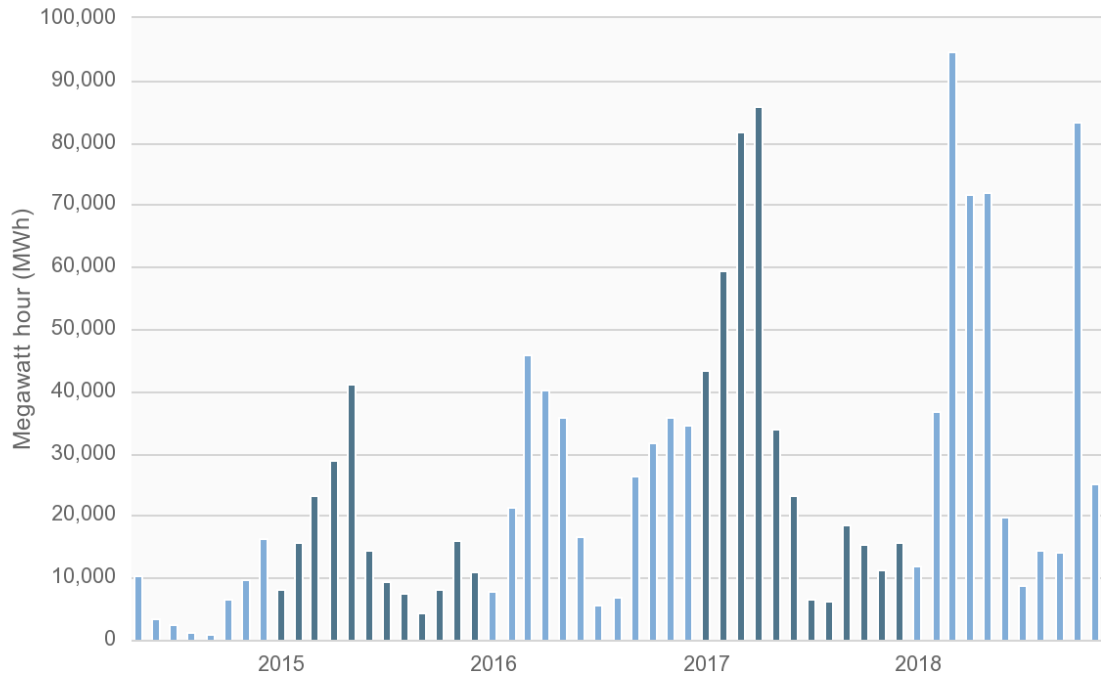


Waste to Energy Technology Session Area

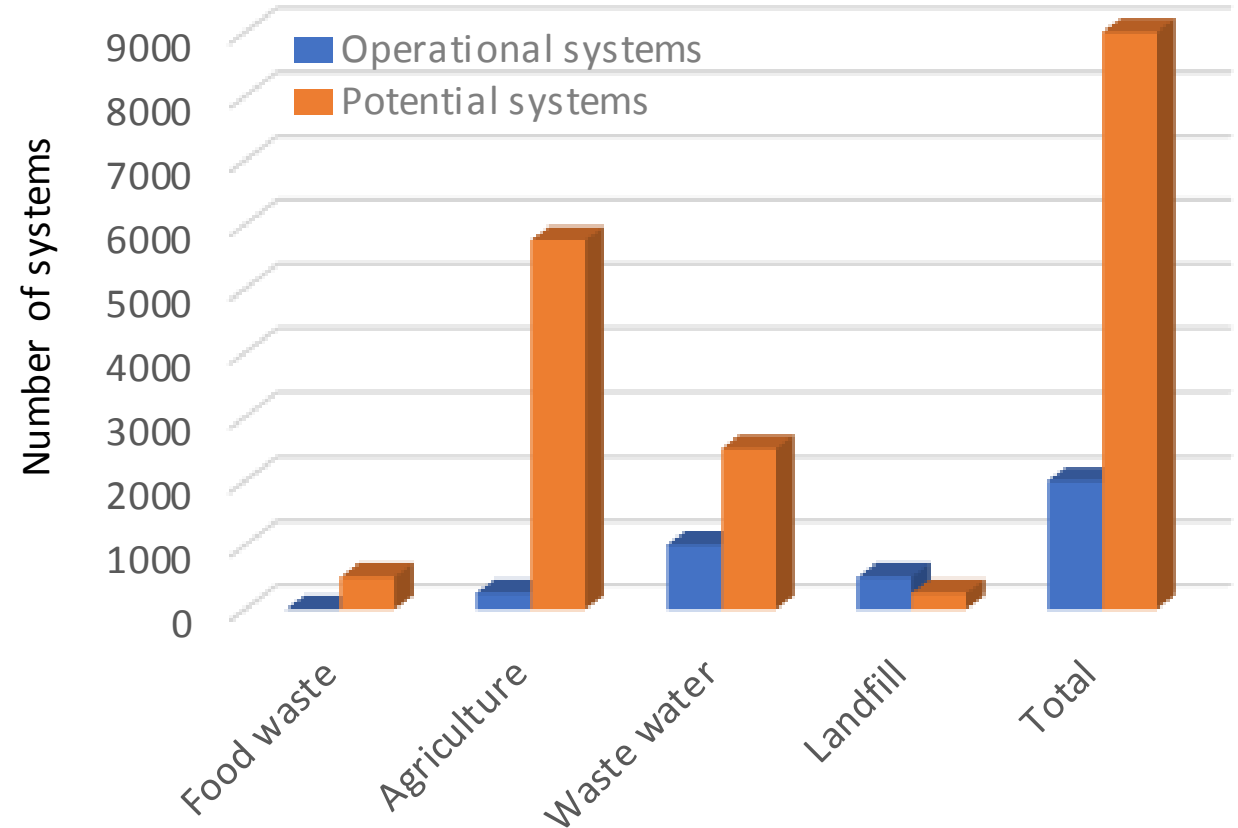
Sarah E. Baker, Lawrence Livermore National Laboratory

# We Need to Better Utilize Carbon-Neutral Energy Sources

Wind and solar curtailment totals by month



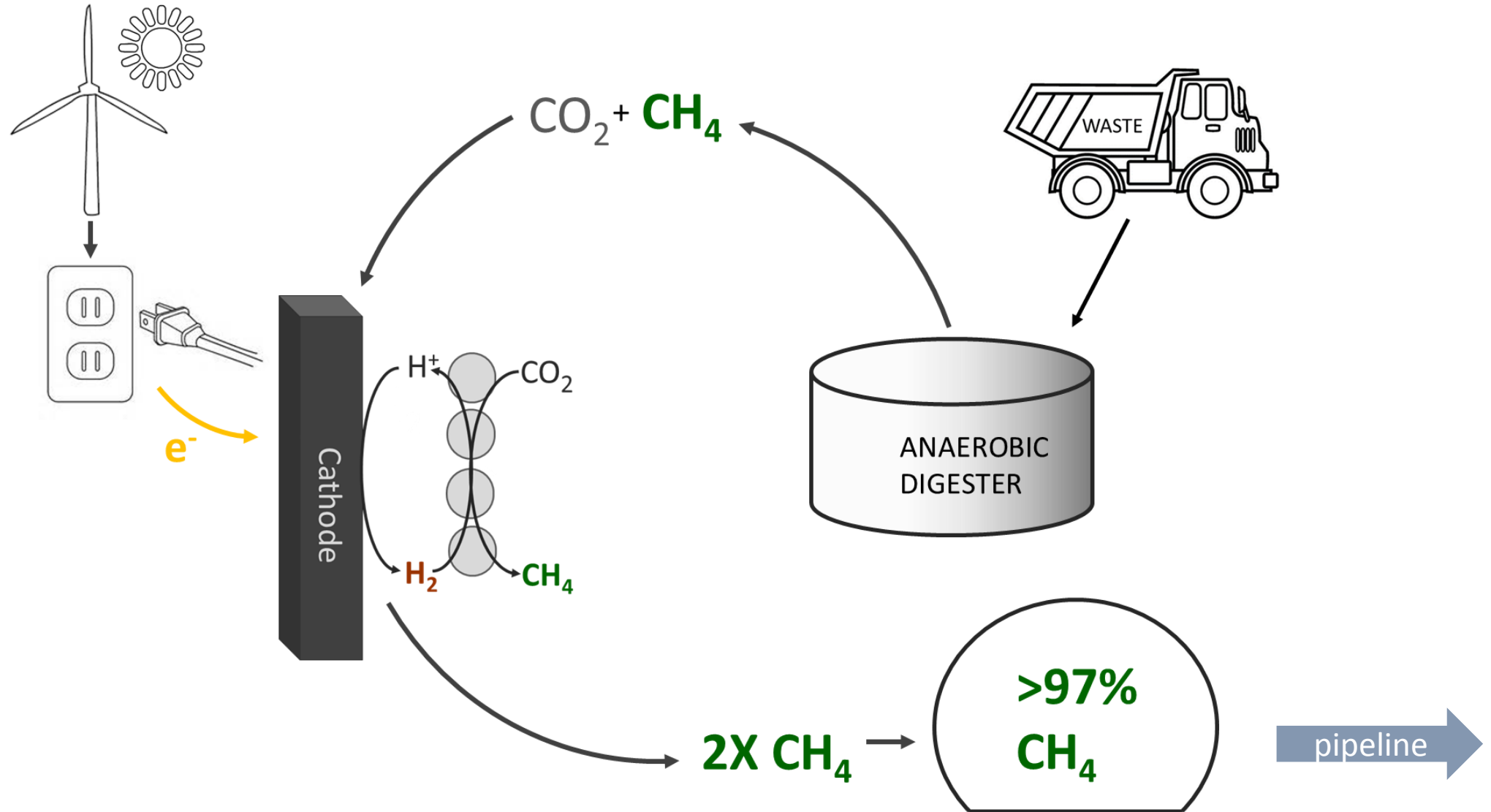
California renewable curtailments are rising; 452,507 MWh in 2018 (which could power 45,000 homes for a year)



Biogas is underutilized, responsible for 25% of US methane emissions, and could replace 46% of grid natural gas or 3% of transportation fuel



# Goal: Renewable Energy Stored in Biogas CO<sub>2</sub>



- $H_2$  generated *in situ*: no need for separate  $H_2$  production, storage, compression
- Low temperature and pressure
- Complete  $H_2S$  utilization is possible
- Microbes are selective



# Challenges

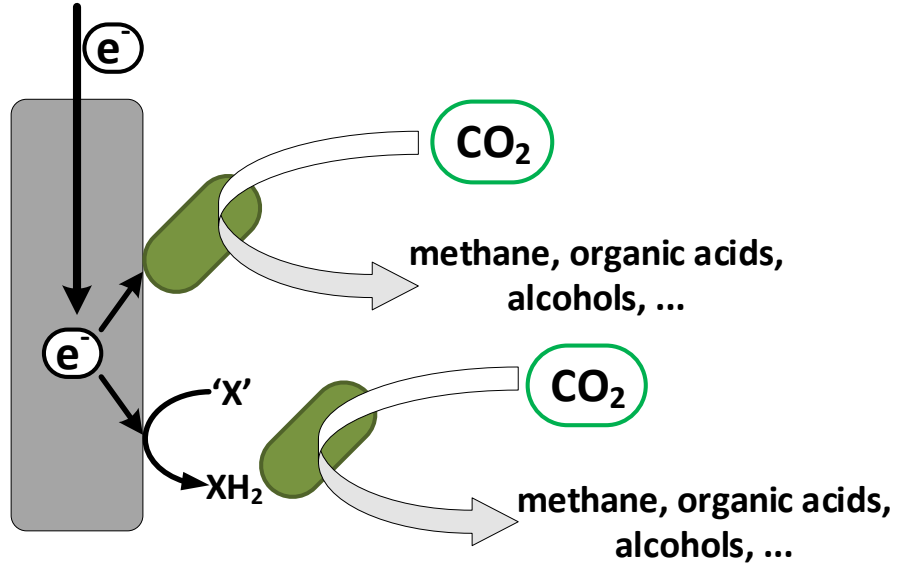
*“The challenge is to harness the [microbial electrochemical cells] into techno-economically viable systems”* \* Key issues: scaling, cost-effective mass production of cathodes, attaining and sustaining economically viable current density.

- Materials, Reactor, Microbe **Compatibility**: efficient methanogens that flourish in non-fouling media with high conductivity. Compatibility of temperatures with membranes.
- Materials, Reactor, Microbe **Stability**: maintaining cultures under high current density conditions in continuous reactors. Eliminating pH fluctuations. Maintaining electrocatalyst activity in microbial media
- Materials, Reactor **Costs**: ensuring all materials are scalable and mass manufacturable. Eliminating precious metals if possible.



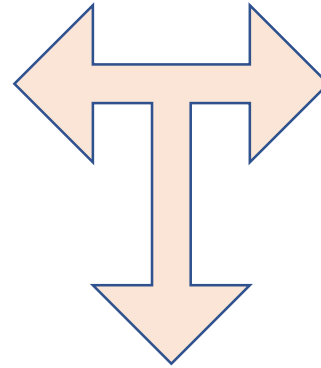
# Project Genesis

## Microbial Electrosynthesis (Stanford)

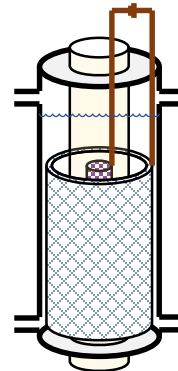


Spormann Lab at Stanford brings world-leading expertise in anaerobic microbes and their application in bioenergy and remediation

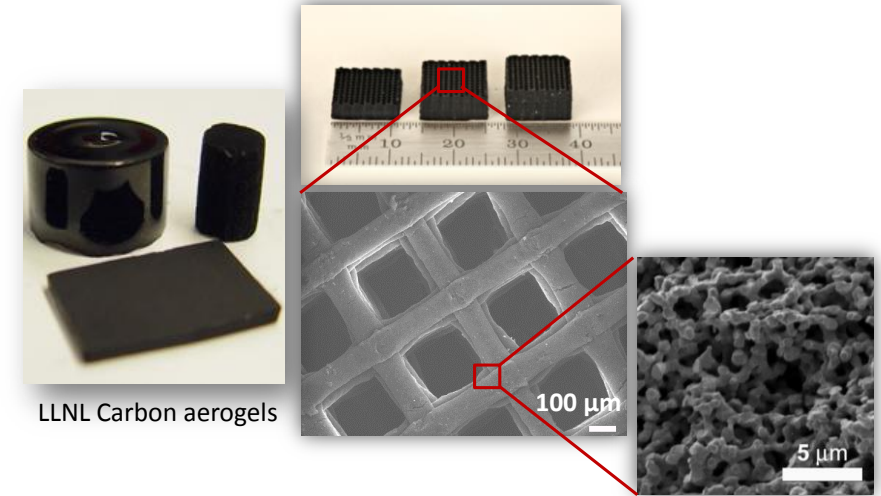
## Industrial Insights (SoCalGas)



## Biogas Upgrading Reactors



## Advanced Materials (LLNL)



LLNL Carbon aerogels

LLNL has been a world leader in synthesis of porous carbon electrodes for over 30 years:

- Capacitive Desalination (pilot scale)
- Supercapacitors (highest power density)
- HER and  $CO_2R$



## Project Goal:

Improve the performance, scalability, and economics of microbial electromethanogenesis for biogas upgrading and energy storage at <1 L scale for multiple days.

## Outcome:

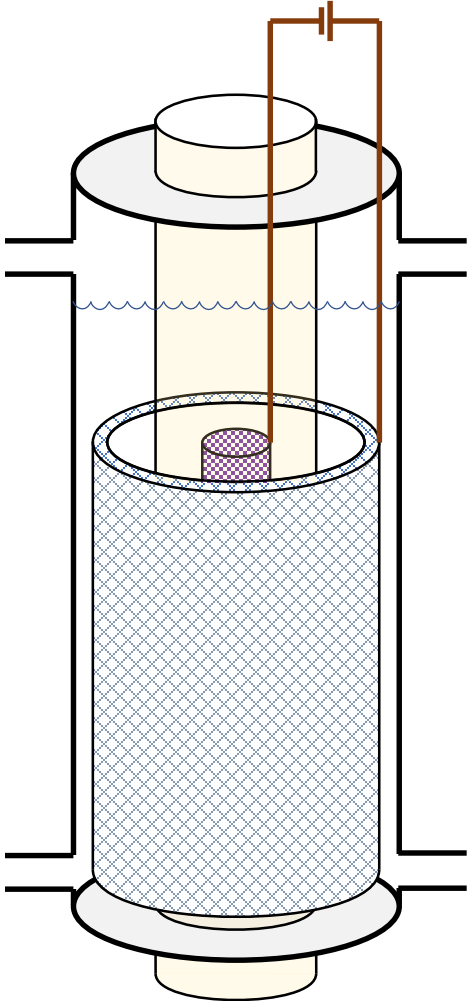
Bench scale device that upgrades biogas to pipeline quality biomethane at 0.03g/Whr for more than 2 days. Sufficient data for informed TEA.

## Relevance:

Enable long term storage of renewable energy using existing natural gas infrastructure; increase capture and utilization of biogas by decreasing process costs of upgrading. Eliminate *both* CO<sub>2</sub> and methane emissions.

# Using Advanced Materials to Integrate Biological and Electrochemical Processes:

*Toward Scalable Conversion Reactors that are Limited Only by the Kinetics of the Microbes*



We will construct proof-of-concept reactor with scalable low cost components that demonstrates materials, reactor, and process requirements for 1) upgrading biogas to pipeline quality 2) at target energy efficiency metric for > 3 days 3) suitable for preliminary TEA.

- *Advanced manufactured, hierarchical materials allow scalable surface area and modular design.*
- *In situ  $H_2$  generation at high surface area catalysts in vicinity of microbes may increase rates and reduce energy of  $H_2$  dissolution;*
- *Demonstrating on Biogas: good  $CO_2$  point source and ready revenue stream through RIN and LCFS;*
- *Microbes may manage  $H_2S$  thus further reducing costs of upgrading*
- *No biofilm → utilize bulk electrolyte, higher current density and less concern about fouling.*



# Approach: Management

DOE/BETO: Beau Hoffman and Mark Philbrick

LLNL/Sarah Baker: Overall Project Management

NREL/ANL: TEA

SoCalGas/Ron Kent: Project Advisor

Stanford/Prof. Spormann: Lead of Stanford Team & Microbial Electrosynthesis Tasks

LLNL/Sarah Baker: Lead of LLNL Team & Reactor Tasks

Dr. Joerg Deutzmann: Microbial Enrichment at Cathodes

Dr. Simon Pang: Reactor Design and Abiotic Testing

Dr. Frauke Kracke: Reactor Design and Biotic Testing

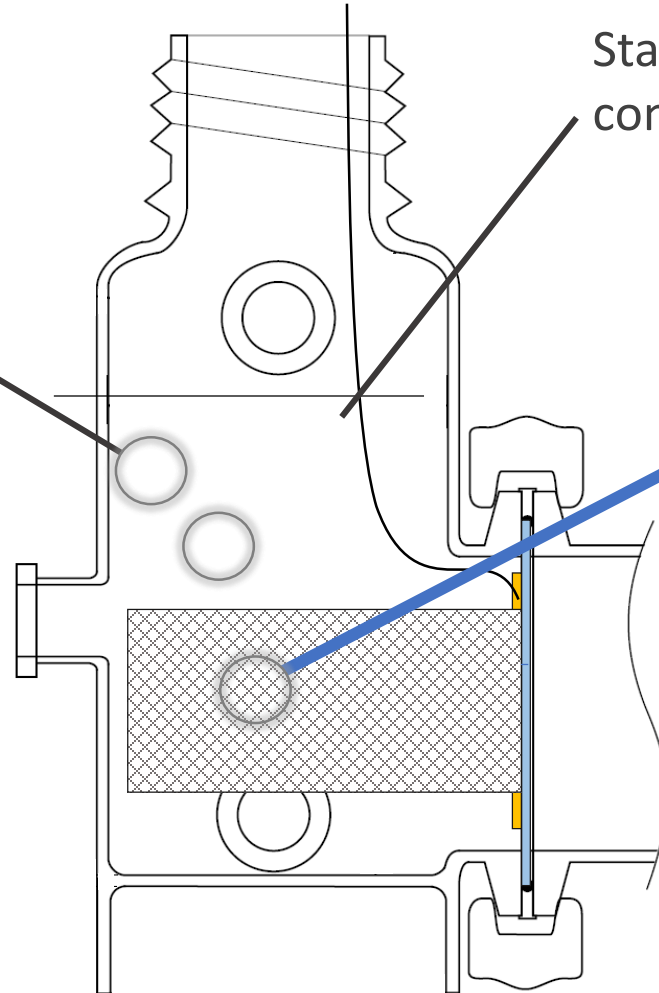
Dr. Swetha Chandrasekaran: Materials Design and Synthesis

Dr. Anna Ivanovskaya: Electrochemistry and Electrode Characterization



# Technical Approach Year 1: Identify Components, Evaluate Stability & Demonstrate Energy Efficiency

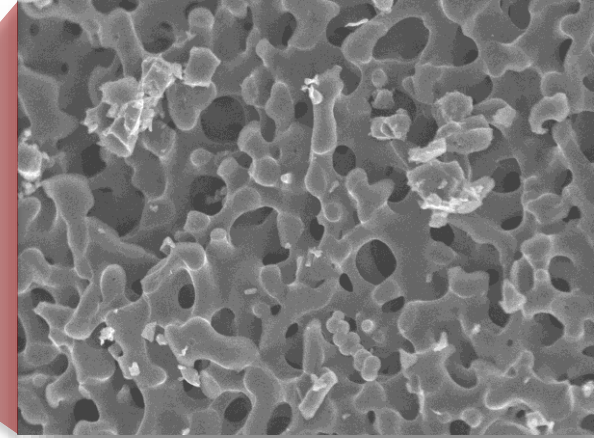
4 Strains  
Tested for  
tolerance to  $>5$   
 $\text{mA}/\text{cm}^2$ ,  
 $>80\%$  FE for  $\text{CH}_4$



Stable and low resistance  
contacts



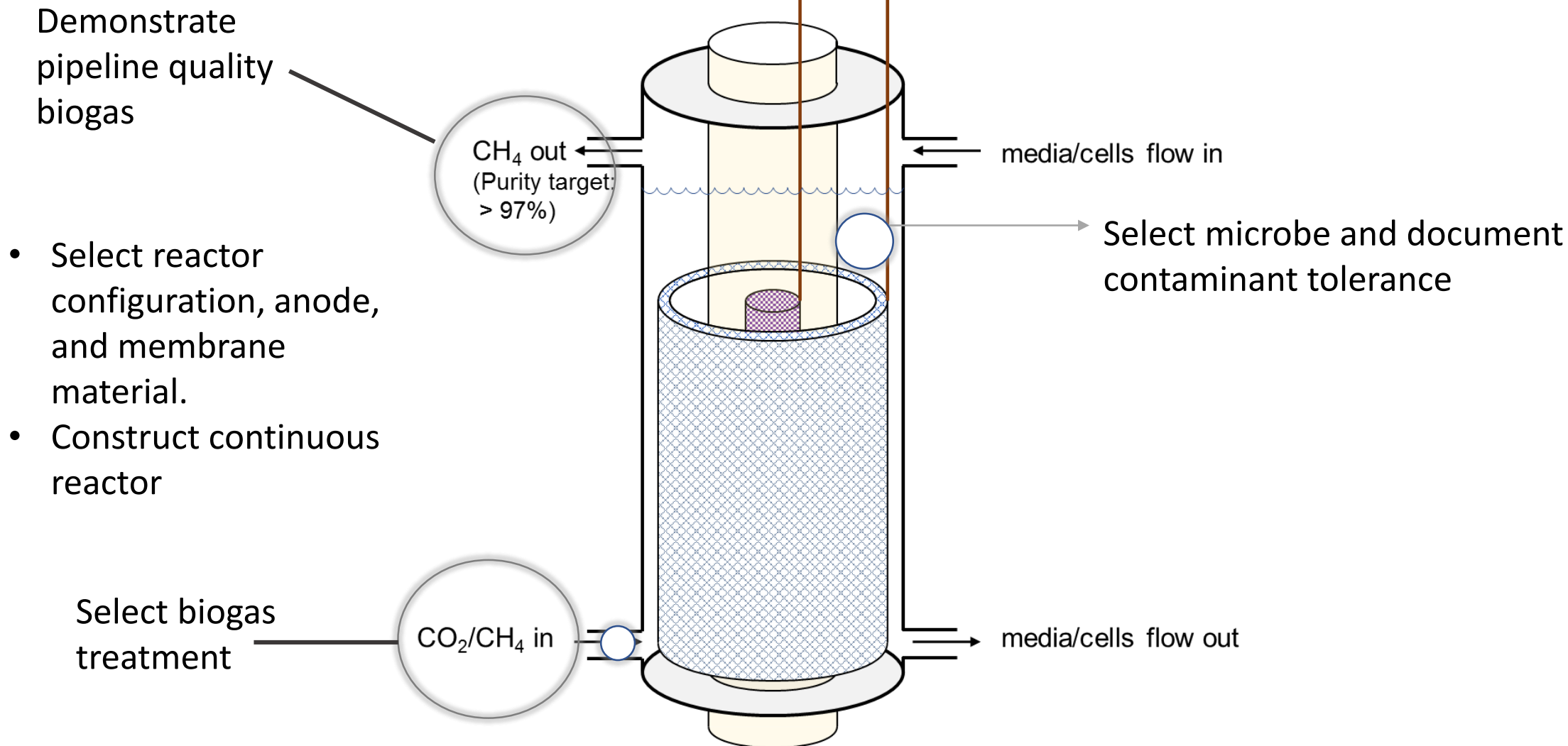
Test two cathode materials to determine  
contaminate tolerance



**Go/No Go: Demonstrate Methane from Biogas for  $> 2$  days at  $> 0.03$  g/Whr**



# Technical Approach Year 2: Continuous system, Biogas purity, TEA

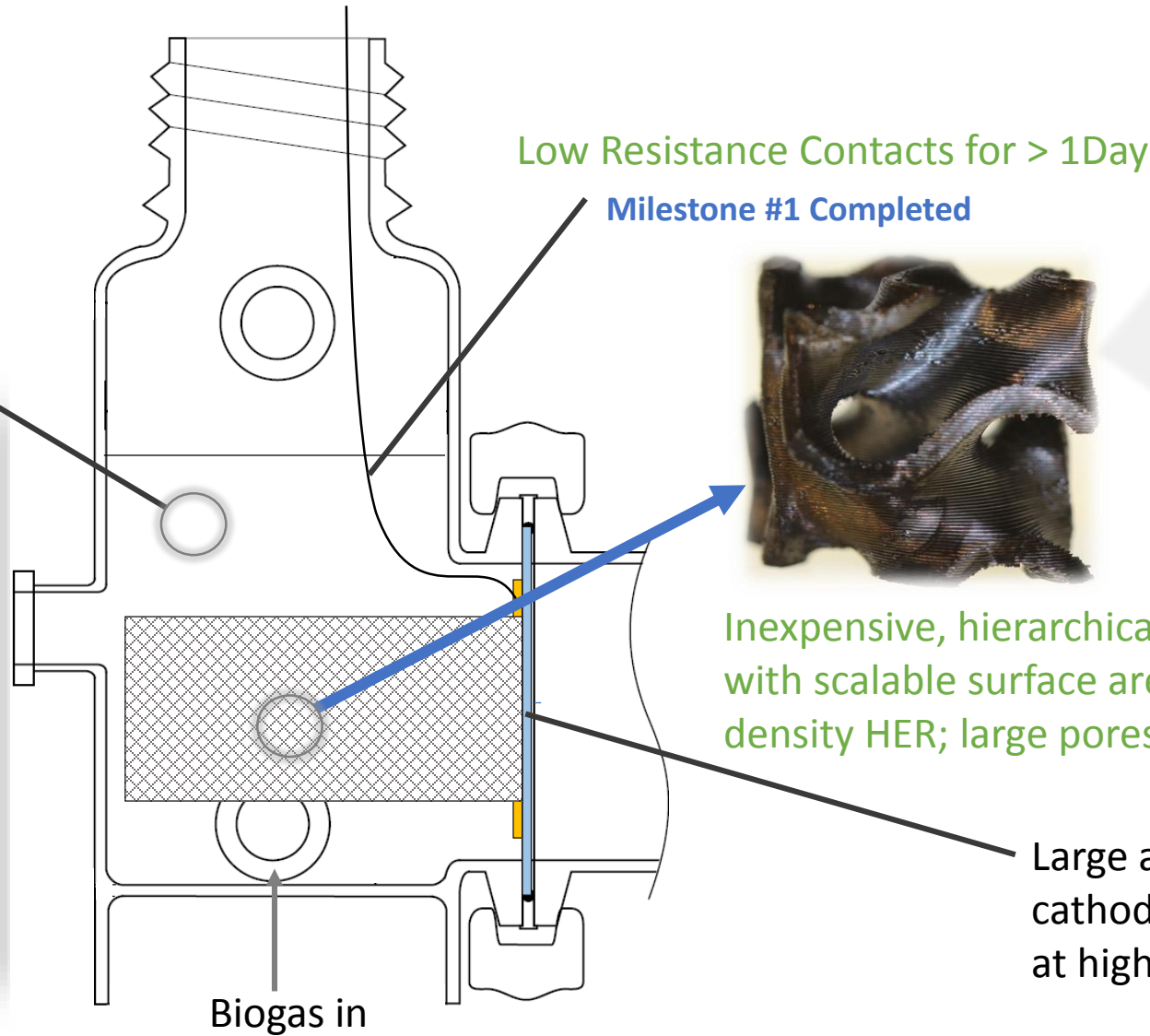


Reactor, process system design and operating strategies for TEA. Completion of TEA



# Designed New Electrochemical Cells for Component Testing

Microbes with good load following, non-fouling media, salt and pH tolerance, tolerance to  $H_2S$

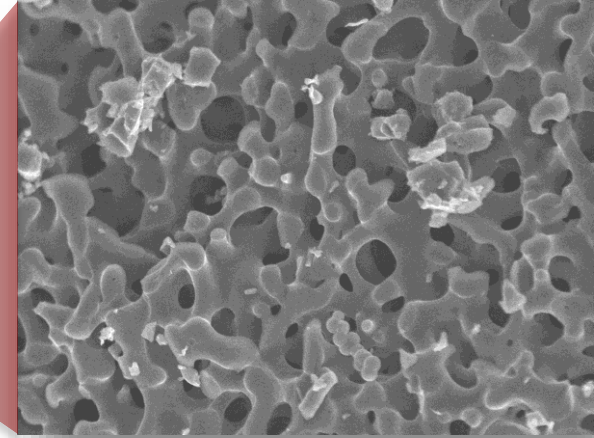


Low Resistance Contacts for > 1Day  
Milestone #1 Completed



Inexpensive, hierarchical conductive cathodes with scalable surface area for high current density HER; large pores for active transport

Large area membrane proximal to cathode to minimize pH instability at high current density



# Milestone 2 Completed: 3 Strains Viable on Raw Biogas



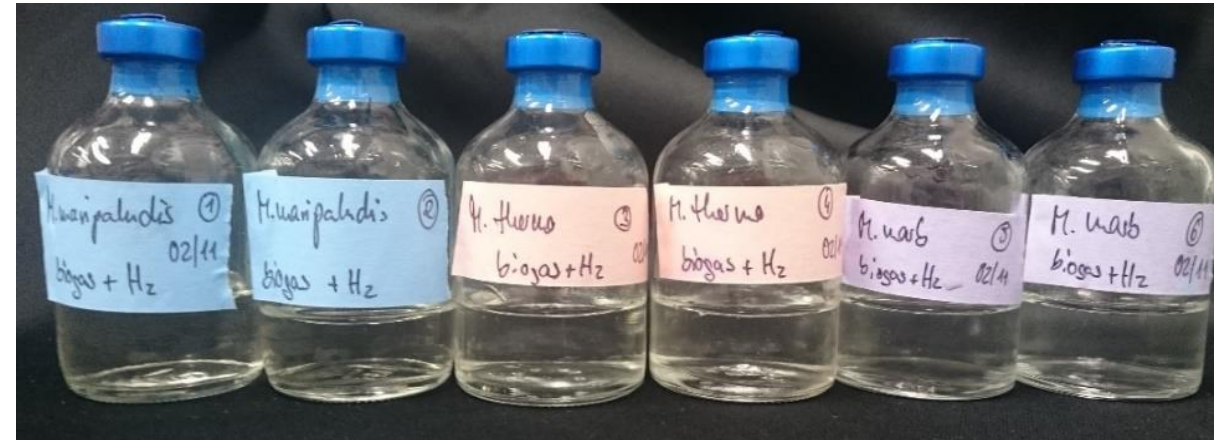
Sampling raw-biogas from Delta Diablo treatment plant.

Strain #1

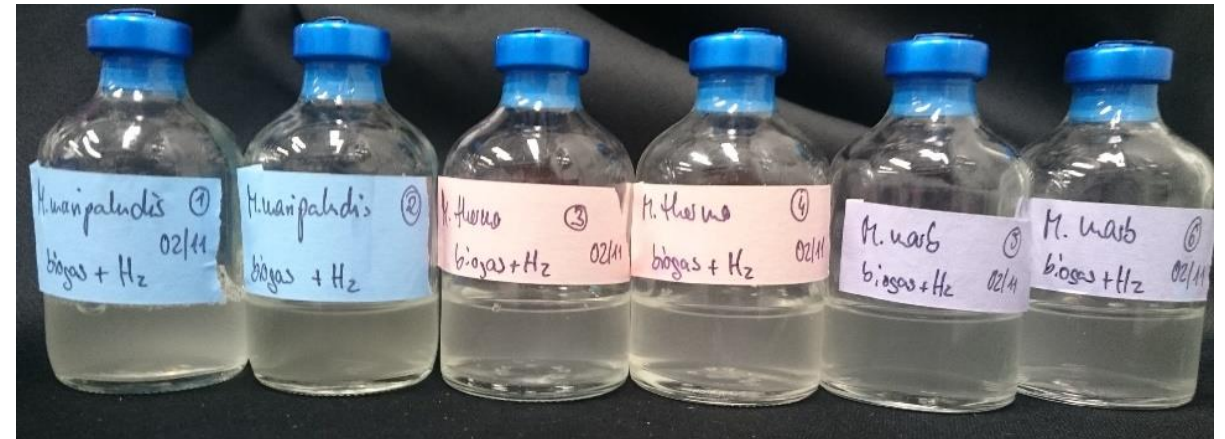
Strain #2

Strain #3

t = 0 h



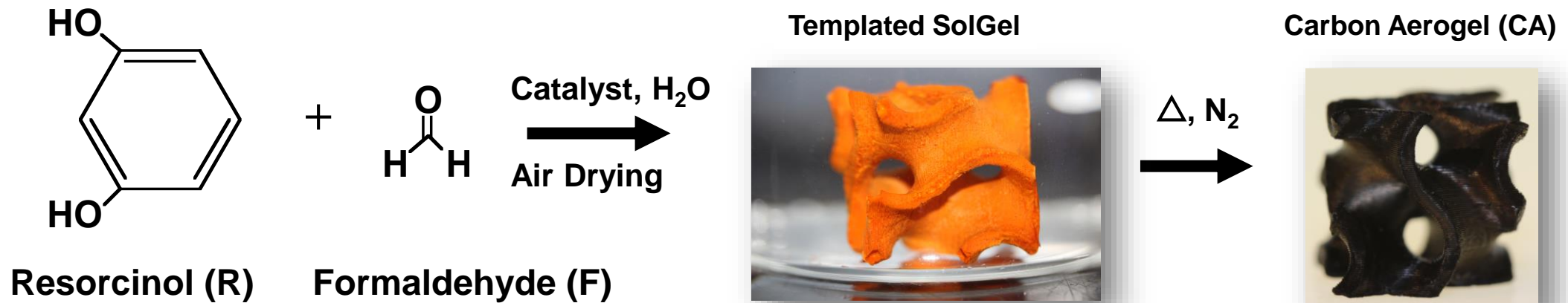
t = 48 h



Serum vials containing methanogenic archaea, raw biogas as the only carbon source, and hydrogen as the **sole** electron source.



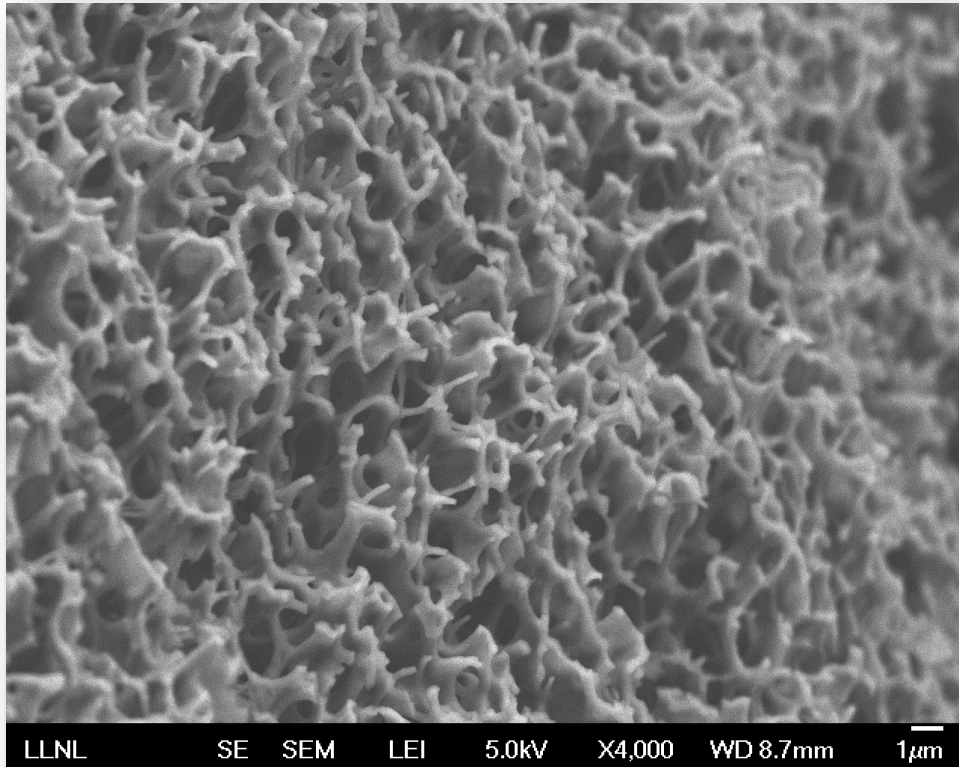
# Developed New Low Cost Molding Method for Patterned Aerogel Synthesis



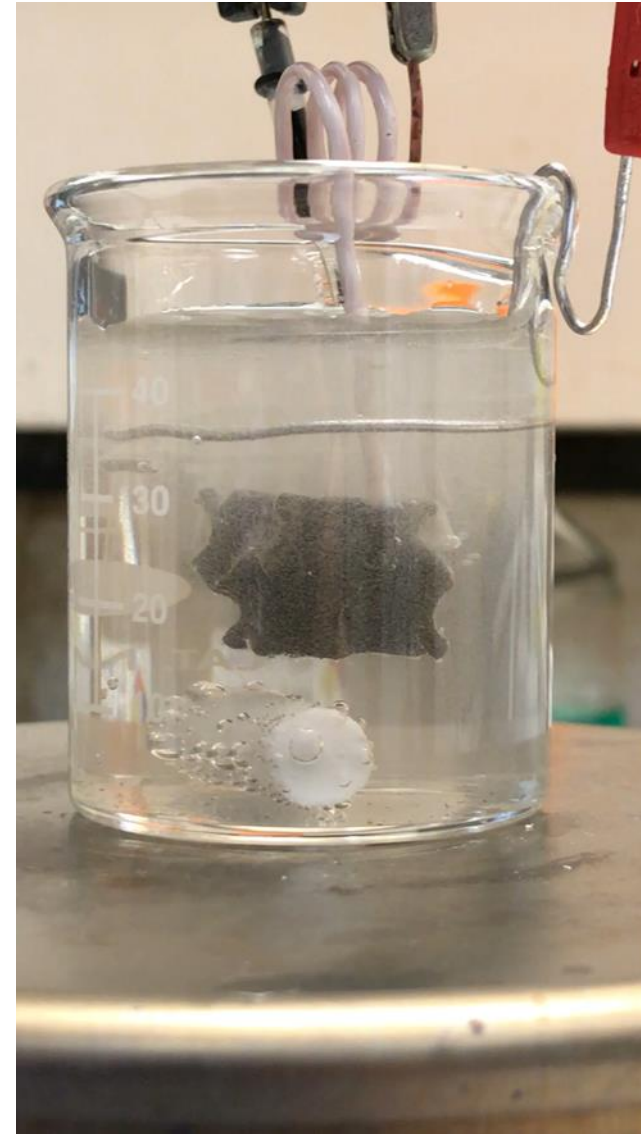
High 3D conductivity, mechanically robust, limitless geometries w/ high surface area



# Conformal Electrodeposition of Hydrogen Evolution Catalyst



**NiMo Coated Aerogel.**



**Hydrogen Evolution**



# Ongoing /Future Work

## Testing systems under continuous gas flow for first time

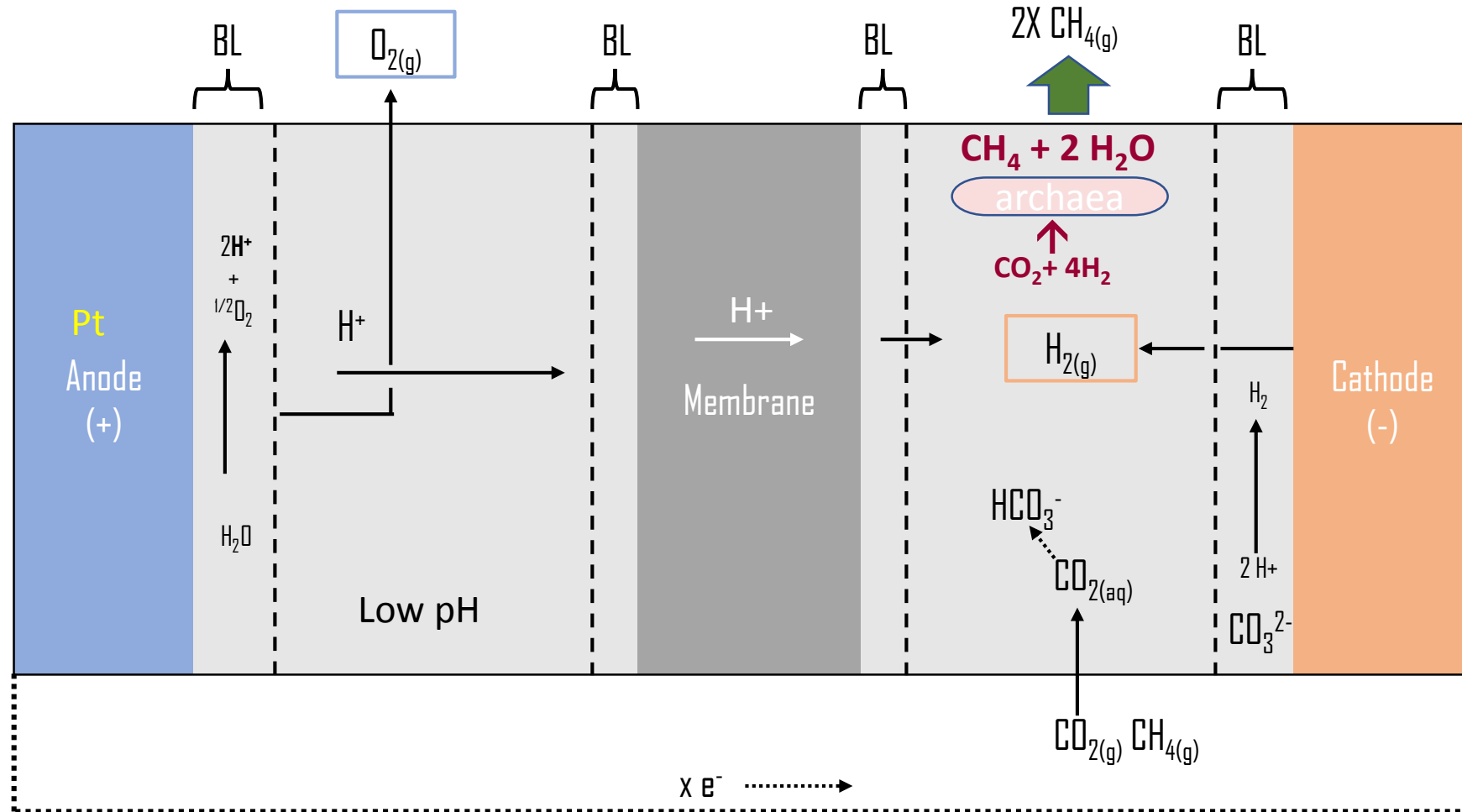
Bubble bottle culture of *M. marburgensis* on H<sub>2</sub>/CO<sub>2</sub> (80/20)  
Optical density: about 1 (~10<sup>9</sup> cell/ml).

- Hydrogen limited (gas recirculation and stirring increase methanogenesis rates)
- Methanogenesis rates of up to 2 ml/min/L
- corresponding to 1 A L<sup>-1</sup> current if H<sub>2</sub> supplied via electricity

***Electrochemical* reactors with the same strain as bubble bottle: Only stable < 1 day**



# pH instabilities arising from proton exchange membrane



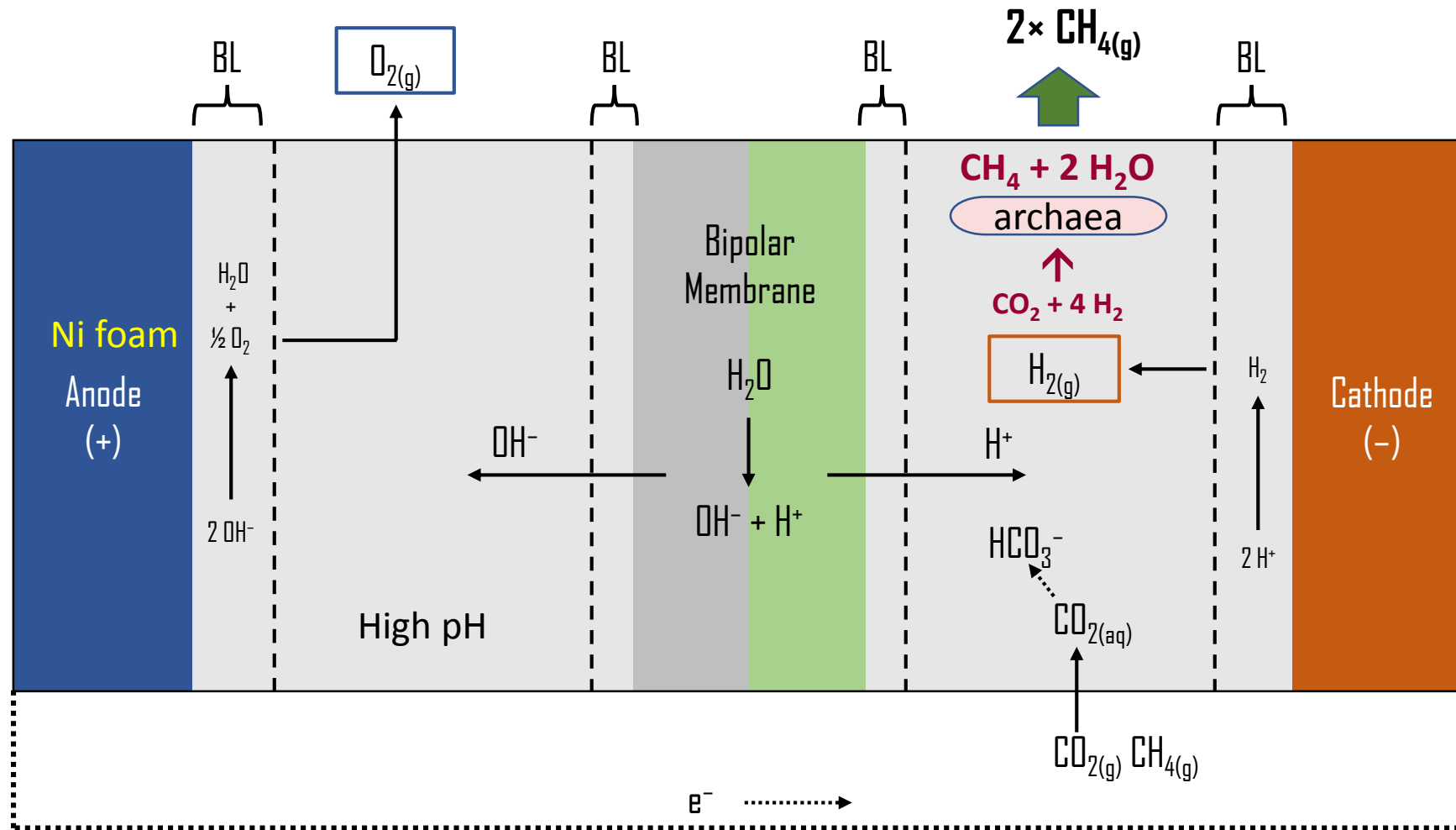
Adapted from Singh, M. R., et. al. *PCCP*. 2015

Tolerates high temperatures (more productive organisms), but requires Pt and pH unstable





# Target system with biopolar membrane and alkaline anode



Adapted from Singh, M. R., et al. *PCCP*, 2015

Stable pH and lower cost materials



# Integration of Microbes in Productive Electrochemical Reactors

Microbial strains tested:

Strains tested	Temp.	Salinity	Density and turnover rates	medium
<i>Methanothermobacter thermautotrophicus</i>	65°C	low	High	Freshwater (DSMZ medium 119)
<i>Methanothermobacter marburgensis</i>	65°C	low	high	Freshwater (DSMZ medium 119)
<i>Methanococcus maripaludis</i>	30°C	high	medium	Sea water (Artificial sea water or DSMZ medium 141)



Delamination of bipolar membrane at elevated temperatures.



Scaling of NiMo coated graphite rod in marine media.

- Most productive pure strain needs high temp and low salt → *membrane breakdown, high IR*
- Lower temp strain allows for high salt but needs Mg → *cathode scaling*



# Overcoming integration challenge : finding “goldilocks” strain *(in progress)*

- **Adaptation/acclimation of freshwater strains for higher salt**

*Successful with Methanothermobacter strains, but requires Nafion membrane because of higher temperature*

- **Isolation of strains in media suitable for electrosynthesis**

*(low Mg/Ca concentrations, high salinity)*

*In progress*

- **Isolation of strains in electrochemical cell while running high current density**

*In preparation*

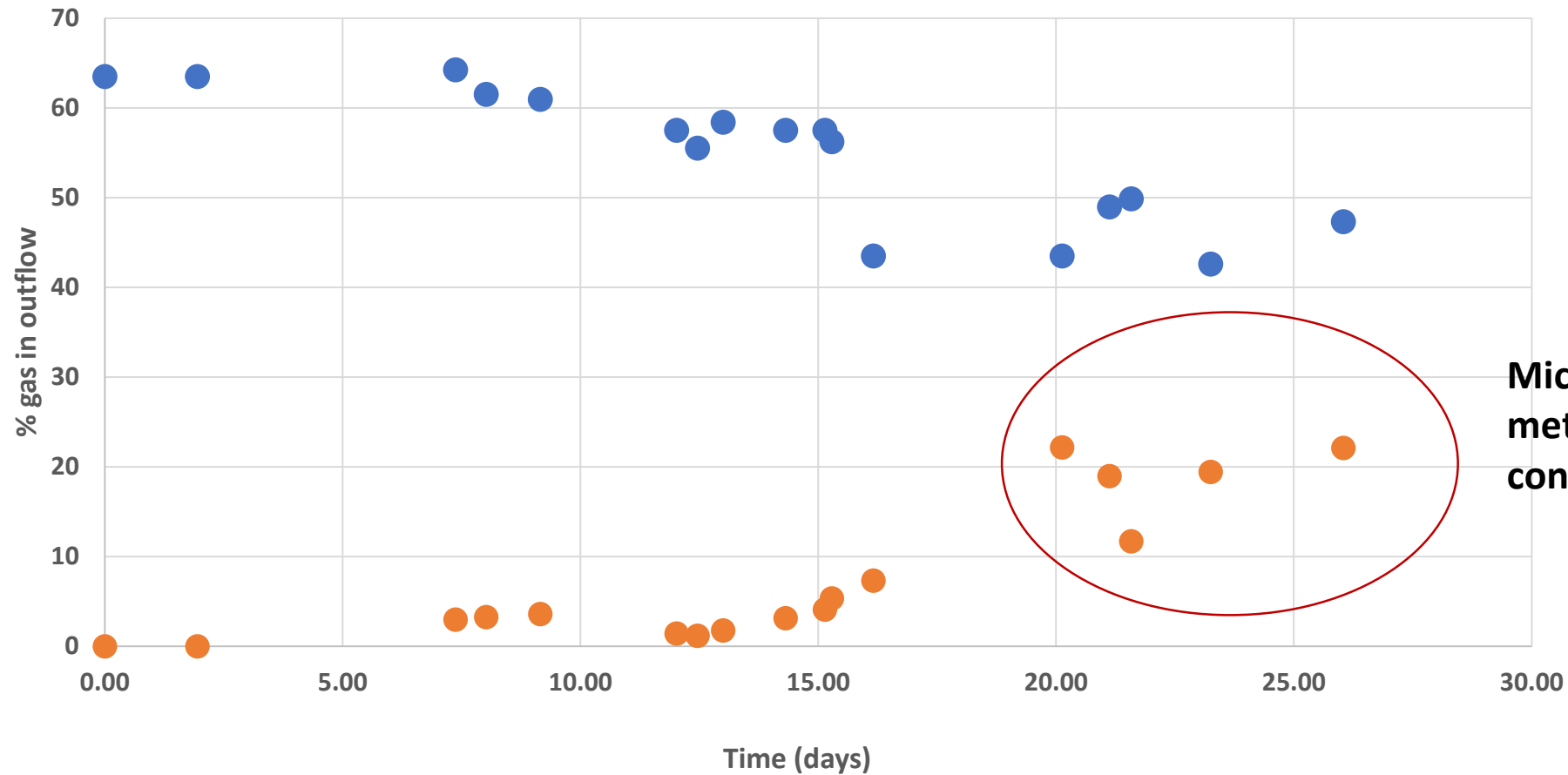
→ **Key Milestones:** Testing of new isolates of 1-3 strains for tolerance to current density  $>5 \text{ mA/cm}^2$  (Q5); selection of strain (Q6)



# Finding “goldilocks strain” from Delta Diablo Sludge

Enrichment reactor at 20 mA (2.5 mA cm<sup>-2</sup>)

● H<sub>2</sub> ● CH<sub>4</sub>

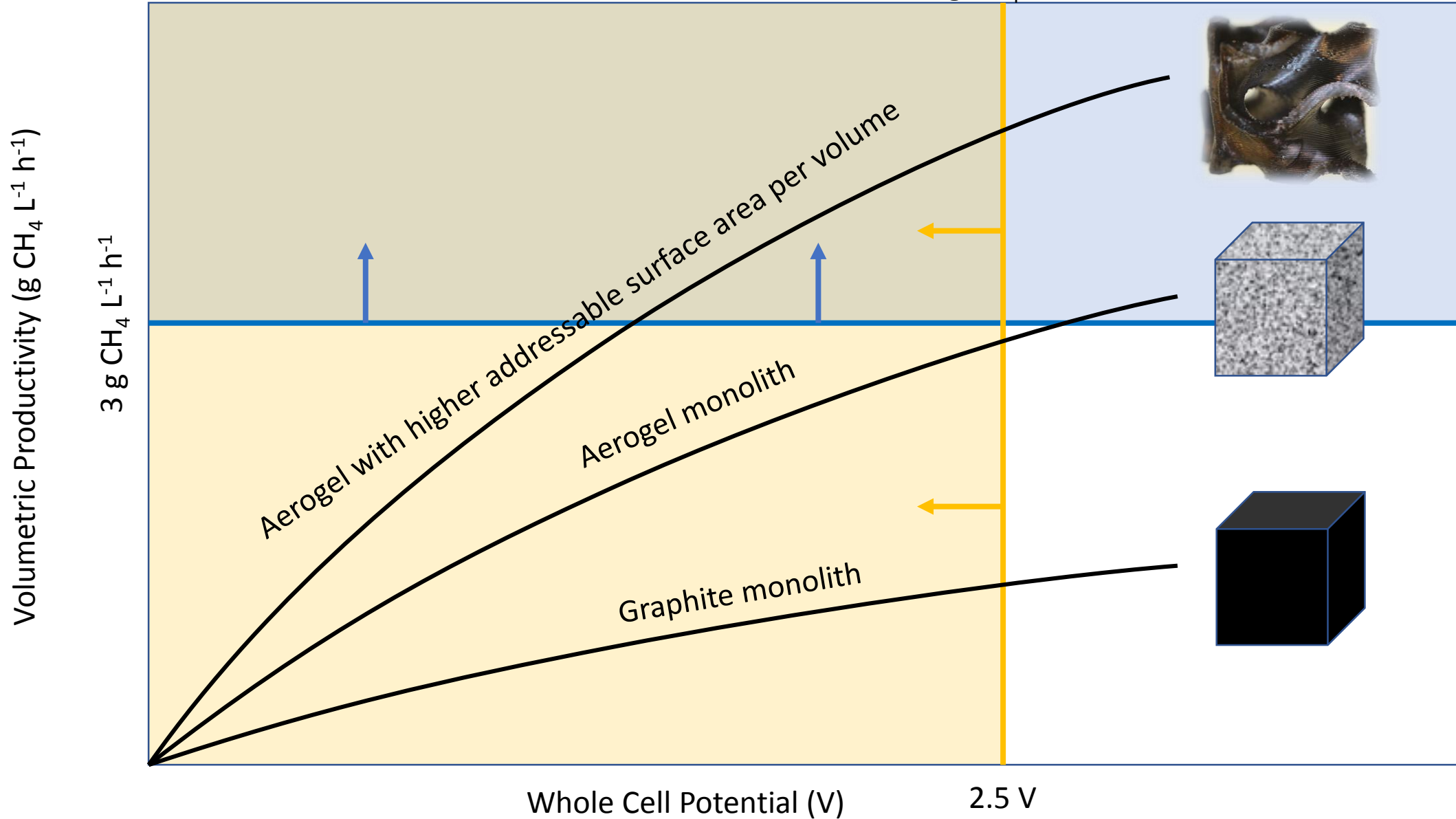


**Microbes evolving methane under constant current**



# Selecting cathode material and geometry (key milestone Q6)

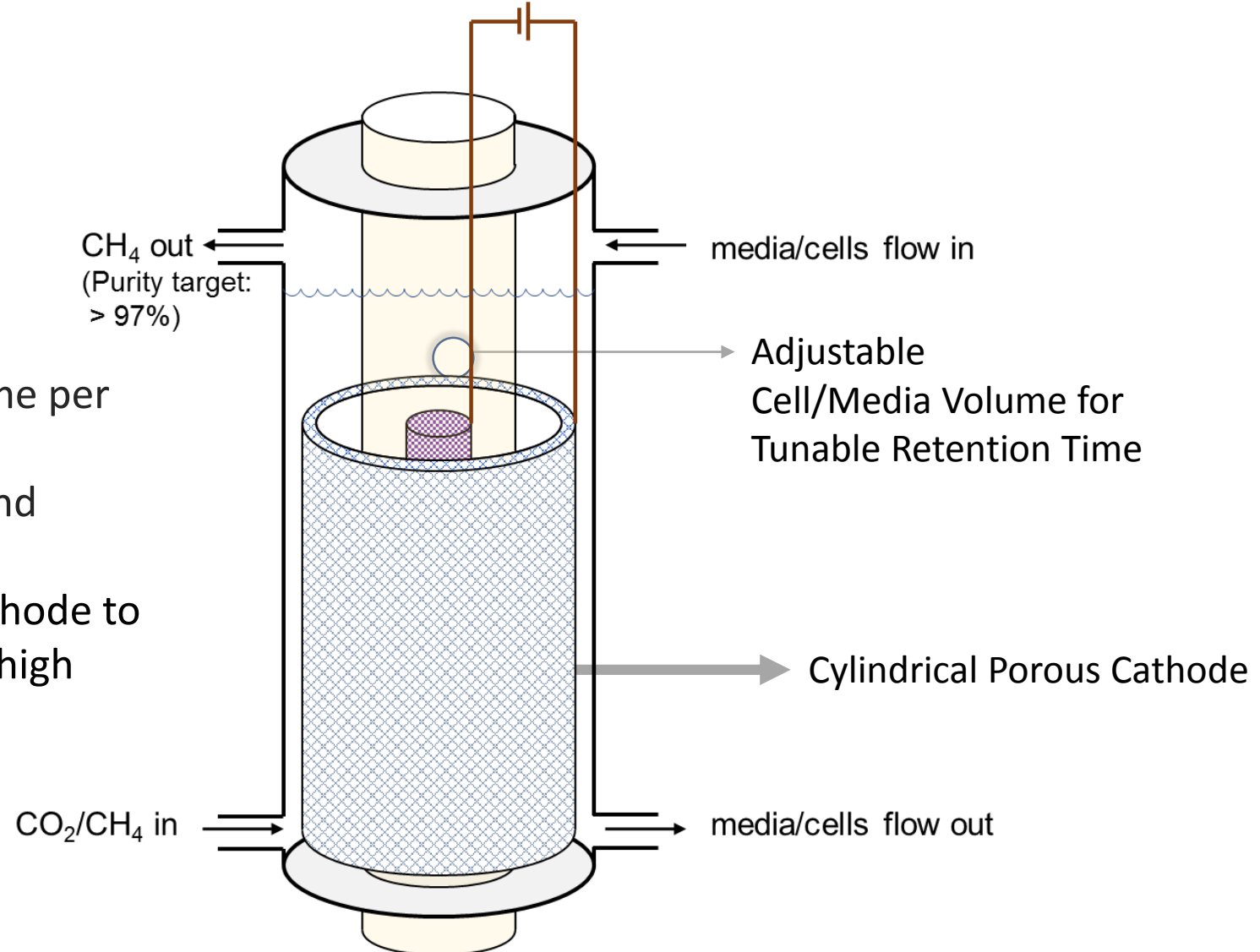
Energy efficiency:  
 $0.03 \text{ g CH}_4 \text{ W}^{-1} \text{ h}^{-1}$



# Building Reactor Around the Selected Microbe and Cathode

## Desired Features:

- Maximize cell/media volume per reactor volume
- All components low cost and scalable
- Membrane proximal to cathode to minimize pH instability at high current density



**Key Milestones: Construction and continuous operation using raw or scrubbed biogas from WWTP (Q7)  
Demonstrate outlet gas purity of 97% CH<sub>4</sub>, <3% CO<sub>2</sub>, <0.2% O<sub>2</sub>, <4 ppm H<sub>2</sub>S, <0.1 mg/m<sup>3</sup> siloxanes at  
0.03g/Whr in continuous reactor (Q8)**



# Strategic Importance

- We aim to **improve the performance** (to reach target energy efficiency, biogas purity) and TRL of Electromethanogenesis by constructing a prototype continuous reactor
- This project will, for the first time, integrate in situ  $H_2$  generation with biogas purification to pipeline quality in a continuous, modular device
- Electromethanogenesis provides a pathway for increased utilization of biomass carbon and renewable energy
- SoCalGas will be integral in advising on technical direction, identifying next step, partners, and potential pilot sites.

**This project directly supports the BETO mission:** to develop and transform domestic renewable biomass into commercially viable biofuels & biopower

- Compatible with today's infrastructure (natural gas pipelines and abundant storage capacity)
- Reduce GHGs by displacing petroleum fuels
- Supports domestic bioenergy industry



# Summary

- Our goal is to upgrade biogas to pipeline quality by coupling (renewable) electricity to methanogenesis.
- Success factors include energy efficiency (0.03 g/Wh) biogas purity (97%) and stability (days)
- We have shown feasibility with individual components and need to focus on isolating suitable microbe and integration with reactor

This document was prepared as an account of work sponsored by an agency of the United States government. Neither the United States government nor Lawrence Livermore National Security, LLC, nor any of their employees makes any warranty, expressed or implied, or assumes any legal liability or responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights. Reference herein to any specific commercial product, process, or service by trade name, trademark, manufacturer, or otherwise does not necessarily constitute or imply its endorsement, recommendation, or favoring by the United States government or Lawrence Livermore National Security, LLC. The views and opinions of authors expressed herein do not necessarily state or reflect those of the United States government or Lawrence Livermore National Security, LLC, and shall not be used for advertising or product endorsement purposes.





# Quad Chart Overview

## Timeline

- Project start date 10/01/18
- Project end date 10/01/20
- Percent complete: 20%

## Barriers addressed

Ct-H. Gas Fermentation Development  
Ct-D. Advanced Bioprocess Development

## Total Planned Funding (FY 19-Project End Date)

<b>DOE Funded</b>	800K
-------------------	------

<b>Project Cost Share*</b>	400K
----------------------------	------

**Partners: SoCalGas and Stanford (400K subcontract from LLNL)**

## Objective

Demonstrate Microbial Electrosynthesis flow reactors feasible for biogas upgrading and grid storage

## End of Project Goal

Production of pipeline quality biogas and Informed TEA of Microbial Electrosynthesis Flow Reactors



EXTRA



## To beat Electrochaea-rates we need about 40 mA/cm<sup>3</sup> cathode volume

Quick update:

Bubble bottle culture of *M. marburgensis* on H<sub>2</sub>/CO<sub>2</sub> (80/20) successful after changing medium composition

- Optical density: about 1 (~10<sup>9</sup> cell/ml).
- Hydrogen limited (gas recirculation and stirring increase methanogenesis rates)
- Methanogenesis rates of up to 2 ml/min/L
- corresponding to 1 A L<sup>-1</sup> current if H<sub>2</sub> supplied via electricity

Electrochemical reactors with the same strain as bubble bottle:

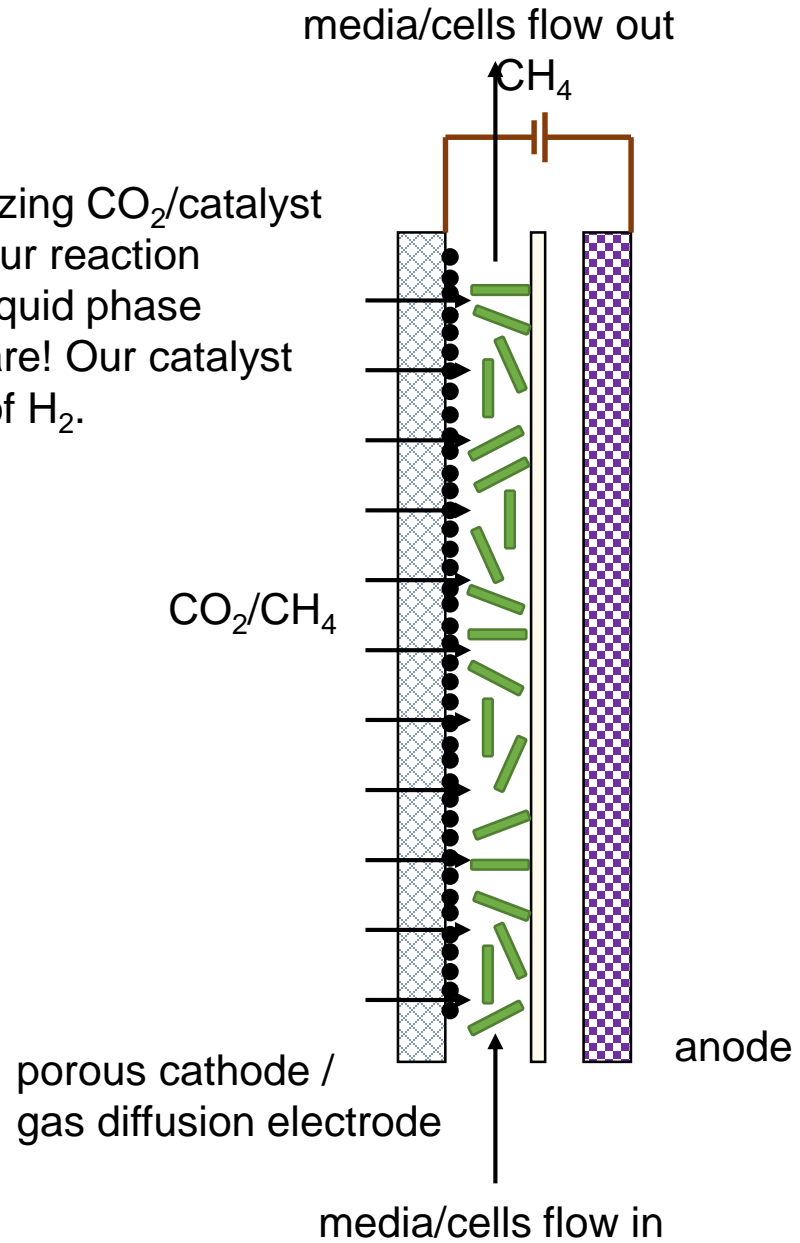
→ not working for more than a few hours

Electrochemical reactor with mixed enrichment from Delta Diablo:

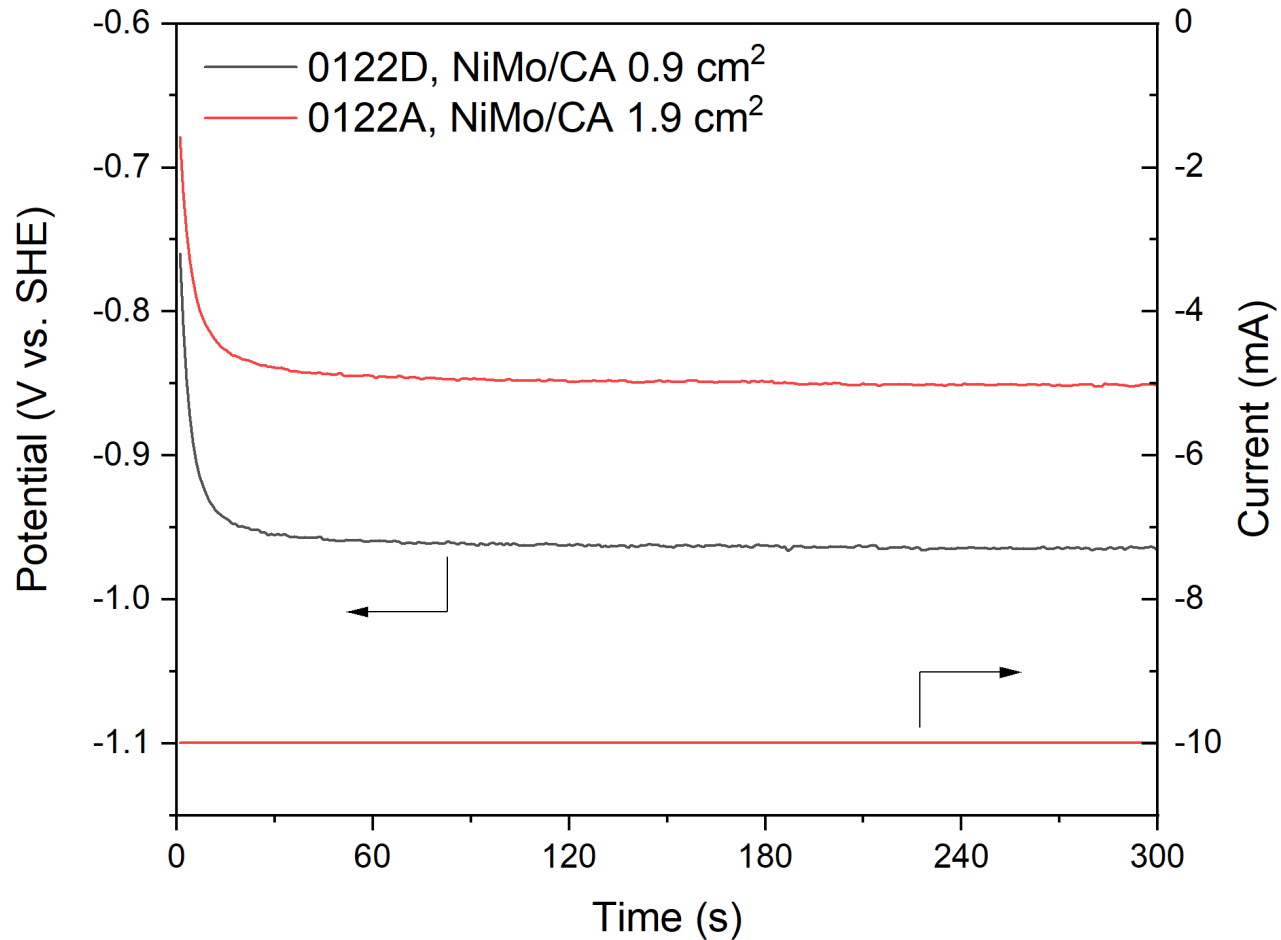
- 30°C
- bipolar membrane
- fed with 200 μl CO<sub>2</sub>/min (lowest our MFC is doing right now)
- 20 mA constant current (ca. 18 mmol e<sup>-</sup>/H<sup>+</sup> d<sup>-1</sup> = ca. 150 μL H<sub>2</sub> min<sup>-1</sup>)
- running for >1.5 months (two medium exchanges)
- hydrogen limited (increased stirring increased methane concentration)
- Slow growing?
- Outflowing gas: 50% H<sub>2</sub>, **11% CH<sub>4</sub>**



Good for maximizing CO<sub>2</sub>/catalyst interaction, but our reaction happens in the liquid phase where the cells are! Our catalyst is just a source of H<sub>2</sub>.



# Higher Surface Area Cathodes Require Less Energy



Potential required to achieve the same current is less negative for higher surface area materials – high surface area electrodes reduce the energy required to supply H<sub>2</sub> *in situ*



