Consortium for Computational Physics and Chemistry (CCPC)

WBS: 2.5.1.301/302/303/304/306

U.S. Department of Energy (DOE)
Bioenergy Technologies Office (BETO)
2017 Project Peer Review

Thermochemical Conversion

March 7th, 2017

Project Leads:

Jim Parks – ORNL
David Robichaud – NREL
Peter Ciesielski – NREL
Roger Rousseau – PNNL
Asanga Padmaperuma – PNNL
Bill Rogers – NETL
Madhava Syamlal – NETL
Rajeev Assary – ANL
Larry Curtiss - ANL

ChemCatBio Structure

Core Catalysis Projects

Catalytic Upgrading of Biochemical Intermediates
(NREL, PNNL, ORNL, LANL)

Liquid Fuels via Upgrading of Indirect Liquefaction Intermediates
(NREL, PNNL)

Fast Pyrolysis and Upgrading
(PNNL, ORNL)

Catalytic Fast Pyrolysis
(NREL, PNNL)

Recovering and Upgrading Biogenic Carbon in Aqueous Waste Streams
(PNNL, NREL)

Zeolites and Metal Oxide Catalysts

Supported Metal Catalysts

Cross-cutting Discussion Groups

Enabling Projects

Advanced Catalyst Synthesis and Characterization
(NREL, ANL, ORNL)

Catalyst Cost Model Development
(NREL, PNNL)

Consortium for Computational Physics and Chemistry
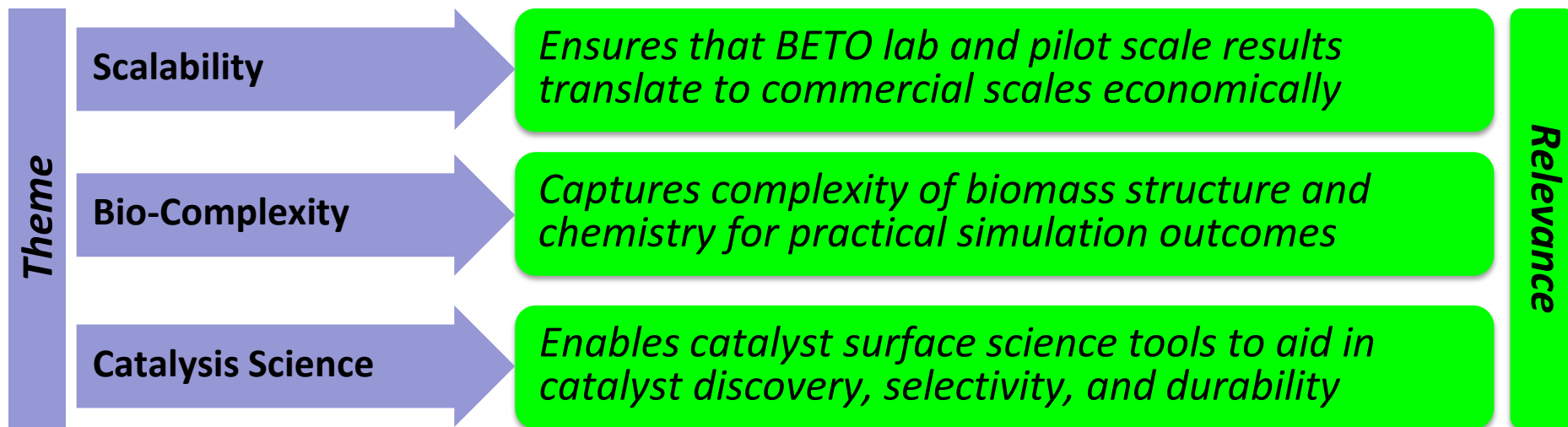(ORNL, NREL, PNNL, ANL, NETL)

Consortium Integration

- Core catalysis projects focused on specific *applications*

- *Collaborative* projects leveraging core capabilities across DOE laboratories

- *Cross-fertilization* through discussion groups

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Goal Statement

Accelerate progress on experimental BETO projects toward critical program verification goals and successful technoeconomic analysis (TEA) outcomes that result in economic sustainability of bioenergy by applying:

(1) **process and reactor models** that incorporate feedstock and catalyst properties, to guide reactor design and operation and inform and understand reactor scale up from lab, to pilot, to commercial scales; and

(2) **catalyst models** that provide active site energetics and entropics to guide the experimental design and discovery of next generation catalysts and improve durability and cost-effectiveness.

Theme		Relevance
Scalability	→	*Ensures that BETO lab and pilot scale results translate to commercial scales economically*
Bio-Complexity	→	*Captures complexity of biomass structure and chemistry for practical simulation outcomes*
Catalysis Science	→	*Enables catalyst surface science tools to aid in catalyst discovery, selectivity, and durability*

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Quad Chart Overview

Timeline

- Project start date: 10/1/2015
- Project end date: 9/30/2018
- Percent complete: 50%

Barriers addressed & Actions

- Ct-A. Feedstock Variability and Ct-F. Efficient High-Temp Deconstruction to Intermediates
  - *Feedstock dependent models coupled with reactor simulations to predict yield variations*
- Ct-H. Efficient Catalytic Upgrading
  - *Atomistic models of catalytic chemistry to accelerate the design of new materials; reactor modeling to determine optimal residence times*
- Ct-J. Process Integration
  - *Scalable reactor/process models that can be coupled to define integrated operations*

Budget

	FY15 Costs	FY16 Costs	Total Planned Funding (FY17-Project End Date)
DOE Funded	$3.3M	$3.2M	$6.3M

*FY17 operating budget reduced to $3.0M

Partners

- NREL (53%), ORNL (24%), ANL (10%), NETL (8%), PNNL (5%)
- ChemCatBio
- Feedstock Conversion Interface Consortium
- Integration and Scale Up Project (NREL)
- 9-member Industry Advisory Panel
- 5 Universities (list in Additional Slides)

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Project Overview

- The CCPC is a **consortium of BETO's modeling expertise** representing a hub for the computational needs for the biofuels program

- **The CCPC is a team with diverse applied computational expertise** where ideas, approaches, and findings can be discussed and advanced via cross-talk

- With modeling collaborations beginning in 2013, the CCPC is now mature with best practices being honed and shared across BETO

3-year Project Timeframe

FY13	FY15	FY16	⭐	Sept FY18	FY22
Collaboration Start	Peer Review		Review->"Go"	Verification	Verification

Objectives:

(1) Provide predictive simulation tools to enable BETO experimental teams to maximize yield and fuel chemistry based on reactor design, operational parameters, feedstock type, and feedstock particle size distributions during pilot scale verification

(2) Simulations of reactor scale up effects and predictive impact on linkage of BETO bench and pilot scale results to full plant TEA

(3) In conjunction with ChemCatBio, more rapid advancements in catalyst formulation and design that result in experimentally observed improvements (yield, selectivity, durability, lifetime, cost)
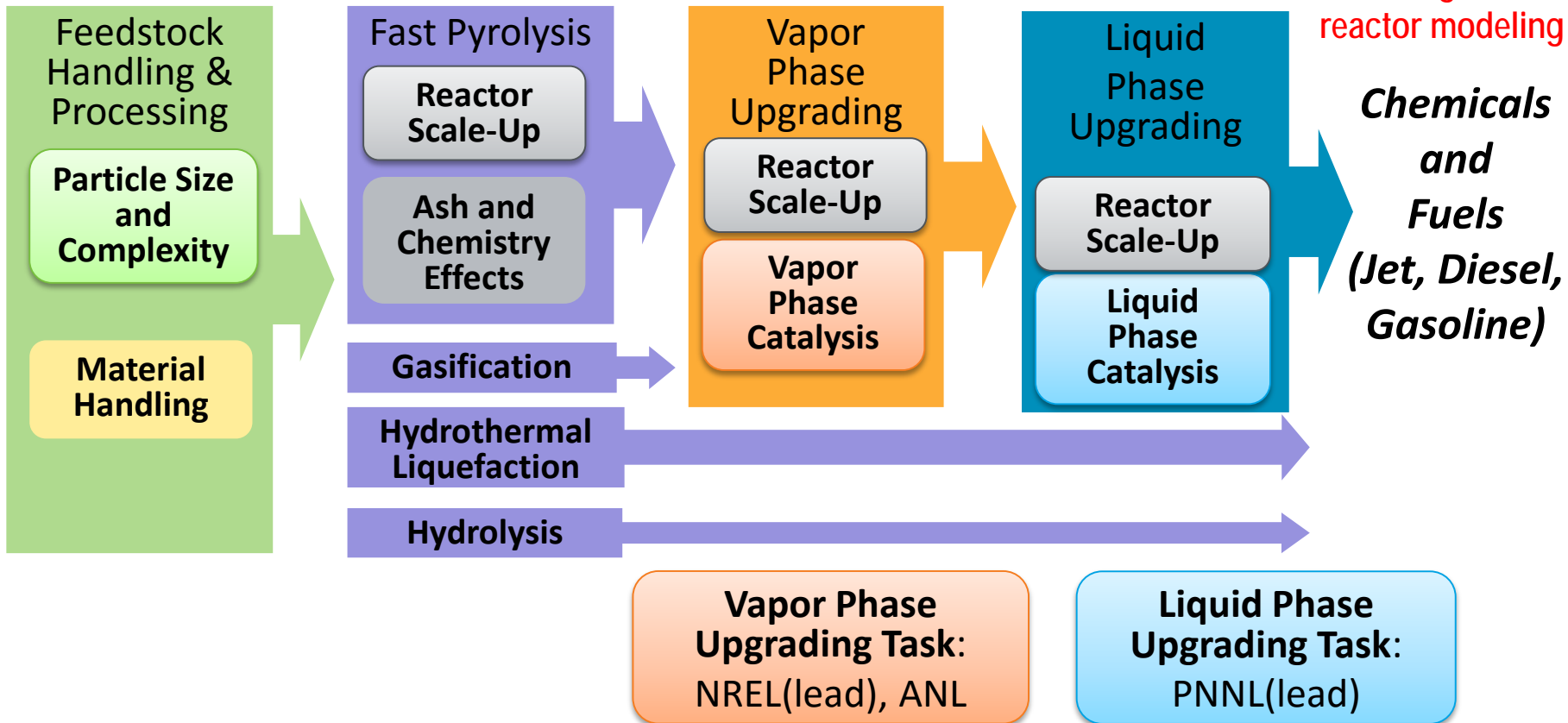
Note: more detailed timeline in additional slides

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Approach (Management): Technical tasks organized around conversion processes

Project Management: ORNL

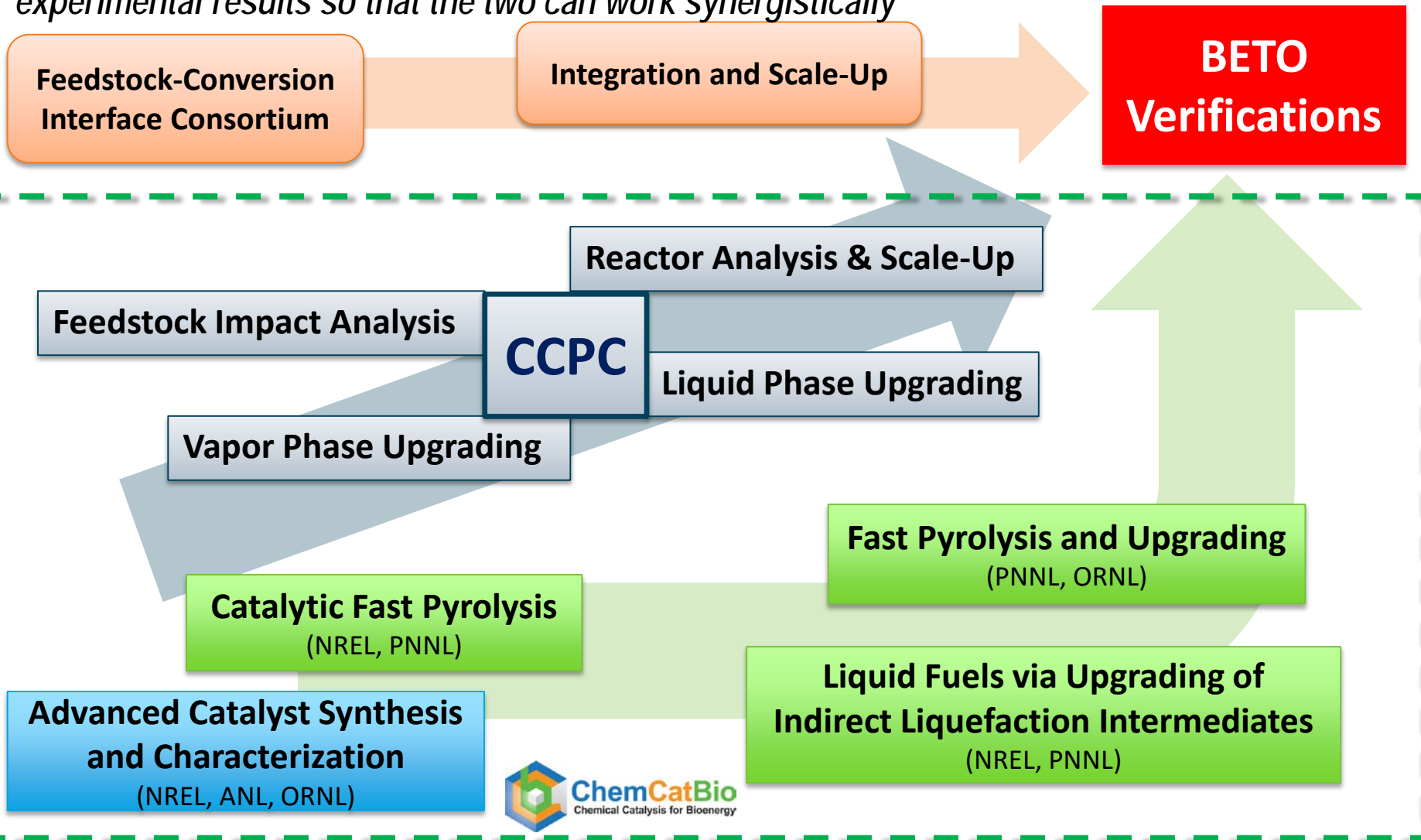**Feedstock Impact Analysis Task**: NREL(lead), ORNL

Reactor Analysis and Scale-Up Task: ORNL(lead), NETL, NREL, PNNL

NETL added in FY17 to strengthen reactor modeling

Feedstock Handling & Processing

Particle Size and Complexity

Material Handling

Fast Pyrolysis

Reactor Scale-Up

Ash and Chemistry Effects

Gasification

Hydrothermal Liquefaction

Hydrolysis

Vapor Phase Upgrading

Reactor Scale-Up

Vapor Phase Catalysis

Liquid Phase Upgrading

Reactor Scale-Up

Liquid Phase Catalysis

Chemicals and Fuels (Jet, Diesel, Gasoline)

Vapor Phase Upgrading Task: NREL(lead), ANL

Liquid Phase Upgrading Task: PNNL(lead)

Approach: 8 joint/linked FY17 milestones* with experimental teams highlight collaborations

8 joint/linked milestones address 2015 reviewer comment *"…tied directly to projects on experimental results so that the two can work synergistically"*

Feedstock-Conversion Interface Consortium

Integration and Scale-Up

BETO Verifications

Reactor Analysis & Scale-Up

Feedstock Impact Analysis

CCPC

Liquid Phase Upgrading

Vapor Phase Upgrading

Fast Pyrolysis and Upgrading
(PNNL, ORNL)

Catalytic Fast Pyrolysis
(NREL, PNNL)

Advanced Catalyst Synthesis and Characterization
(NREL, ANL, ORNL)

Liquid Fuels via Upgrading of Indirect Liquefaction Intermediates
(NREL, PNNL)

ChemCatBio
Chemical Catalysis for Bioenergy

*see additional slides for full list of milestones

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Project overview – Integrated approach

Establish an integrated and collaborative portfolio of catalytic and enabling technologies
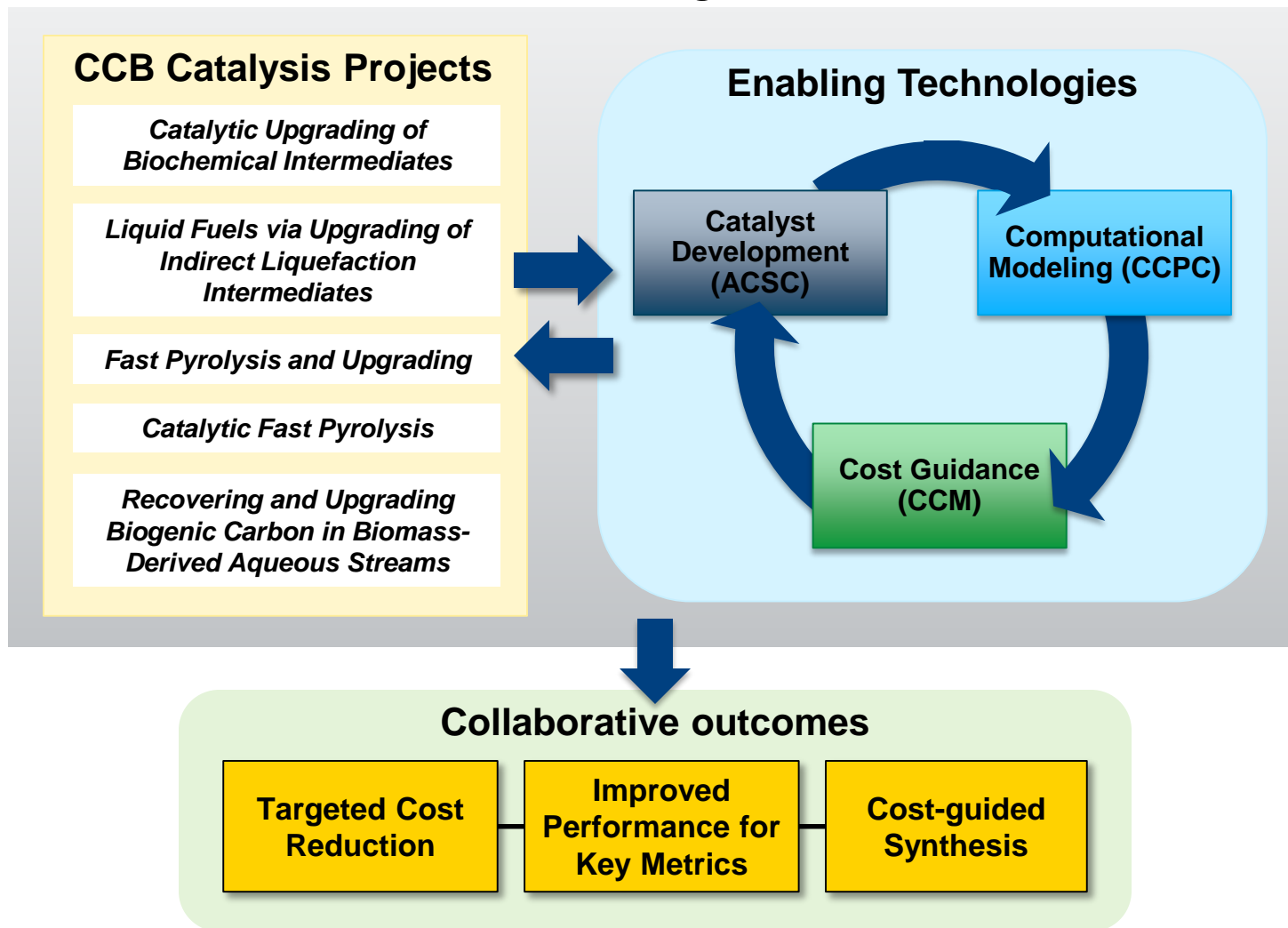
Approach: Exchange across technical community provides guidance, relevance, and direction

Inputs

Industry Advisory Panel: reviews detailed progress quarterly

ChemCatBio: experimentalist requests

Techno-Economic Analysis (TEA)

CCPC Technical Webinar Series: Academic experts

Communication in CCPC

Quarterly Face-to-Face meetings (location rotates among labs)

Monthly/bi-weekly telecoms (with full team, task teams, and experimental teams)

Public Outputs

Publications and Presentations: at peer review journals and core bioenergy conferences

CCPC Website: public outreach at cpcbiomass.org

Open-source Code: CCPC model code on GitHub

Industry Advisory Panel [*representing >100 years of combined experience*]

David Dayton (**RTI**), George Huff (**MIT, retired BP**), Jack Halow (**Separation Design Group**), Mike Watson (**Johnson Matthey**), Randy Cortright (formerly **Virent Energy Systems**), Richard Quann (**ExxonMobil**), Steve Schmidt (**WR Grace**), Tom Flynn (**Babcock & Wilcox**), Rick Wessel (**Babcock & Wilcox**)

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Approach: Focus on physics and chemistry that gives impactful tools to accelerate bioenergy processes

CCPC Focused Outcomes

- Biomass Particle Models
- Residence Time Distributions
- Surface Chemistry Energetics
- Reaction Kinetic Rates
- Coking and Fouling Rates

Critical Success Factors:
Our tools used by community to accelerate experiments and improve Techno-Economic Analyses

Python™ - www.python.org

GitHub - github.com

GitLab - about.gitlab.com

Git - git-scm.com

MATLAB® - www.mathworks.com

COMSOL Multiphysics®
www.comsol.com

C3M - mfix.netl.doe.gov/c3m

MFiX - mfix.netl.doe.gov/mfix

C3M
Carbonaceous Chemistry for Computational Modeling

MFiX DEM
MFiX TFM

Notable Tech Transfer
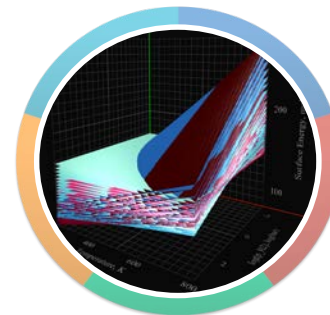
Surface Phase Explorer
spe.nrel.gov (public)

CSFMB©/CeSFaMB™
CCPC assisted Prof. de Souza-Santos in including biomass pyrolysis chemistry into new version of CSFMB© commercial software (Brazil)
www.csfmb.com

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Technical Approach: Challenges and Success Factors

Process Modeling

Challenge

Enable vastly diverse biomass feedstock to be modeled *efficiently* across scales of processes to maintain yield and selectivity from bench to commercial scale

Critical Success Factors

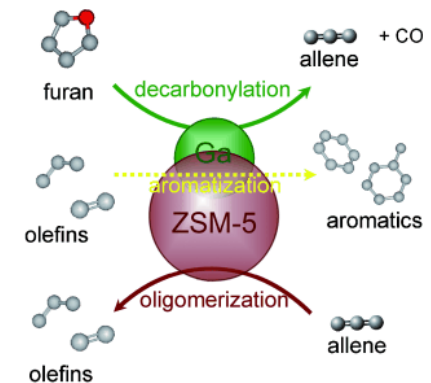Models that capture feedstock *complexity* and accurately predict reactor performance *at multiple scales*

Catalysis Modeling

Challenge

Develop tools to *quickly* determine catalyst structure and surface chemistry reactions to enable synthesis of improved catalysts

Critical Success Factors

Predictions and testable hypotheses that *accelerate* ChemCatBio's synthesis of new catalysts with improved lifetime, activity, & selectivity

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Technical Approach: Complex realism to effective simplicity

Complex effects of biomass particles captured in low-order particle models for use in reactor scale models

Complex, 3D particle model

Results fit to low-order model

Low order particle model that capture complex behavior

Reactor-scale model

Resulting reactor models enable scalable prediction of pyrolysis yield

2" Fluidized Bed Reactor

DCR Fluidized Bed Reactor

TCPDU Entrained Flow Reactor

0.5 kg/hr

2 kg/hr

15 kg/hr
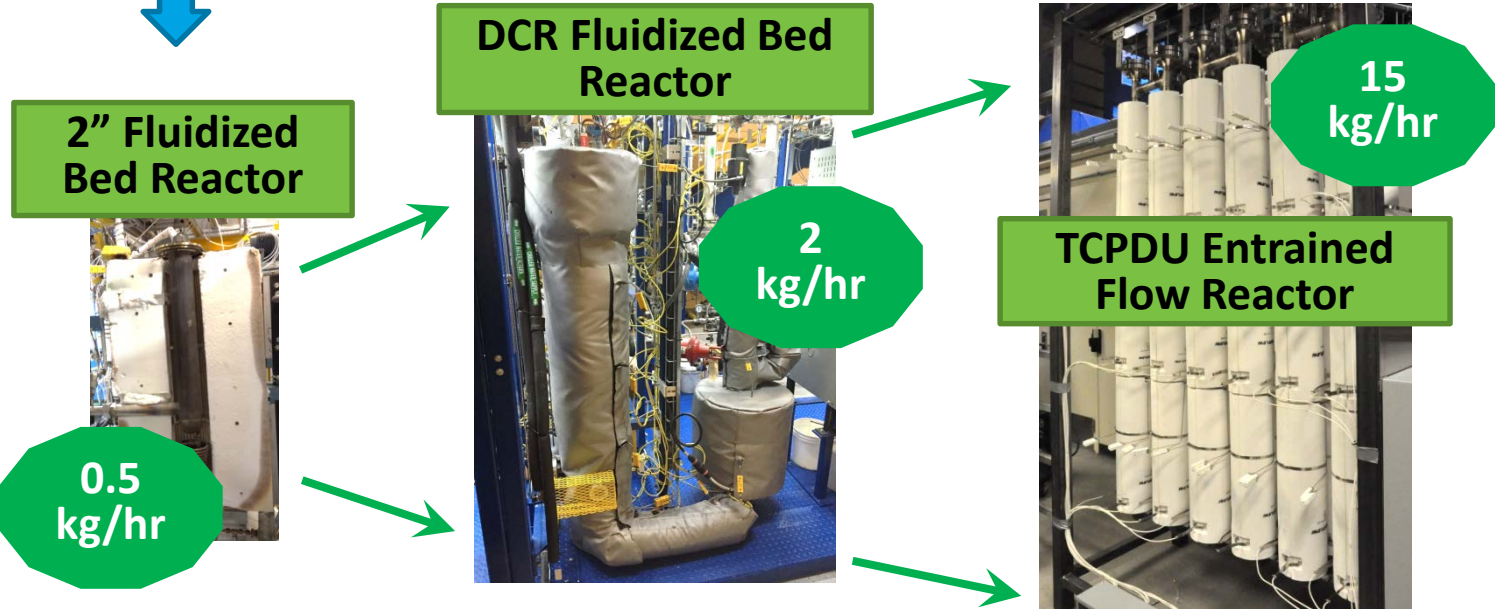
All Three Reactors at NREL

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Accomplishments: Reduced order particle models capture biomass complexity in practical form for reactor models

Objective: Develop reduced order biomass particle models to facilitate integration with reactor-scale simulations.

Accomplishments:
- Performed sensitivity analysis using fully-resolved 3D models to determine which complexities are most impactful
- Developed fast, 1D model that replicates behavior of 3D models using effective particle dimensions and properties

Relevance:
The reduced order particle models enable reactor-scale simulations over 100x faster while still capturing effects from biomass complexity

Time=0 Surface: Temperature (degC)

0.5 mm poplar particle

2 mm poplar particle

Temperature (°C)

Model from direct XCT reconstruction

Model with explicit, simplified microstructure

Model with similar shape and bulk volume

Spherical model with similar bulk volume

Increasing computational speed

Increasing accuracy
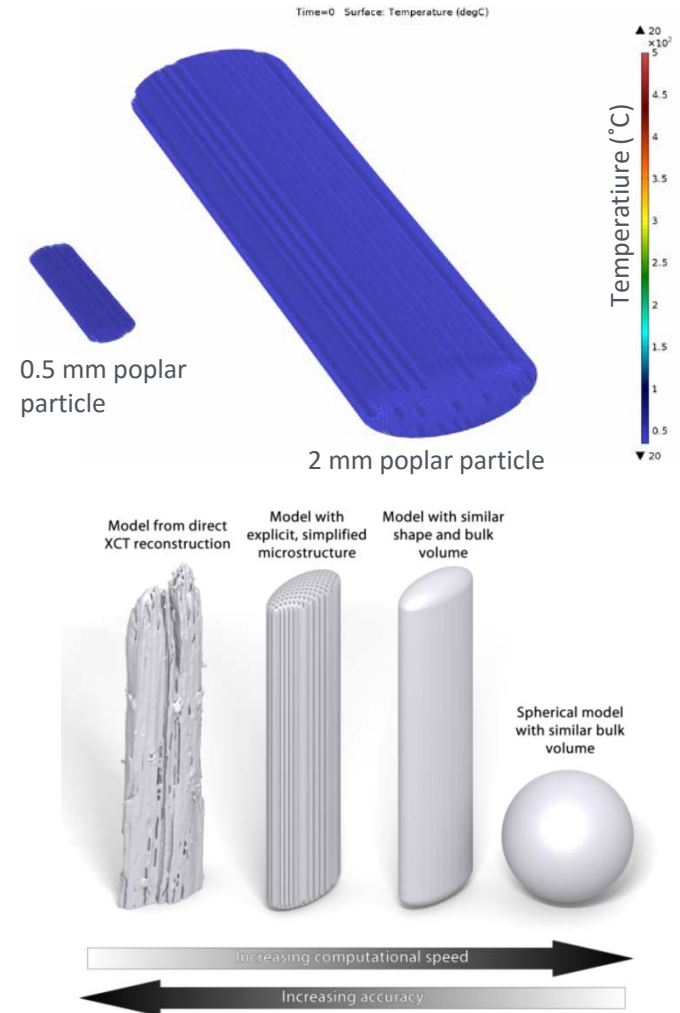
Top: Heating transfer simulation for poplar particles of 2 different sizes.
Bottom: visualization of order-reduction in biomass particle modeling

Biomass Feedstock → **Pyrolysis** → **Vapor Phase Upgrading** → **Liquid Phase Upgrading**

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Accomplishments: Optimal residence time predicted based on feedstock-specific parameters

Objective: Predict optimal residence time (i.e., time of peak tar yield) as a function of feedstock-specific parameters

Accomplishments:

• Coupled heat transfer, mass transfer, fluid dynamics, and chemical reaction for particle scale models of fast pyrolysis

• Simulations account for important process variables such as **particle size, shape, biomass species, moisture content, and reactor temperature**

• Provides estimates of time-resolved product evolution

Above: Simulation of product evolution during pyrolysis of a ~3 mm pine particle at 500 °C.
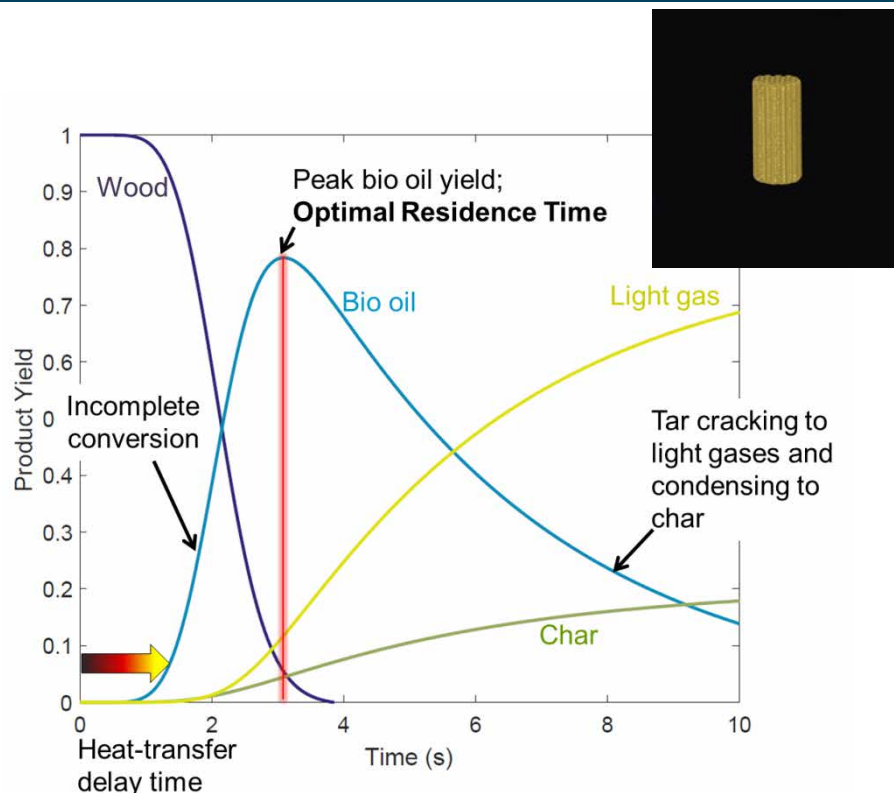
Relevance: Simulations provide estimates of optimal operating conditions, including reactor temperature and residence time, for pyrolysis experiments.

Biomass Feedstock → Pyrolysis → Vapor Phase Upgrading → Liquid Phase Upgrading

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Accomplishments: Low-order reactor model captures multiphase residence time distributions

Objective: Predict product yields (gas, tar, char) from fast pyrolysis of biomass particles in a bubbling fluidized bed reactor.

Accomplishment: Constructed low-order reactor mixing models to estimate residence times of biomass particles and the resulting oil yield.

Bubbling fluidized bed reactor at NREL for biomass fast pyrolysis experiments.

Reactor simulated with different levels of mixing.
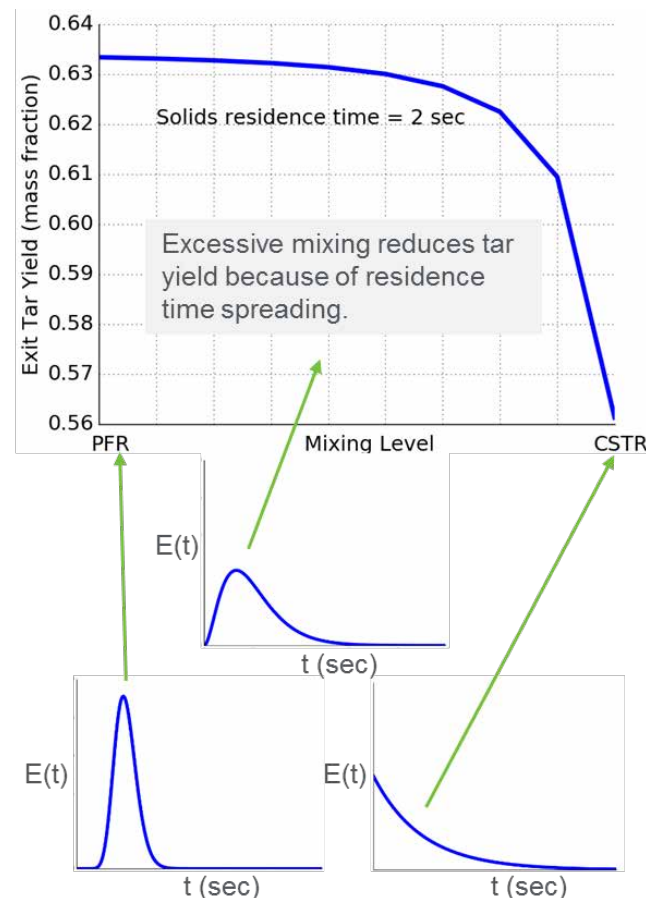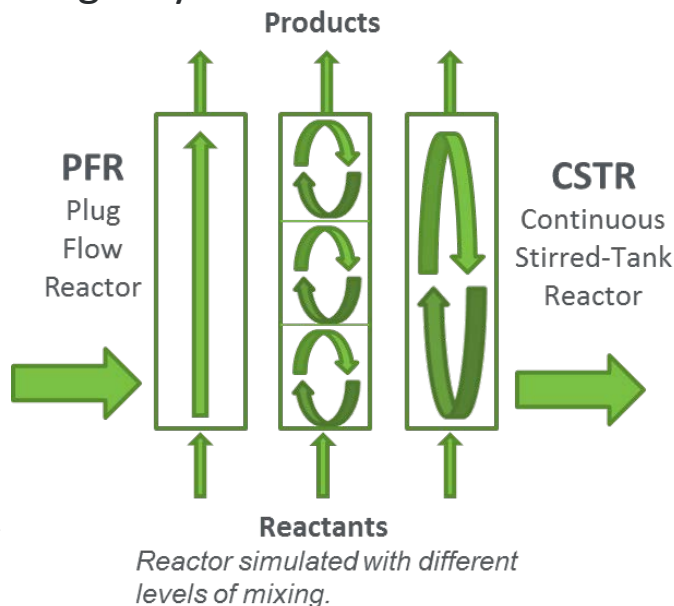
Residence time distributions as a function of time for different mixing regimes.

Relevance: Computationally efficient and scalable approach provides accurate residence time distribution for predicting pyrolysis yield.

Biomass Feedstock → Pyrolysis → Vapor Phase Upgrading → Liquid Phase Upgrading

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Major Accomplishments: Combined particle and reactor models to predict accurate yields for two different feedstock size distributions
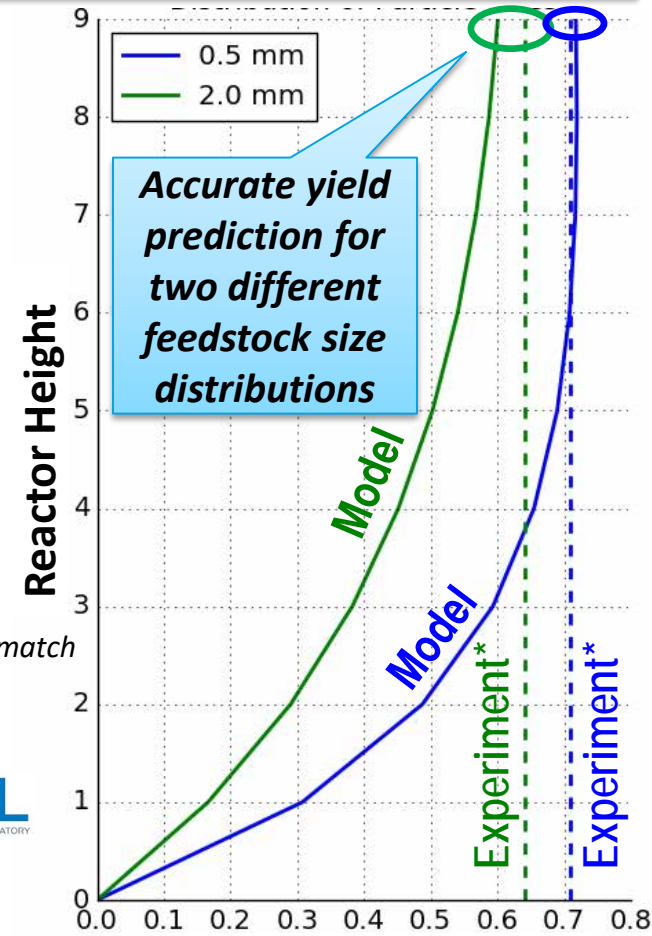
Accomplishments:

- Combined particle and reactor simulations
- Validated pyrolysis model for 2" fluidized bed reactor against two different particle size distributions and moisture contents of pine with FCIC experimental team
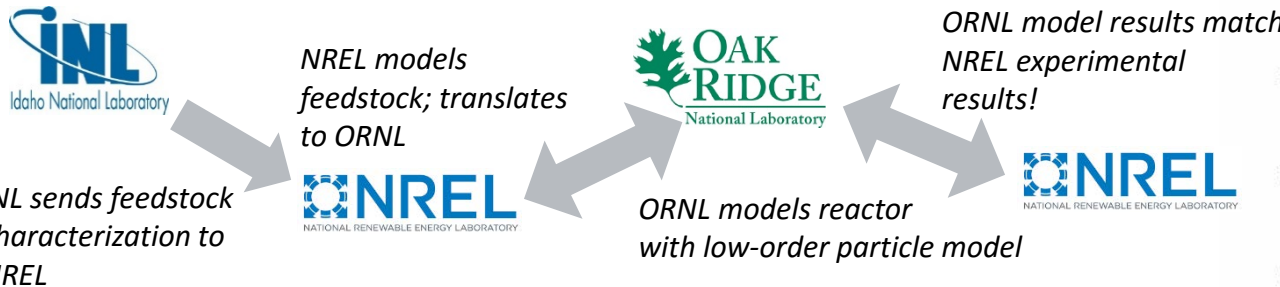
Relevance: Coupled multiscale simulations predicted bio-oil yields within 2% of experimental error.

- drive out-year experimental design and process optimization in FCIC
- inform scale up between 0.5 kg/hr bench and 15 kg/hr pilot systems.

Cross-cutting NL-NL and modeling-experimental collaboration and workflow

INL sends feedstock characterization to NREL

NREL models feedstock; translates to ORNL

ORNL models reactor with low-order particle model

ORNL model results match NREL experimental results!

CCPC Publication: Ciesielski, Wiggins, & Daw in <u>Fast Pyrolysis of Biomass</u>, eds. Robert Brown & Kaige Wange. In press

Yield Predictions for 0.5 mm and 2.0 mm Particle Size Distribution (PSD) Ensembles

Accurate yield prediction for two different feedstock size distributions

Legend: 0.5 mm, 2.0 mm

Y-axis: **Reactor Height**
X-axis: **Yield (mass fraction)**
data from NREL 2"FBR reactor

Biomass Feedstock → Pyrolysis → Vapor Phase Upgrading → Liquid Phase Upgrading

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Accomplishments: Catalyst packing geometry can be used to optimize flow path and minimize fouling

Objective: Reduce fouling of hydrotreating reactor

Accomplishments:

- Porosity and permeability in a tubular down-flow reactor have been shown to affect multi-phase flow in wall region
- Channeling from the high porosity of the bed at the wall creates hydrogen-rich and hydrogen-starved zones → gunking occurs in the latter
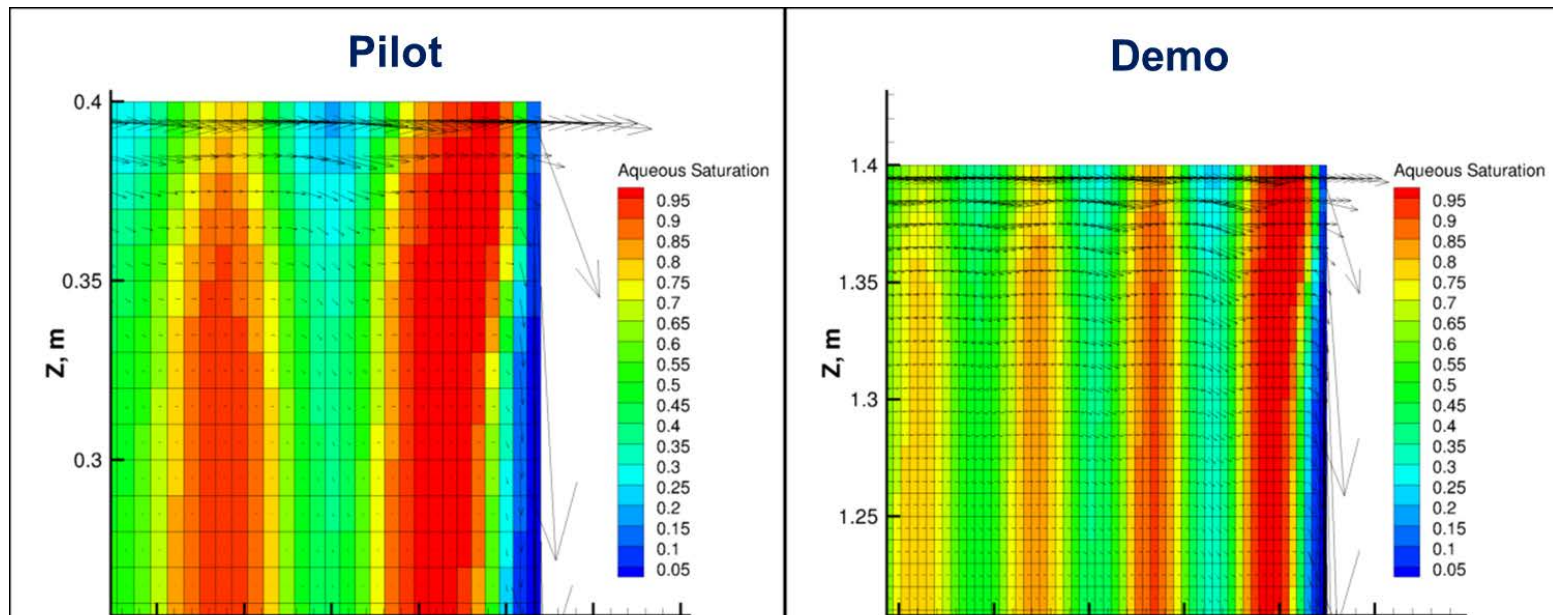
Relevance: Reactor engineering shows pathways to minimize maldistribution which can reduce hydrogen consumption and minimize fouling processes

Biomass Feedstock → Pyrolysis → Vapor Phase Upgrading → **Liquid Phase Upgrading**

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Relevance: Process Modeling: Bio-Complexity & Scalability

Pine (softwood)   Poplar (hardwood)   Corn stover (grass)

2 mm   2 mm   2 mm

Models capturing complexities of particle size, shape, speciation, and chemistry

Reactor models capturing multiphase flows and residence times

yield

t (sec)

2" Fluidized Bed Reactor

0.5 kg/hr

DCR Fluidized Bed Reactor

2 kg/hr

TCPDU Entrained Flow

15 kg/hr

Scalable Yield Optimization
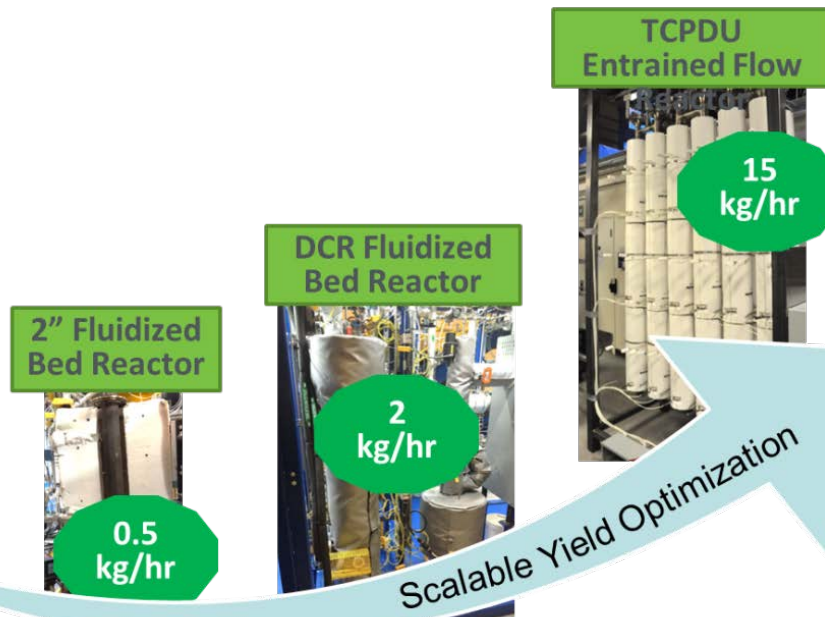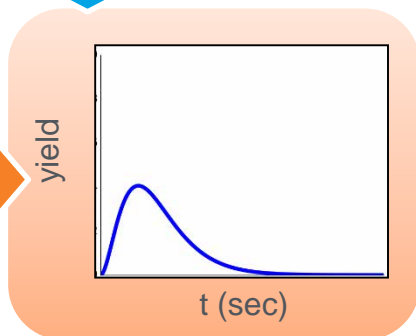
Relevance to BETO and Industry:

The models developed in the CCPC provide a 'window into the reactor'. This enables the BETO platform and industry to:

- Troubleshoot issues with reactors as they arise, reducing system downtime
- Conduct commissioning of new systems more efficiently
- Facilitate scale-up of processes and new catalyst formulations from the bench to pilot scale
- Methodology is being used to extend modeling success to *in situ* and *ex situ* CFP

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Future Work: Biomass particle models advancing for pelletized/crushed and blended feedstocks

- Pelletization alters microstructure and intra-particle transport behavior
  - We are developing particle models for pelletized feedstocks based on micro X-ray computed tomography data (with Colorado School of Mines)
- Particle models also advancing for blended feedstocks for verification
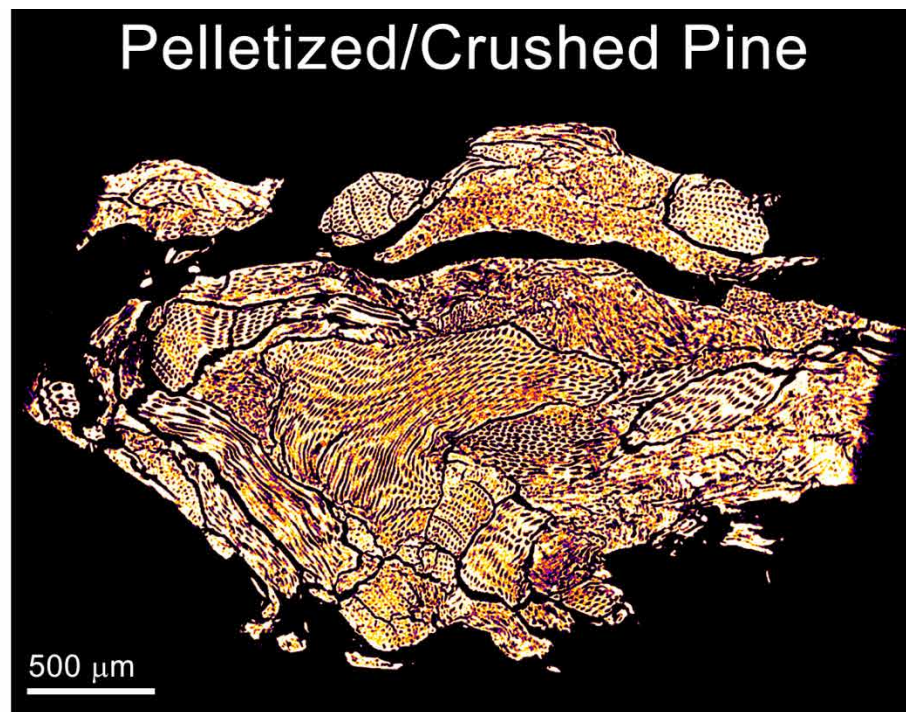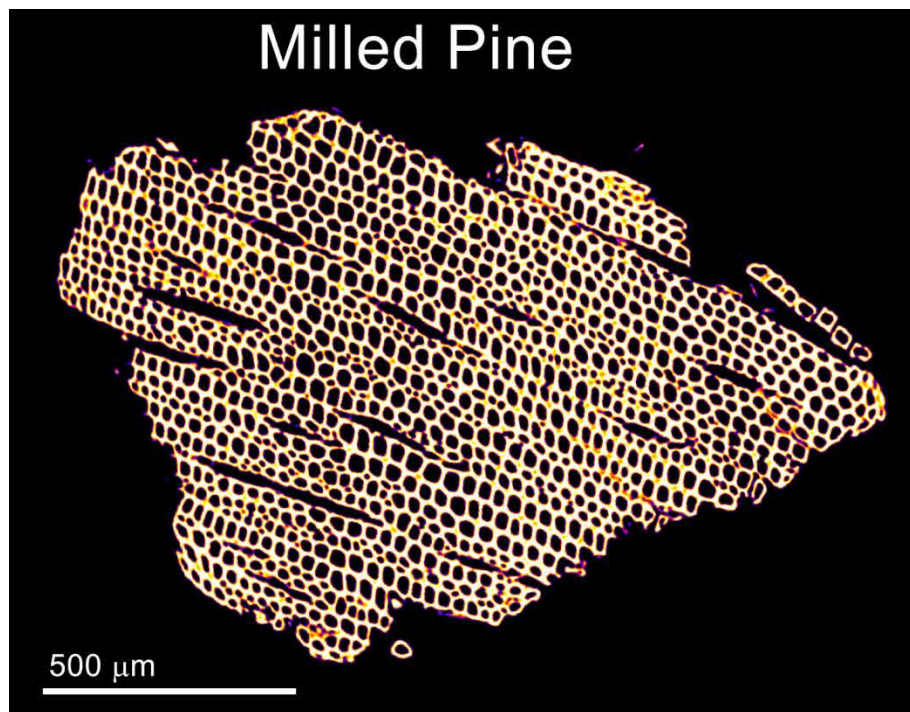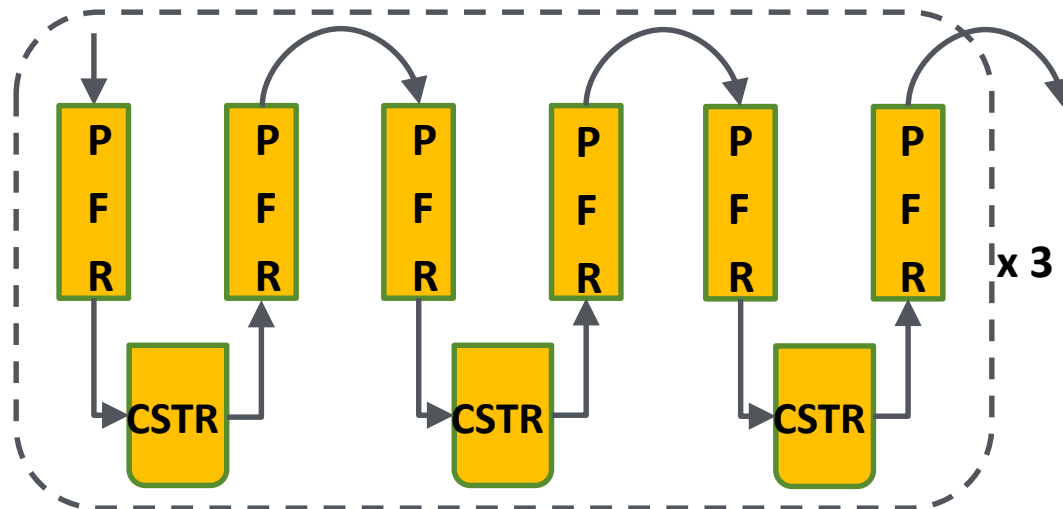

Images: B. Kappes (CSM), P. Ciesielski (NREL)

Annual Milestone LINKED with Integration and Scale-Up project (WBS 2.4.1.301)

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Future Work: Scalability - extend low-order pyrolysis model to TCPDU Entrained Flow Reactor
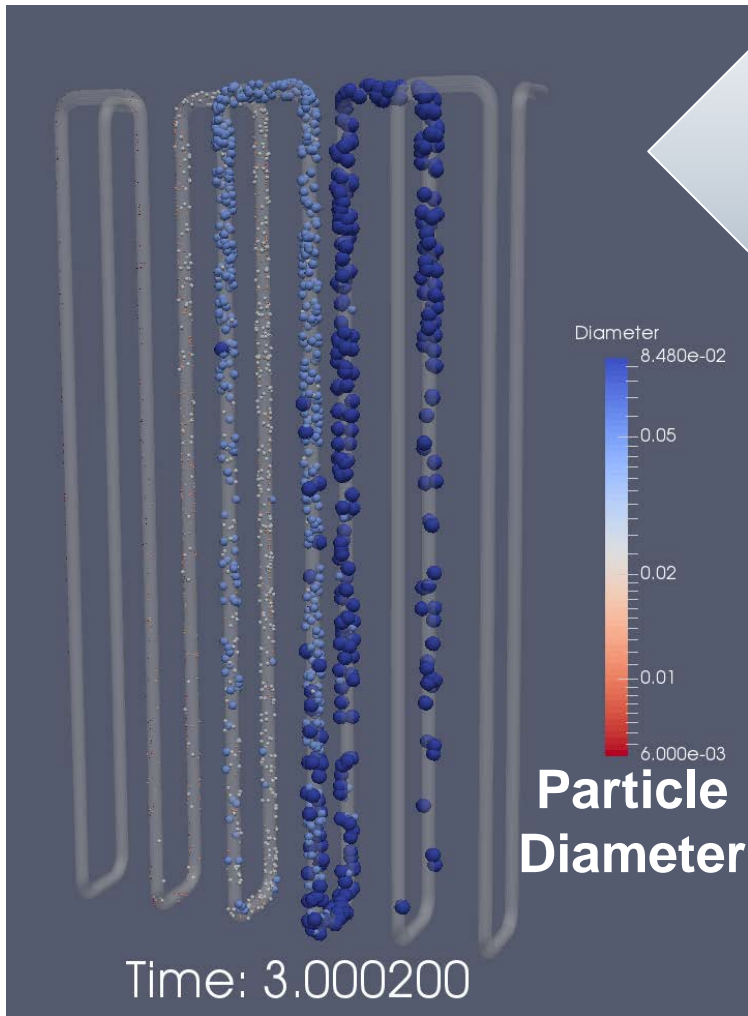
Larger size biomass particles have higher residence times due to reactor geometry
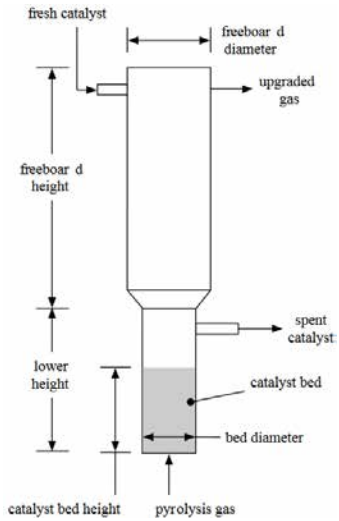*Note: for visualization, particles shown at 50x diameter (relative to reactor scale)*

Progress to-date: MFiX-DEM model (left) of Entrained Flow Reactor to determine residence time distributions for low-order model (below)

Diameter
8.480e-02

0.05

0.02

0.01

6.000e-03

Particle Diameter

Time: 3.000200

x 3

Annual Milestone LINKED with Integration and Scale-Up project (WBS 2.4.1.301)

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Future Work: Developing scalable upgrading reactor models to support verification success

2" Fluidized Bed Reactor Upgrader*

Davison Circulating Riser (DCR) Reactor*

TCPDU R-Cubed Upgrader*
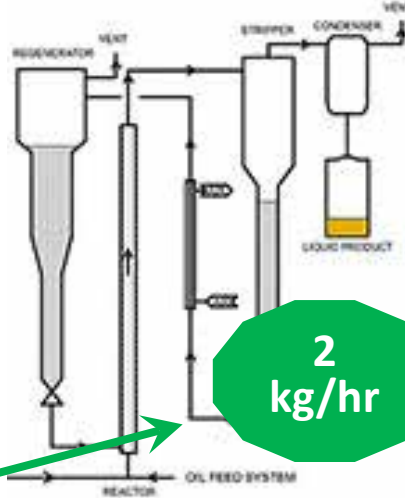
15 kg/hr

2 kg/hr

0.5 kg/hr

WR Grace
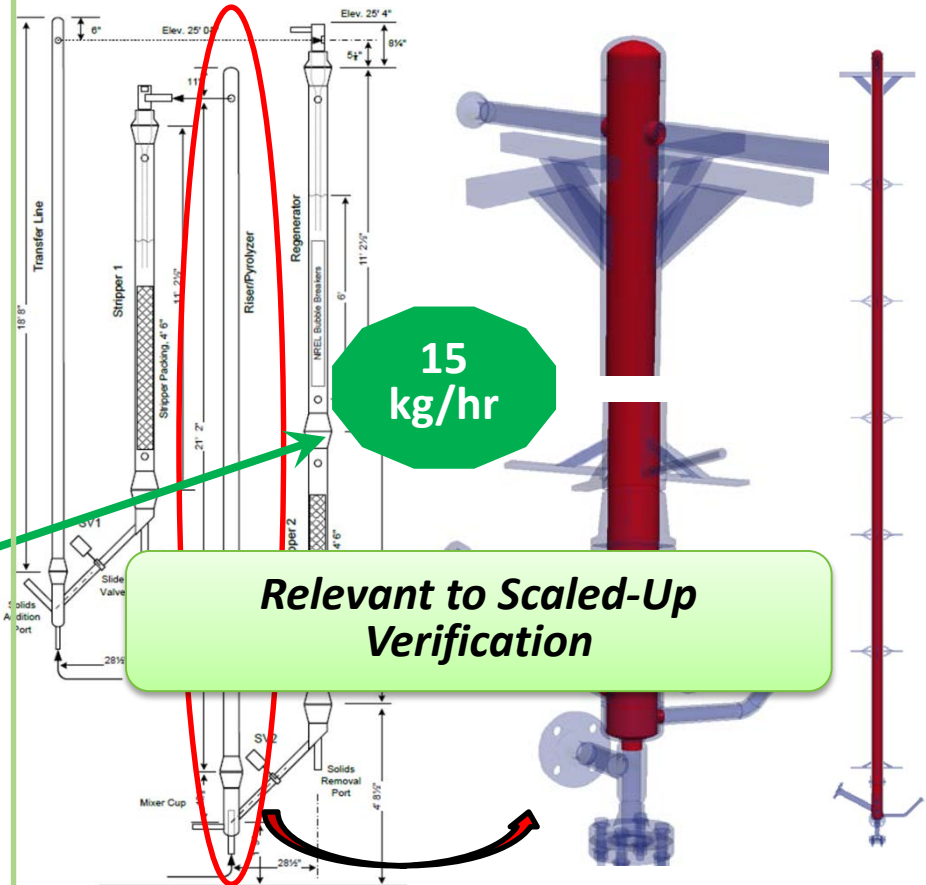
Relevant to Scaled-Up Verification

PSRI (redesign)

Relevant to new BETO catalysts

Relevant to Industry

Computational Domain in Red

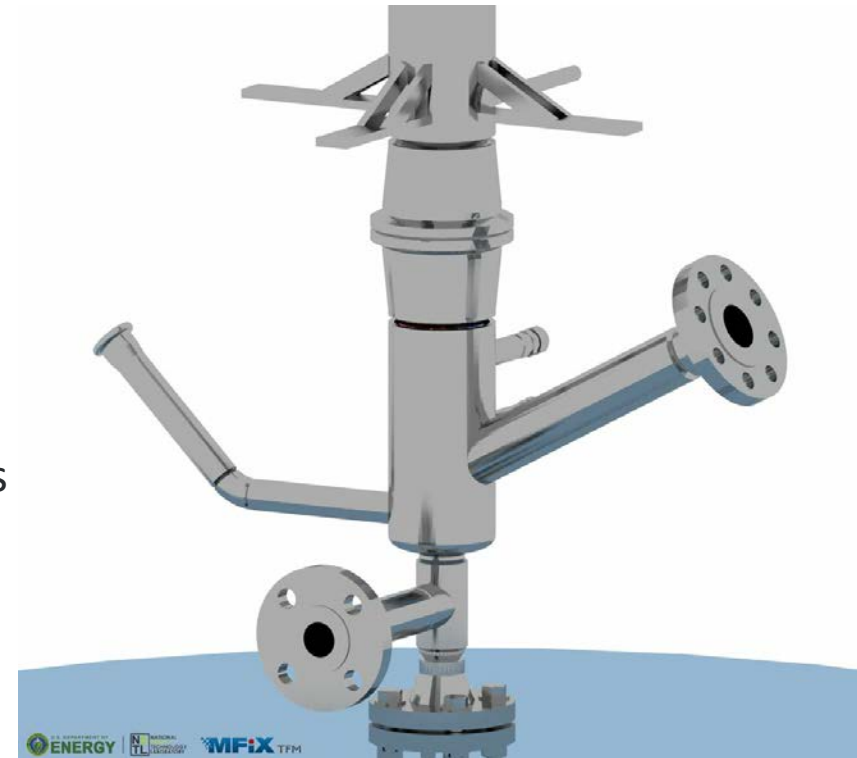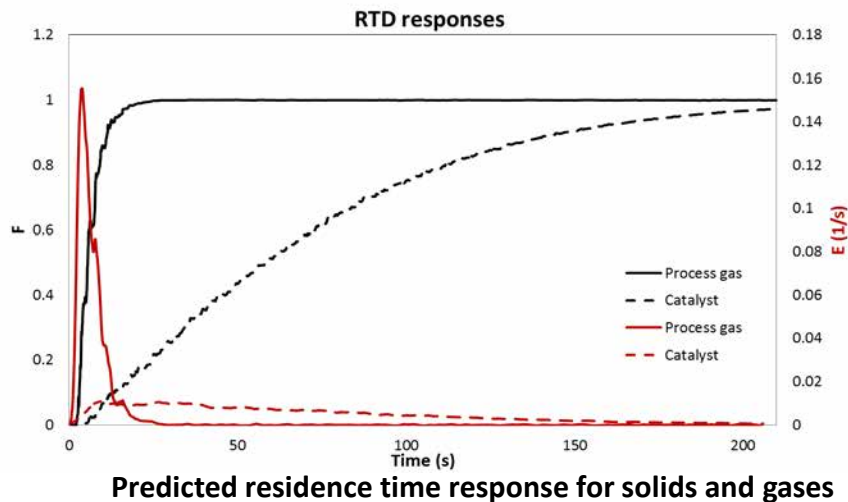**Stretch Annual Milestone LINKED with Integration and Scale-Up (WBS 2.4.1.301)**

All (3) Reactors at NREL

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Objective: Accelerate commissioning of R-cubed riser reactor.

Accomplishments:

- Constructed initial R-cubed model in MFiX based on collaboration with Integration and Scale Up
- Currently using model to investigate impact of process conditions on residence time distributions of pyrolysis gases and catalyst solids

Predicted residence time response for solids and gases

Relevance: Simulations provide expectations on reactor performance *prior* to commissioning. Will enable faster commissioning and optimization.

Stretch Annual Milestone LINKED with Integration and Scale-Up (WBS 2.4.1.301)

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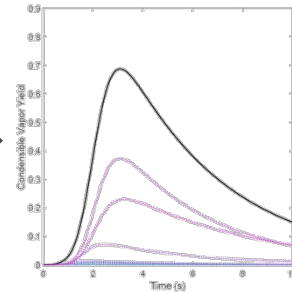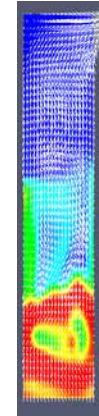# Technical Approach: Challenges and Success Factors

Process Modeling

Challenge

Enable vastly diverse biomass feedstock to be modeled *__efficiently__* across scales of processes to maintain yield and selectivity from bench to commercial scale

Critical Success Factors

Models that capture feedstock *complexity* and accurately predict reactor performance *at multiple scales*

Catalysis Modeling

Challenge

Develop tools to *quickly* determine catalyst structure and surface chemistry reactions to enable synthesis of improved catalysts

Critical Success Factors

Predictions and testable hypotheses that *accelerate* ChemCatBio's synthesis of new catalysts with improved lifetime, activity, & selectivity

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Technical Approach: Catalyst Models Cover Range of Materials

Mixed metal phosphides characterization

- Catalytic upgrading of pyrolysis products
- Correlate H and CO absorption energies with experimental observations to guide new catalyst discovery

Structural design of zeolites

- ChemCatBio
- Determine impact of explicit mesopores on mass transport in zeolites

Supported metal catalyst design

- ACSC & IDL
- Design structure function relations to enhance HDO over metal catalysts

Tailoring dopants in zeolites

- CFP and Aqueous Reforming
- Design catalysts with improved activities and test these hypothesis

Controlling solvophilicity

- FP + upgrading
- Reduce gunking in HT reactors

RuSn active phase identification

- Catalytic Upgrading of Sugars
- Identify opportunities to avoid poisoning of catalysts by Ni

Active phase for Cu-Beta hydrogenation

- ACSC & IDL
- Enhance alkane activation and increase yields of diesel/jet fuels from IDL

Understanding Mo_2C coke from batch to continuous feed

- ChemCatBio (CFP) & ACSC
- Comparing H and aromatic absorption to answer experimental observation of coke formation under different reaction conditions
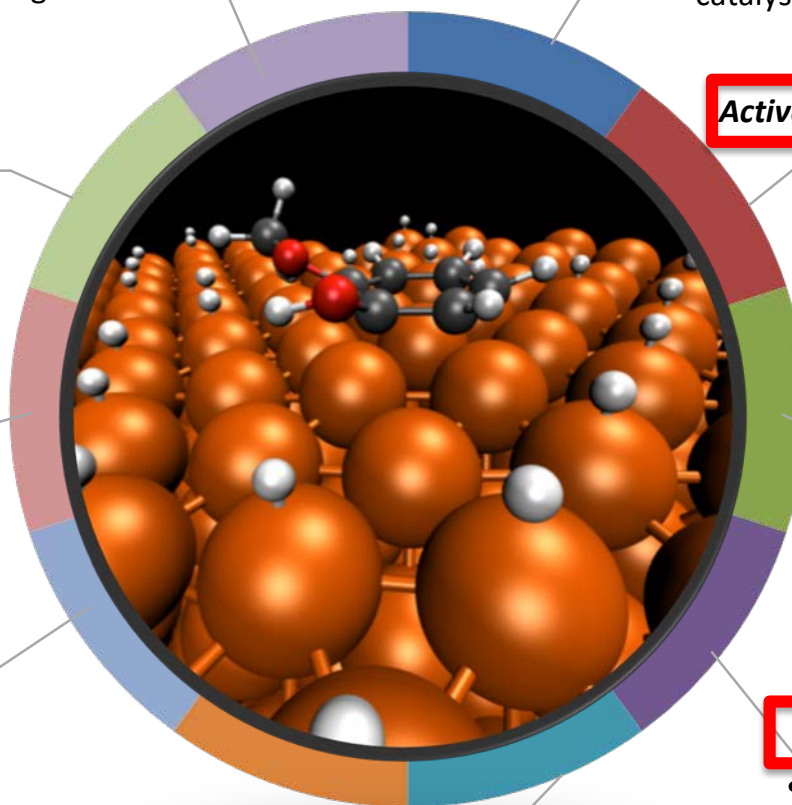
Optimize catalytic activity of Mo_2C

- ChemCatBio (CFP)
- Reactivity of Ni* or /Ca* doped Mo_2C surfaces towards hydrogenation - 'Carbon-Carbon' coupling balance in the vapor phase
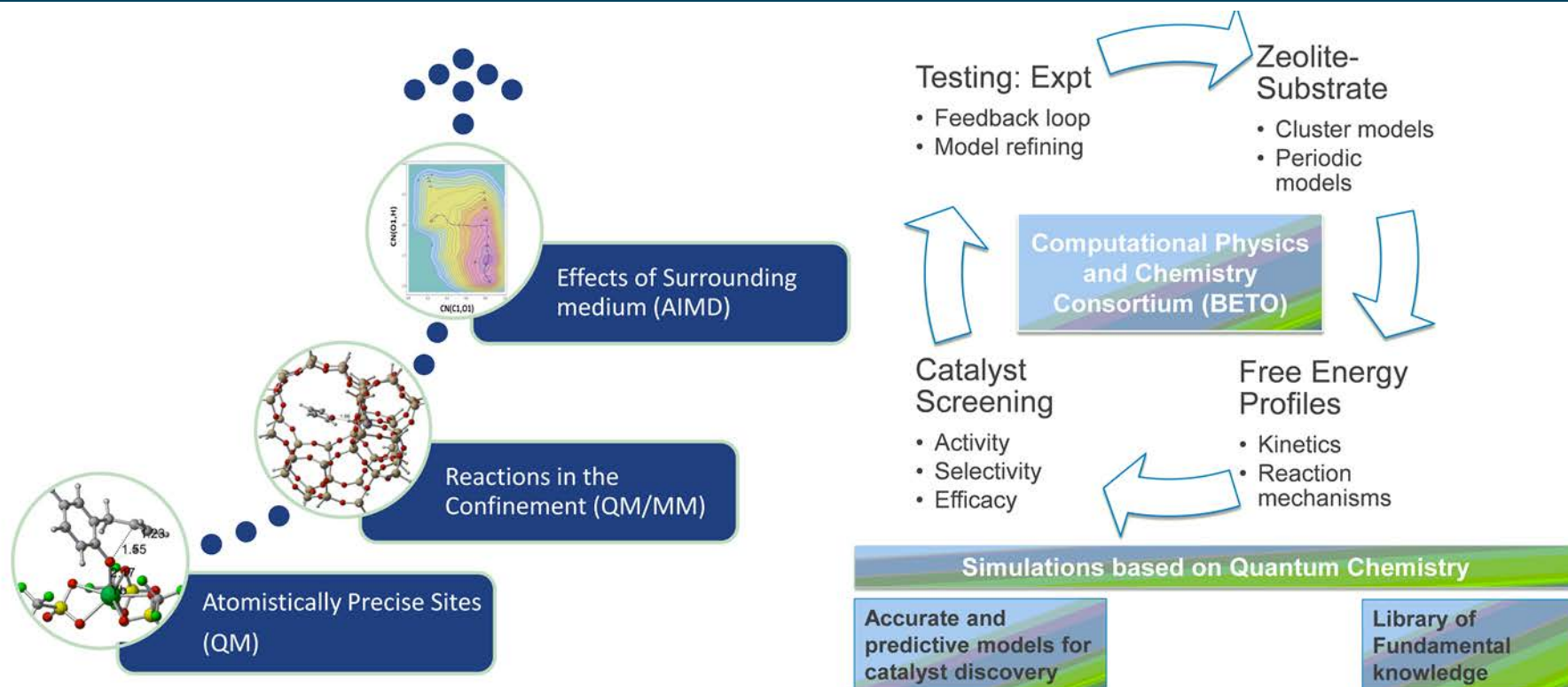
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Technical Approach: Models for Catalysis Design

Atomistic simulations using static to dynamic models to support CCB:

- *Understand* catalyst activity and yield selectivity
- *Guide* new catalyst syntheses (ACSC)
- *Optimize* reactor conditions

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Accomplishments: Designing more effective Mo_2C catalysts

Objective: Provide guidelines to improve the Mo_2C catalysts for the upgrading of bio-oil

Accomplishment:
- Developed DFT models of Mo_2C and Ni/Mo_2C catalytic sites
- Investigated thermodynamics and kinetics of sorption and desorption of intermediates (O, OH, H_2O) on various sites
  - crucial step in the deactivation of catalysts

Presence of Ni improves stability of Mo_2C via decreasing catalytic deactivation
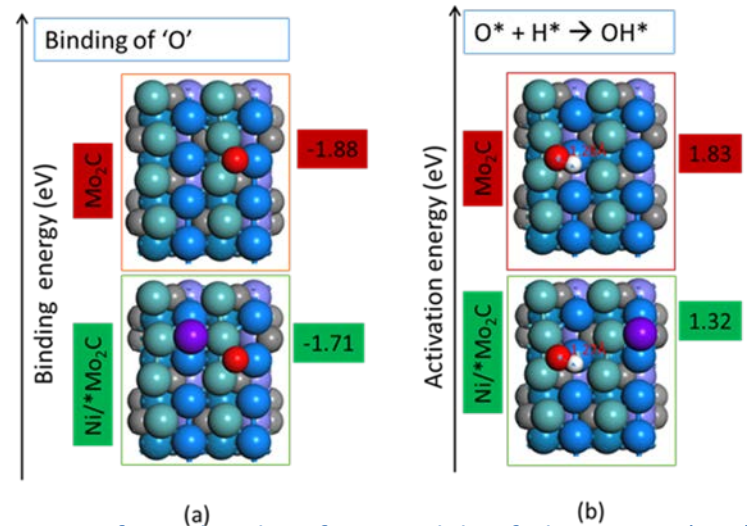
Schematic of simulated surface models of clean $Mo_2C(100)$ and Nickel doped Mo_2C catalysts for (a) binding energies of 'O' and (b) activation energy required to form OH species in the gas phase

Relevance: Screening a wider parameter space of dopants to improve catalysts by promoting desired reactions (deoxygenation, C-C coupling) will reduce catalyst discovery time and cost.

Biomass Feedstock → Pyrolysis → **Vapor Phase Upgrading** → Liglid Phase Upgrading

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Accomplishments: Identified active site and mechanism for C4 product upgrading with beta zeolite

Objective: With IDL and ACSC identify the active site structure responsible for low-temperature alkane activation in Cu-Beta.

Accomplishment:

- Using DFT, identified the location, oxidation state, and reactivity of isobutane dehydrogenation over Cu-Beta

- In isolated Al-acid sites, copper is located in the wall of the straight channels of Beta zeolite in the +1 oxidation state – consistent with experimental results.

- Model predicts if framework aluminums are located in pairs, Cu(II) would be the preferred active site with all barriers below the exit channel (ideal situation).
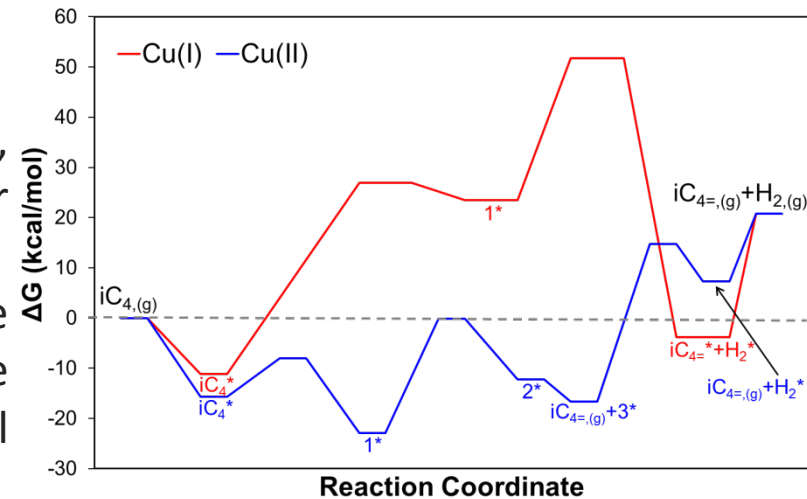
Comparison of Cu(I) – 1 Al, and Cu(II) – 2 Al sites for dehydrogenation of isobutane in Cu-Beta

Relevance: Consistency between modeling and experiment has set the groundwork for computationally guided catalyst design. Recent work[1] suggests that Al-pairing can be tuned over a wide range and opens this up as a potential new knob in the synthesis toolbox going forward.

[1]Pashkova, J. *Chemistry - A European Journal* **2016,** 3937.

Biomass Feedstock → Pyrolysis → Vapor Phase Upgrading → Liquid Phase Upgrading

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Accomplishments: Developed a tool for identifying catalytic surfaces under reaction conditions

Objective: Develop a quick-turnaround tool that can show the thermodynamic state of a catalyst surface under experimental reaction conditions.

Accomplishment:
- Developed a web-based tool (Surface Phase Explorer,[*] www.spe.nrel.gov) that can provide phase diagrams and absorption profiles under reaction conditions
- Focus on thermochemistry reduces computational costs, resulting in quick turnaround for experimental teams (weeks, not months).
- SPE is being used (or has been used) on 6 different projects to date – both biochem and thermochem applications.
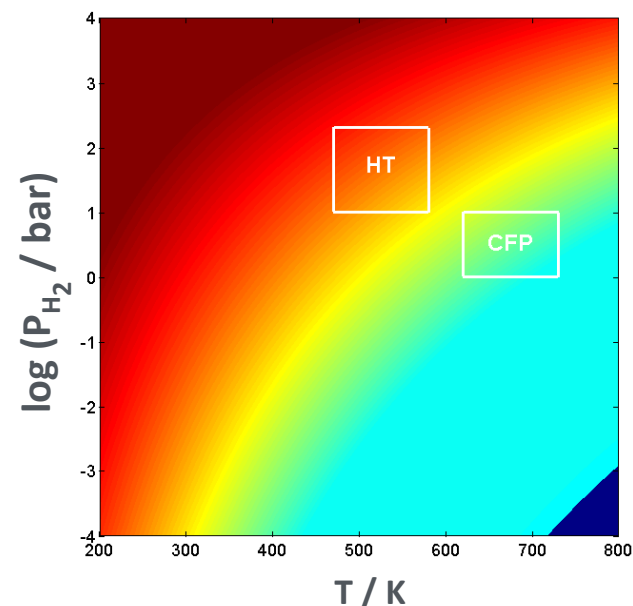
Hydrogen coverage on Rh_2P. Boxes highlight experimentally relevant regimes.

Relevance: Reduced computational costs and fast turnaround allows the CCPC to impact multiple catalyst design projects without worry of resource dilution. This capability brings computational modeling one step closer to being a standard tool in the catalyst designers toolbox akin to NH_3 TPD or X-ray characterization techniques.

Biomass Feedstock → Pyrolysis → **Vapor Phase Upgrading** → Liquid Phase Upgrading

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Accomplishments: Providing in-silico diffusivity measurements for porous materials

Objective: Develop a rapid use model of zeolite mass transport for use by experimental partners

Accomplishment:
- Developed an effective method for computationally measuring diffusivity in micro and mesopores of zeolites
- Method has been used to determine diffusivity of multiple pyrolysis-relevant species
  - Cannot be experimentally determined
- Constructed catalyst particle models (similar to biomass particle models) that can be used for screening of conditions and inclusion of coking/pore blocking
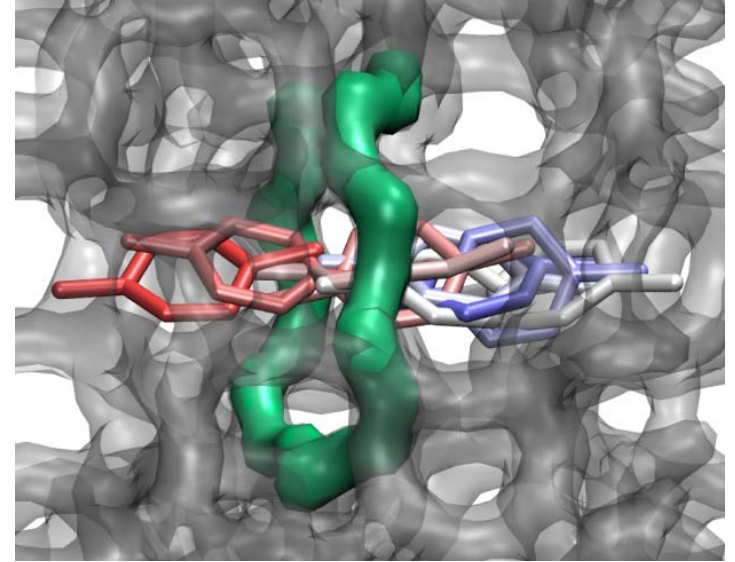
Frame depicting the transport of xylene through a pore in HZSM-5.

Relevance: Zeolites are ubiquitous in catalysis, yet mass transport in these systems is poorly explored. The combination of the modeling scales will provide an efficient means of investigating mass transport, including guiding synthesis to include mesopores to maximize access to catalytic sites and reduce mass loss to coking.

Biomass Feedstock → Pyrolysis → **Vapor Phase Upgrading** → Liquid Phase Upgrading

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Accomplishments: Control of catalyst solvophilicity can improve conversion

Objective: Optimize catalyst conversion by controlling solvophilicity of catalyst surface

Accomplishment:

- Simulated the kinetics and thermodynamics of catalysts in multicomponent solvents with sufficient detail to capture conversion dependence on
  - Temperature and composition of fluid phase
  - Composition of the support (hydro or lipophilic)
  - Size of metal particles

lipophilic   hydrophilic

Relevance: Project has motivated and guided a cross-laboratory effort to synthesize (ACSC/NREL) new catalysts with controlled solvophilicity which will be tested in hydrotreating reactors (CCB/PNNL) to gauge impact on fouling

Biomass Feedstock → Pyrolysis → Vapor Phase Upgrading → Liquid Phase Upgrading

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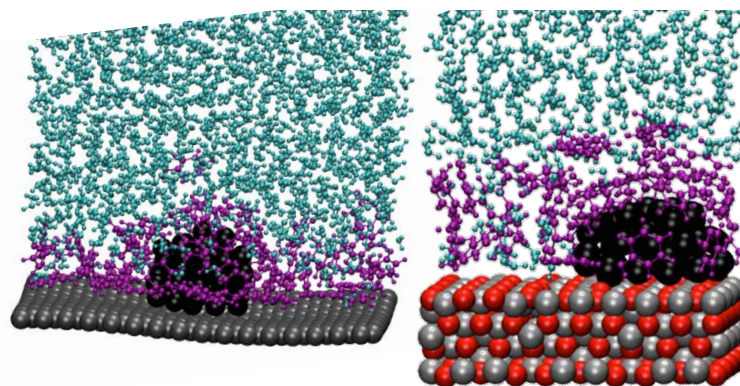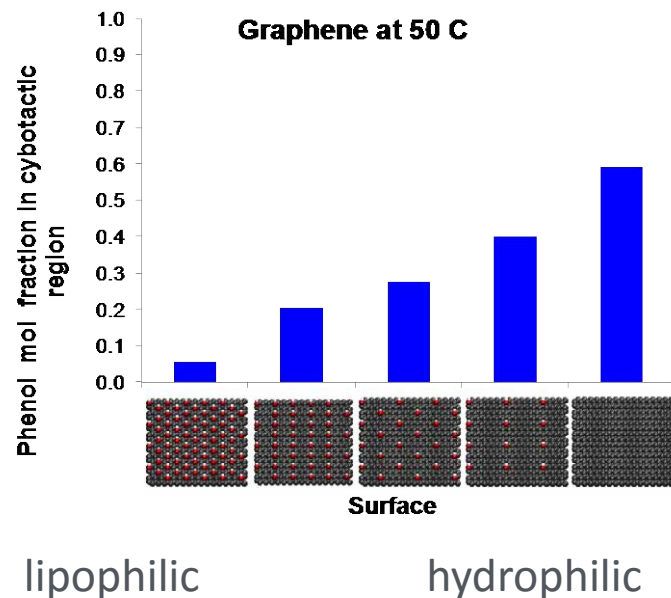
Relevance: Catalyst modeling accelerates discovery

Collaborative projects with ChemCatBio result in:

Understanding of catalyst active sites (structure-function relations) and deactivation/fouling mechanisms

Tool development that has led to faster turnaround and higher impact on experimental projects
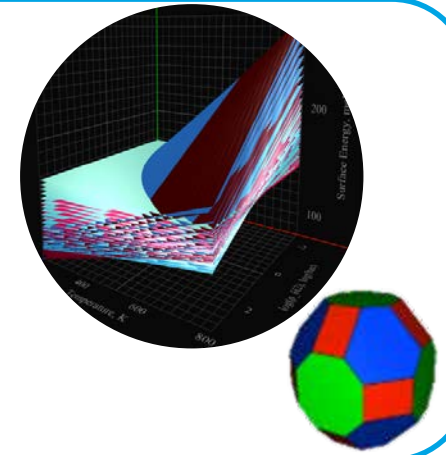
Guiding catalyst discovery through testable hypotheses
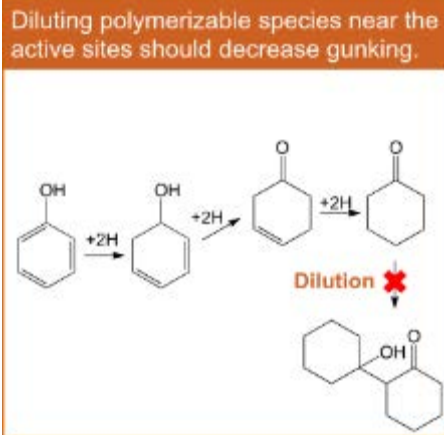
Process optimization based on computationally derived kinetics and mass transport that can link catalyst design to reactor models
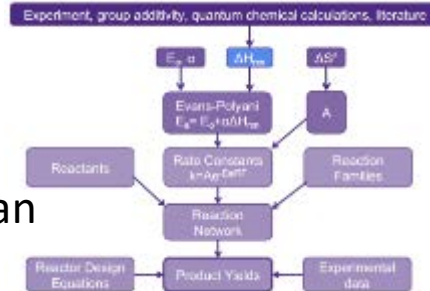
Modeling accelerates catalyst discovery for lower cost, more durable catalysts

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Future Work: Enhancement of zeolites with Lewis metals to tailor reactivity

- Investigate influence of extra-framework Lewis metals on catalyst reactivity on both Brønsted and Lewis reactivity

Possible interactions between Lewis and Brønsted reactive centers.
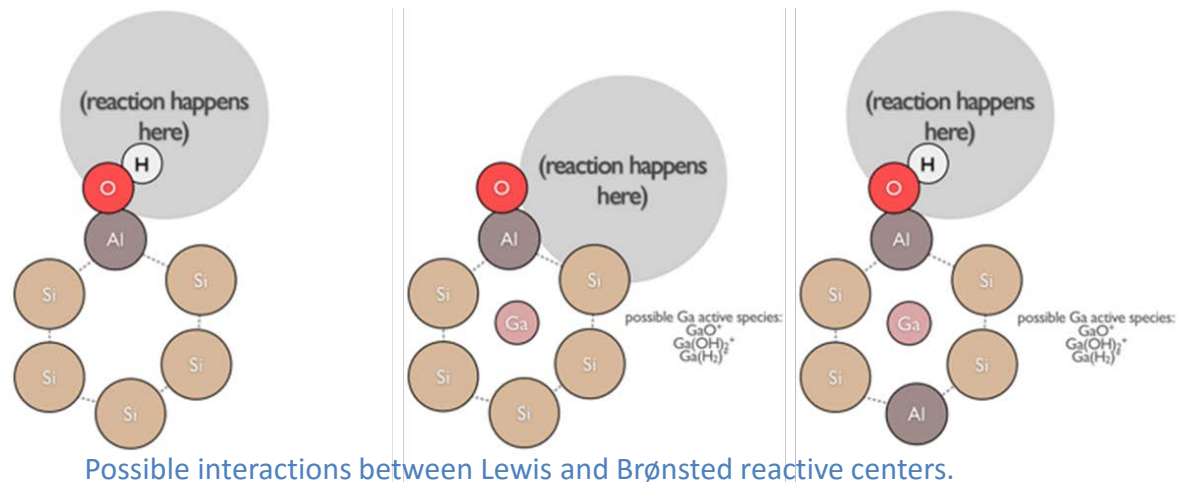
- Develop database of model reactions to increase responsiveness to new experimental requests

Ga – enhanced reactivity for sugar decarbonylation.
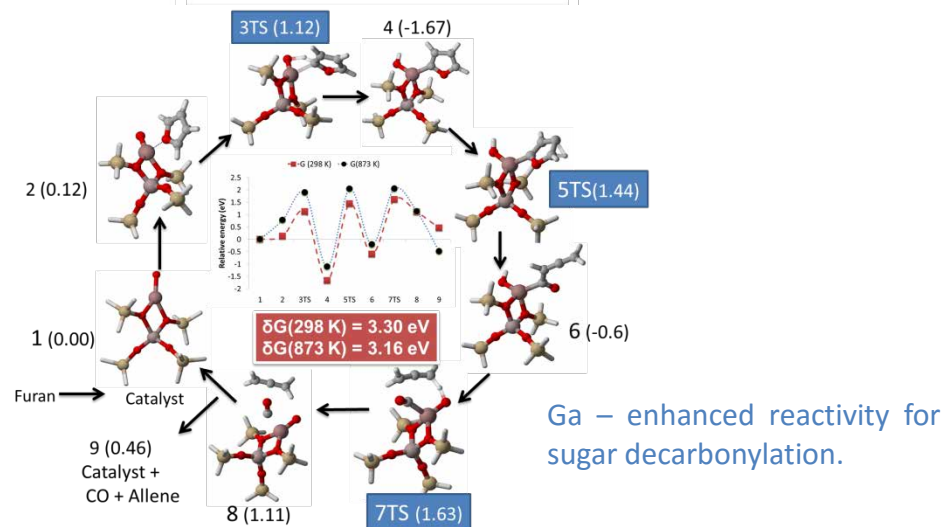
Quarterly Milestone Linked to FY18 ChemCatBio Milestones

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Future Work: Catalysis modeling of complex liquid phase upgrading

- Construction of **ab-initio** microkinetic models for LPU including
  - Particle size and support effects
  - Temperature effects
  - Species concentration

- Positions us for reactive CFD on bench and demo scale with higher fidelity than can be achieved with macrokinetics

- Direct comparison of theory predictions with experiment, 2nd generation model for enhanced performance and refined hypotheses

- The data can be used to avoid Edisonian serial research
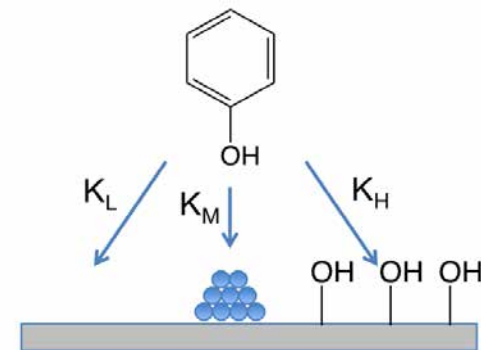
$$\frac{K_M}{K_L} \simeq 3 \ll \frac{K_M}{K_H} = 70$$
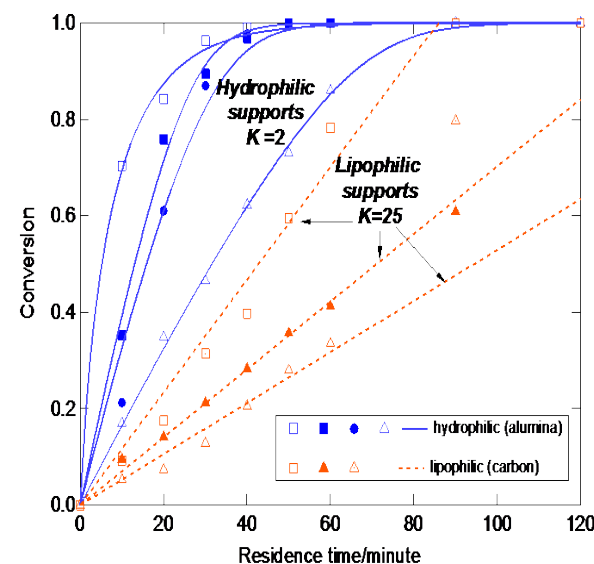
Quarterly Milestone supporting Liquid Phase Upgrading experiments

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Future work: Multiscale modeling of zeolite transport and deactivation to enhance access to active sites

Molecular Scale

Micro/Meso Scale

Whole-Particle Scale

ACSC

CCPC

10 nm

3 µm

250 µm

D_{gas}

D_Z

Bulk vapor-phase transport

Darcy's Law

Molecular dynamics to estimate D_Z

FEM simulations reaction/diffusion to estimate permeability

FEM Simulations reaction/convection/diffusion with Darcy's Law
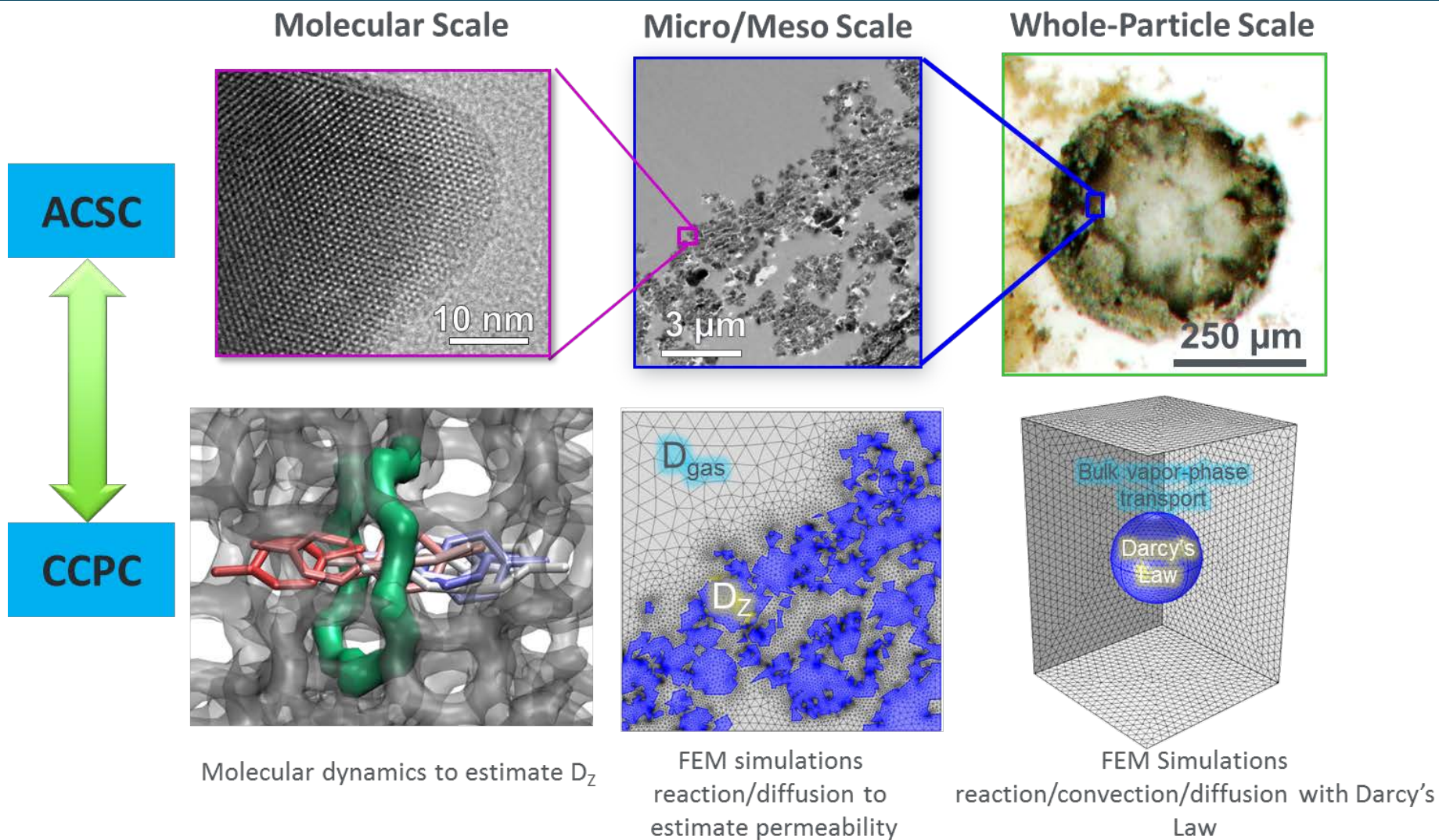
Quarterly Milestone LINKED to Milestone on Advanced Catalyst Synthesis and Characterization

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Summary: Models span scale and complexity to accelerate cost-effective biomass-to-fuel processes

Approach: key inputs from Industry Advisor Panel and technical community plus close-coupling to experimentalists enables success

Feedstock Handling & Processing	**Fast Pyrolysis**	**Vapor Phase Catalysis**	**Liquid Phase Upgrading**	***Chemicals and Fuels (Jet, Diesel, Gasoline)***
Particle models ensure diverse feedstock blends can efficiently be utilized	Critical residence times & kinetics enable scalability of reactor designs	Surface chemistry models accelerate design of efficient & selective catalysts	Reactor & reaction designs enable durable catalysis & minimal fouling	

Relevance: accelerating deployment of biomass conversion technologies through process and catalysis modeling

- **30 publications and 29 presentations (since last Peer Review)***
- Tech transfer via web tools and key parameter input to modeling codes

*Publication/presentation lists in additional slides

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Acknowledgements

OAK RIDGE National Laboratory

Jim Parks
Gavin Wiggins
Stuart Daw
Emilio Ramirez
Jessica Torres
Sreekanth Pannala
Charles Finney

NREL National Renewable Energy Laboratory

David Robichaud
Peter Ciesielski
Seonah Kim
Lintao Bu
Tom Foust
Vassili Vorotnikov
Carrie Farberow
Mark Nimlos
Brandon Knott

Pacific Northwest National Laboratory

Roger Rousseau
Bob Weber
Vanda Glezakou
David Cantu
Asanga Padmaperuma

NETL National Energy Technology Laboratory

Bill Rogers
Madhava Syamlal
Tingwen Li
Dirk VanEssendelft
Balaji Gopalan

Argonne National Laboratory

Larry Curtiss
Rajeev Assary
Lei Cheng
Cong Liu
Dale Pahls

Industry Advisory Panel

David Dayton (RTI), George Huff (MIT, retired BP), Jack Halow (Separation Design Group), Mike Watson (Johnson Matthey), Randy Cortright (formerly Virent Energy Systems), Richard Quann (ExxonMobil), Steve Schmidt (WR Grace), Tom Flynn (Babcock & Wilcox), Rick Wessel (Babcock & Wilcox)

ChemCatBio Chemical Catalysis for Bioenergy

A multi-scale problem … A multi-lab solution

1D Model
2D Continuum Model
3D Continuum Model
Micro-kinetics/ Particle Scale
Atomistic and Electronic Structure

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Additional Slides

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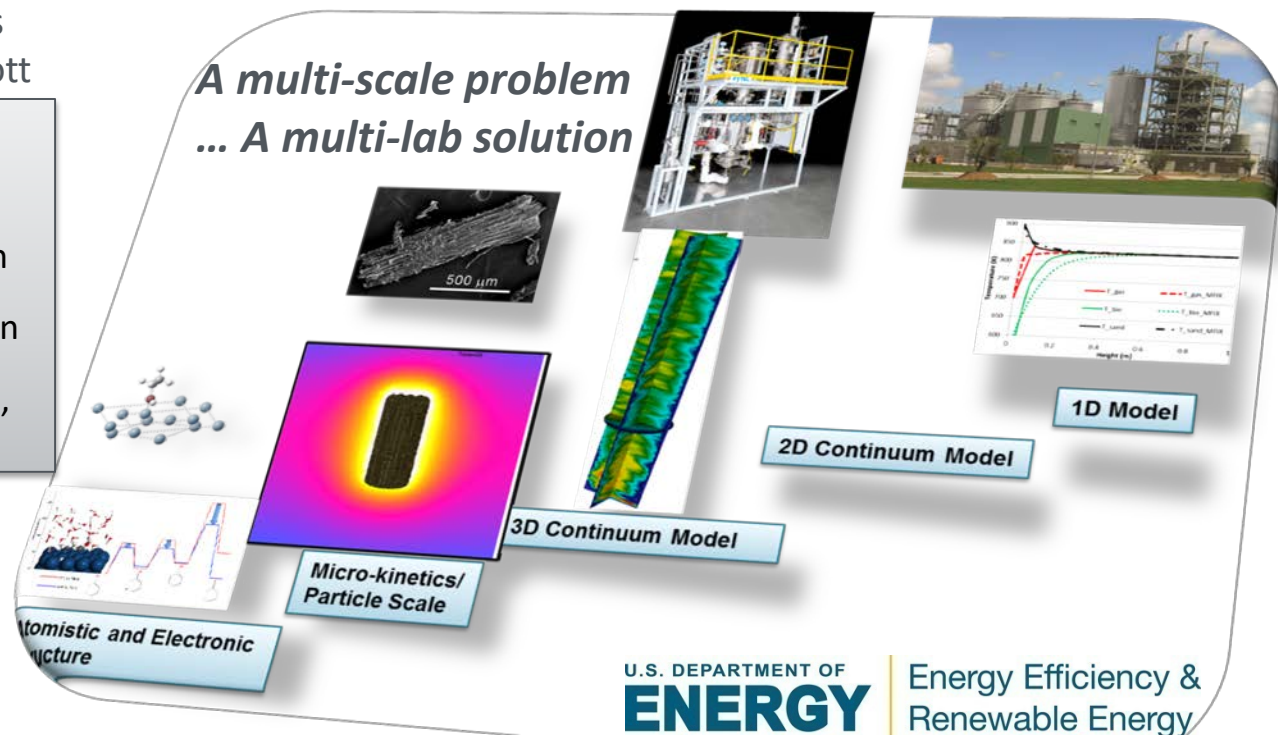
Contents of Additional Slides

- Responses to 2015 Reviewers' Comment

- Project Timeline: CCPC History and Path to Success

- Go/No-Go Review [August 2016]

- Publications (since 2015 Peer Review)

- Presentations (since 2015 Peer Review)

- Commercialization & Technology Transfer

- Milestones

- List of Collaborating BETO Projects

- List of Collaborators and Partners

- Industry Advisory Panel Expertise Matrix

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- Overall, project scored well during 2015 Peer Review

Overall Project Score: 7.9

This Project

2015 Thermochemical Conversion Peer Review Average for 2015 Existing Project Evaluation Criteria
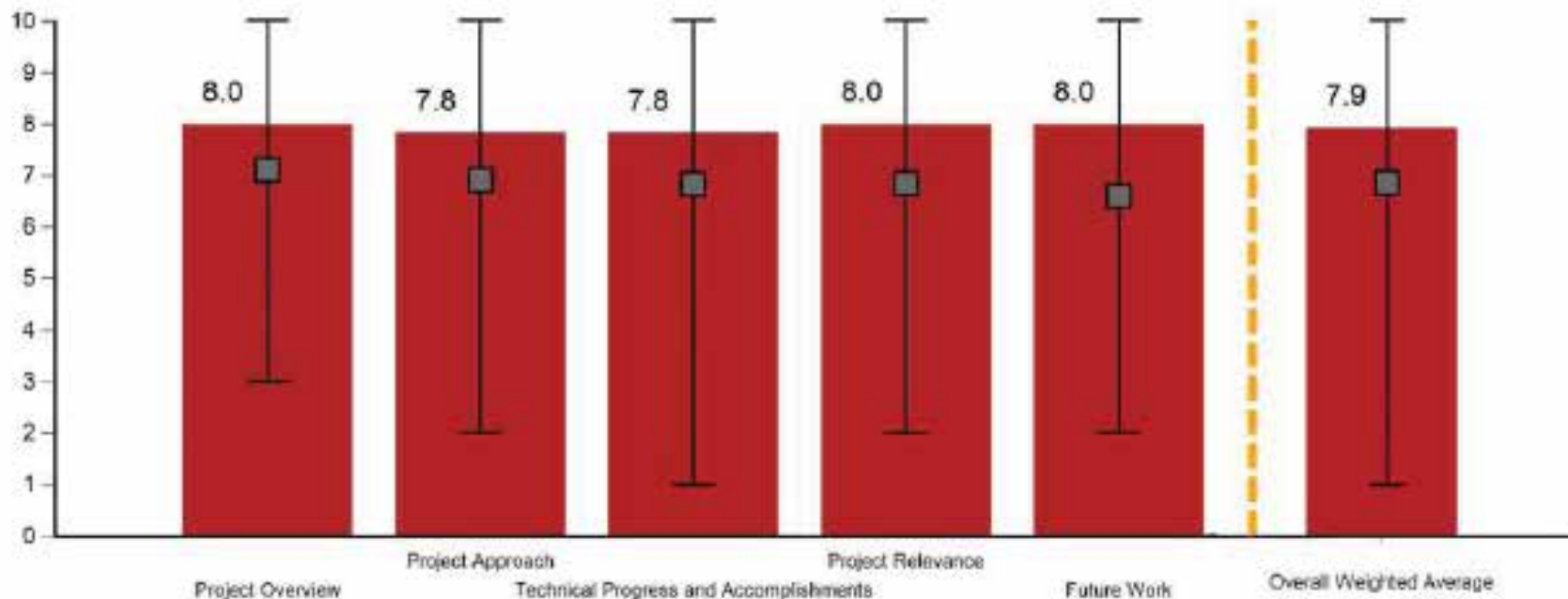
Whiskers represent the range of scores for each evaluation criteria across all projects reviewed in this technology area.

Note: The 2015 Peer Review Report is publicly available at
https://energy.gov/eere/bioenergy/2015-project-peer-review
(the CCPC project is on pages 352-353)

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Generally Positive Comments (from 2015 Peer Review):

- *"Clearly, a well-planned and coordinated effort that will help establish technical fundamentals, which can be leveraged by others."*

- *"The consortium provides a very useful way to focus the computational capabilities of the laboratories on biomass problems."*

- *"The inclusion of an external advisory committee with significant industry representation is a very useful way to keep this group focused."*

- *"Excellent program that brings modeling/computing technical expertise to this field to identify critical science, engineering, and economic critical issues and directions. Very critical to have modeling aid in the scale-up of a new process technology. Brings together a larger organization and communication across the laboratories."*

CCPC Response/Actions:

- Keep our collaborative approach and coordination

- Keep utilizing the valuable external industry advisory committee

Comments on Scope (from 2015 Peer Review):

- *"It seems scope of the project is way too large; might be better to concentrate on two or three areas."*

- *"The consortium should determine sooner rather than later which approaches have the most promise and focus on them."*

- Regarding *"broad-scoped approach"…"It [the project] now needs to work toward a focused outcome, otherwise its value to subsequent projects is diluted."*

CCPC Response/Action:

- The project has continued to be broad in scope, and we agree that poses a challenge with regard to maintaining focus on a concentrated set of deliverables. However, funding resources have been able to support our broad scope, and active program management by DOE has enabled the most promising results to be moved forward. Adjustments have been made to resource distribution (see Go/No-Go slides) in this regard. Also, the Industry Advisory Panel has been quite helpful in maintaining focus on the critical outcomes from the project tasks.

Note: Response/Action continued on next slide

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Comments on Scope (from 2015 Peer Review):

CCPC Response/Action (continued from previous slide):

- For process modeling tasks, we focused a significant portion of our efforts in the last two years pyrolysis step (i.e. significant reduction in VPU reactor modeling) resulting in a win for modeling pine pyrolysis. Going forward we are rebalancing resources to again make VPU a priority and are leveraging lessons learned from the pyrolysis modeling effort.

- For the catalyst design tasks, we have been setting up those tasks to become a standard tool (similar to DRIFTS or TPD) that experimental teams can use for their catalyst design work. As such, many of our catalyst design projects are short, focused efforts to answer well defined questions and our aim is fast turnaround and impact (months). We only maintain a few (1-2) long term projects on catalyst design that extend past a single fiscal year.

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Responses to 2015 Reviewers' Comments (5/6)

Comment on Experimental Ties (from 2015 Peer Review):

- *"Modeling work also needs to be tied directly to projects on experimental results so that the two can work synergistically together."*

CCPC Response/Actions:

- Excellent comment. We have increased our engagement with experimental projects, and each CCPC task is now collaborating closely with multiple projects. In addition, "joint" and "linked" milestones between CCPC and experimental projects further combine efforts between modeling and experimental activities in BETO.

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Comment on Catalytic Pyrolysis (from 2015 Peer Review):

- *"One of the issues facing catalytic pyrolysis is determining which reactions are catalytic and which are not. Will the modeling work address this?"*

CCPC Response/Actions:

- Yes. While most of our activities are focused on separate pyrolysis and catalytic upgrading processes, defining which pyrolysis reactions are catalytic is part of our approach. Furthermore, the catalytic effects of ash can affect pyrolysis yields and needs further study/definition (literature sparse related to ash effects); our project is addressing this issue which is critical for enabling effective utilization of herbaceous feedstocks.

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Project Timeline: CCPC History and Path to Success

End of 3-year project cycle
- Demonstrate pyrolysis predictions across multiple reactors and feedstocks
- Validate VPU models
- Address 'kinetics' risk

Goal for 2022
- Al a carte modeling tools that are publicly available to predict performance of pyrolysis, ex situ and in situ CFP
- Address kinetics issue for CFP
- Link to LPU/Hydrotreating for unified modeling toolset
- Explore advanced issues with modeling (aerosols, reactor coking/plugging, etc) as motivated by IAB

Collaborations Began
Initiated multi-NL collaboration on modeling

Peer Review Feedback
Focused efforts on pyrolysis in response to reviewer 'dilution' comment

FY13   **FY15**   **FY16**   **Sept FY18**   **FY22**

FY17
- Brought in NETL to work on VPU reactors
- Follow success of pyrolysis approach to VPU (combine particle, kinetic, and reactor modeling with validation against multiple systems at NREL).

2015 Peer Review
- Demonstrated 3D biomass particle models for heat transfer
- Validated hydrodynamics of pyrolysis reactor
- Constructed preliminary model of DCR riser VPU

Aug. 2016 (mid-cycle Go-NoG review passed → "Go")
- Validated 1D particle models that capture 3D heat transport effects
- Combined 1D particle, kinetic, and reactor models to predict moisture and particle size distribution effects on bio-oil yield.
- Kinetic models are major source of uncertainty

Project Start
CCPC 3-year project started building off of initial collaboration

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On August 2, 2016, a Go/No-Go review of the CCPC was conducted.

The Criteria for the Go/No-Go review were:

1) Using particle scale modeling and reactor simulations, demonstrate ability to predict pyrolysis oil yields from a fast pyrolysis reactor;

2) Show two examples (one VPU, one LPU) in which modeling has been used to inform an experimental BETO project.

The results from the Go/No-Go review were:

"Conditional Go"; rescope (Criterion 2B) and redistribution of funds required for FY17.

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Specific directions from the Go/No-Go review included:

Moving forward, criterion 1 and 2A should continue, and also consider expansion of scope in lieu of large LPU modeling efforts; significant redistributions of funding within CPC and rescope must be considered prior to the start of FY17's AOP, as this is necessary to support more value-add and relevant tasks. LPU modeling should be decreased to CPC's "minimum planning level" until experimentation can validate preliminary models, such that the feedback "cyclic-interconnected development continuum" loop closure can be demonstrated in a useful, transformative manner.

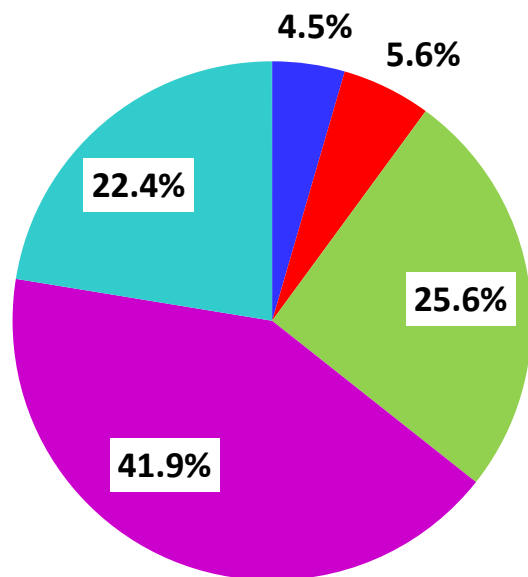## CCPC Actions in Response to Go/No-Go Review Feedback:

- The CCPC redistributed resources across the tasks and made significant funding additions to the Feedstock Impact Analysis task. Modest funding additions were also made for the Reactor Analysis and Scale-Up and Vapor Phase Upgrading (VPU) tasks.

- The Liquid Phase Upgrading (LPU) task was scaled back significantly. Recommendations from the LPU task were made to experimental teams, and the project is awaiting results from those experiments before next steps.

Graphs summarizing the resource redistribution are shown on the next slide

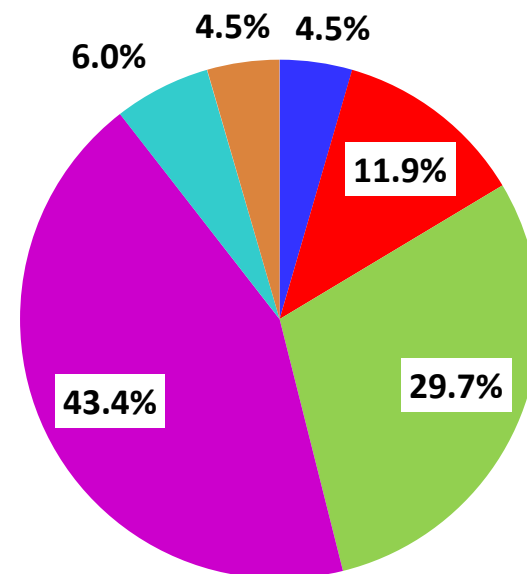U.S. DEPARTMENT OF **ENERGY** | Energy Efficiency & Renewable Energy

CCPC Actions in Response to Go/No-Go Review Feedback:

- Revised funding resource allocation for FY17 based on feedback

Legend:
- Task 1 (Coordination)
- Task 2 (Feedstock and Particle)
- Task 3 (Reactor Modeling and Scale Up)
- Task 4 (Vapor Phase Upgrading)
- Task 5 (Liquid Phase Upgrading)
- Task 6 (IDL)

Original FY17 Task Resource Allocation

Original values: 4.5%, 5.6%, 22.4%, 25.6%, 41.9%

Revised FY17 Task Resource Allocation

Revised values: 4.5%, 4.5%, 6.0%, 11.9%, 29.7%, 43.4%

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2. Mark Nimlos and Robert Weber, "Strike a happy medium: Identifying appropriate reaction conditions for upgrading bio-oil", 249th ACS National Meeting, Denver, CO, COMP division.

3. Yoon Y, RJ Rousseau, RS Weber, D Mei, and JA Lercher, "First-principles Study of Phenol Hydrogenation on Pt and Ni Catalysts in Aqueous Phase", 249th ACS National Meeting, Denver, CO, COMP division.

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7. Robert Weber, "Reactions in Complex Media", Keynote Lecture to 18th Brazilian Congress on Catalysis. Porto Seguro, Brazil, September, 2015

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12. G. Wiggins, C. S. Daw, P. Ciesielski. "Modeling the Impact of Biomass Particle Size Distribution and Shape on Heating Behavior During Fast Pyrolysis", Symposium on Thermal and Catalytic Sciences for Biofuels and Biobased Products, Chapel Hill, NC, November 2, 2016.

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15. G. Wiggins, C. S. Daw, E. Ramirez, "Modeling the Impact of Biomass Particle Residence Time on Fast Pyrolysis Yield and Composition," AIChE National Meeting, San Francisco, CA, November 15, 2016.

16. E. Ramirez, C. E.A. Finney, S. Pannala, C. S. Daw, J. Halow, Q. Xiong, "Computational study of the bubbling-to-slugging transition in a laboratory-scale fluidized bed", NETL 2016 Workshop on Multiphase Flow Science, Morgantown, WV, August 9, 2016.

17. E. Ramirez, C.E.A. Finney, C. S. Daw, J. Halow, "Optimizing fluidized bed hydrodynamics for biomass fast pyrolysis oil yield", East Tennessee Collegiate Division Meeting of the Tennessee Academy of Science, Knoxville, TN, April 22, 2016.

18. E. Ramirez, C.E.A. Finney, C. S. Daw, J. Halow, "Resolving hydrodynamic transitions in bubbling bed biomass pyrolysis reactors", ORAU Annual Meeting on Application of Big Data Analytics, Oak Ridge, TN, March 9, 2016.

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20. E. Ramirez, C. S. Daw, S. Pannala, Q. Xiong, C.E.A. Finney, "Resolving hydrodynamic transitions in bubbling bed biomass pyrolysis reactors", NETL 2015 Workshop on Multiphase Flow Science, Morgantown, WV, August 12, 2015.

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22. Cong Lu, Cheng Lei, Rajeev Assary, Larry Curtiss, In silico zeolite catalyzed carbon-carbon coupling reactions for furan upgrading, American Society Meeting, March 25, 205, Denver, CO.

23. Cheng Lei, Larry A. Curtiss, Rajeev Assary, First-principles studies of furan upgrading by Ga/ZSM-5" American Chemical Society Meeting, Aug16-20, 2015, Boston, MA

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24. Rajeev S. Assary, Larry A. Curtiss, Lei Cheng, Cong Liu, Modeling catalytic vapor phase upgrading using first principles", American Chemical Society Meeting, Aug 21, 2016, Philadelphia

25. Ferguson, GA; Vorotnikov, V; Wunder, N; Clark, J; Gruchalla, K; Bartholomew, T; Robichaud, D; Beckham, GT, "Multi-dimensional phase diagrams for the coadsorption of aromatic oxygenates and hydrogen on metallic surfaces," ACS National Meeting, Philadelphia, PA; August 2016.

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29. Peter Ciesielski. Improving Biomass Conversion Processes through Advanced Imaging, Modeling, and Simulation. Workshop on Second Generation Bioethanol 2016, Brazilian Bioethanol Science and Technology Laboratory (CTBE), Campinas, Brazil. Dec 1st, 2016.

In addition, CCPC has been active in organizing the following conferences/meetings:

- Symposium organizer, "Advances in Computational Catalysis" (CATL division), American Chemical Society Meeting 2016, August, Philadelphia

- Symposium organizer, "Advances in Computational Catalysis-II" (CATL division), American Chemical Society Meeting 2017, August, Washington DC

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Commercialization & Technology Transfer

(1) Public release of "Surface Phase Explorer"

- Surface Phase Explorer is a web-based tool for exploring phase diagrams (based on ab initio data) associated with the coadsorption of two species on a surface.

- Available to the public at spe.nrel.gov
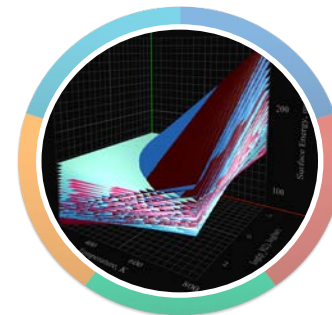
(2) Assist Including Biomass Parameters in *CSFMB©/CeSFaMB™*

- CCPC assisted Prof. de Souza-Santos in including biomass pyrolysis chemistry into new version of CSFMB© commercial software (Brazil)

- See www.csfmb.com

(3) Public release of CCPC code on GitHub

- CCPC code and bioenergy specific modeling parameters (kinetics, thermal properties, etc.) have been loaded to GitHub

- Available to the public at github.com/pyrolysis

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Milestones: Feedstock Impact Analysis (Task 2)

Due	Annual Milestone
Q3 (June 30, 2017)	**Task 2&3. Predict pyrolysis yields on feedstocks between 2FBR and TCPDU.** Use feedstock characterization data provided by INL (WBS 2.2.1.501) for 2 pelletized feedstocks, namely Clean Pine and TCPDU Blend 2 (45% clean pine, 25% forest residues, 30% construction and demolition waste) to construct representative biomass particle models. Develop reactor-flow conversion simulations coupled to ensemble calculations to predict pyrolysis yields of these feedstocks blends in the TCPDU entrained flow reactor and the 2" fluidized bed reactor. Validate the entrained flow reactor model with experimental results reported by 2.4.1.301 to achieve particle-scale pyrolysis simulations that are sufficiently predictive (i.e., can predict yields within measured experimental error). Provide physics-based understanding of any differences observed in the Q2 milestone on 2.4.1.301/2.2.1.304 between the two reactor scales as well as recommendations on how to align residence times and heat transfer between the two reactors to 2.4.1.301/2.2.1.304. [NREL lead with ORNL] NOTE: This Annual Milestone is linked to the FY17 Q1 milestone in the Integrated and Scale-Up project at NREL (WBS 2.4.1.301)
Linked Milestone	**LINKED MILESTONE in Integrated and Scale-Up project at NREL (WBS 2.4.1.301):** Provide the CPC task (WBS 2.5.1.301-5) with mechanical drawings of the TCPDU entrained flow and ex-situ CFP reactors, temperature profiles and other process data from recent operations, crushed feed samples taken from the feed-train and other information as requested to achieve the CPC milestones of developing particle-scale simulations and scaled reactor modeling. (FY17 Q1 milestone)

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Milestones: Reactor Analysis and Scale-Up (Task 3)

Due	Quarterly Progress Milestone
Q1	Define validation experiments to run during R3 Upgrader reactor commissioning process and provide to 2.4.1.301 at NREL [ORNL lead, NETL and NREL assist] Note: feeds into Annual Milestone for R3 Upgrader. Linked to Q1 milestone on 2.4.1.301.

Due	Stretch Annual Milestone
Q4 (September 30, 2017)	Develop initial R3 Upgrader model in MFiX and provide predictions of residence time and heat transfer and compare to 2" bubbling bed upgrading reactor for scale-up comparison. Enables rapid optimization of R3 Upgrader operation to achieve BETO goals and provides analysis of scale-up feasibility for a 2" bubbling bed upgrading reactor ("Baldwin reactor") to R3 Upgrader reactors which is critical to attaining value from ChemCatBio catalyst development activities. [ORNL lead, NETL assist] NOTE: This Annual Milestone is linked to the FY17 Q1 milestone in the Integrated and Scale-Up project at NREL (WBS 2.4.1.301)
Linked Milestone	**LINKED MILESTONE in Integrated and Scale-Up project at NREL (WBS 2.4.1.301):** Provide the CPC task (WBS 2.5.1.301-5) with mechanical drawings of the TCPDU entrained flow and ex-situ CFP reactors, temperature profiles and other process data from recent operations, crushed feed samples taken from the feed-train and other information as requested to achieve the CPC milestones of developing particle-scale simulations and scaled reactor modeling. (FY17 Q1 milestone)

Also links to Qtly

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Milestones: Vapor Phase Upgrading (Task 4)

Due	Quarterly Progress Milestone
Q1 *Joint Milestone*	**Identify the active-site structure(s) responsible for low-temperature alkane activation and reincorporation into the chain-growth cycle on modified beta zeolite catalysts.** Understand C4 activation over the Cu/BEA catalyst to inform catalyst design to maximize/control C4 reincorporation, and thereby, increase carbon yield from DME to C5+ gasoline products and consequently decrease the MFSP. This is a joint milestone with the ACSC (WBS#2.5.4.304) and the CCPC (WBS#2.5.1.302), where in-situ/operando XAS analysis of the ionic Cu site structure(s) and computational modeling of the energetics of C4 activation at the ionic Cu sites will be coupled with experimental C4 activation studies. These combined results will inform an iterative computational effort to identify and explore additional ionic metal sites (non-Cu-based) that will enable catalyst design to maximize C4 reactivation and reincorporation into the chain growth pathway. These new, predicted catalyst formulations will be identified as synthetic targets for the next generation of catalysts within this project. [NREL lead] NOTE: This milestone is a Joint Milestone with Advanced Catalyst Synthesis and Characterization (2.5.4.304) and Liquid Fuels via Upgrading of Syngas Intermediates (2.3.1.305). Subcontract with UCLA. Feeds into Q2 milestone on CCPC.
Q3 *Linked Milestone*	**Evaluate the changes in reaction energetics of a Ni-doped Mo2C for furan coupling in the condensed phase.** Investigate the vapor phase carbon-carbon coupling of furan molecules in Ni/Mo2C (longer term catalysts) to understand the reaction mechanisms and the catalyst deactivation. Reaction energetics, including rate determining steps, will be provided to ChemCatBio (WBS # 2.3.1.301), along with a more detailed understanding of the role of nickel in the Mo2C catalyst and a prediction of the optimum weight percentage of nickel to guide future synthesis and catalyst optimization. [ANL lead] NOTE: This Quarterly Milestone support activities on ChemCatBio (2.3.1.301).
Q3 *Linked Milestone*	**Computationally screen Lewis-acidic zeolites across 4 reaction classes to guide compositional synthesis for improved activity and selectivity.** Model the kinetics of dehydration, dehydrogenation, cyclization, and decarbonylation in zeolite catalyst modified with 5 different Lewis metals. Metals are chosen based on candidates proposed by 2.3.1.314 and will include at least Cu and Ga (remaining 3 TBD) as well as oxidation states and different terminations (oxide vs hydroxide). Using this kinetic analysis, make recommendations that can be experimentally tested that will prove the hypothesis that zeolites can be designed to enhance dehydration/dehydrogenation (good reactions) and reduce cyclization/decarbonylation (bad reaction, coke former). [NREL lead, ANL assist] NOTE: This Quarterly Milestone is linked to planned milestones in FY18 on ChemCatBio (2.3.1.315 and 2.3.1.305).
Q4 *Linked Milestone*	**Identify optimal macroporousity in zeolites for CFP to guide catalyst structural synthesis.** Using 3D structural models of a ZSM-5 catalyst particle, investigate the relationship between mesoporous volume fraction and coking/product yields. Models will include mesoporous/microporous diffusion of species, and utilize kinetics from Adajay et al. kinetic scheme (or best available). Models will be informed by and compared to image data produced by the ACSC (ORNL). Recommend optimal range of mesoporous volume fraction based on catalyst reactor residence times to ACSC for targeted synthesis and benchmark results against standard zeolite (e.g. Nexceris) via CCB. [NREL lead] NOTE: This Quarterly Milestone is linked to milestones on the Advanced Catalyst Synthesis and Characterization (2.5.4.303-5).

Milestones: Vapor Phase Upgrading (Task 4)

Due	Annual Milestone (Regular)
Q2 March 31, 2017 *Linked Milestone*	**Evaluate effect of subsurface oxygen on reaction energetics over Mo2C catalysts.** Model the effect of surface and subsurface oxygen coverage in Mo2C catalysts on surface oxygen binding energies and reaction energetics of ethanol dehydration. Compare modeling results against experimental ethanol dehydration work on CCB (2.3.1.314). Based on modeling/experimental results determine if oxygen binding is an appropriate descriptor of catalyst activity and make recommendations for improved catalyst design (e.g. dopants to reduce oxygen binding strength). [NREL lead] NOTE: This Annual Milestone is linked to FY18 milestone on ChemCatBio (2.3.1.314).

Milestones: Liquid Phase Upgrading (Task 5)

Due	Quarterly Progress Milestone
Q1	Homologation with NETL and ORNL to devise a path towards use of CFD to model the complex flow in LPU. Determine whether the NETL software, MFIX, is suitable for modeling the 4-phase flow in an LPU reactor to help determine how to avoid flow mal-distributions that can lead to localized fouling, poor utilization of hydrogen and ineffective utilization of the catalyst. [PNNL lead with NETL and ORNL]
Q3	Task 5. Full LPU catalyst model relating optimal particle size and support effects. Subsequent suggested catalyst targets to experimental team. [PNNL lead]

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Collaborating BETO Projects

- All ChemCatBio Projects

- Integration and Scale Up – NREL (WBS 2.4.1.301)

- Thermochemical Feedstock Interface – NREL (WBS 2.2.1.304)

- Feedstock-Conversion Interface Consortium

- Multi-scale Physical and Structural Particle Mechanics - INL (Feedstock Program - WBS 1.2.1.3)

- Bio-oil quality improvement and catalytic hydrotreating of bio-oils – PNNL and ORNL (WBS 2.3.1.301,302)

- Thermochemical Platform Analysis Update – NREL and PNNL

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Collaborators and Partners (outside of National Labs)

Universities

- UCLA (Ken Houk)
- Colorado School of Mines (Cristian Ciobano, Brandon Knapps)
- Northwestern Univ. (Linda Broadbelt)
- Washington State Univ. (Brennan Pecha, Manuel Garcia-Perez)
- University of Tennessee (Nour Abdoulmoumine)

Industry

- Industry Advisory Panel Entities:
  - RTI
  - Johnson Matthey
  - WR Grace
  - Babcock & Wilcox
  - Separation Design Group
  - ExxonMobil
  - BP (via George Huff, retired)
  - Virent Energy Systems
- PSRI (Particulate Solid Research, Inc)

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Industry Advisor Panel Expertise Matrix

The table below provides a matrix of the experience areas for the CCPC Industry Advisor Panel. The panel represents a diverse range of expertise covering all activity areas of the CCPC.

	David Dayton (RTI)	Tom Flynn (B&W)	Richard Quann (Exxon Mobil)	Randy Cortright (formerly Virent)	Mike Watson (Johnson Matthey)	Jack Halow (Separation Design)	George Huff (formerly BP)	Steve Schmidt (WR Grace)	Rick Wessel (B&W)
Feedstock	X	X							X
Reactor analysis		X	X			X	X		X
VPU catalysis	X		X		X	X		X	
LPU catalysis	X		X	X	X			X	