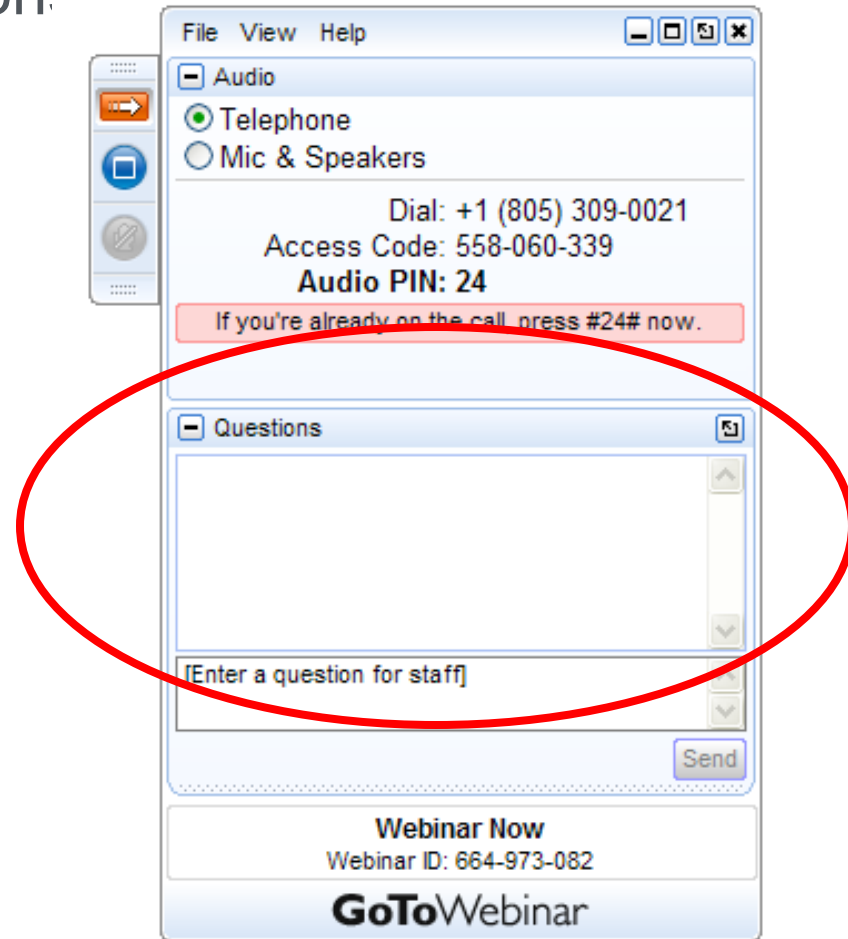


Presenter:  
Voya (Vojislav)  
Stamenkovic  
Argonne National  
Laboratory

DOE Host:  
Dimitrios  
Papageorgopoulos  
Fuel Cell Technologies  
Office

U.S. Department of Energy  
Fuel Cell Technologies Office  
October 13<sup>th</sup>, 2016

- Please type your question into the question box



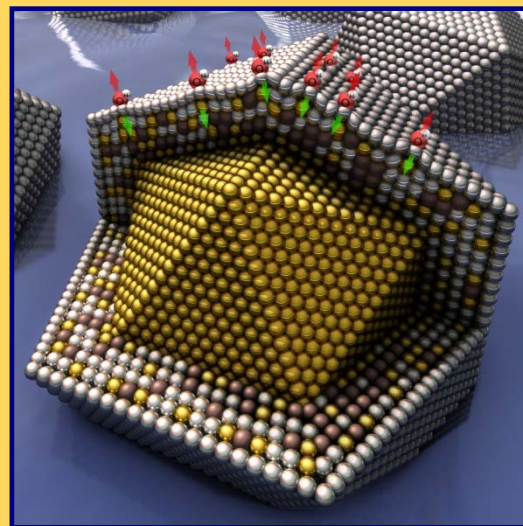


... for a brighter future

# Past, Present and Future Challenges in Electrocatalysis for Fuel Cells

Materials Science Division  
Argonne National Laboratory

Vojislav Stamenkovic



U.S. Department of Energy

UChicago ►  
Argonne<sub>LLC</sub>



A U.S. Department of Energy laboratory managed by UChicago Argonne, LLC

DOE EERE Fuel Cell Technology Office Webinar Series

October 13, 2016



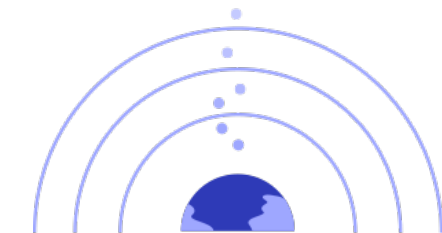
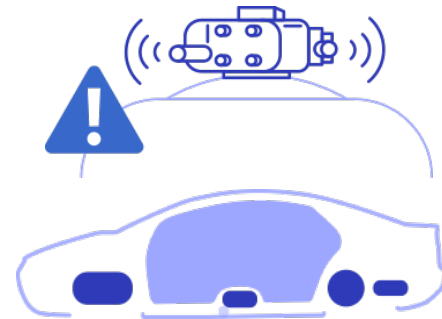
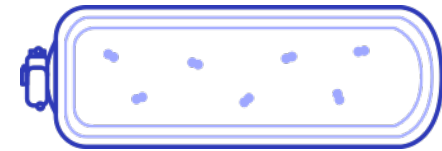
## 2016 Toyota Mirai

**\$499/month 36-month lease**  
**\$57,500 MSRP**

### The first production fuel cell vehicle

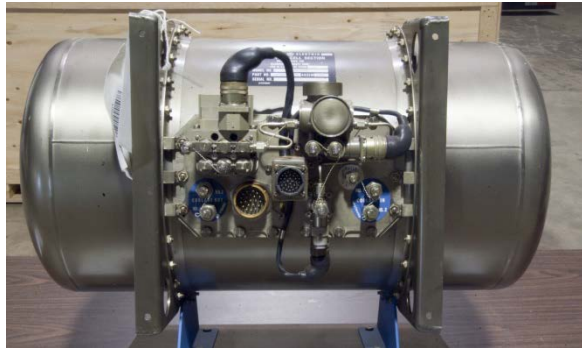
The Mirai is at the forefront of a new age of hydrogen fuel cell cars that allows you to enjoy long distance zero-emissions driving. As well as only producing water from its tailpipe – which means no impact on our planet when you're driving – Mirai brings the unique Toyota Hybrid driving experience to a new level.

**HYDROGEN SAFETY**  
Science behind the safety  
Safety was our primary objective when we engineered the Mirai. Our proprietary safety system is based on four fundamental principles.





'60s



PEM FC

unsupported Pt catalyst

loading:  $28 \text{ mg}_{\text{Pt}}/\text{cm}^2$

membrane: Nafion

$T \sim 21^\circ\text{C}$



'60-70s



Alkaline FC

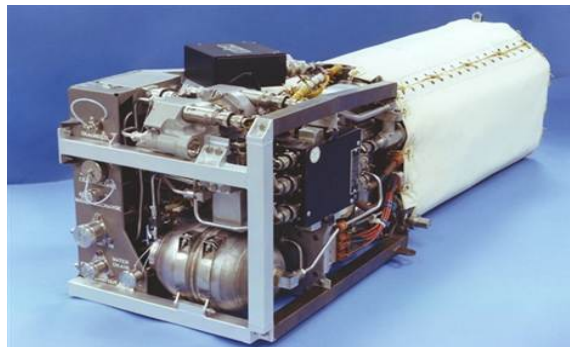
Ni based catalyst

$T \sim 250^\circ\text{C}$

Operating time: 400-690h



'80-2011



Alkaline FC

Pt and PtAu catalysts

loading: 10 and  $20 \text{ mg}_{\text{Pt}}/\text{cm}^2$

$T \sim 93^\circ\text{C}$

Operating time: > 16 days

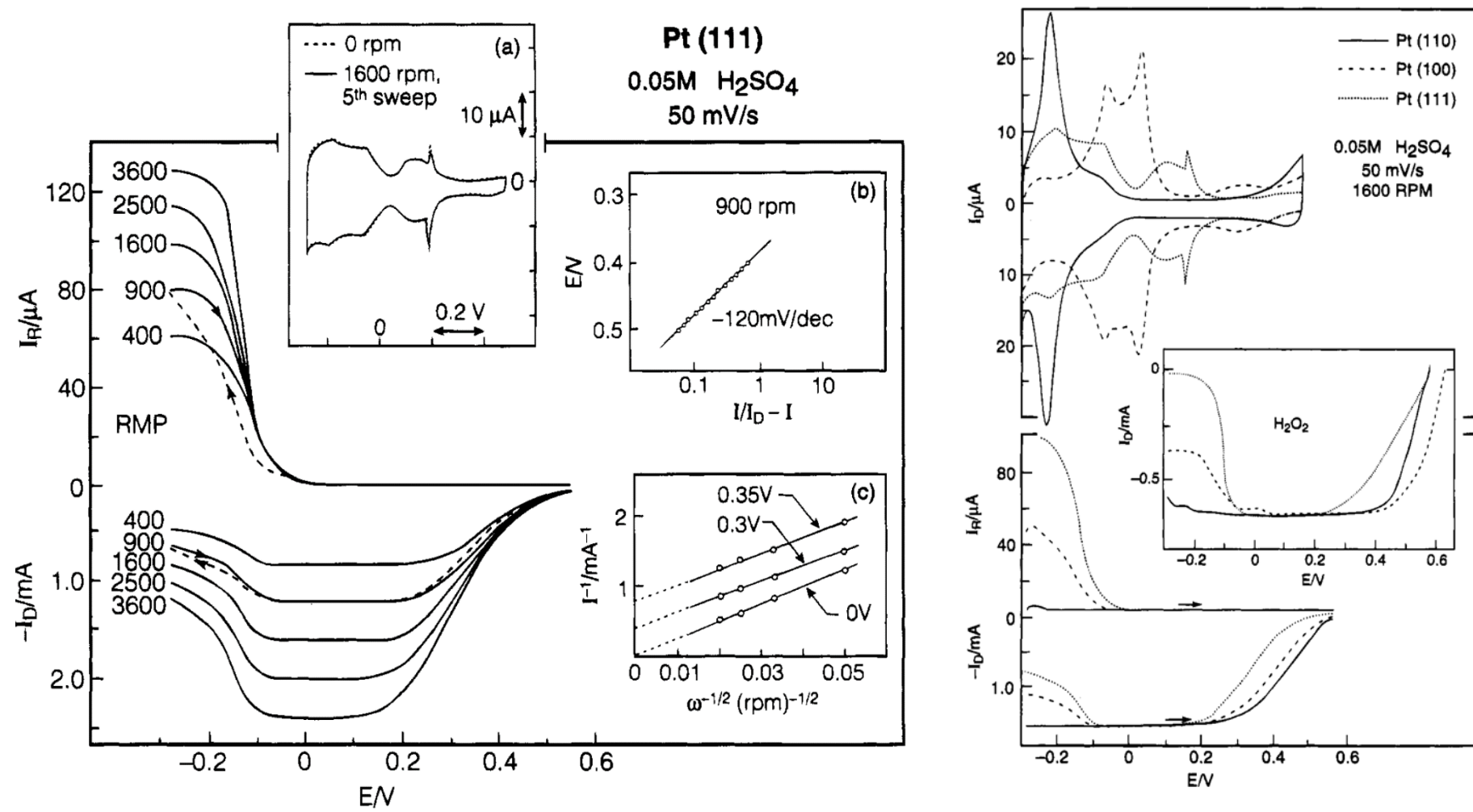
# Oxygen Reduction on Platinum Low-Index Single-Crystal Surfaces in Sulfuric Acid Solution: Rotating Ring–Pt(*hkl*) Disk Studies

Nenad M. Marković,\* Hubert A. Gasteiger, and Philip N. Ross, Jr.

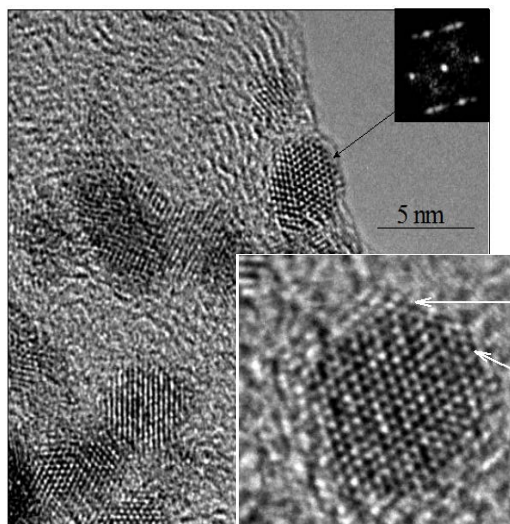
Materials Science Division, Lawrence Berkeley Laboratory, Berkeley, California 94720

Received: September 28, 1994; In Final Form: December 16, 1994<sup>®</sup>

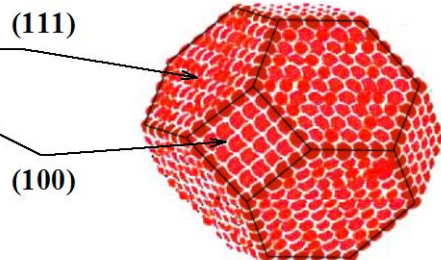
3414 *J. Phys. Chem.*, Vol. 99, No. 11, 1995



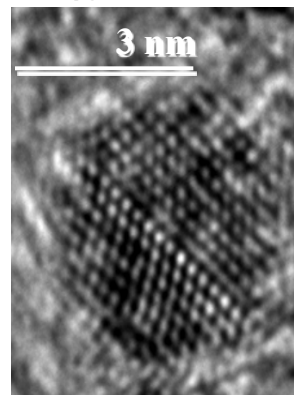
# Particle Size Effect



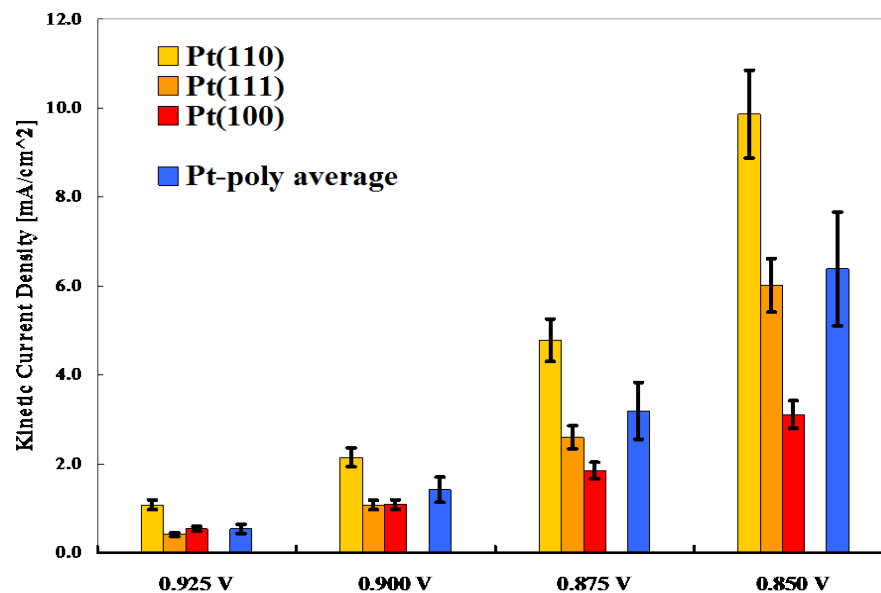
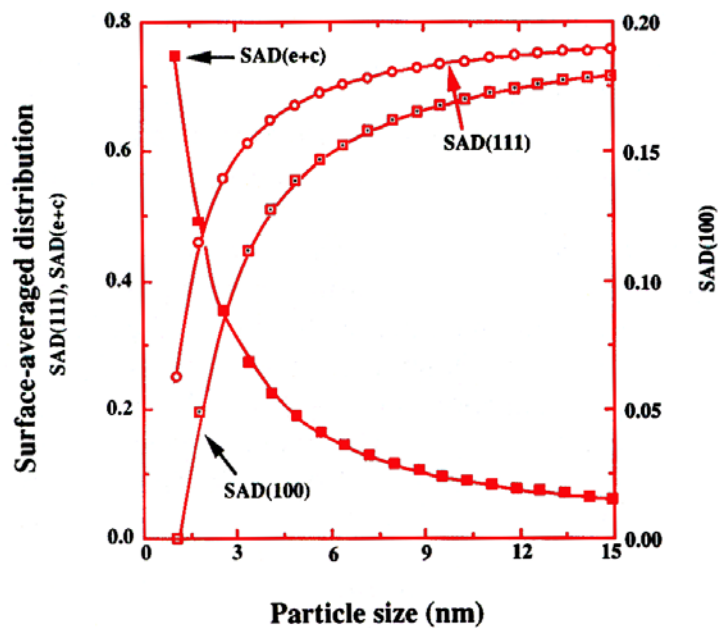
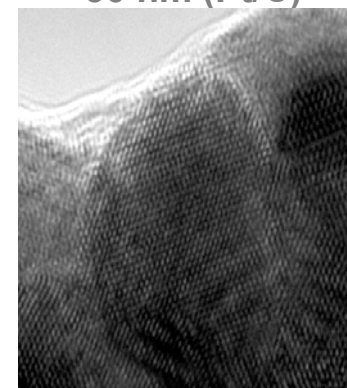
□ cubo-octahedral particles



10 % Pt/Vulcan

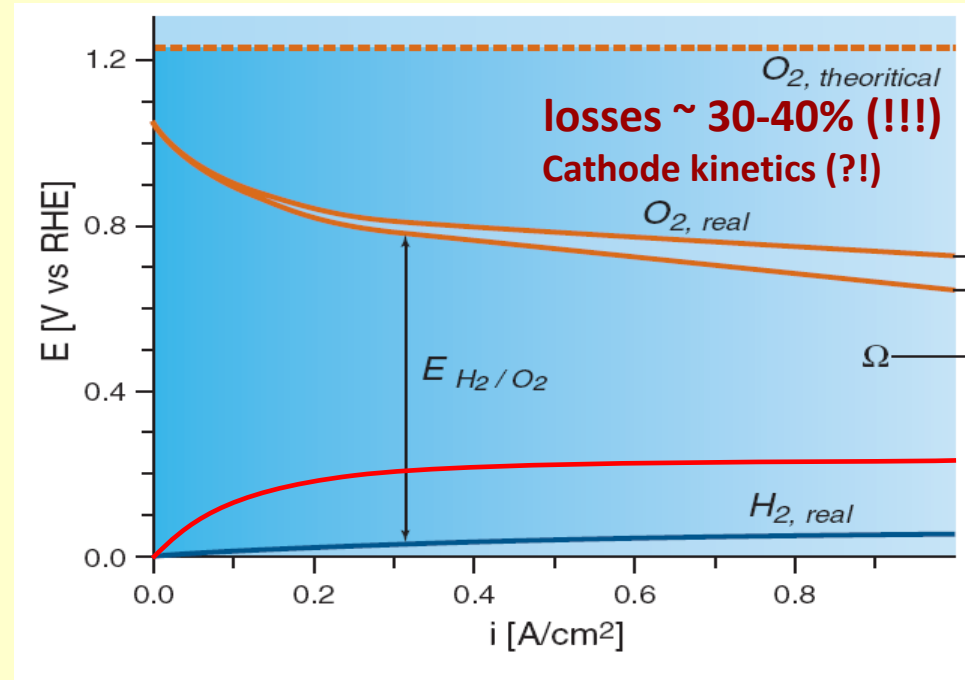


30 nm (Pt/C)



## 2020 DOE Technical Targets

- Mass activity @0.9V: 0.44 A/mg<sub>Pt</sub>
- Electrochemical area loss: < 40%
- PGM Total content: 0.125 g/kW
- PGM Total loading: 0.125 mg/cm<sub>2</sub><sub>electrode</sub>
- Durability w/cycling (80°C): 5000 hrs



### Main limitations in PEM fuel cell technology:

- 1) Activity: Pt/C = Pt-poly/10
- 2) Durability: (Pt catalyst dissolves)
- 3) Pt loading: Cost Issues



**Activity**

**Durability**

**Cost**

Specific/Mass Activity

Electrochemical Stability

Loading

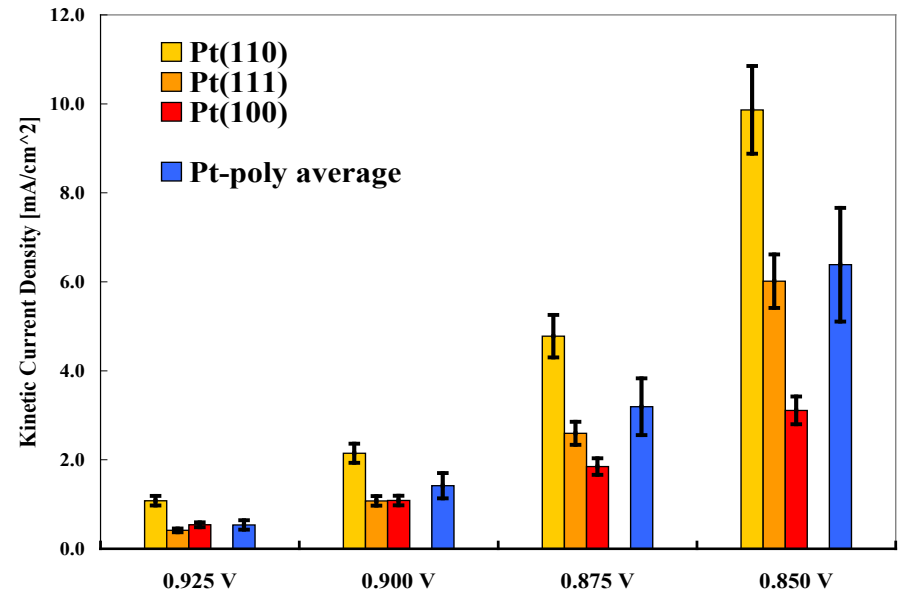
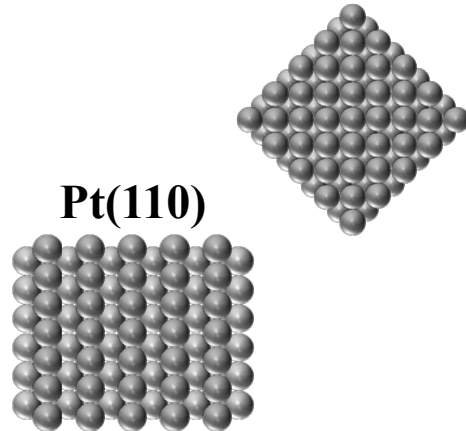
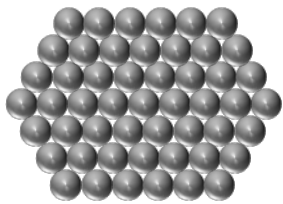
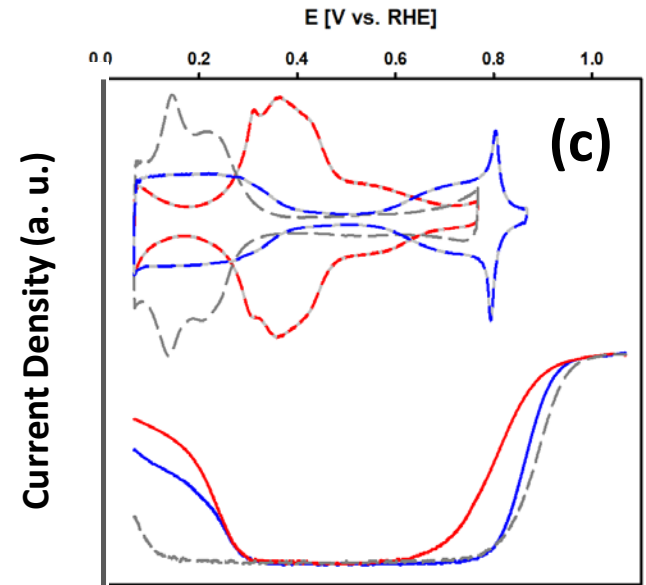
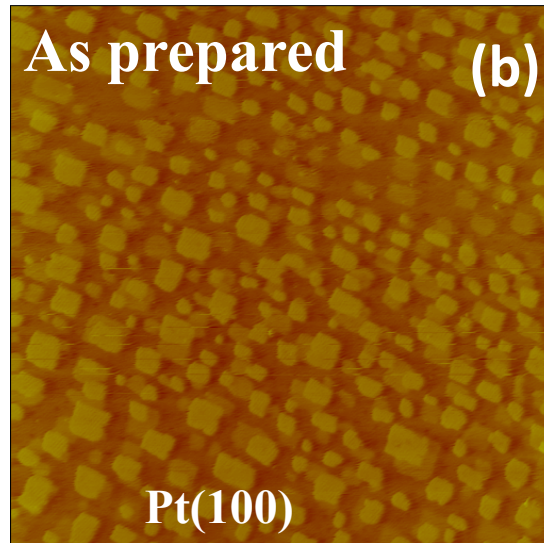
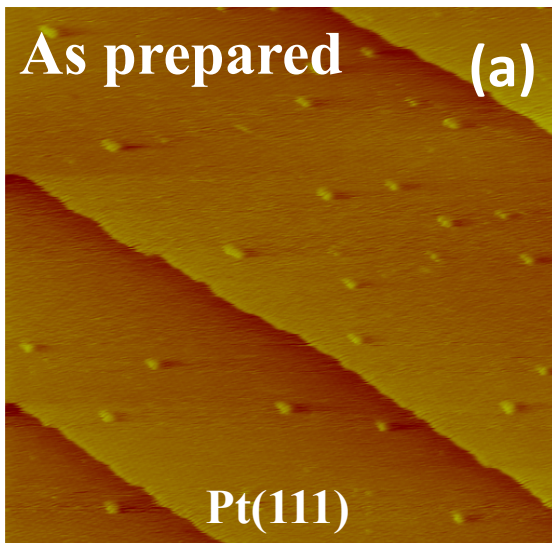
**1° Structure-Function**

**2° Composition-Function**

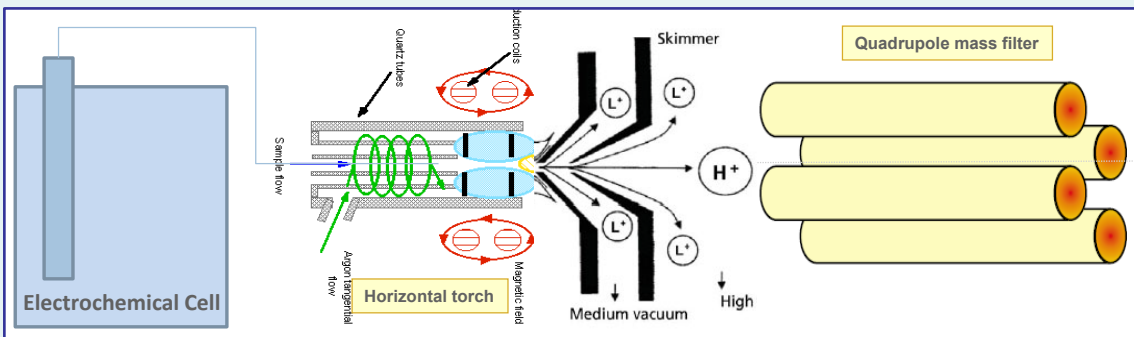
**3° Surface Modifications**

**4° Tailored Electrolytes**

# STM: Pt Single Crystals

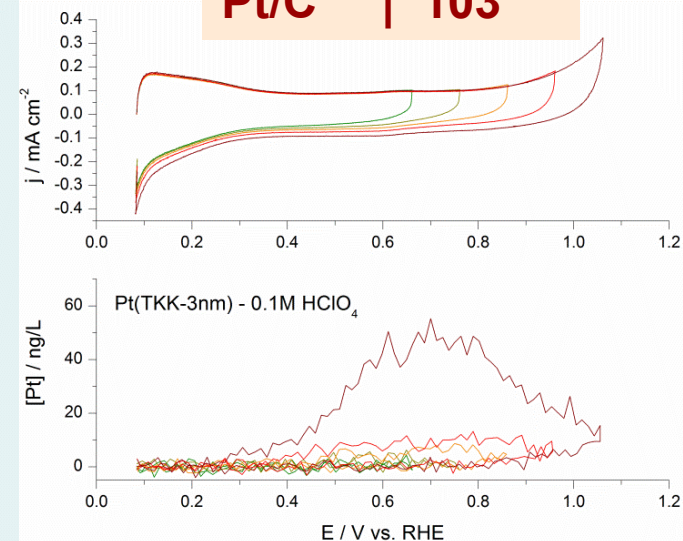
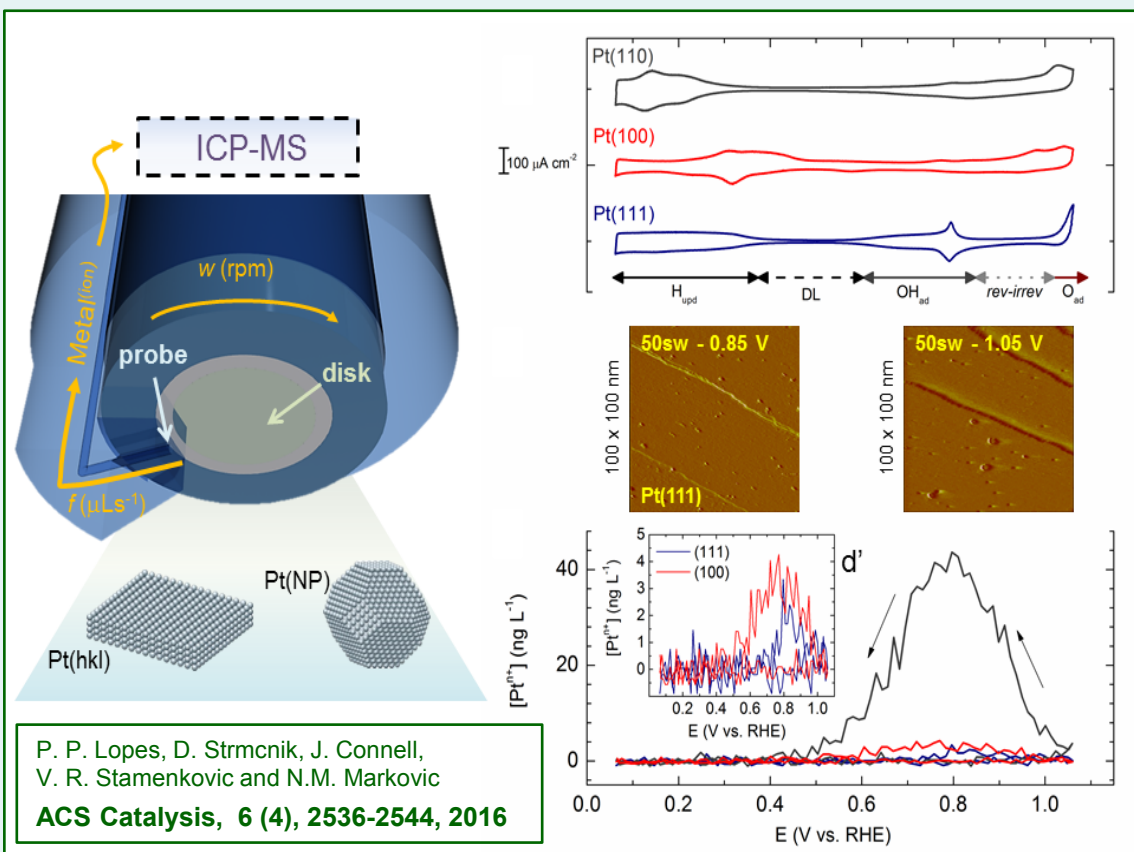


# In-Situ EC-ICP-MS Pt(hkl)-Surfaces vs. Pt/C



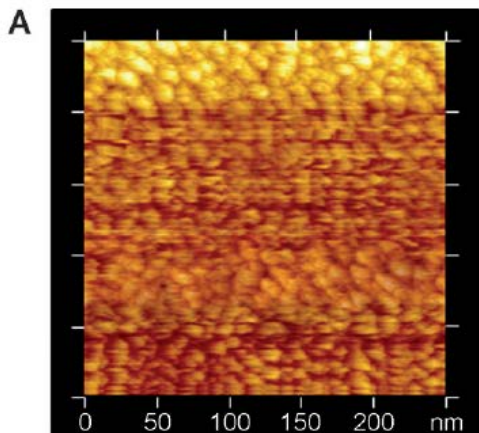
Total Pt loss over one potential cycle up to 1.05 V for distinct Pt surface morphologies, indicating the stability trend follows the coordination number of the surface sites

Pt Surface	Dissolved Pt per cycle [μML]
Pt(111)	2
Pt(100)	7
Pt(110)	83
Pt-poly	36
<b>Pt/C</b>	<b>103*</b>

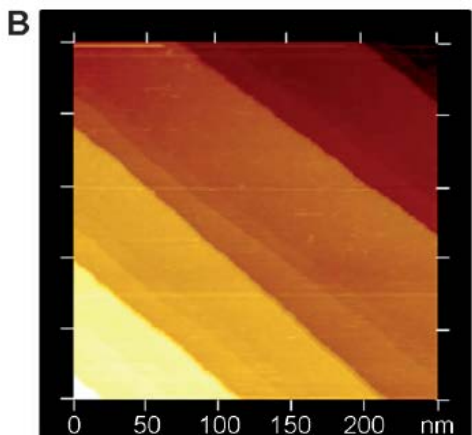


# Surface Structure + Composition: $Pt_3Ni[hkl]$ Surfaces

**STM**

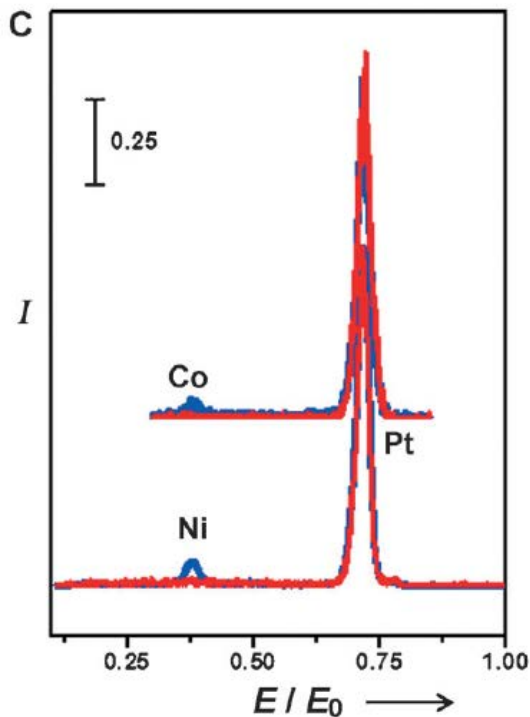


*Sputtered*

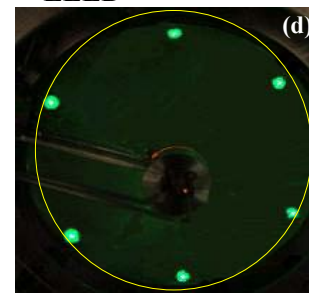


*Annealed*

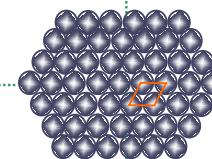
**LEIS**



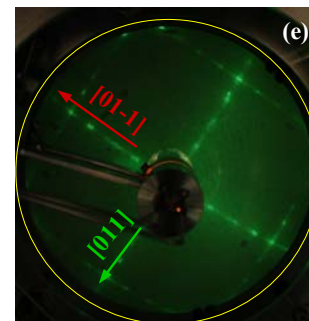
**LEED**



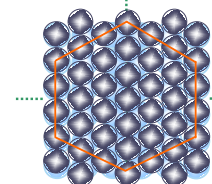
$Pt_3Ni(111)$



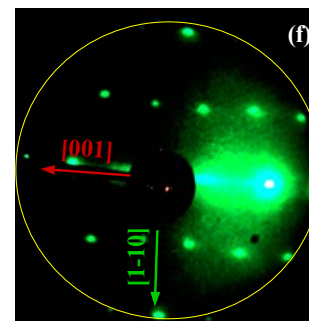
$p(1 \times 1)$



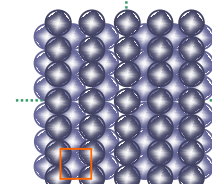
$Pt_3Ni(100)$



$c(5 \times 1)$



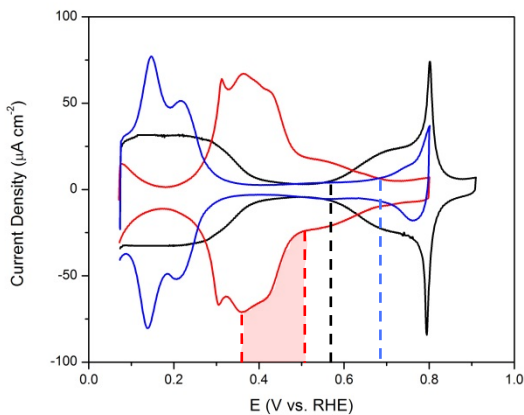
$Pt_3Ni(110)$



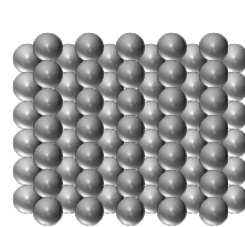
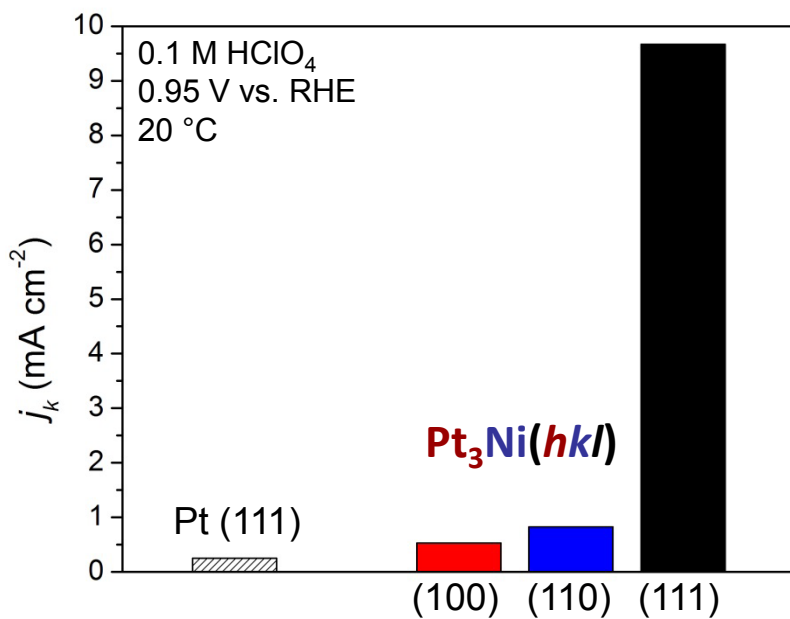
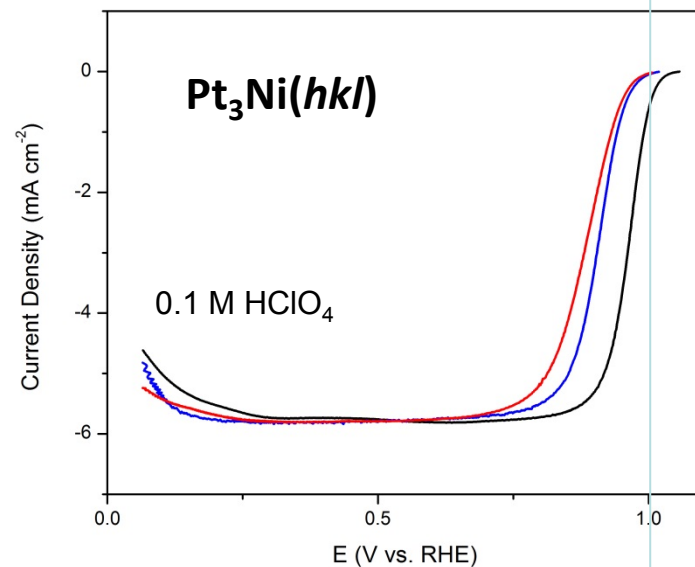
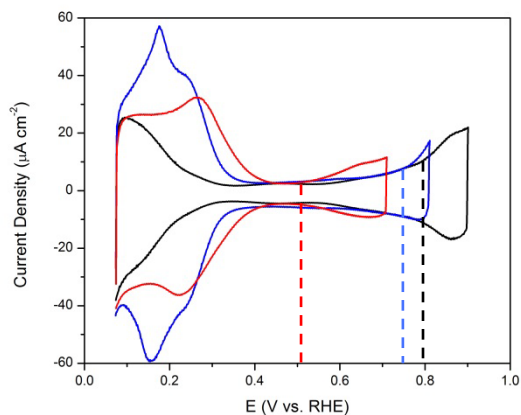
$(110)-(1 \times 1)$

# Activity: ORR Platinum Alloy Surfaces

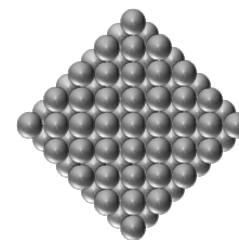
**Pt(hkl)**



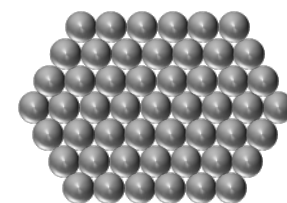
**Pt<sub>3</sub>Ni(hkl)**



**Pt<sub>3</sub>Ni(110)**



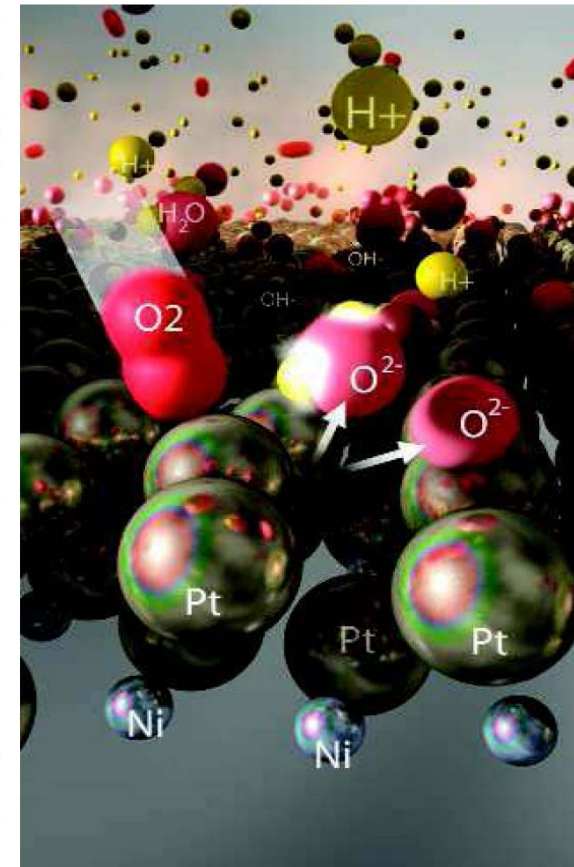
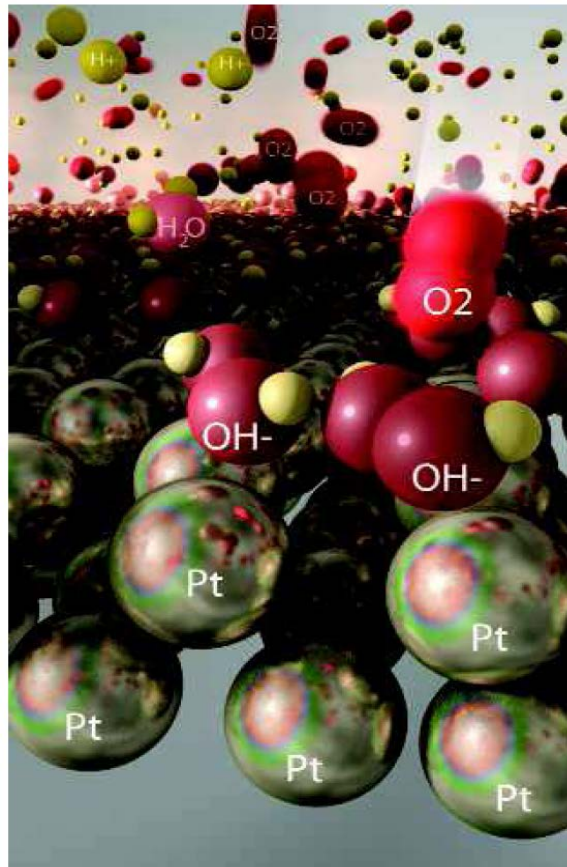
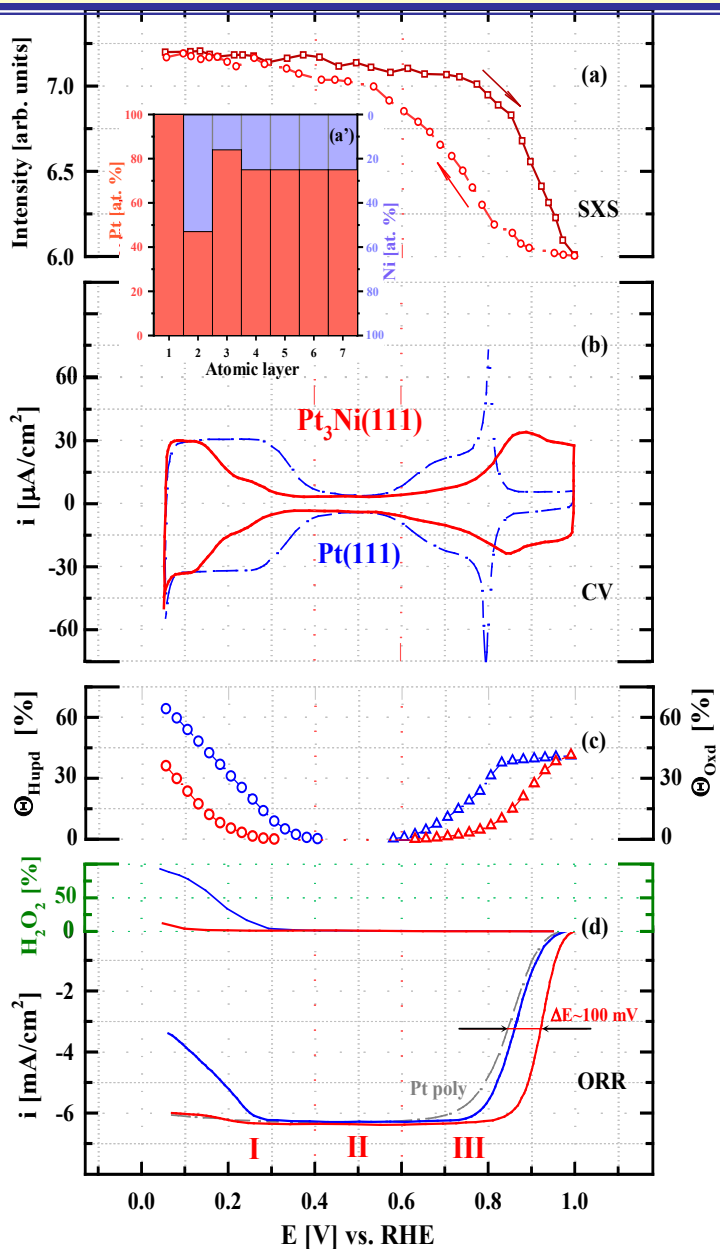
**Pt<sub>3</sub>Ni(100)**



**Pt<sub>3</sub>Ni(111)**

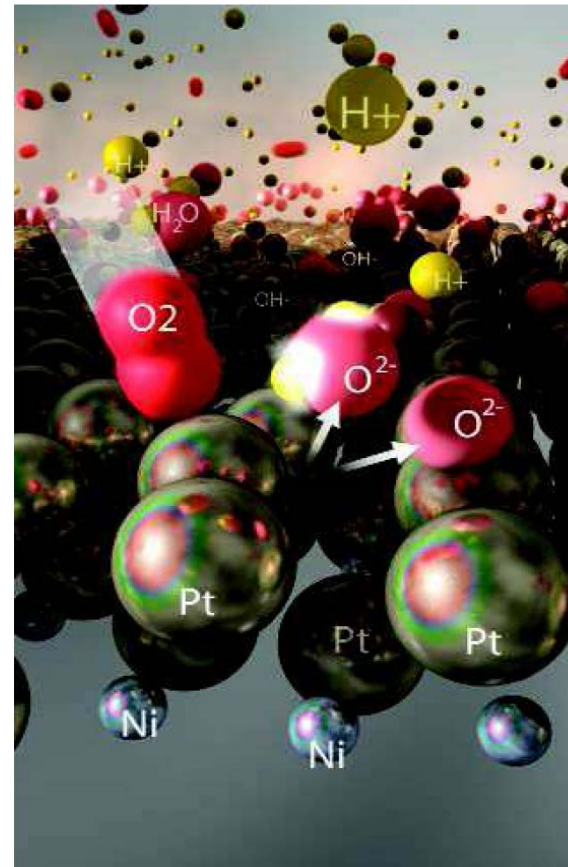
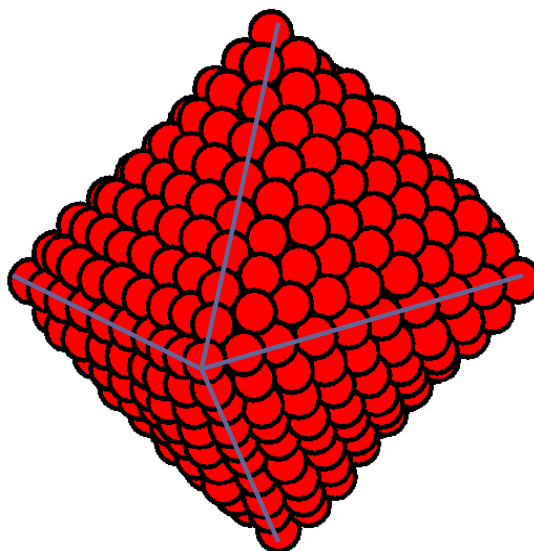
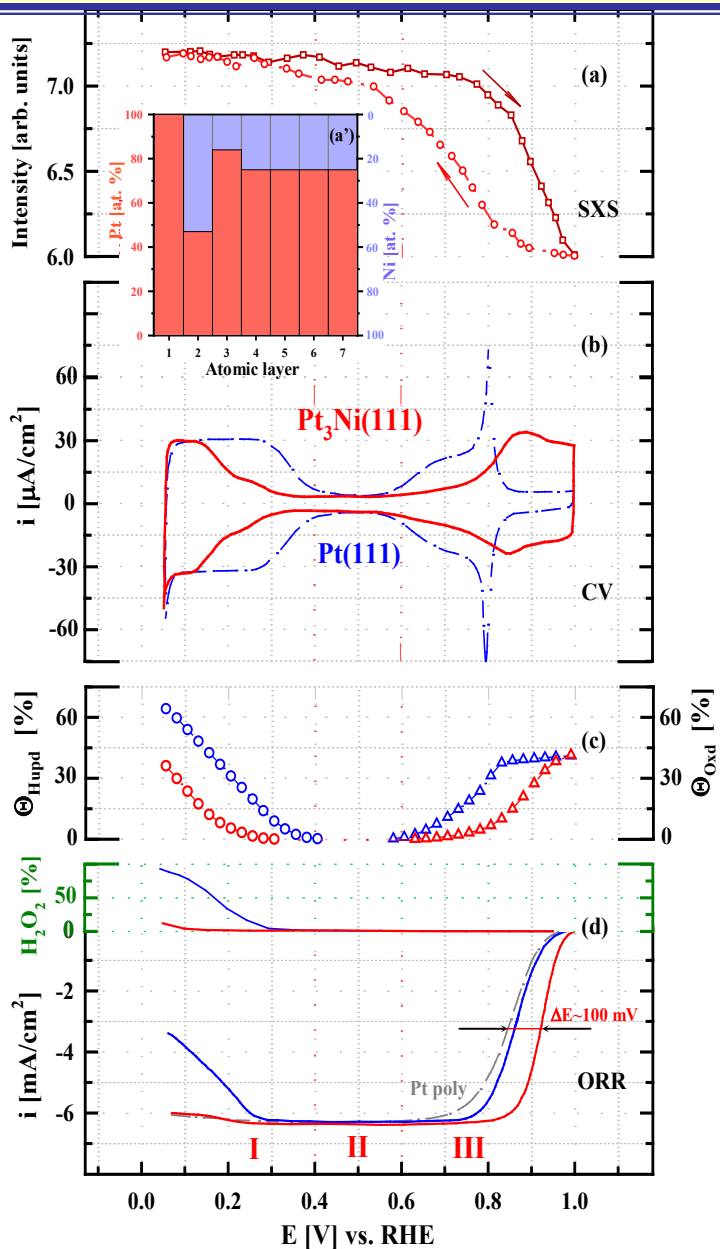
**Pt<sub>3</sub>Ni(111)/Pt-Skin Surface is the most active catalyst for the ORR**

# Subsurface Composition + Surface Structure: $Pt_3Ni(111)$



**$Pt_3Ni(111)/Pt$ -Skin Surface is the most active catalyst for the ORR (100-fold enhancement)**

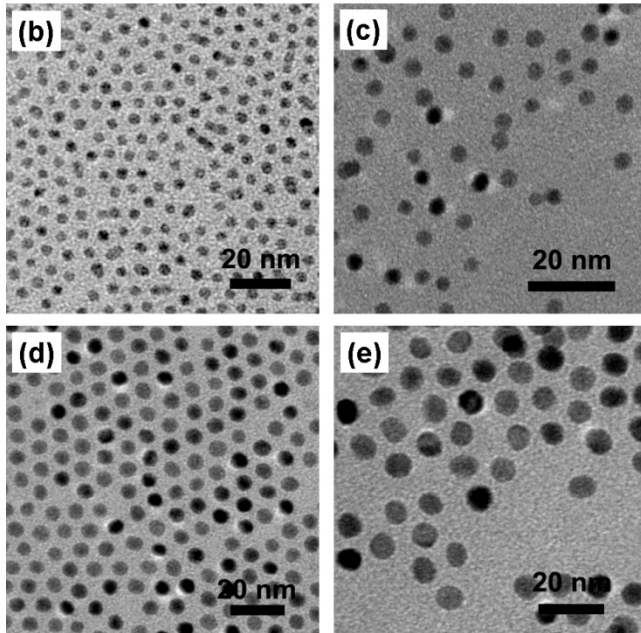
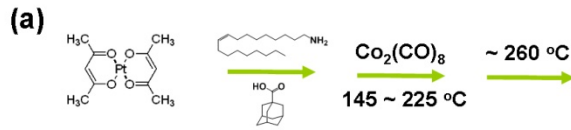
# Subsurface Composition + Surface Structure: $Pt_3Ni(111)$



$Pt_3Ni(111)/Pt$ -Skin Surface is the most active catalyst for the ORR (100-fold enhancement)

# Controlled Synthesis: *Multimetallic Nanocatalysts*

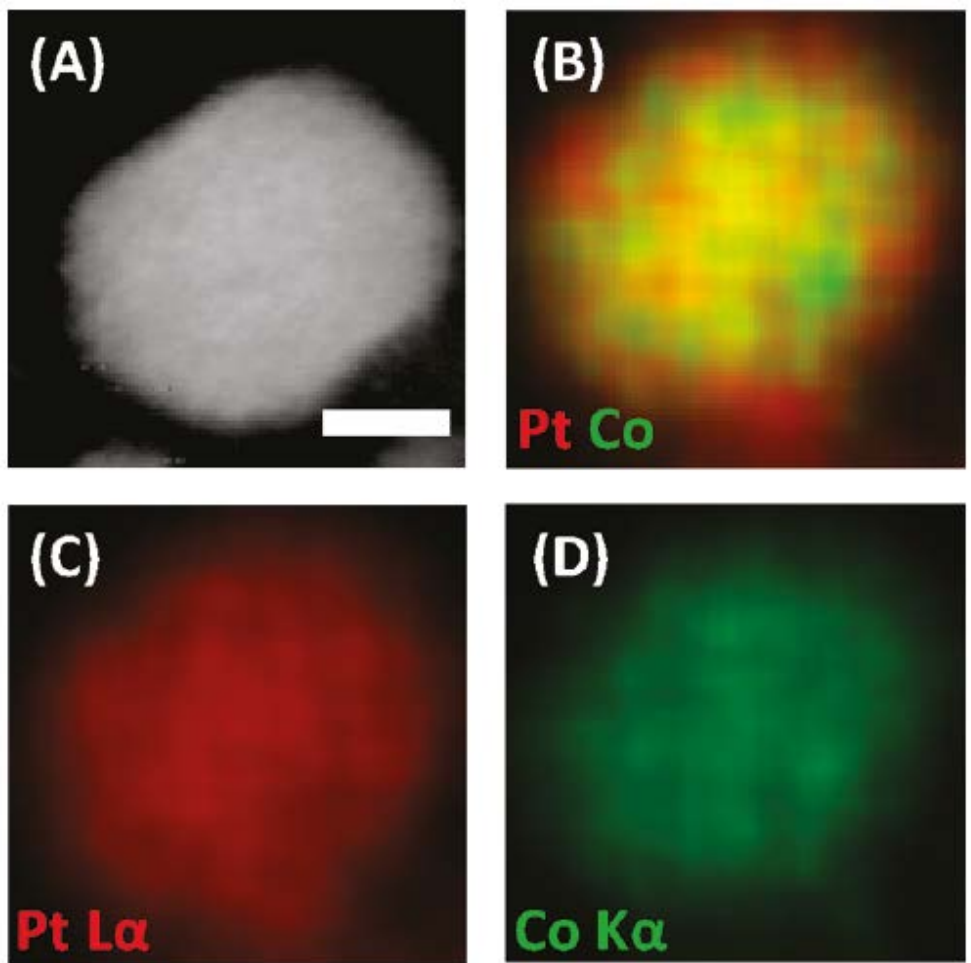
**Colloidal solvo - thermal approach** has been developed for monodispersed PtM NPs with **controlled size and composition**



**Efficient surfactant removal** method does not change the catalyst properties



## HAADF - STEM



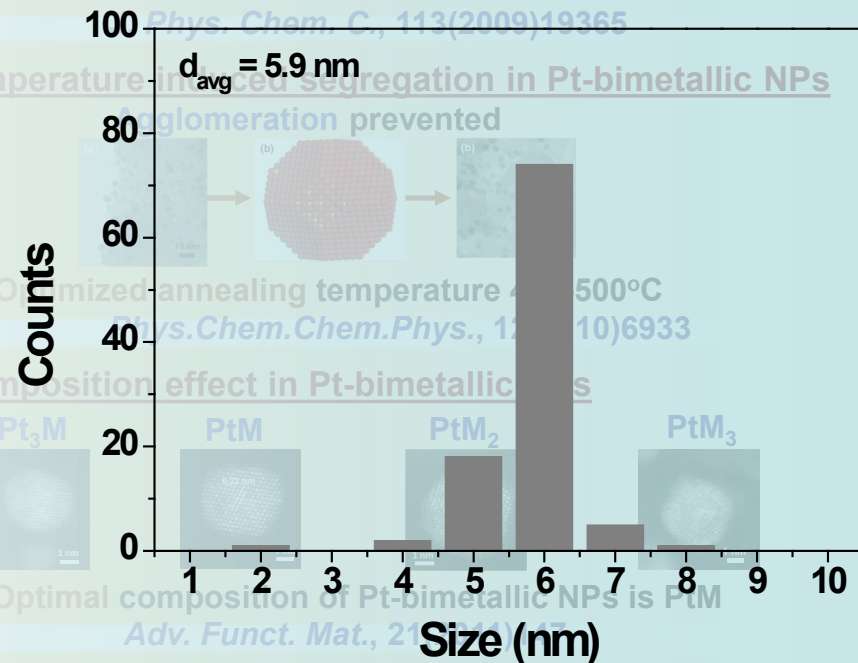
## 1° Particle size effect applies to Pt-bimetallic NPs

Specific Activity increases with particle size: 3 < 4.5 < 6 < 9 nm

Mass Activity decreases with particle size

Optimal size particle size ~5 nm

## Particle size distribution

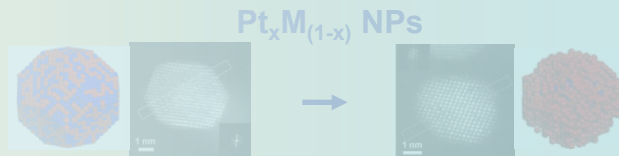


Optimized annealing temperature 400-500°C  
*Phys. Chem. Chem. Phys.*, 12 (2010) 6933

Composition effect in Pt-bimetallic NPs

Optimal composition of Pt-bimetallic NPs is PtM  
*Adv. Funct. Mat.*, 21 (2011) 1143

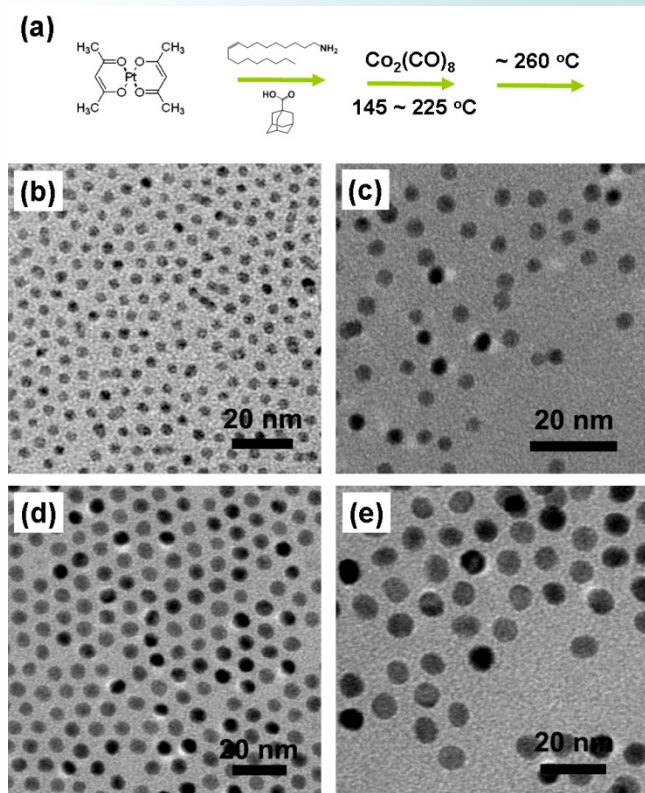
Surface chemistry of homogeneous Pt-bimetallic NPs



Dissolution of non Pt atoms forms Pt-skeleton surface

# Controlled Synthesis: *Multimetallic Nanocatalysts*

**Colloidal solvo-thermal approach** has been developed for monodispersed PtM NPs with **controlled size and composition**



**Efficient surfactant removal** method does not change the catalyst properties

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**Specific Activity** increases with particle size:  $3 < 4.5 < 6 < 9 \text{ nm}$

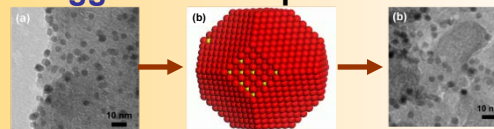
**Mass Activity** decreases with particle size

**Optimal size particle size** ~5nm

*J. Phys. Chem. C.*, 113(2009)19365

## 2° Temperature induced segregation in Pt-bimetallic NPs

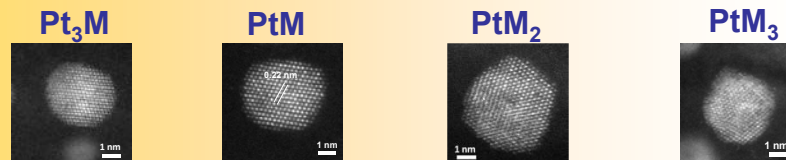
**Agglomeration prevented**



**Optimized annealing temperature** 400-500°C

*Phys.Chem.Chem.Phys.*, 12(2010)6933

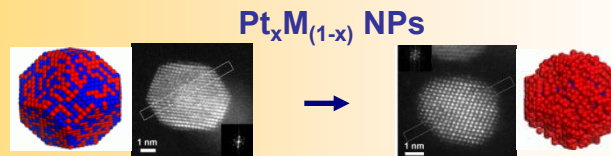
## 3° Composition effect in Pt-bimetallic NPs



**Optimal composition** of Pt-bimetallic NPs is PtM

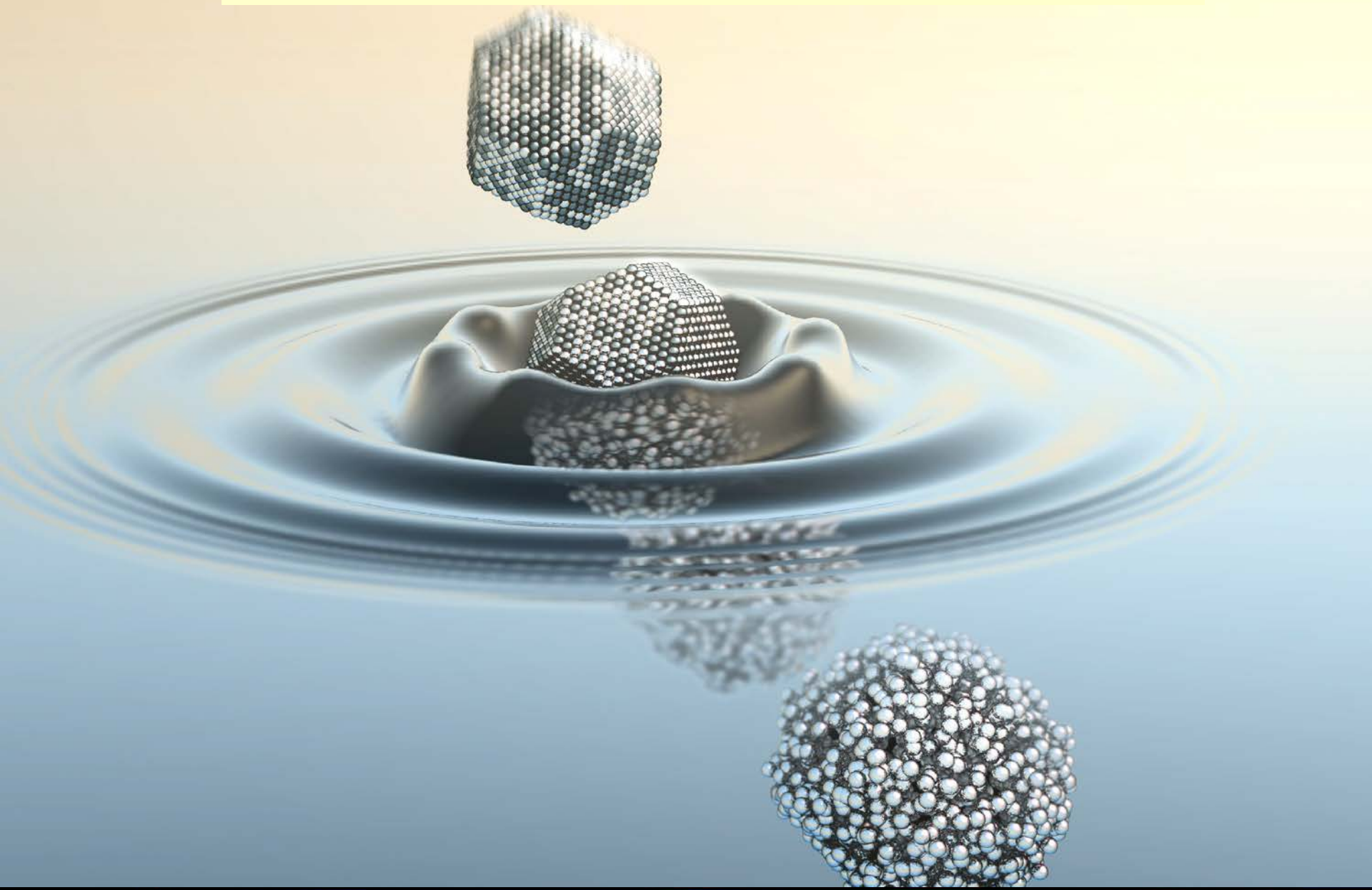
*Adv. Funct. Mat.*, 21(2011)147

## 4° Surface chemistry of homogeneous Pt-bimetallic NPs

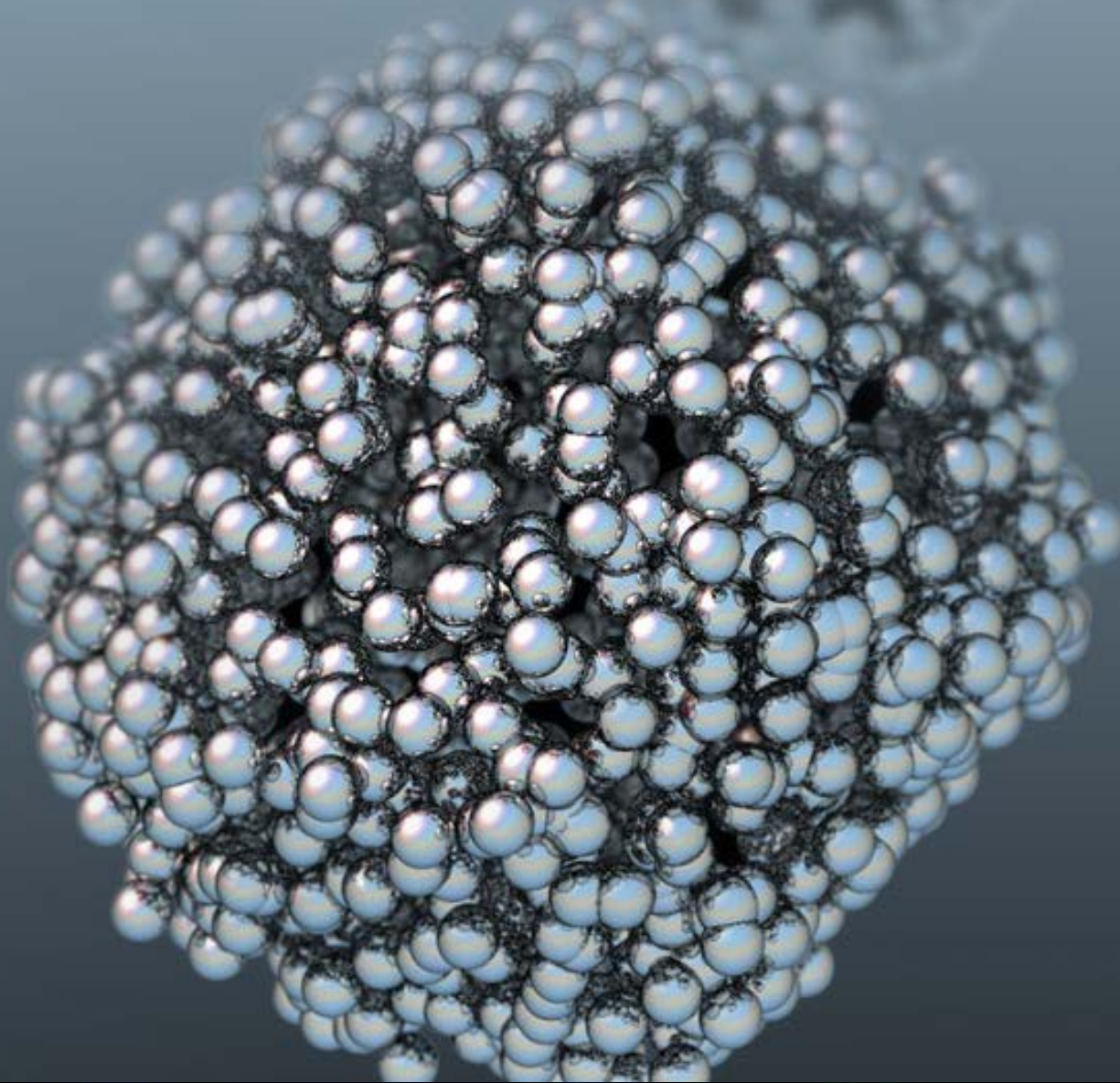


**Dissolution** of non Pt atoms forms **Pt-skeleton** surface

**$Pt_xNi_{1-x}$ : Surface Chemistry and Composition Effect**

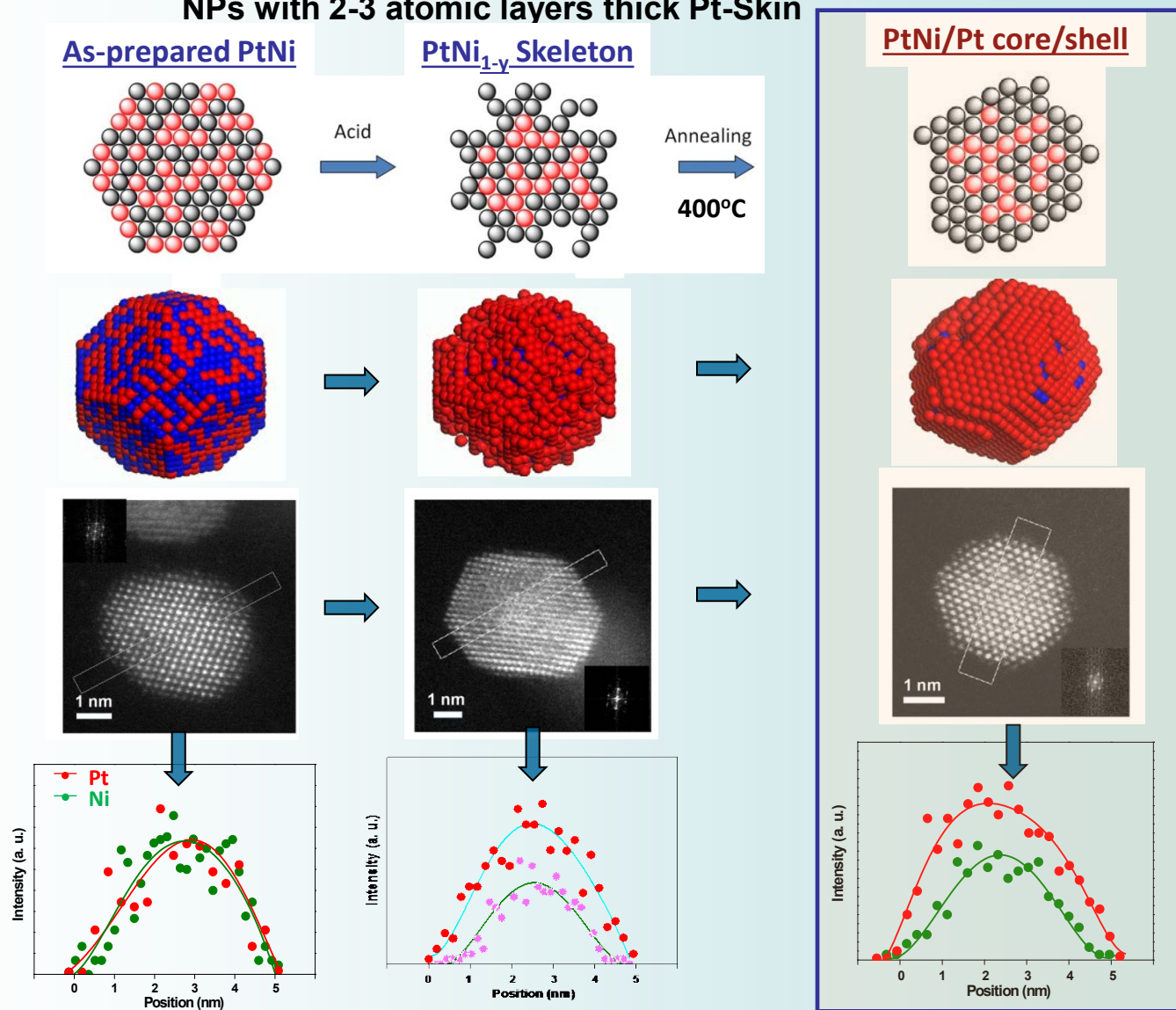


$Pt_xNi_{1-x}$ : *Surface Chemistry and Composition Effect*



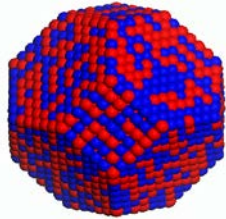
# PtNi with multilayered Pt-Skin Surfaces : *Tailoring Nanoscale Surfaces*

Temperature annealing protocol used to transform PtNi<sub>1-x</sub> skeletons to multilayered PtNi/Pt NPs with 2-3 atomic layers thick Pt-Skin

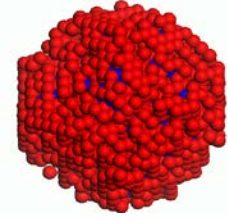


# NPs with multilayered Pt-Skin Surface: *PtNi/C*

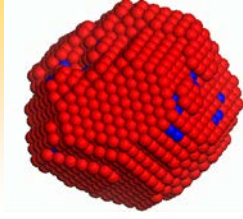
As Synthesized



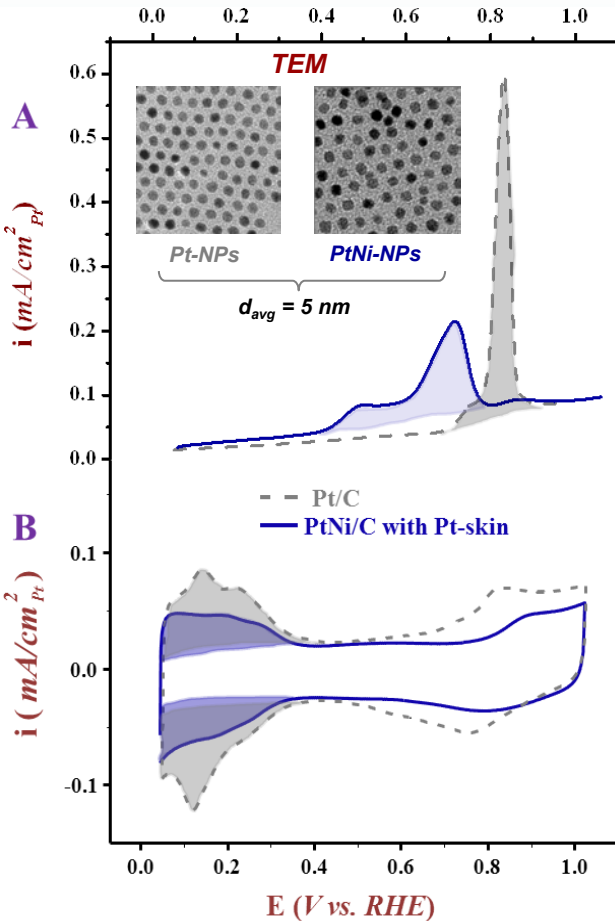
Leached



Annealed



Multilayered Pt-skin NP



Catalysts with multilayered Pt-skin surfaces exhibit substantially lower coverage by  $H_{upd}$  vs. Pt/C (up to 40% lower  $H_{upd}$  region is obtained on Pt-Skin catalyst)

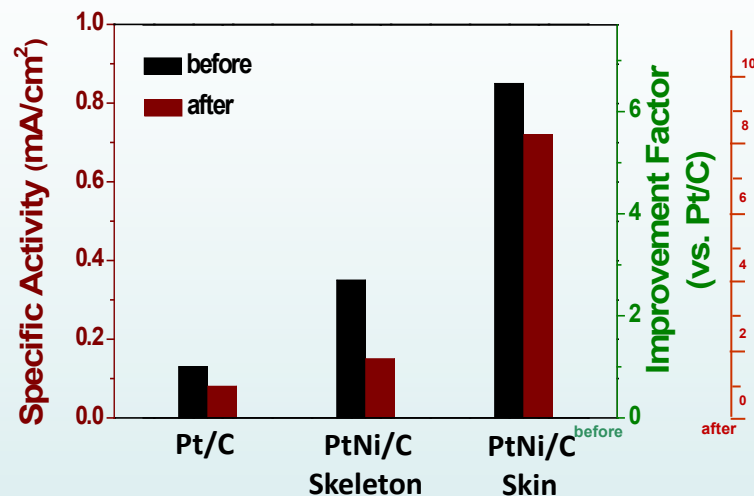
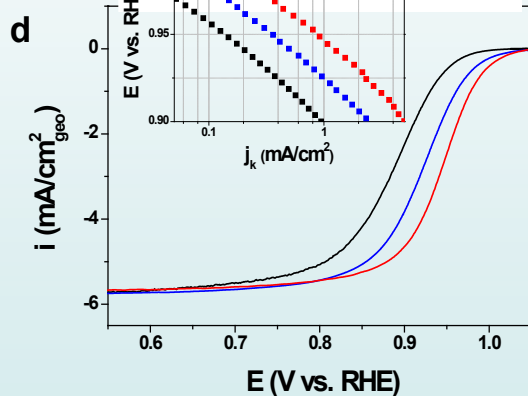
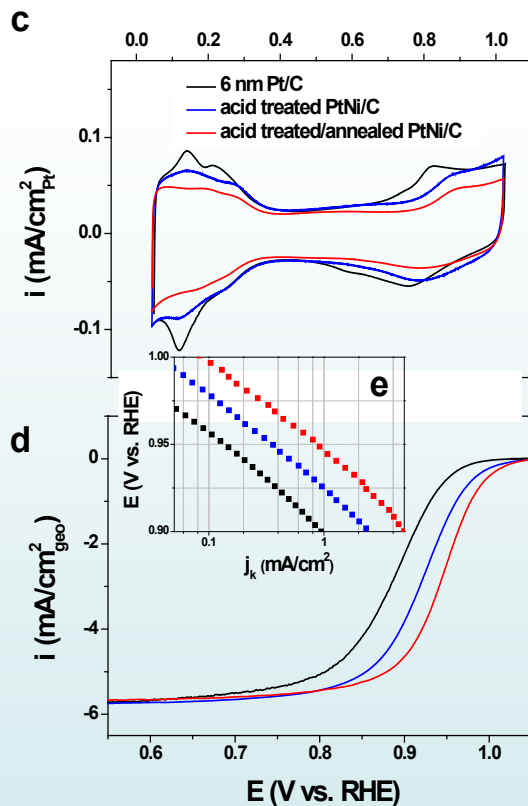
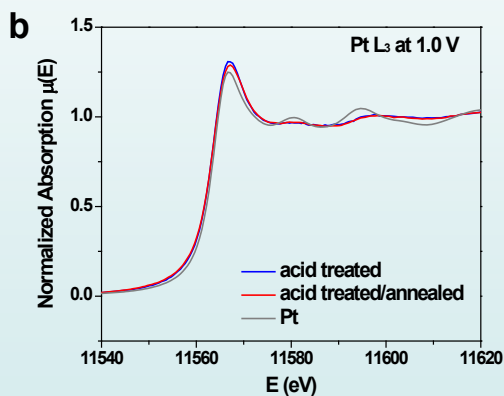
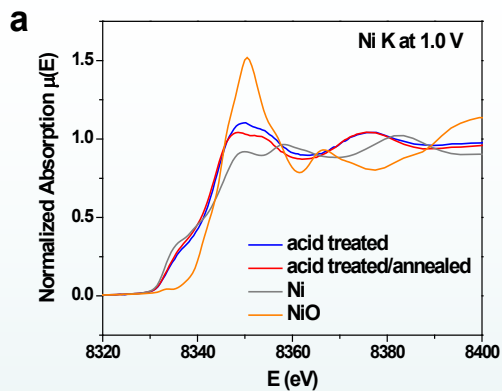
Surface coverage of adsorbed CO is not affected on Pt-skin surfaces

Ratio between  $Q_{CO}/Q_{H_{upd}} > 1$  is indication of Pt-skin formation

Catalyst	$Q_H$ ( $\mu\text{C}$ )	$ECSA_H$ ( $\text{cm}^2$ )	$Q_{CO}$ ( $\mu\text{C}$ )	$ECSA_{CO}$ ( $\text{cm}^2$ )	$Q_{CO}/2Q_H$
Pt/C	279	1.47	545	1.41	0.98
PtNi/C	292	1.54	615	1.60	1.05
PtNi-skin/C	210	1.10	595	1.54	1.42

Electrooxidation of adsorbed CO (CO stripping) has to be performed for Pt-alloy catalysts in order to avoid underestimation electrochemically active surface area and overestimation of specific and mass activities

# PtNi Catalyst: RDE Studies of Multilayered Pt-Skin Surfaces



**TEM/XRD:** Content of Ni is maximized and allows formation of the multilayered Pt-skin by leaching/annealing

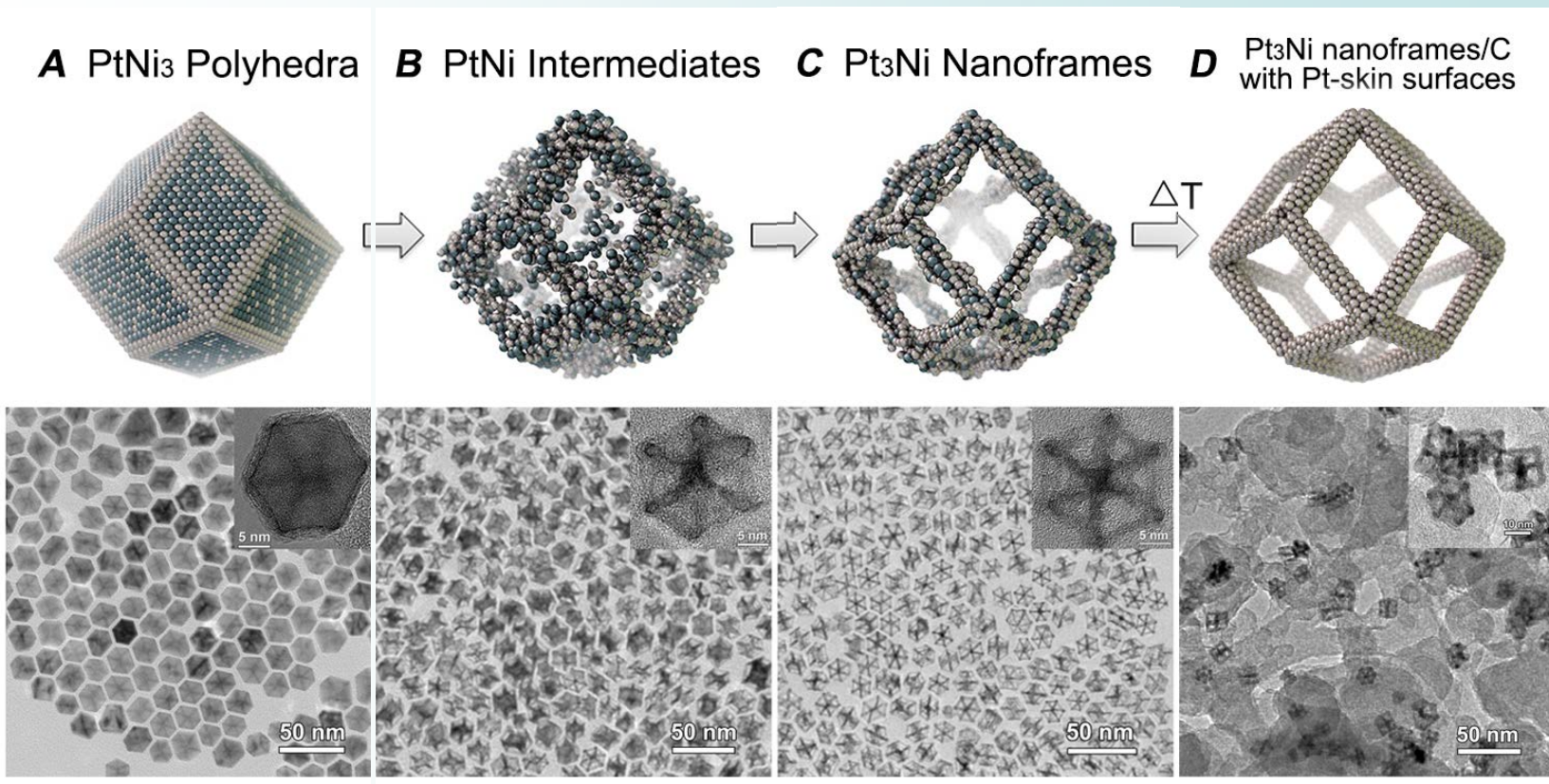
**RDE:** PtNi-Skin catalyst exhibits superior catalytic performance for the ORR and is highly durable system

**In-Situ XANES:** Subsurface Ni is well protected by less oxophilic multilayered Pt-skin during potential cycling

**Durability:** Surface area loss about 10%, SA 8 fold increase and MA 10 fold increase over Pt/C after 20K cycles

# Mass Activity Enhancement by 3D Surfaces: *Multimetallic Nanoframes*

In collaboration with Peidong Yang, UC Berkeley

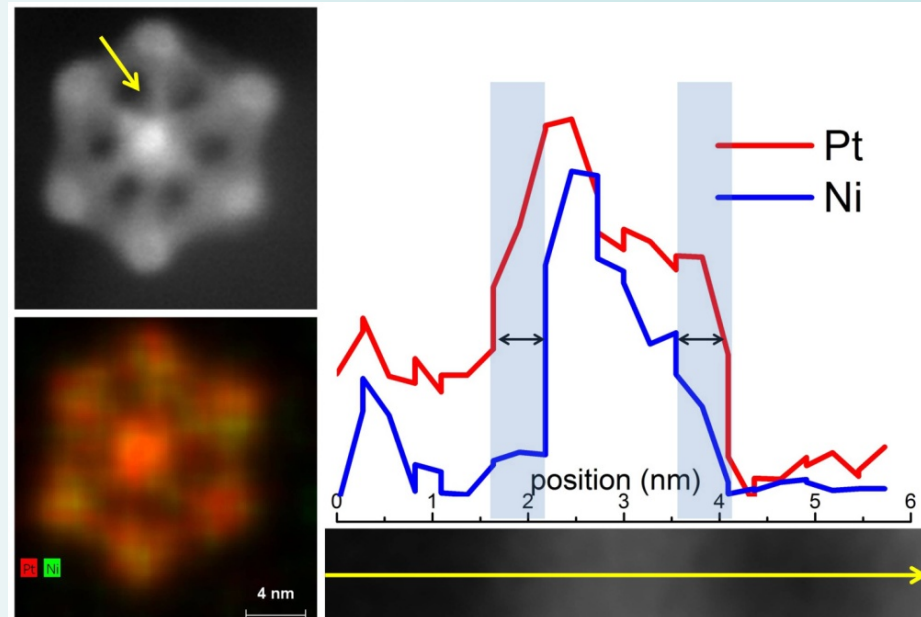
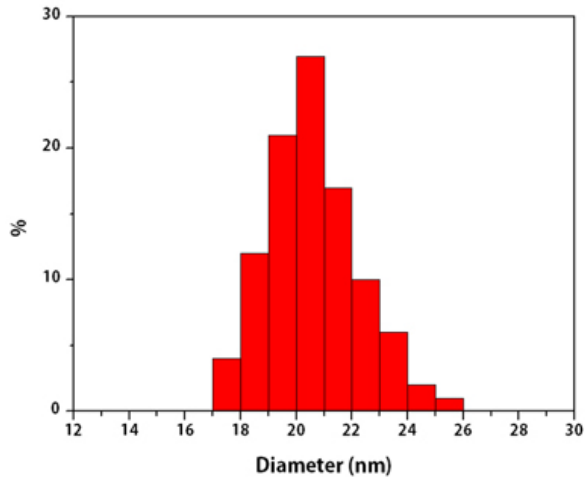


- H<sub>2</sub>PtCl<sub>6</sub> and Ni(NO<sub>3</sub>)<sub>2</sub> react in oleylamine at 270°C for 3 min forming solid PtNi<sub>3</sub> polyhedral NPs
- Reacting solution is exposed to O<sub>2</sub> that induces spontaneous corrosion of Ni
- Ni rich NPs are converted into Pt<sub>3</sub>Ni nanoframes with Pt-skeleton type of surfaces
- Controlled annealing induces Pt-Skin formation on nanoframe surfaces



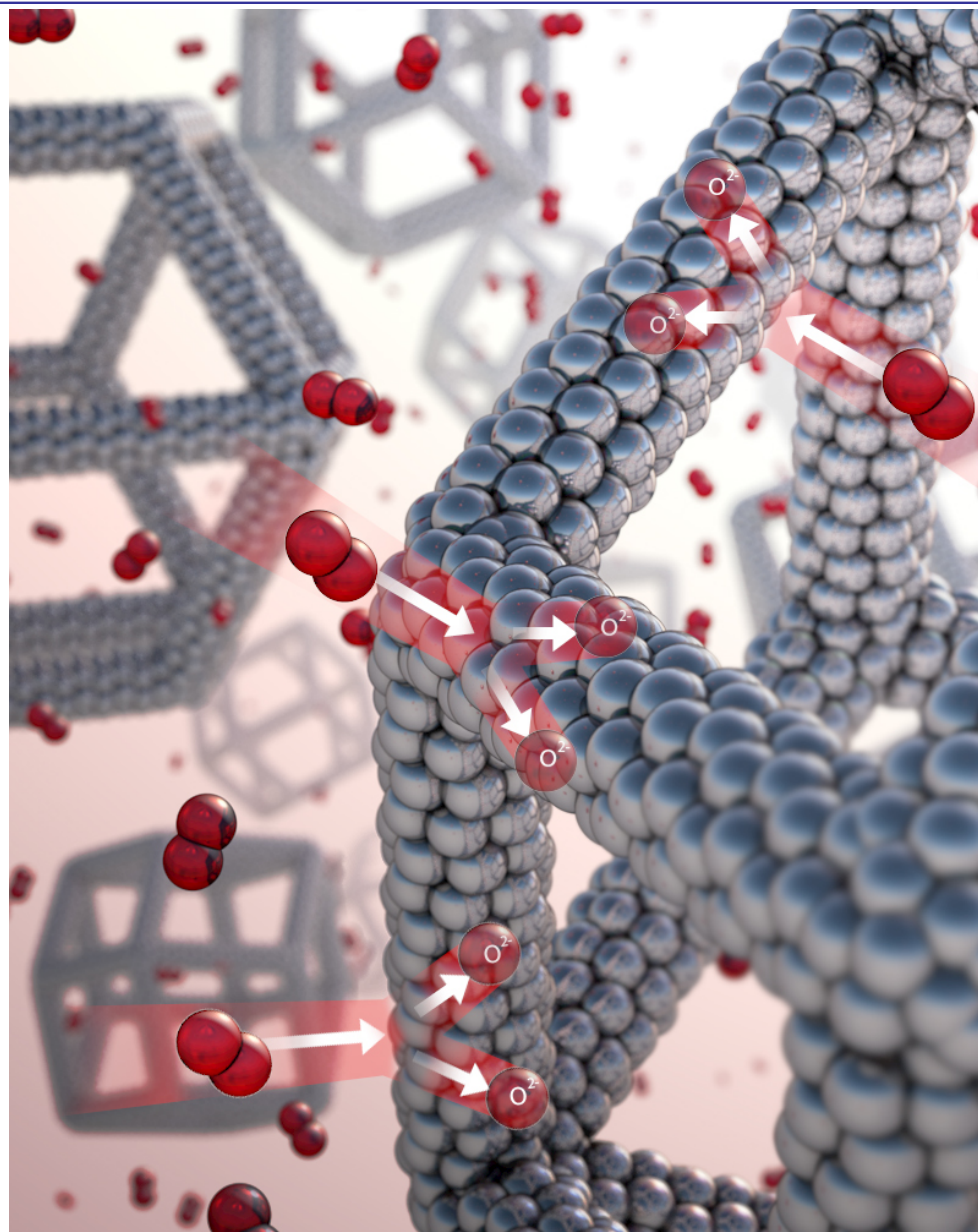
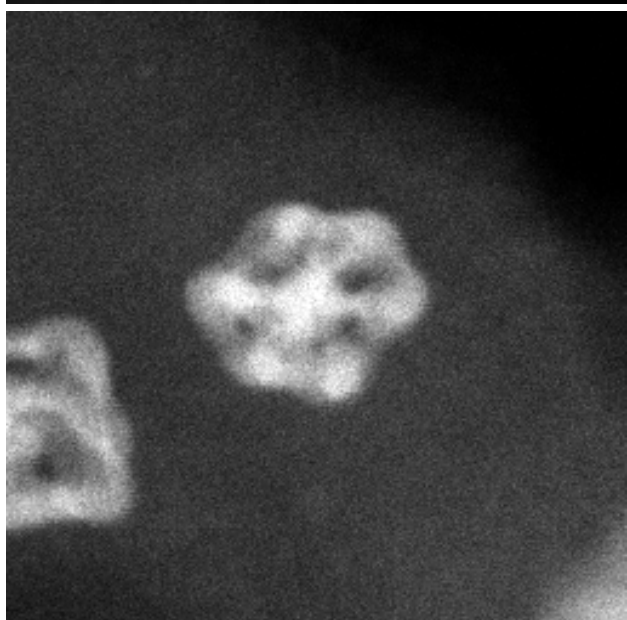
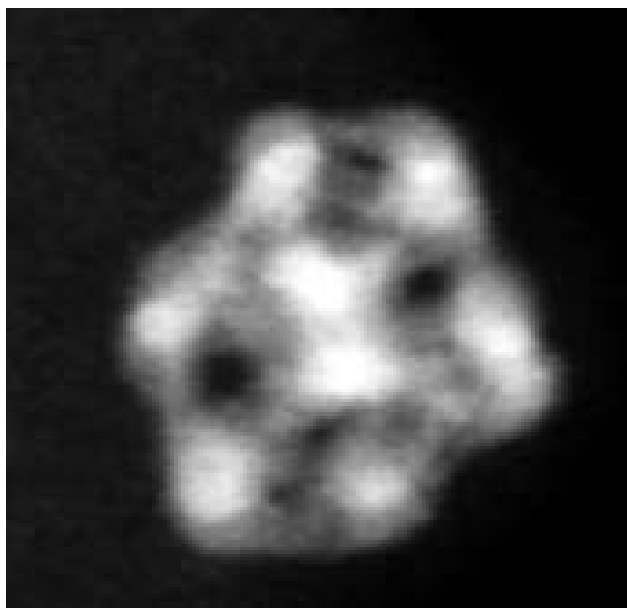
# Compositional Profile: *PtNi Nanoframes with Pt-skin Surfaces*

Pt<sub>3</sub>Ni Frames  
20.6 ± 1.6 nm



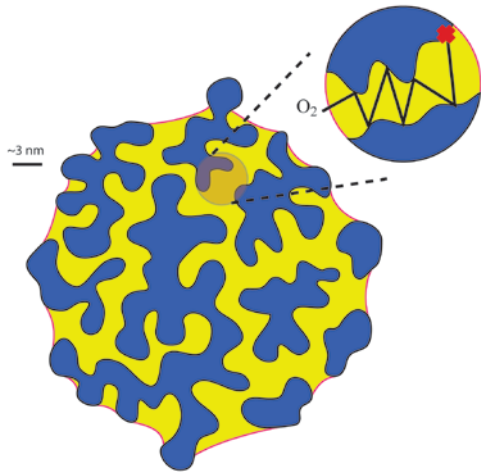
- Narrow particle size distribution
- Hollow interior
- Formation of Pt-skin with the thickness of 2ML
- Surfaces with 3D accessibility for reactants
- Segregated compositional profile with overall Pt<sub>3</sub>Ni composition

# Multimetallic Nanoframes with 3D Electrocatalytic Surfaces



# Improving the ORR Rate by *Protic Ionic Liquids*

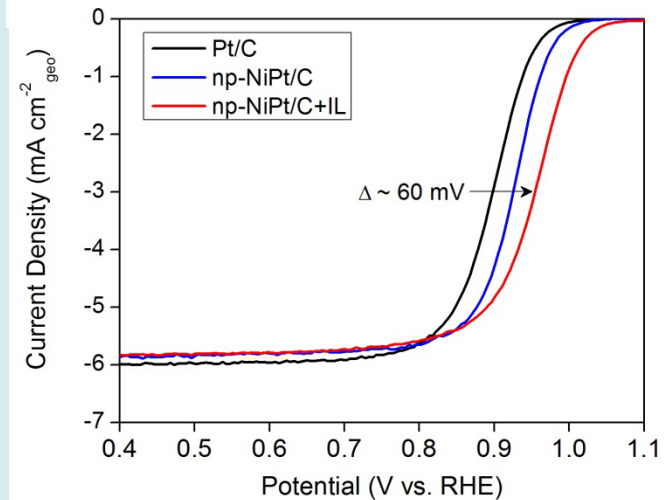
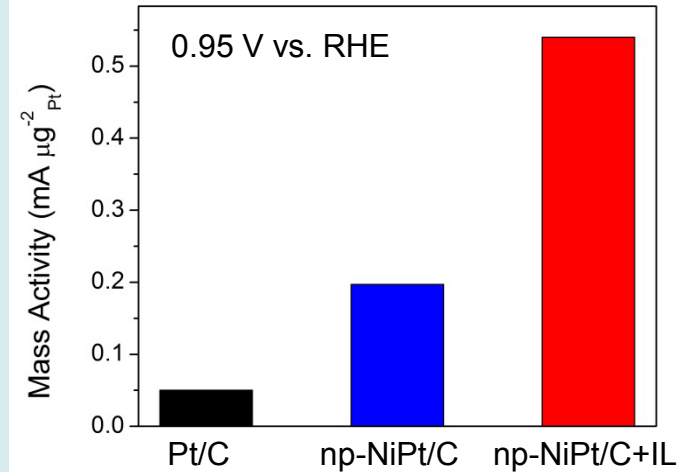
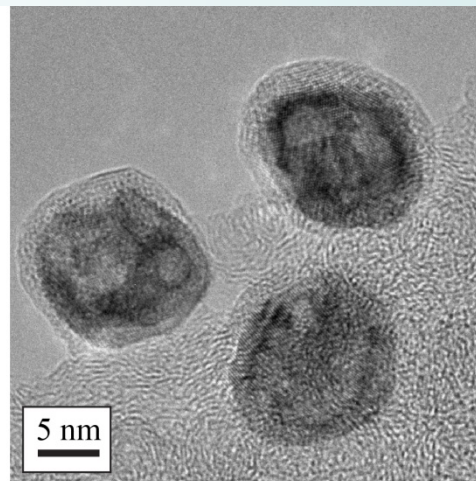
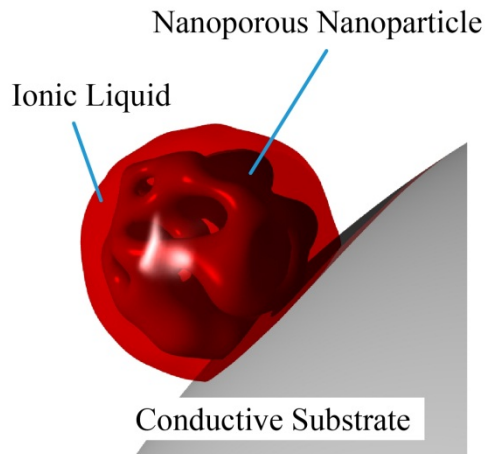
[MTBD][beti]



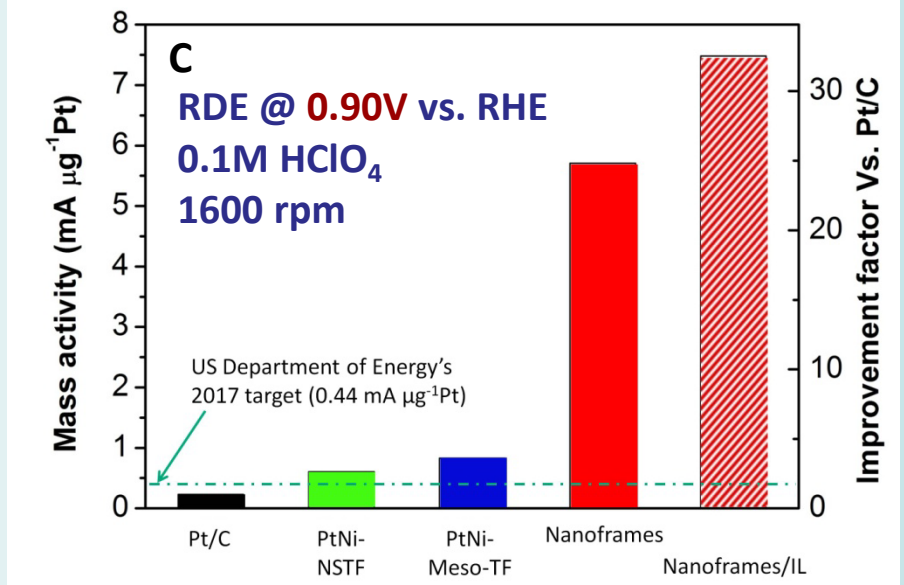
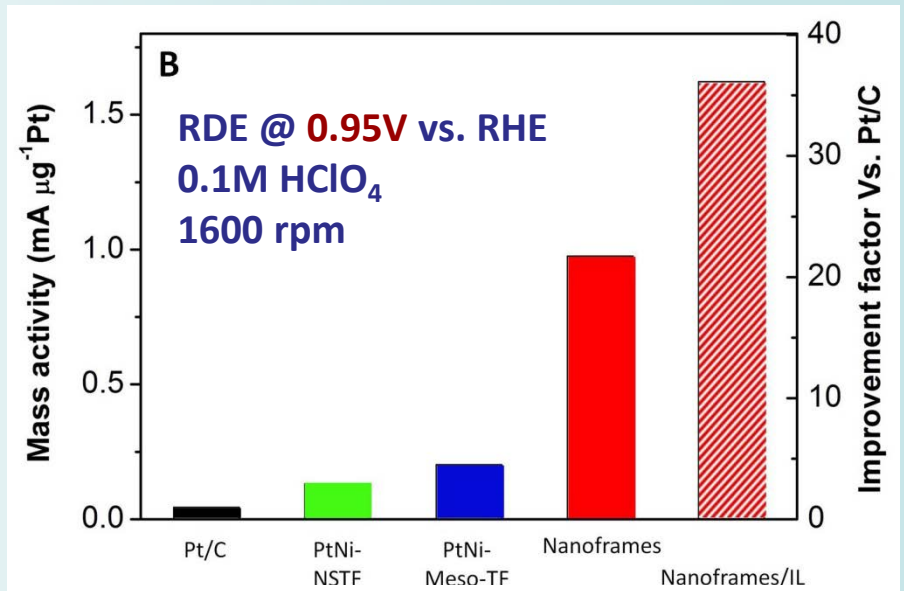
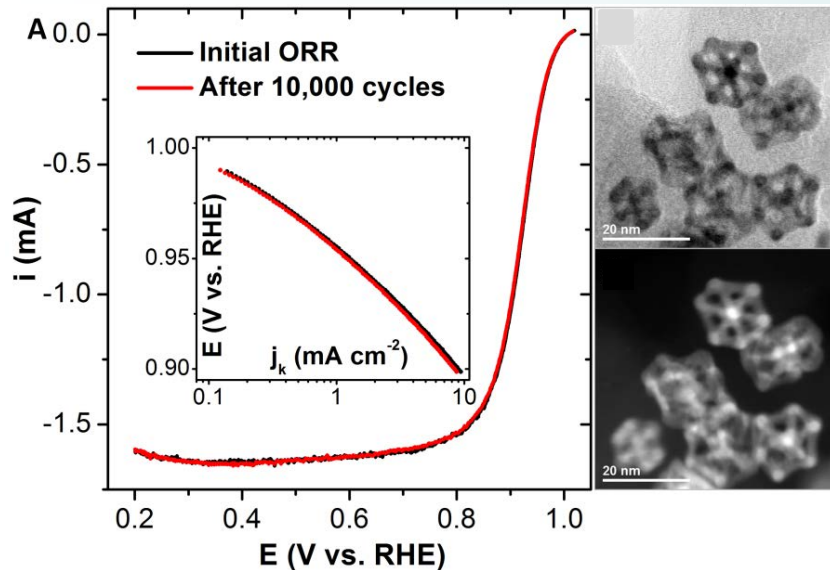
**Chemically Tailored Interface**  
 High O<sub>2</sub> solubility along with hydrophobicity yield improved ORR kinetics

- Higher O<sub>2</sub> solubility than H<sub>2</sub>O
- Protic (high proton conductivity)
- Hydrophobic
- Thermally Stable

$$\frac{C_{O_2, [MTBD][beti]}}{C_{O_2, HClO_4}} = 2.40 \pm 0.013$$

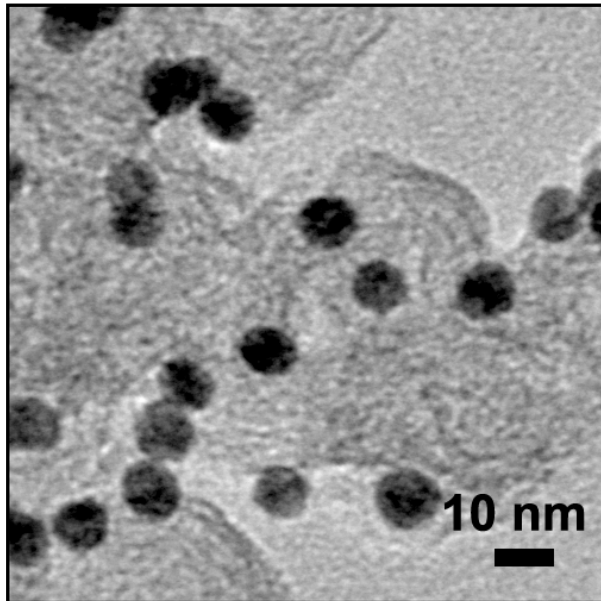


# Tailoring Activity: PtNi Nanoframes as the ORR Electrocatalyst

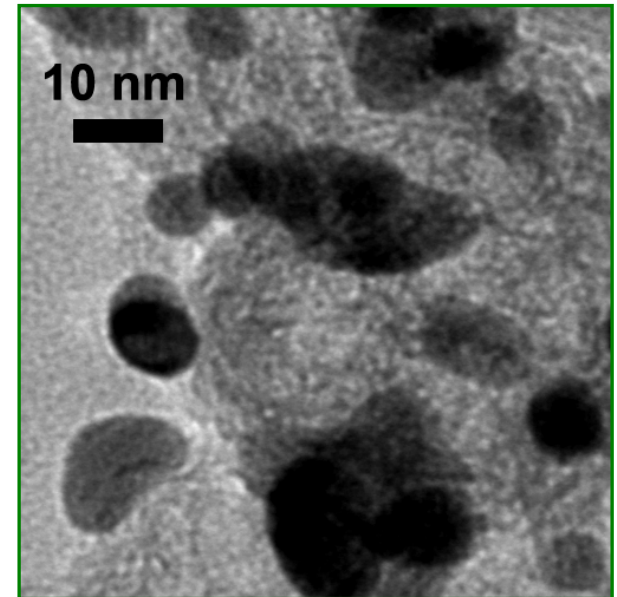


- No change in activity after 10K cycles 0.6 – 1.0 V
- Specific activity increase over 20-fold vs. Pt/C
- Mass activity increase over 35-fold vs. Pt/C
- Increase in mass activity over 15-fold vs. DOE target

**DURABILITY: Pt/C**



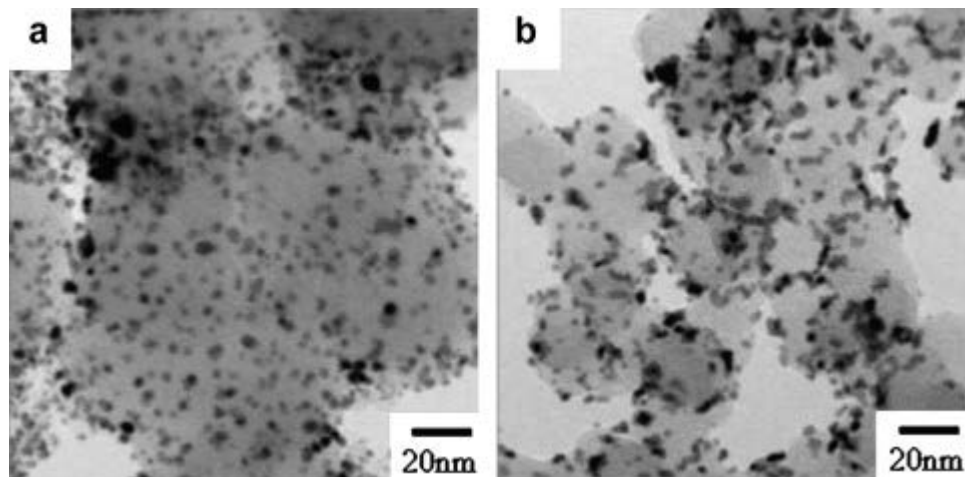
**Initial morphology**



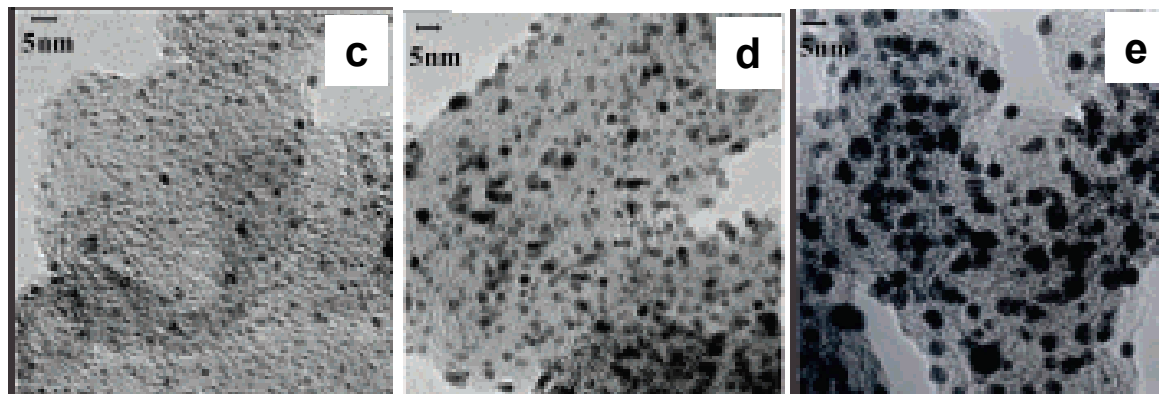
**After 60,000 cycles**

**Potential Range: 0.6-1.0V**

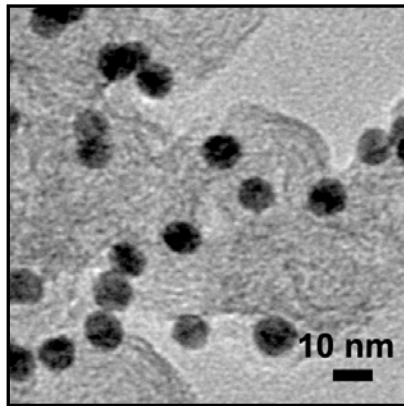
## Commercial Pt/C Catalysts



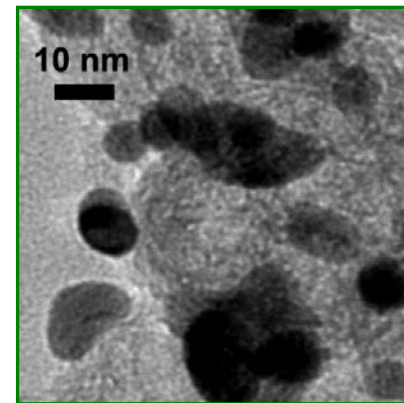
- Commercial catalysts are usually made by impregnation methods.
- Poor control
  - Broad size distribution
  - Different, undefined morphologies, but everyone calls them “cubo-octahedral”, which is, in fact, not correct!



**DURABILITY: *Pt/C***



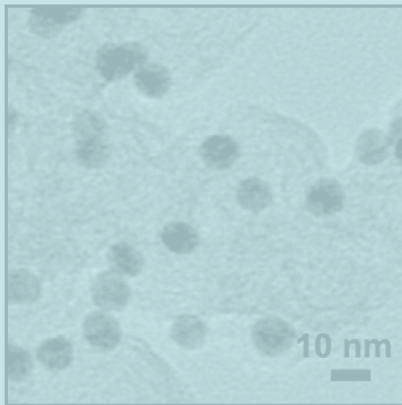
**Initial morphology**



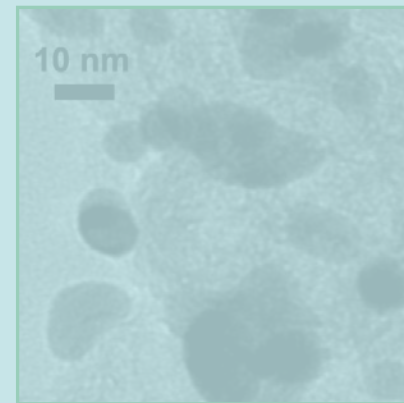
**After 60,000 cycles**

**Potential Range: 0.6-1.0V**

**DURABILITY: Pt/C**

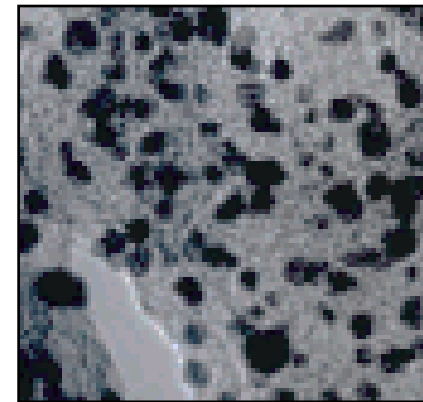
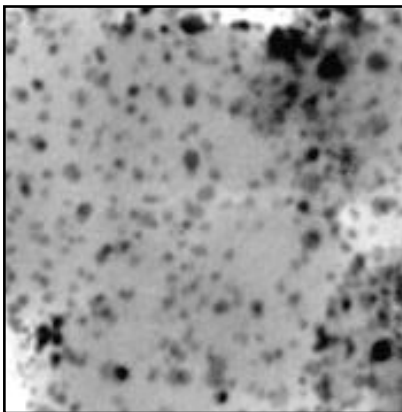


**Initial morphology**



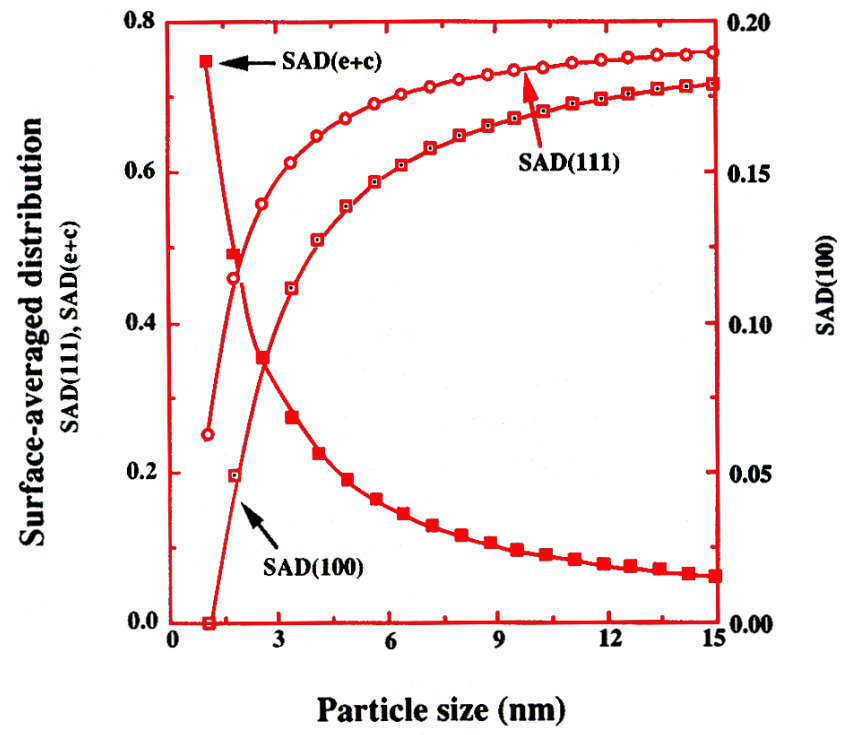
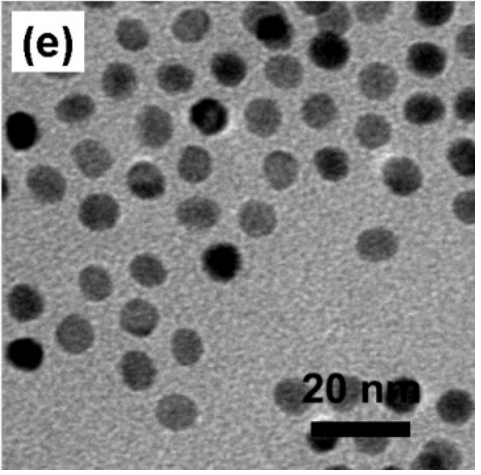
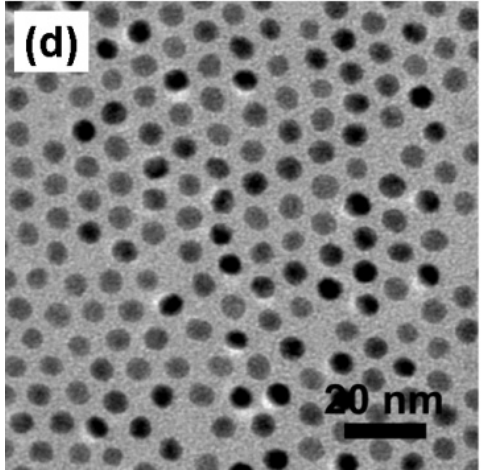
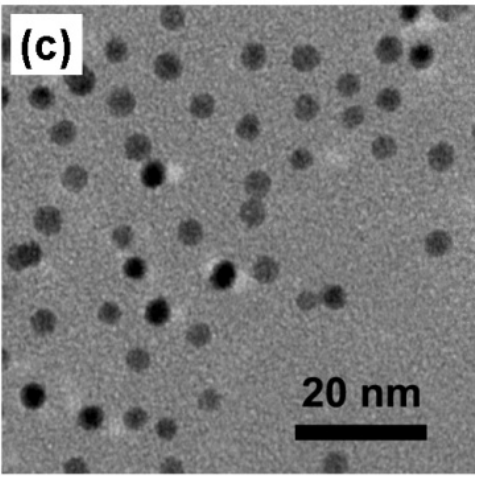
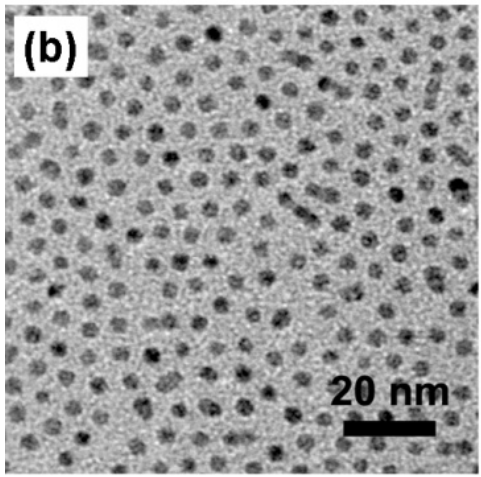
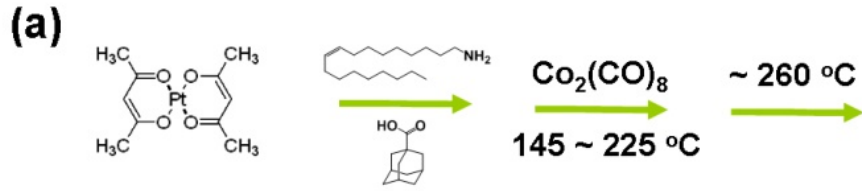
**After 60,000 cycles**

**Potential Range: 0.6-1.0V**

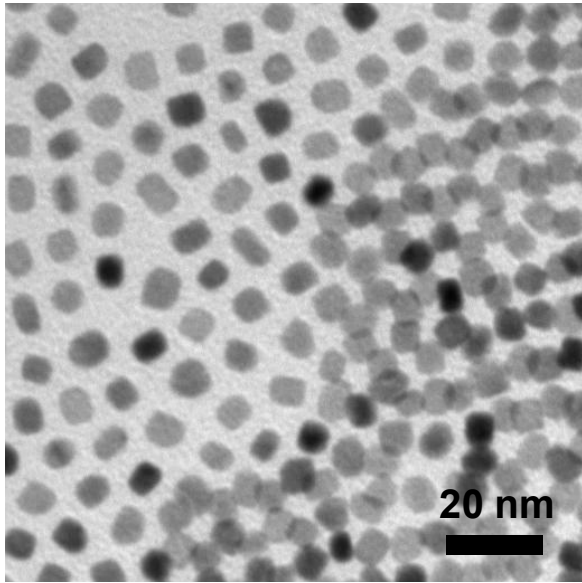




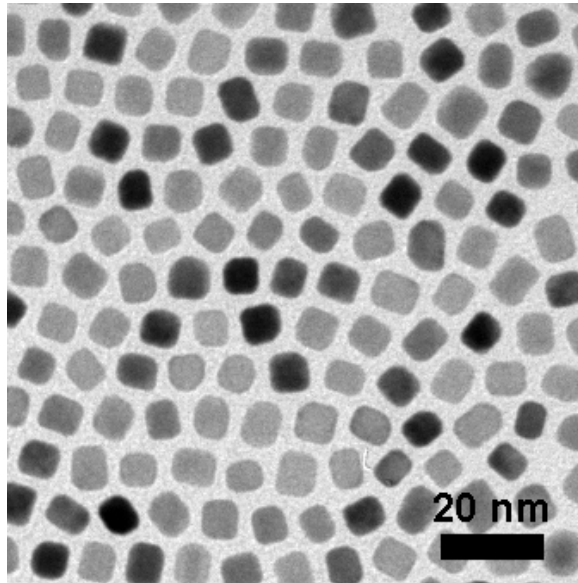
# SIZE EFFECT(s)? Pt/C



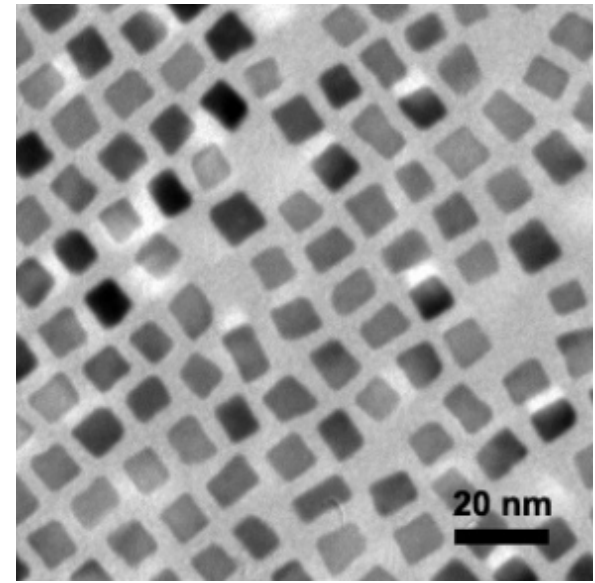
SHAPE EFFECT(s)? *Pt/C*



cubo-octahedron



truncated cube

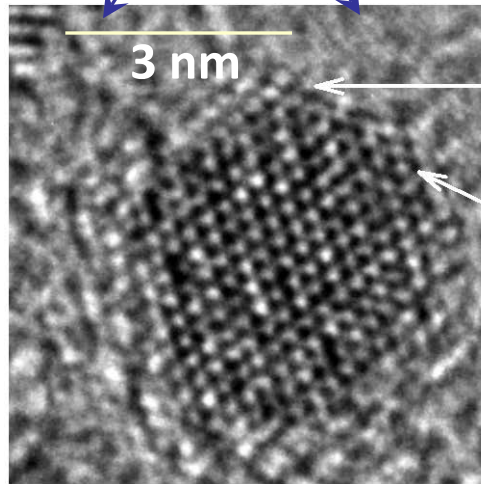
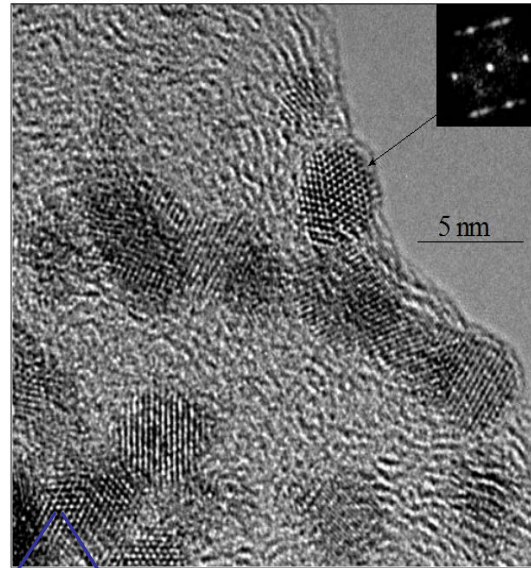
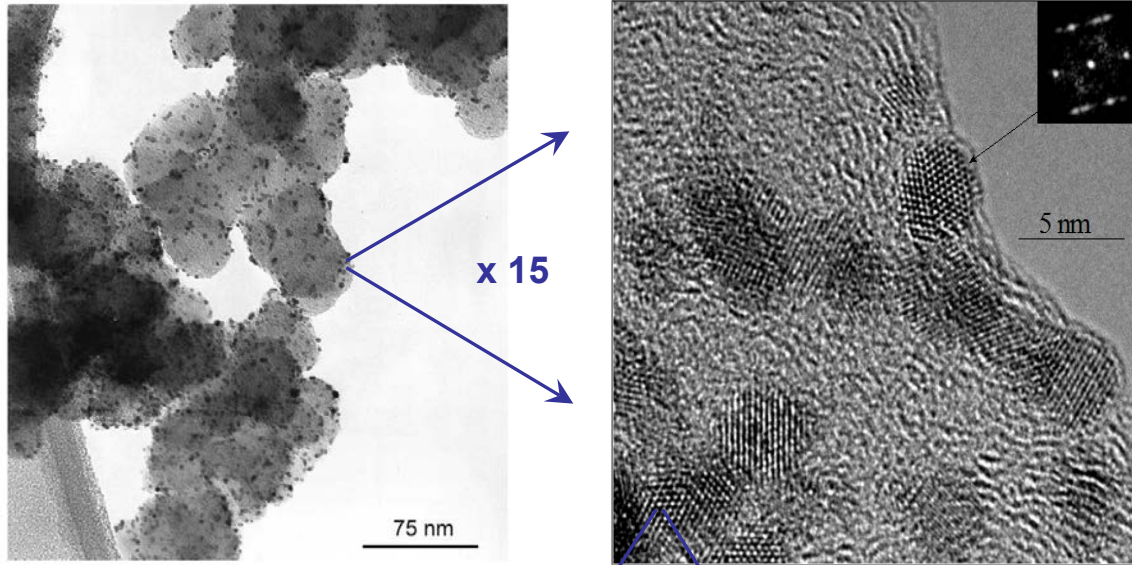


cube

- Uniform morphology
- Size control

octahedron (?)  $\rightarrow$  cubo-octahedral  $\rightarrow$  Cube

# HR-TEM: Characterization of Nanoscale Pt/C Catalyst



(111)

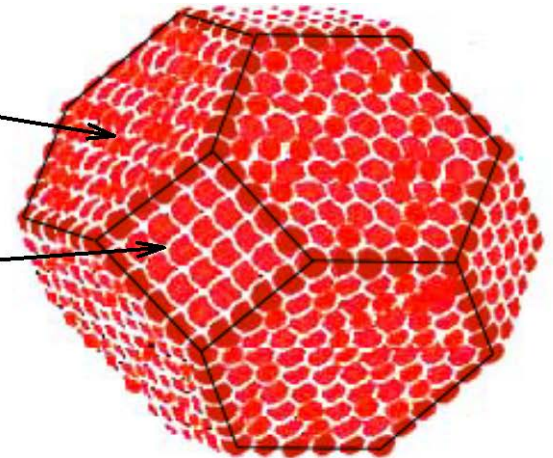
(100)

1) Shape: cubooctahedron

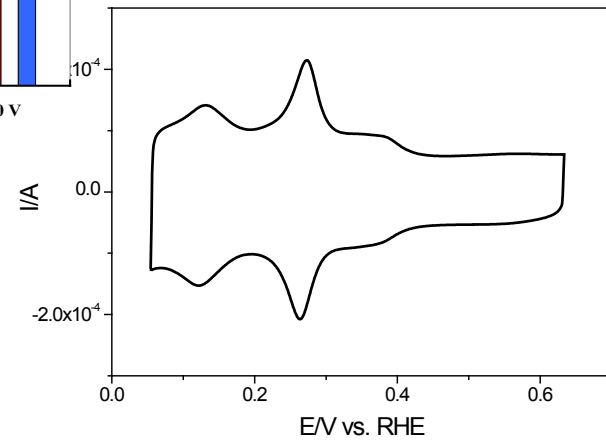
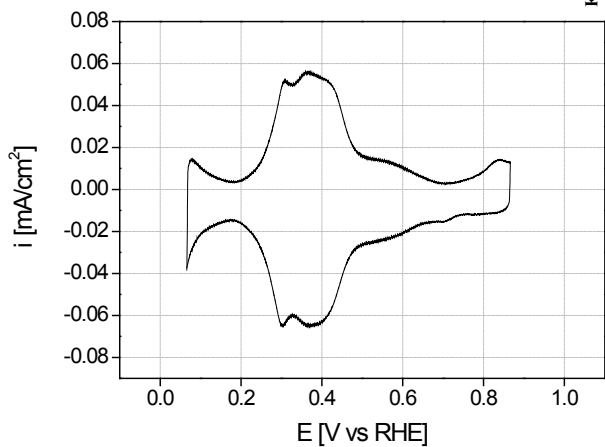
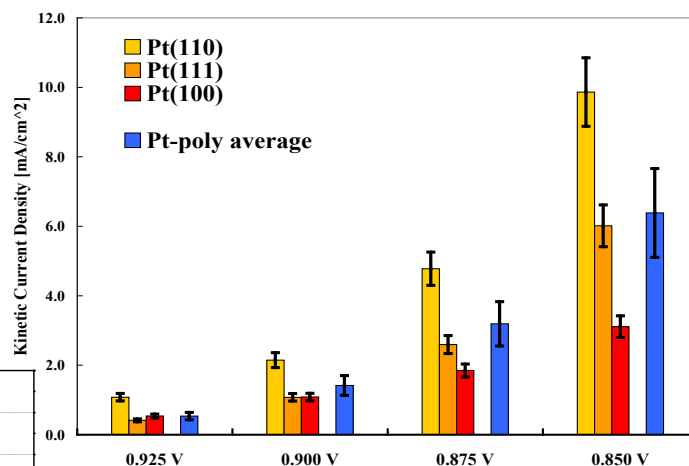
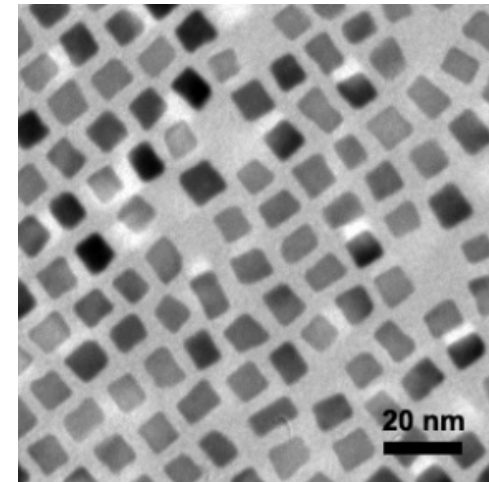
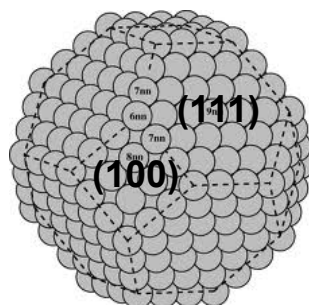
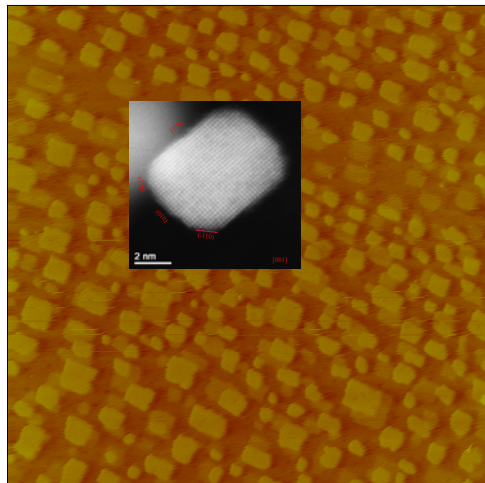
2) Size distribution: 2-15 nm

3) Composition: Pt, C

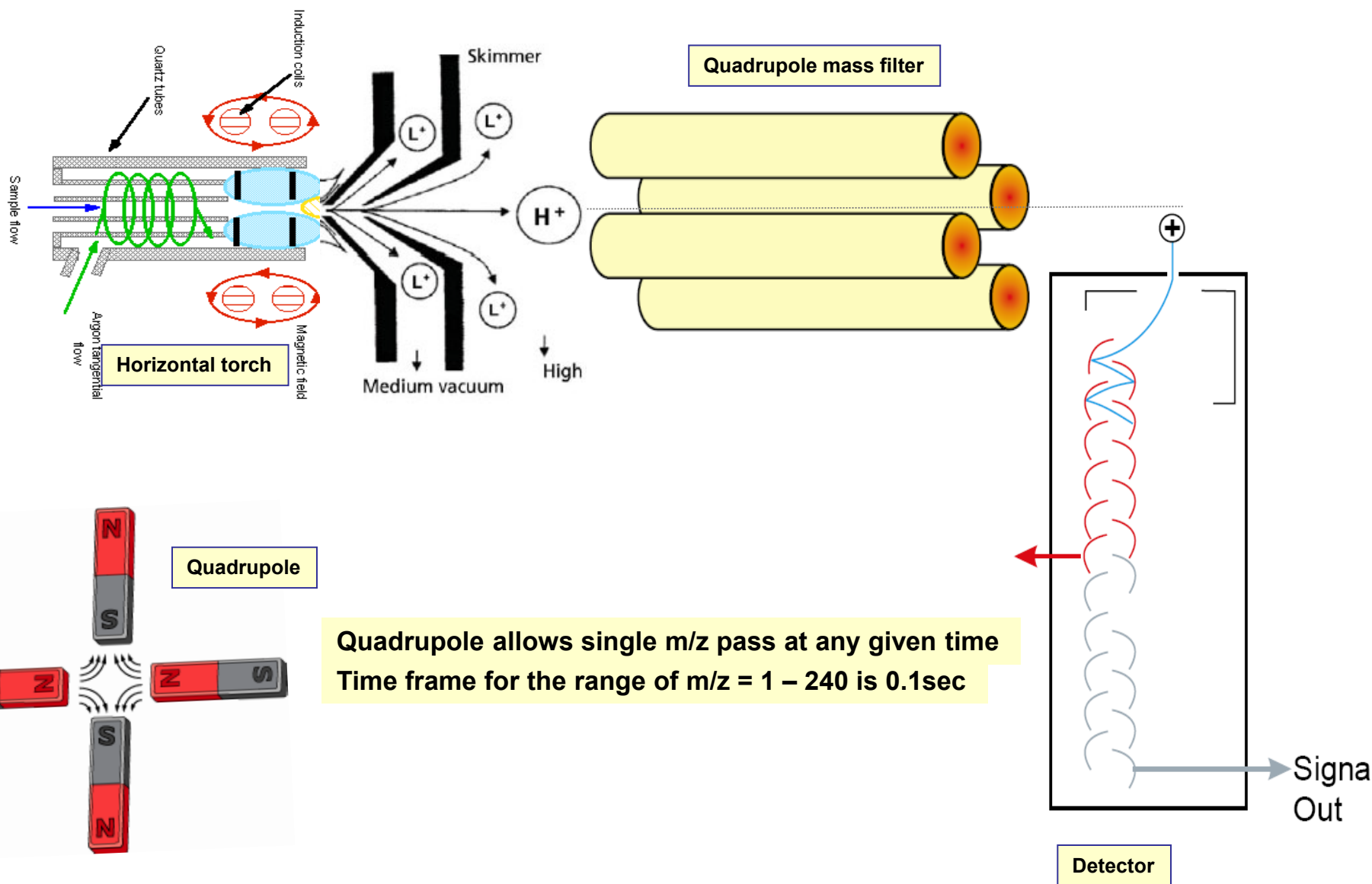
4) Side Orientation: [111], [100]



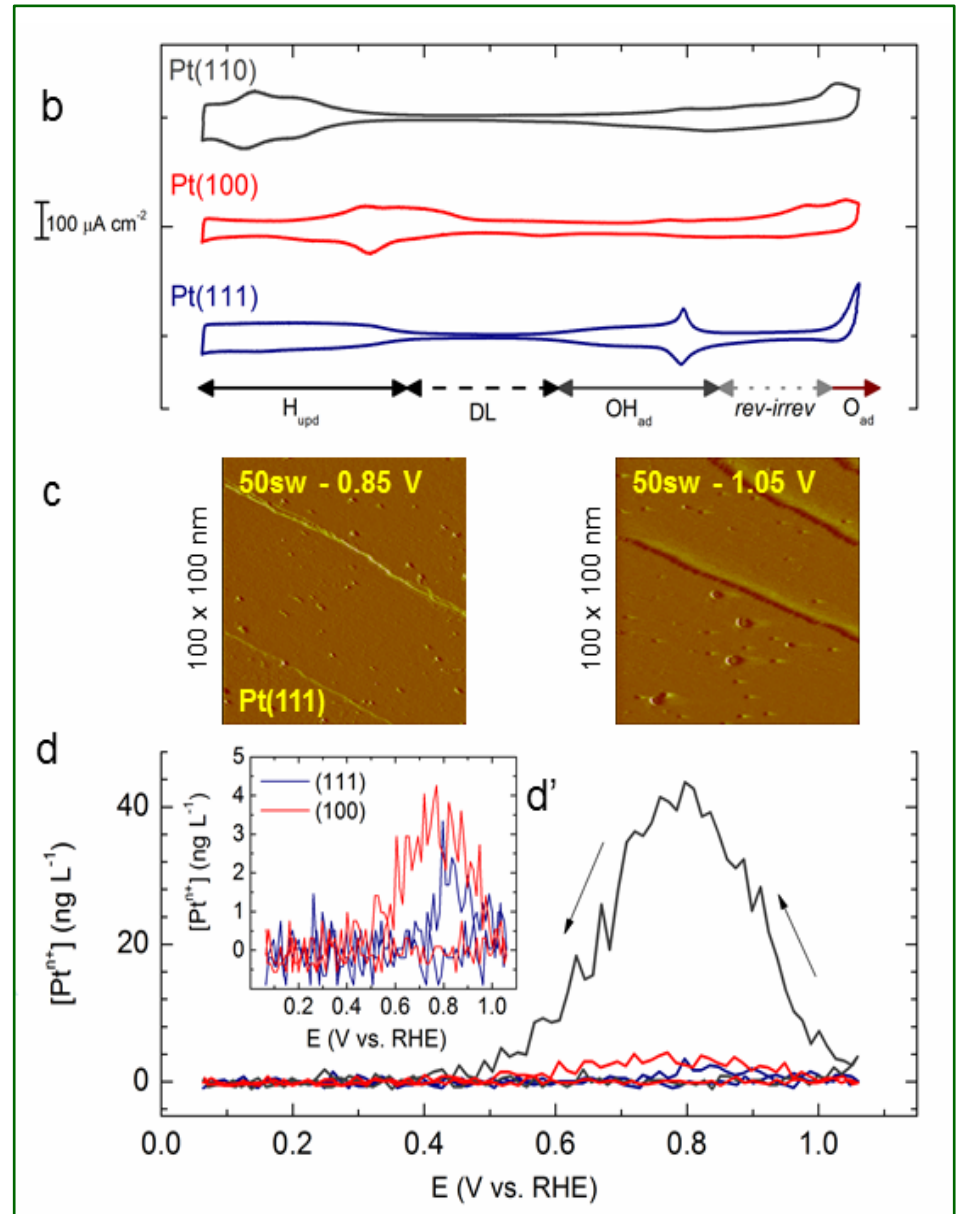
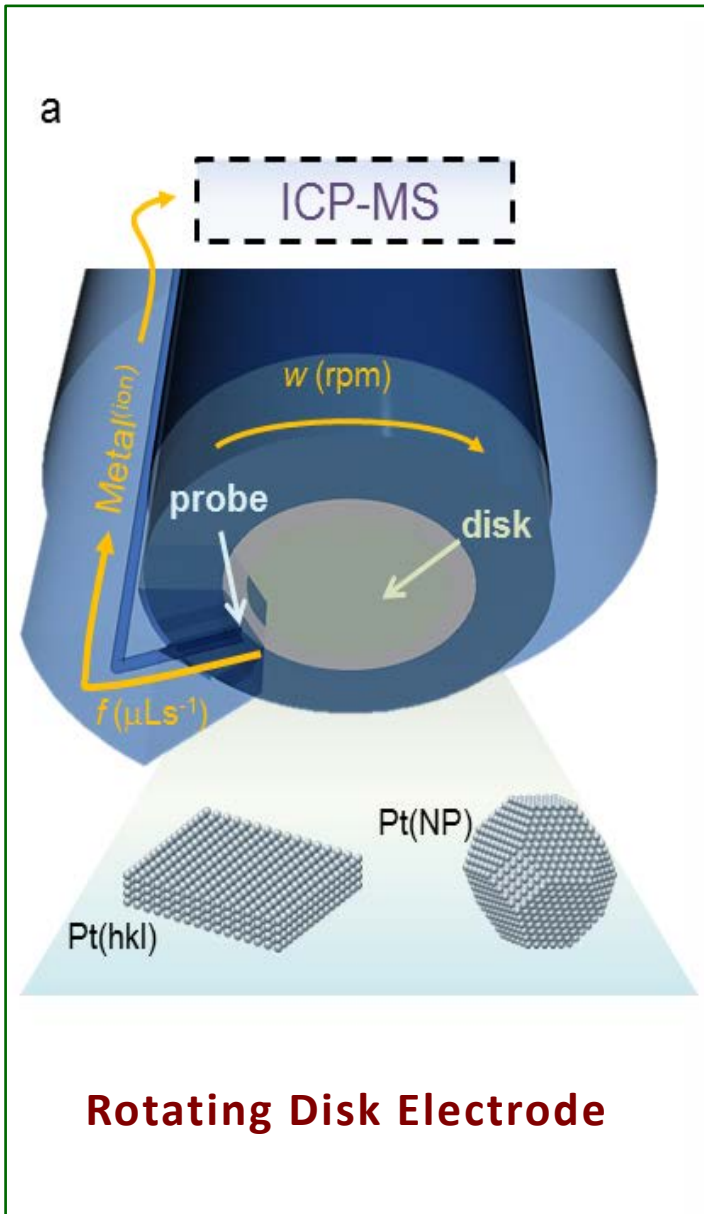
# APPROACH: Well-Defined Systems (ext & nano)



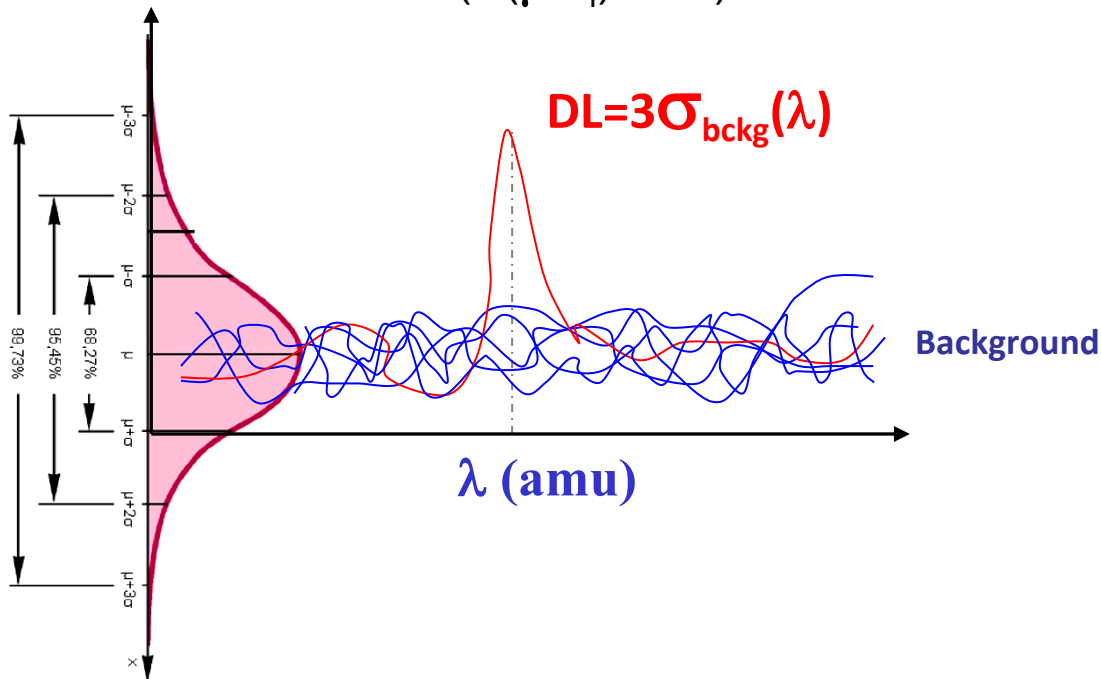
# ICP-MS: Principle of Operation



# RDE/ICP-MS: Pt(hkl)



Standard Deviation  $\sigma = (\sum(\mu - x_i)^2 / n - 1)^{1/2}$

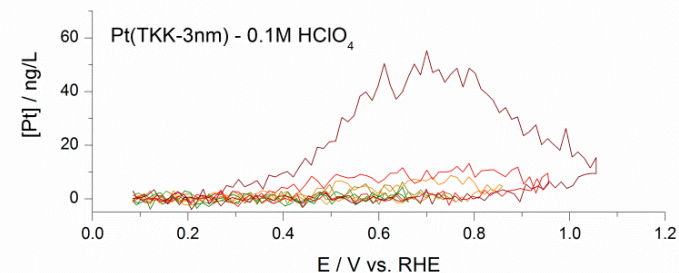
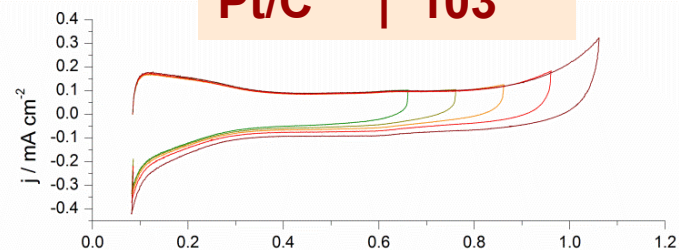


❑ Method detection limit (DL) is applied to blank sample prepared with all analytical steps related to given methodology, since each step is potential error source

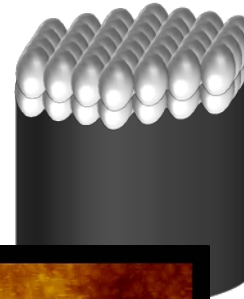
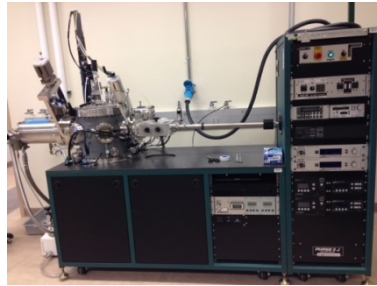
❑ Limit of quantification (LOQ) is 3 times DL

Total Pt loss over one potential cycle up to 1.05 V for distinct Pt surface morphologies, indicating the stability trend follows the coordination number of the surface sites

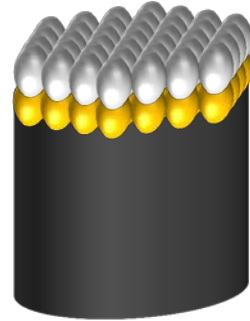
Pt Surface	Dissolved Pt per cycle [ $\mu\text{ML}$ ]
Pt(111)	2
Pt(100)	7
Pt(110)	83
Pt-poly	36
<b>Pt/C</b>	<b>103*</b>



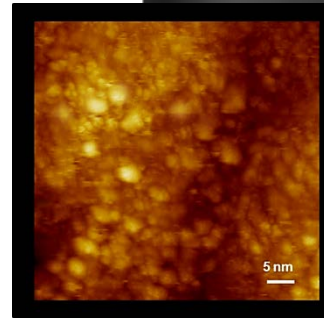
# In-Situ RDE / ICP-MS: Pt/C, Pt and Pt/Au Well-Defined Surfaces



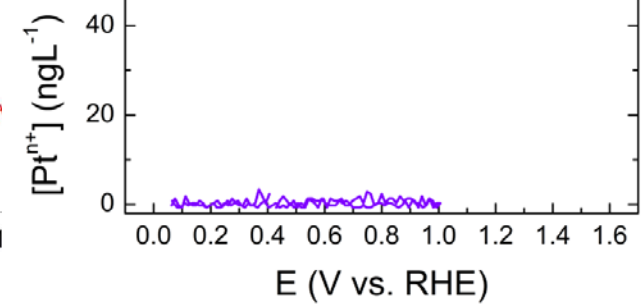
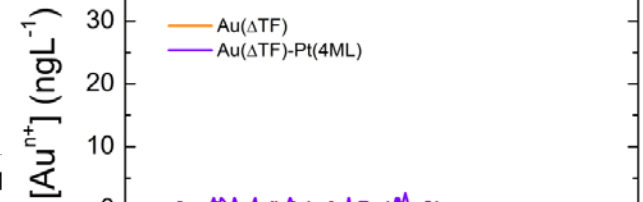
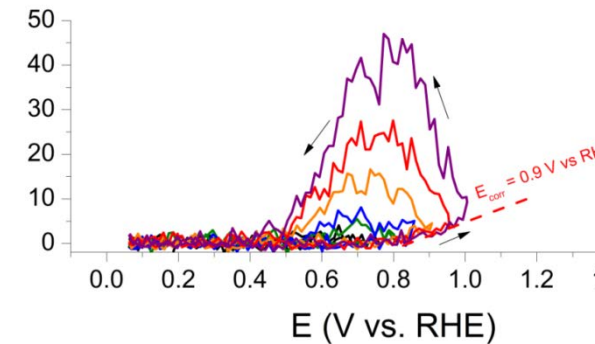
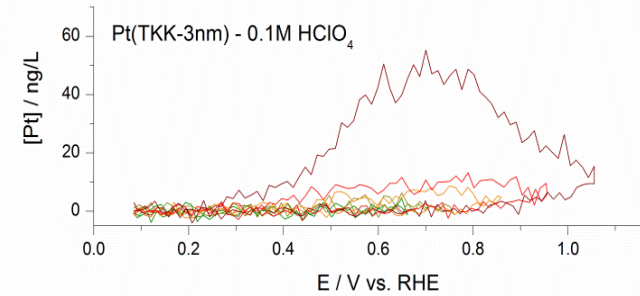
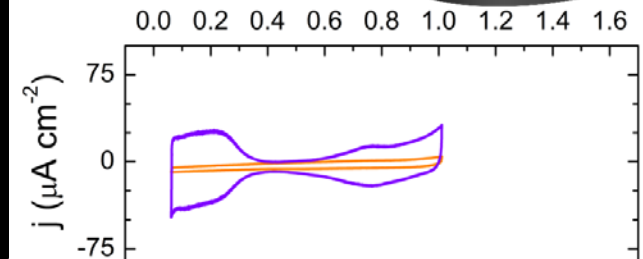
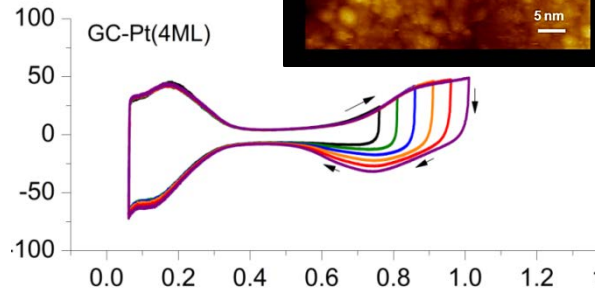
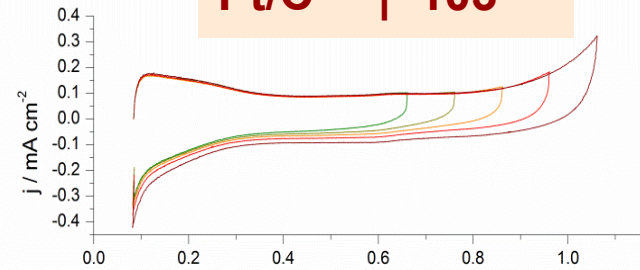
GC-Au-Pt(4ML)



GC-Pt(4ML)

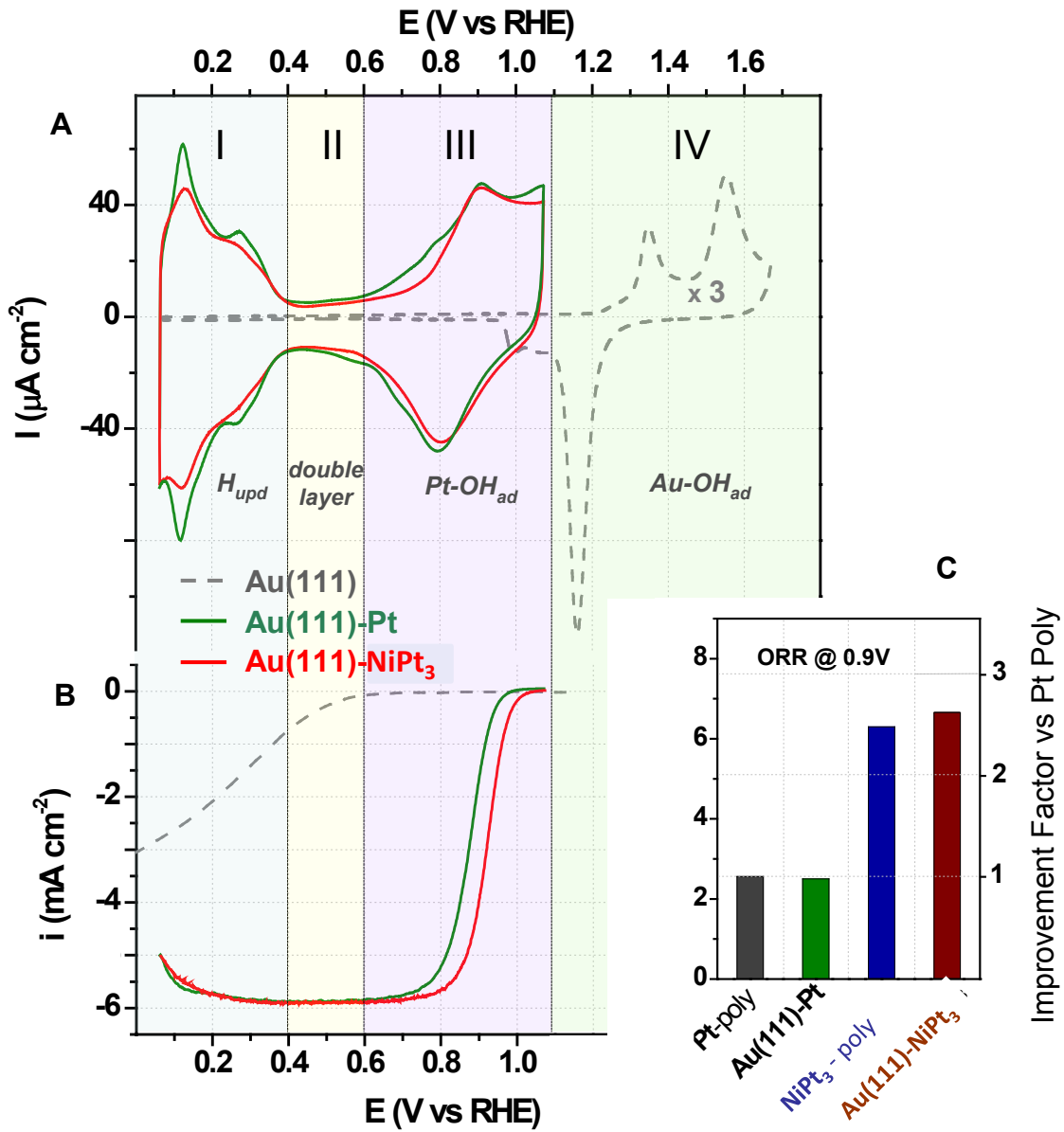


Pt/C | 103\*

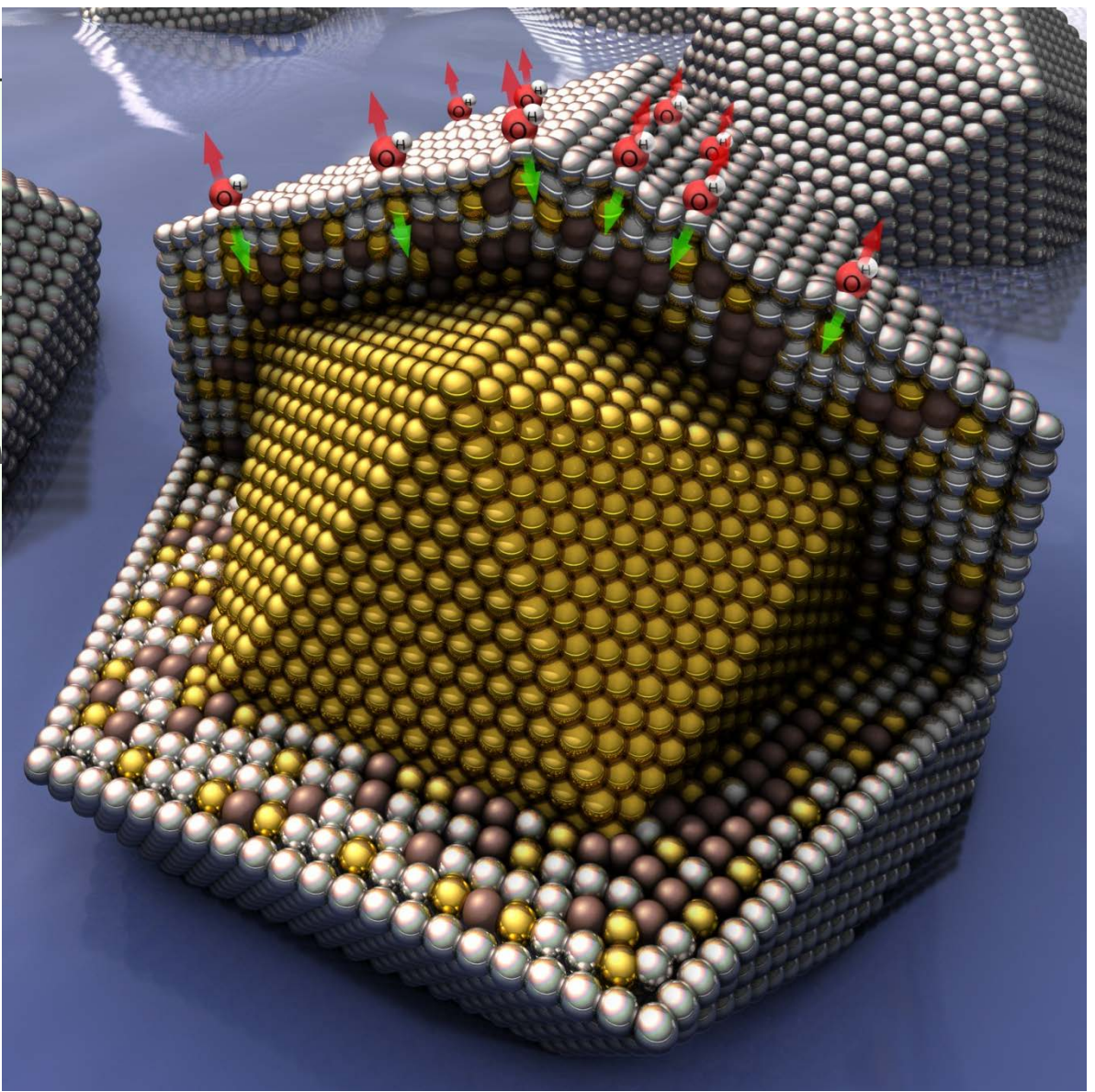
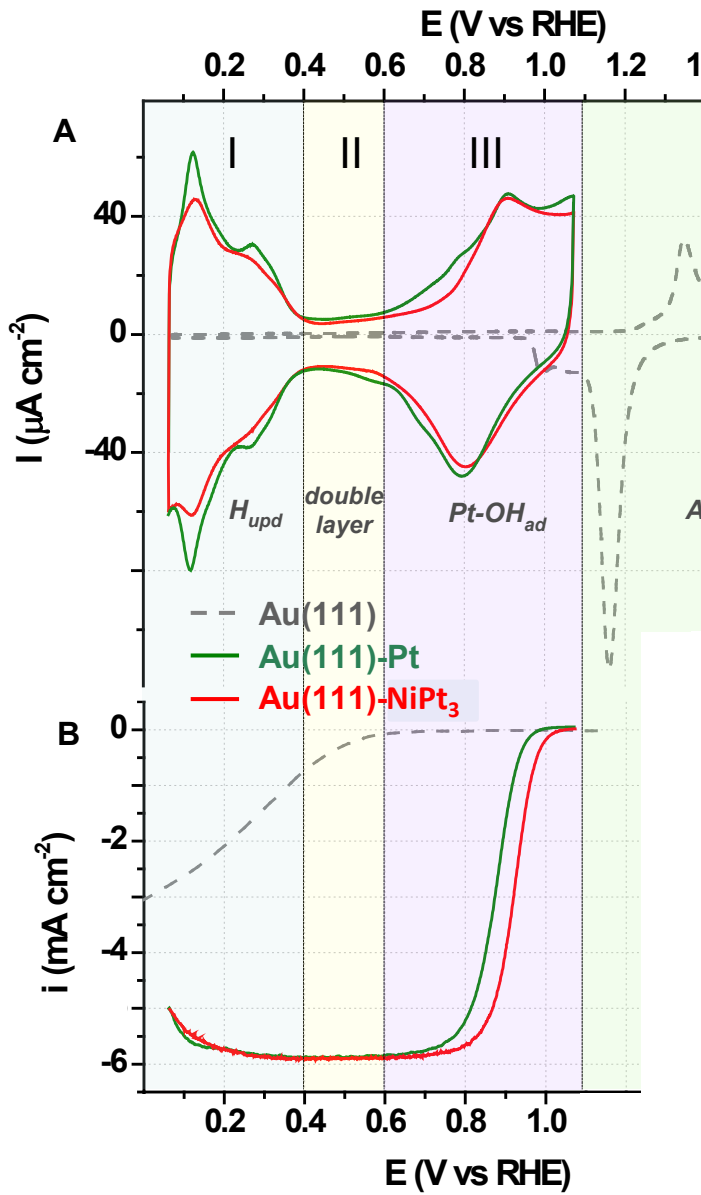




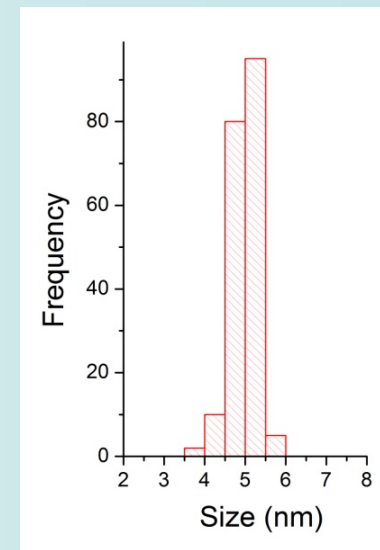
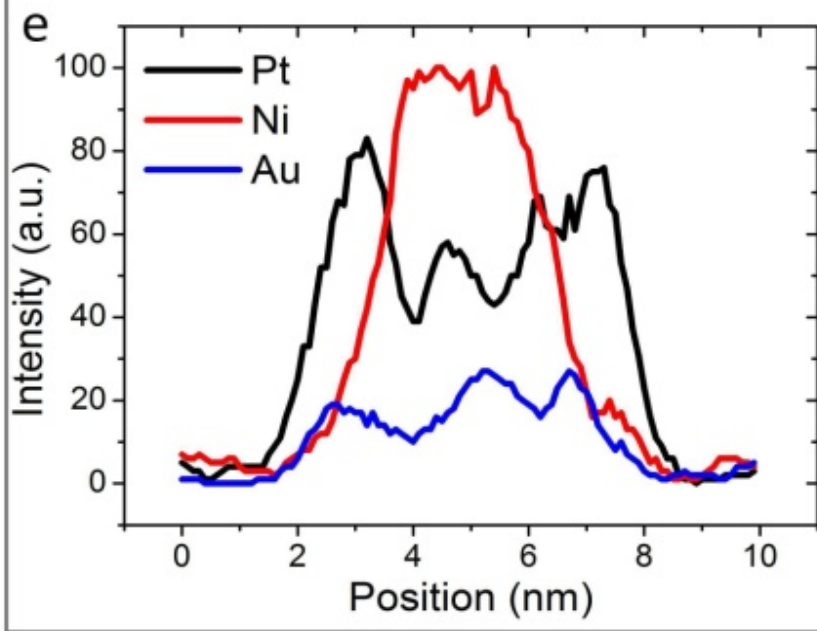
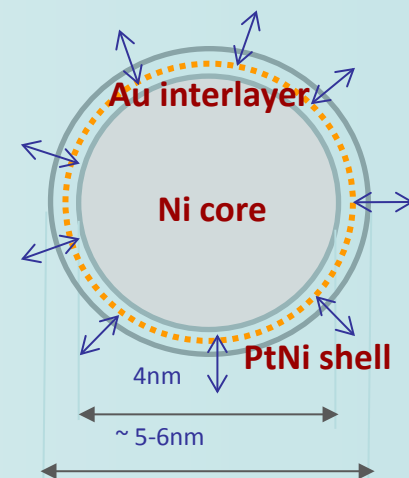
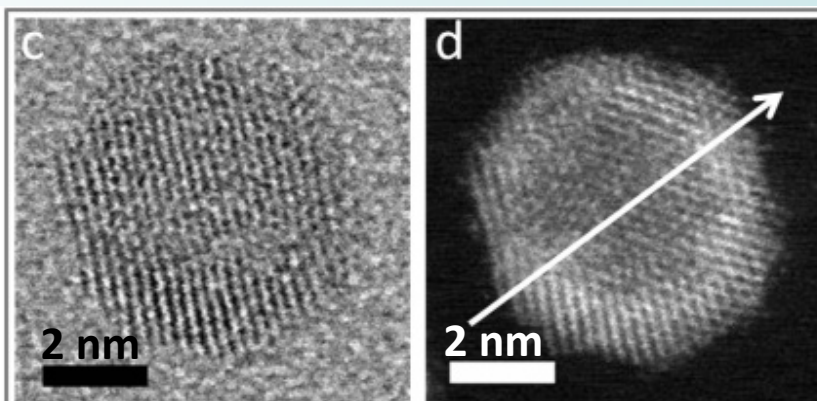
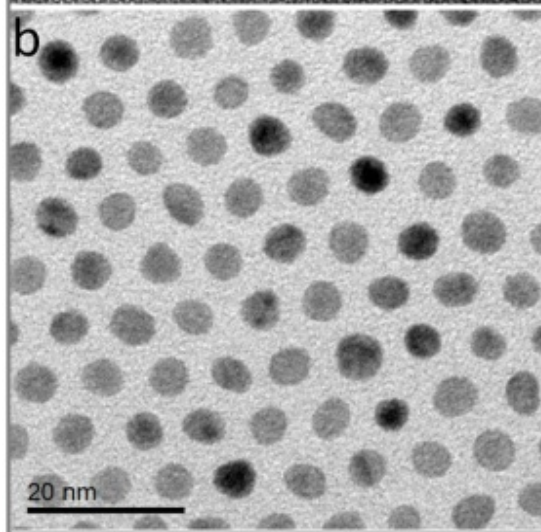
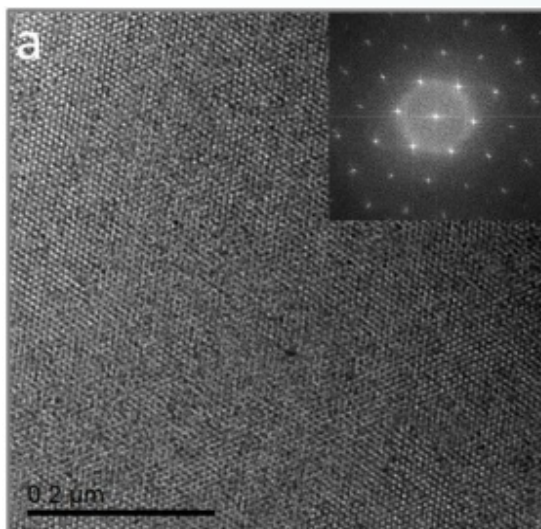
# DURABLE NPs: Core-Interlayer-Shell Particles



# DURABLE NPs: Core-Interlayer-Shell Particles

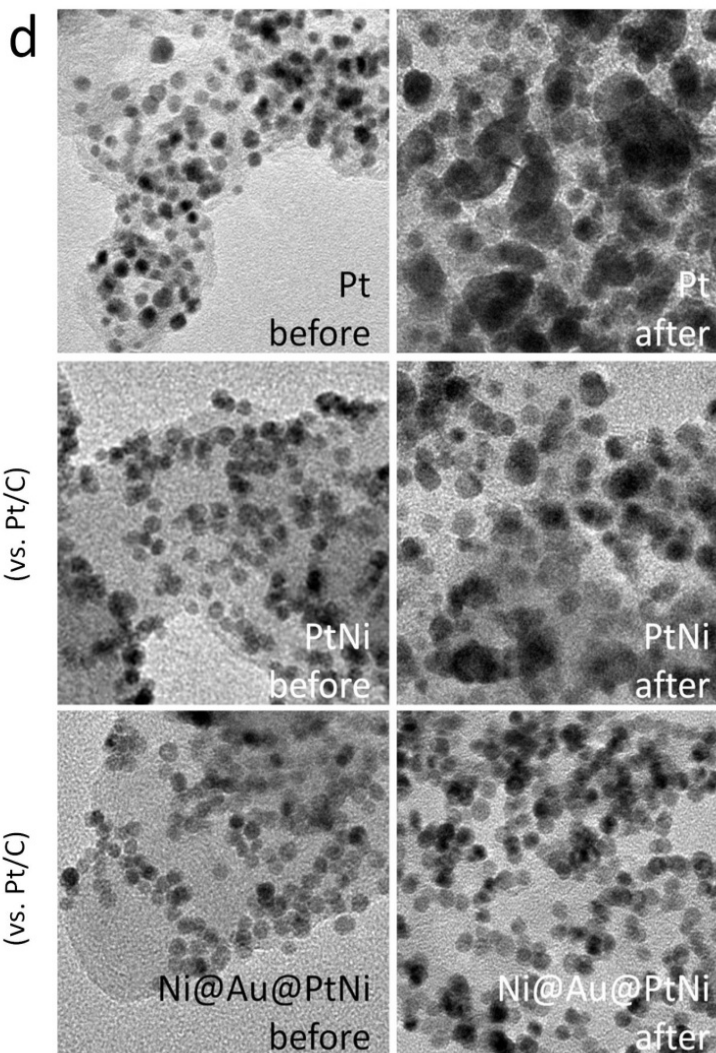
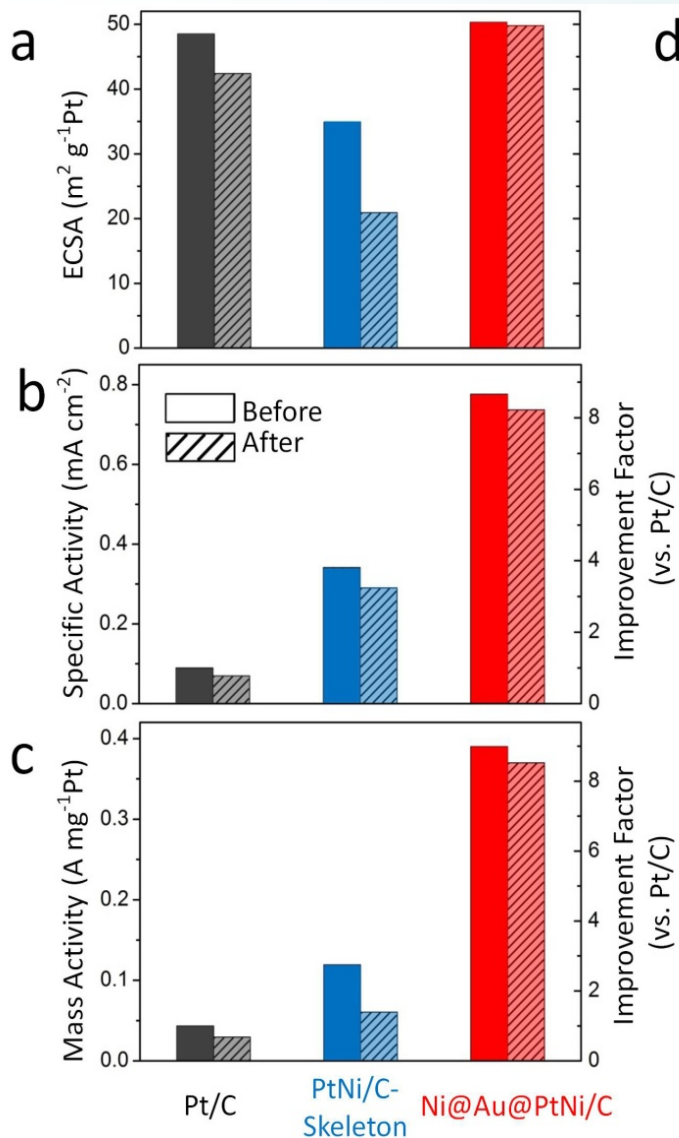


# Compositional Profile: *Core/Interlayer/Shell Electro*catalysts

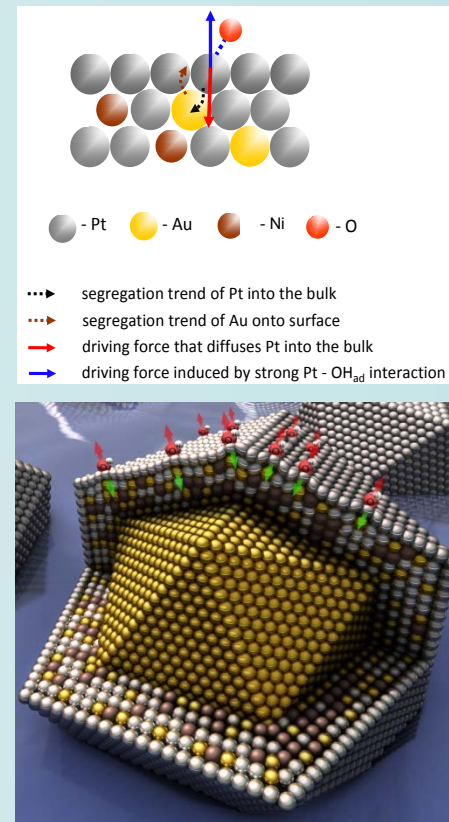


Monodisperse , Core/Interlayer/Shell NPs: Ni core / Au interlayer / PtNi shell

# Durable ORR Catalysts: Core/Shell NPs with Au Interlayer



## Stabilization mechanism



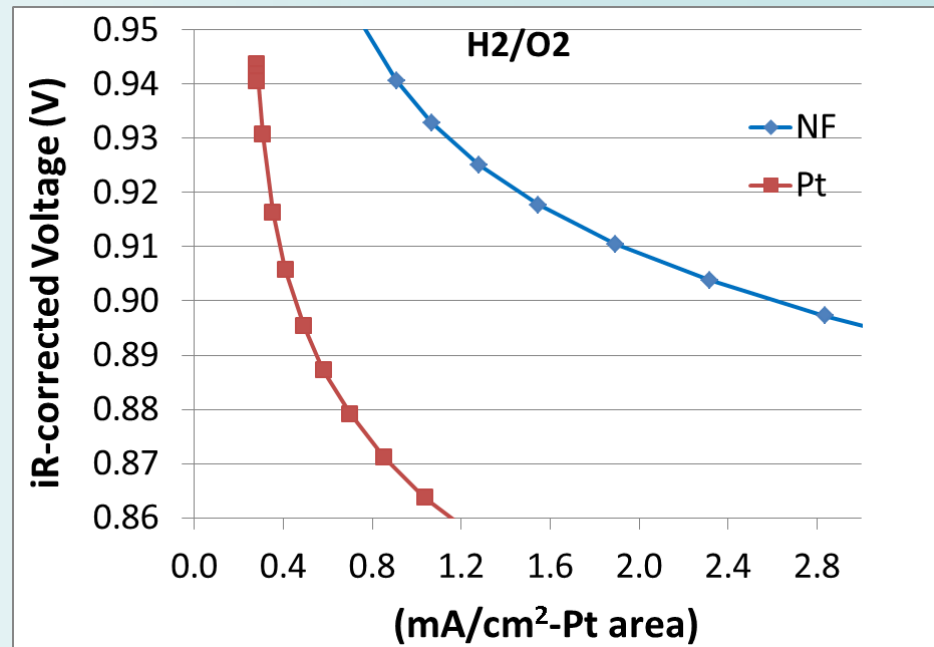
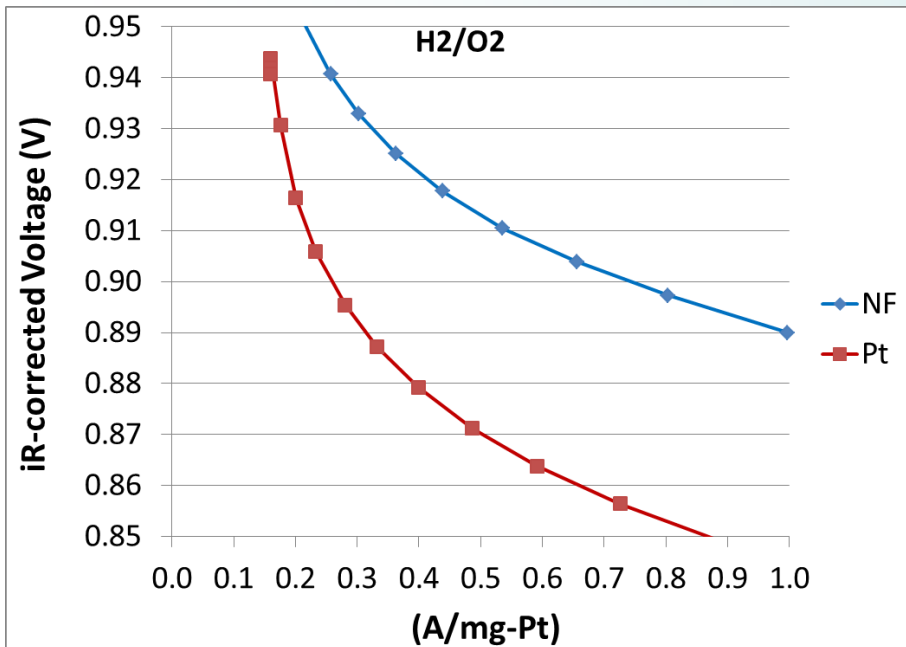
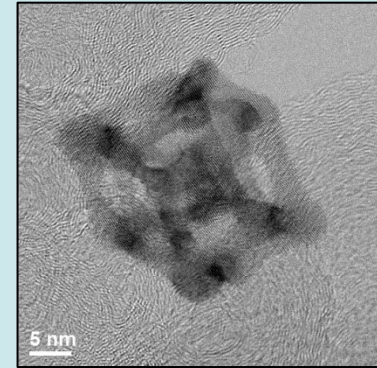
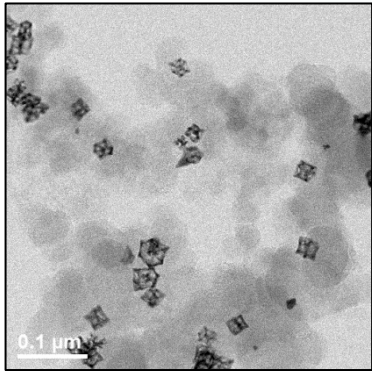
# Durable Systems: PtNi Nanoframes in MEA

in collaboration with Debbie Myers, ANL - CSE

Nanoframes in 5cm<sup>2</sup> MEA ANL and ORNL

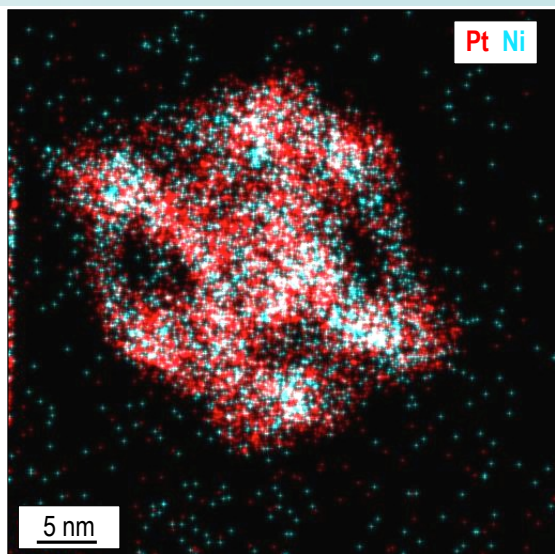
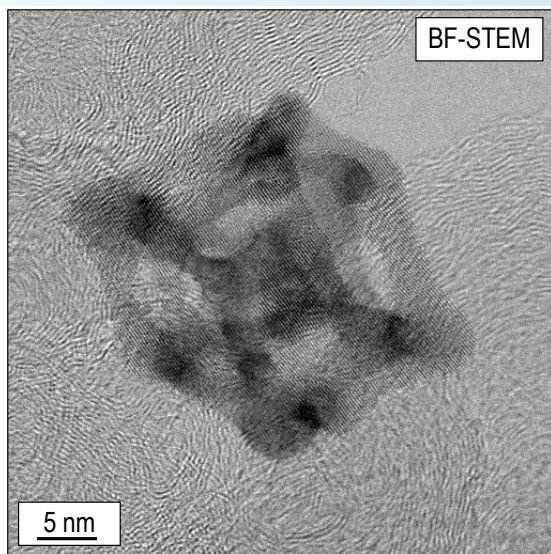
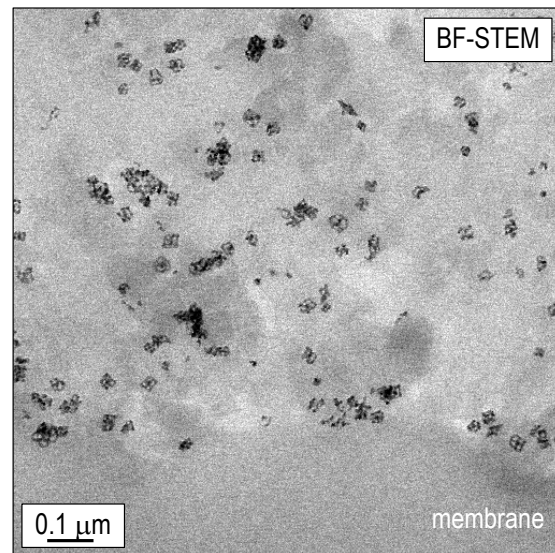
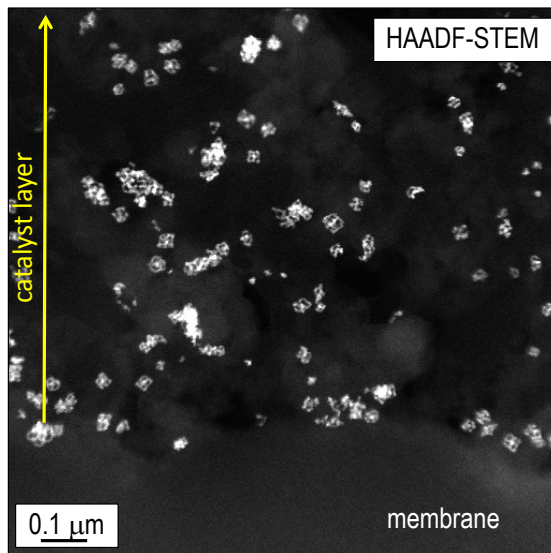
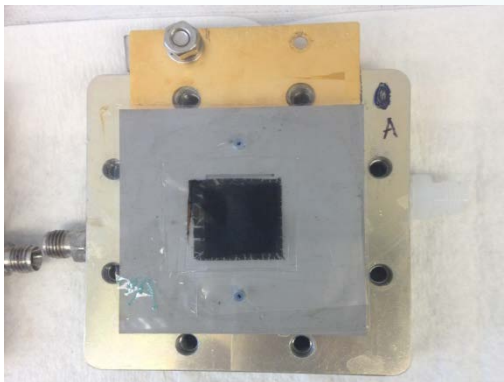
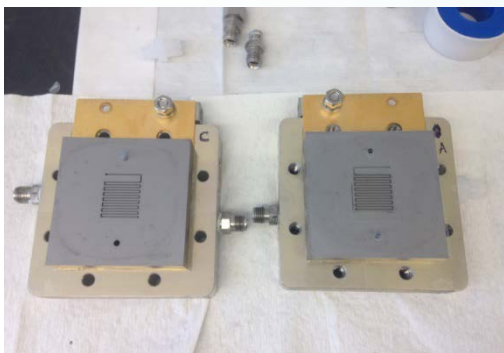
Cathode Loading: 0.035 mg-Pt/cm<sup>2</sup>, I/C = 0.8  
H<sub>2</sub>/O<sub>2</sub>, 80°C, 150 kPa(abs), 100%RH

**ORR Activity @ 0.9V:** Mass Activity x3.5 Specific Activity x6.5  
TKK 20 wt%Pt/C: 0.22 A/mg-Pt 0.39 mA/cm<sup>2</sup>-Pt  
PtNi Nanoframes: 0.76 A/mg-Pt 2.60 mA/cm<sup>2</sup>-Pt



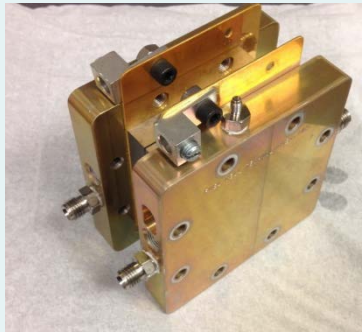
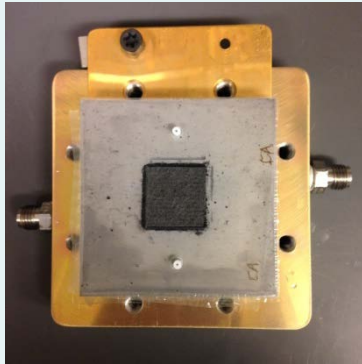
# Durable Systems: PtNi Nanoframes (before and after)

Nanoframes in 5cm<sup>2</sup> MEA ANL and ORNL



# Durable Systems: PtNi with Multilayered Pt-Skin Surfaces

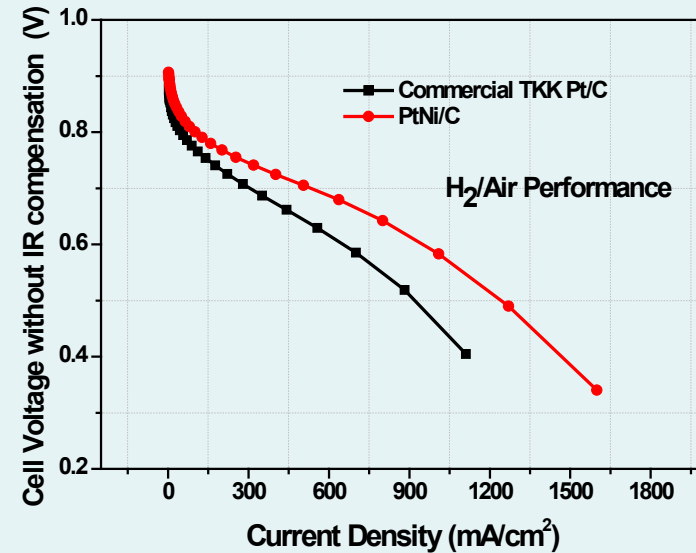
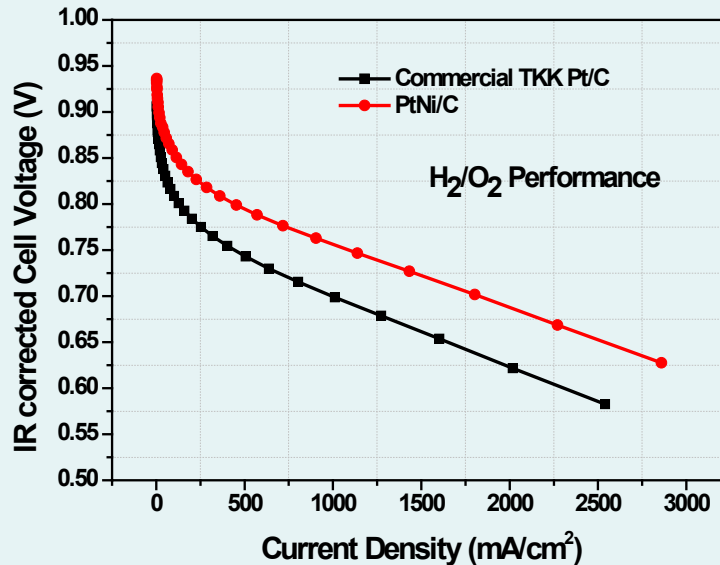
in collaboration with Debbie Myers, ANL - CSE



Cathode Loading: 0.046 mg-Pt/cm<sup>2</sup>  
I/C = 1, H<sub>2</sub>/O<sub>2</sub> (or Air),  
80°C, 150 kPa(abs), 100%RH

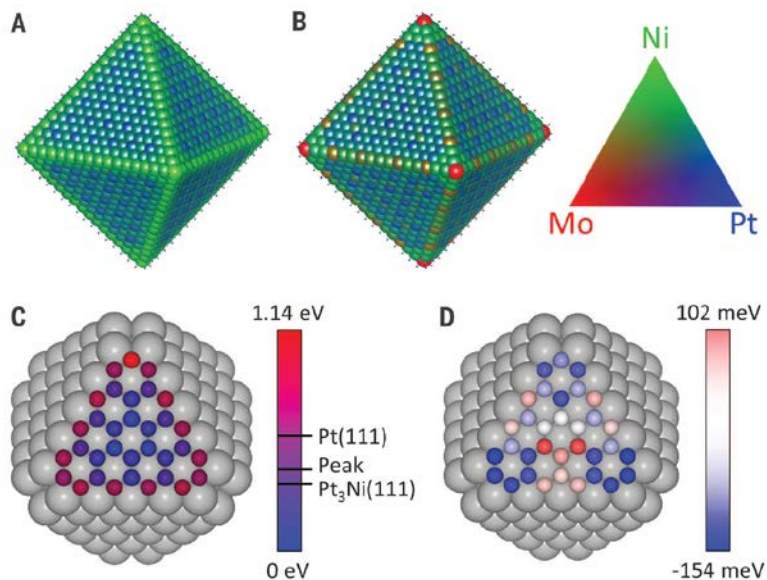
TKK 20 wt%Pt/C

PtNi 16.7 wt%Pt/C

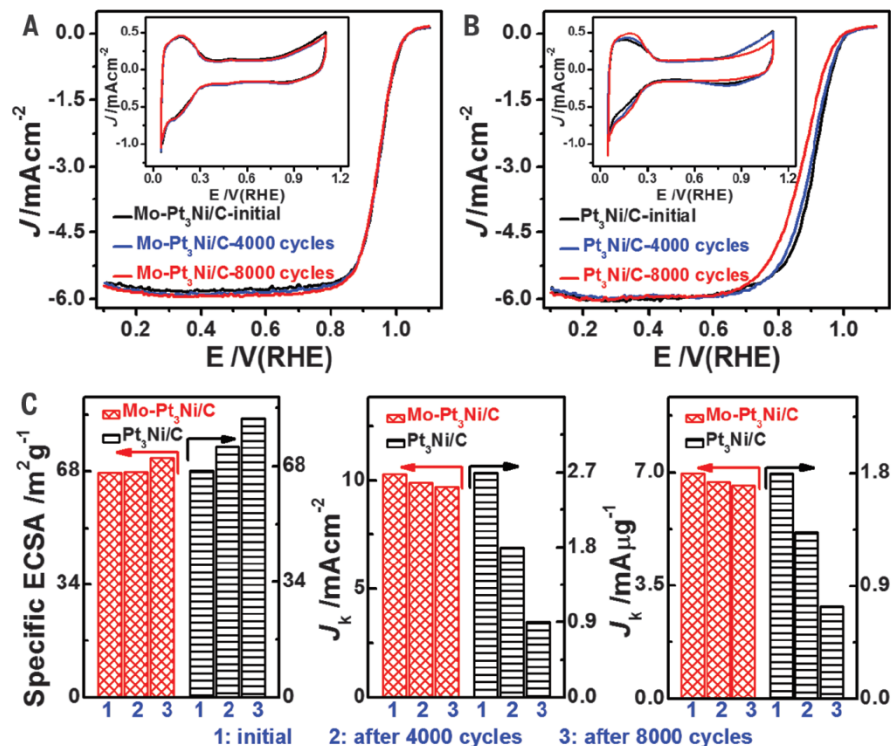
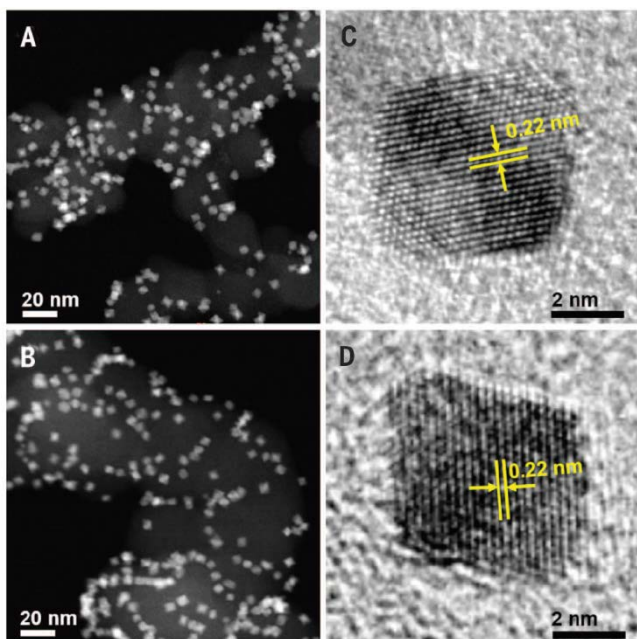


	Units	PtNi	TKK Pt
Pt loading	mg <sub>PGM</sub> /cm <sup>2</sup> <sub>geo</sub>	0.045	0.045
Mass Activity (H <sub>2</sub> -O <sub>2</sub> )	A/mg <sub>PGM</sub> @ 0.9 V <sub>iR-free</sub>	0.60	0.27
Specific Activity (H <sub>2</sub> -O <sub>2</sub> )	mA/cm <sup>2</sup> <sub>PGM</sub> @ 0.9 V <sub>iR-free</sub>	1.85	0.39
MEA performance (H <sub>2</sub> -Air)	mA/cm <sup>2</sup> @ 0.8 V	101	47
ECSA	m <sup>2</sup> /g <sub>PGM</sub>	35.10	52.5

# TM doped Pt<sub>3</sub>Ni Octahedra



Catalyst	ECSA (m <sup>2</sup> /g <sub>Pt</sub> )	Based on H <sub>upd</sub>				Based on CO stripping			
		Specific activity (mA/cm <sup>2</sup> )		Mass activity (A/mg <sub>Pt</sub> )		Specific activity (mA/cm <sup>2</sup> )		ECSA (m <sup>2</sup> /g <sub>Pt</sub> )	
		@ 0.9 V	@ 0.95 V	@ 0.9 V	@ 0.95 V	@ 0.9 V	@ 0.95 V	@ 0.9 V	@ 0.95 V
This work	Mo-Pt <sub>3</sub> Ni/C	67.7	10.3	2.08	6.98	1.41	83.9	8.2	1.74
This work	Pt <sub>3</sub> Ni/C	66.6	2.7	0.55	1.80	0.37	81.9	2.2	0.45
(53)	PtNi/C	50	3.14	NA	1.45	NA	NA	NA	NA
(24)	PtNi/C	48	3.8	NA	1.65	NA	NA	NA	NA
(21)	PtNi <sub>2.5</sub> /C	21	NA	NA	3.3	NA	31	NA	NA
(28)	Pt <sub>3</sub> Ni/C nanoframes	NA	NA	NA	5.7	0.97	NA	NA	1.48

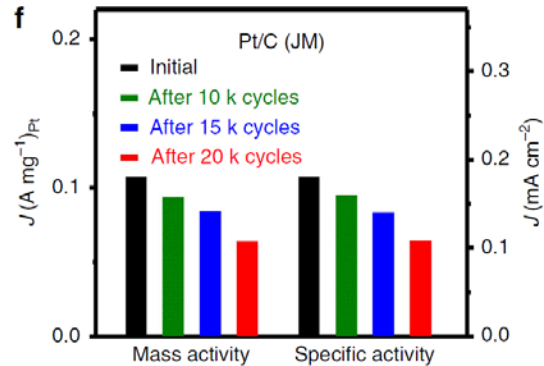
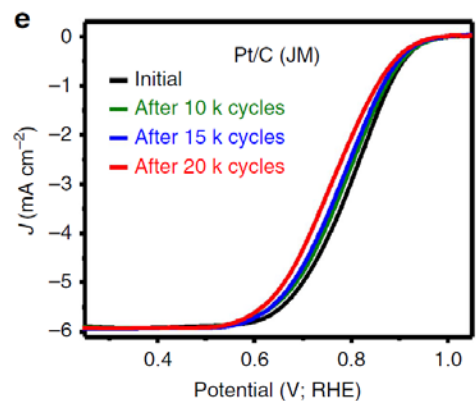
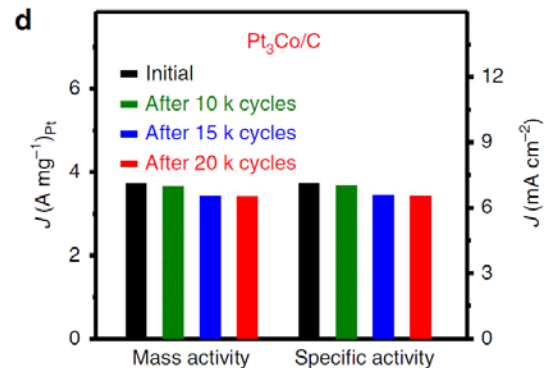
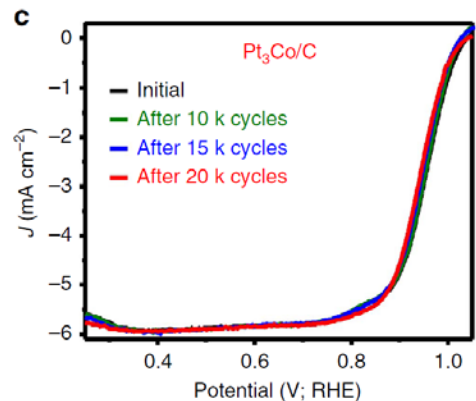
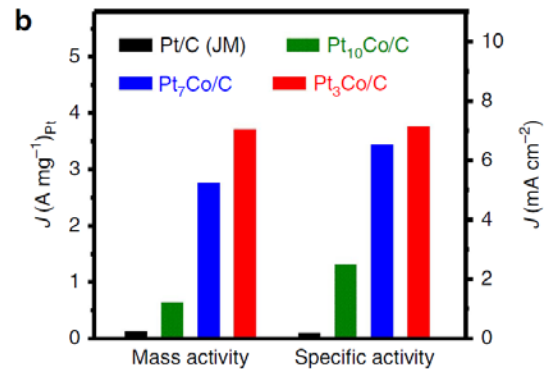
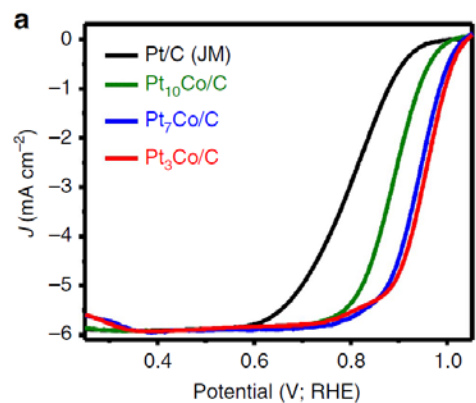
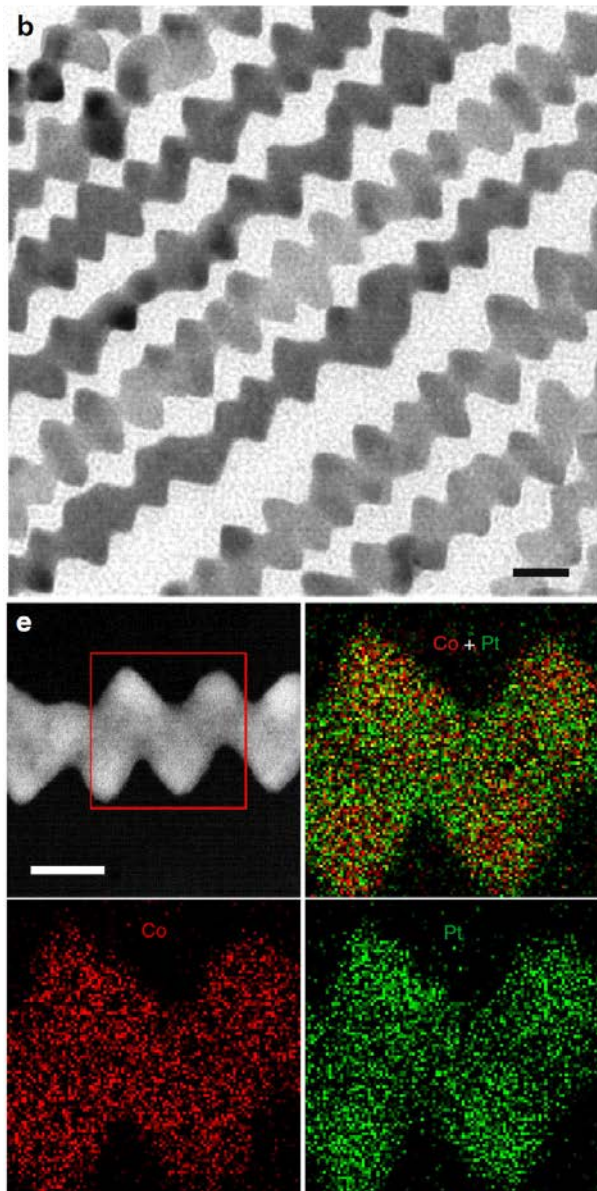


SA and MA over 70-fold vs. Pt/C

Huang et al. Science, 348 (2015) 1230

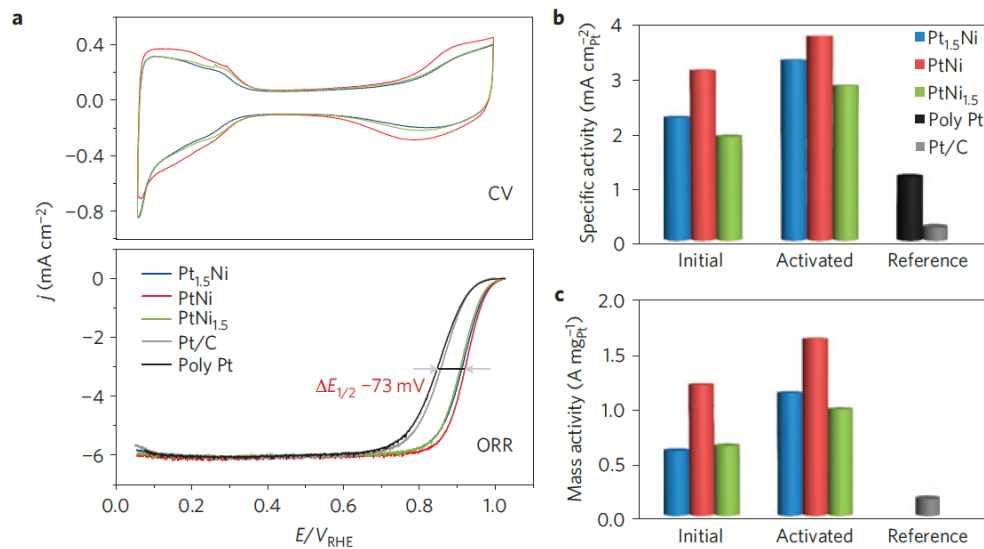
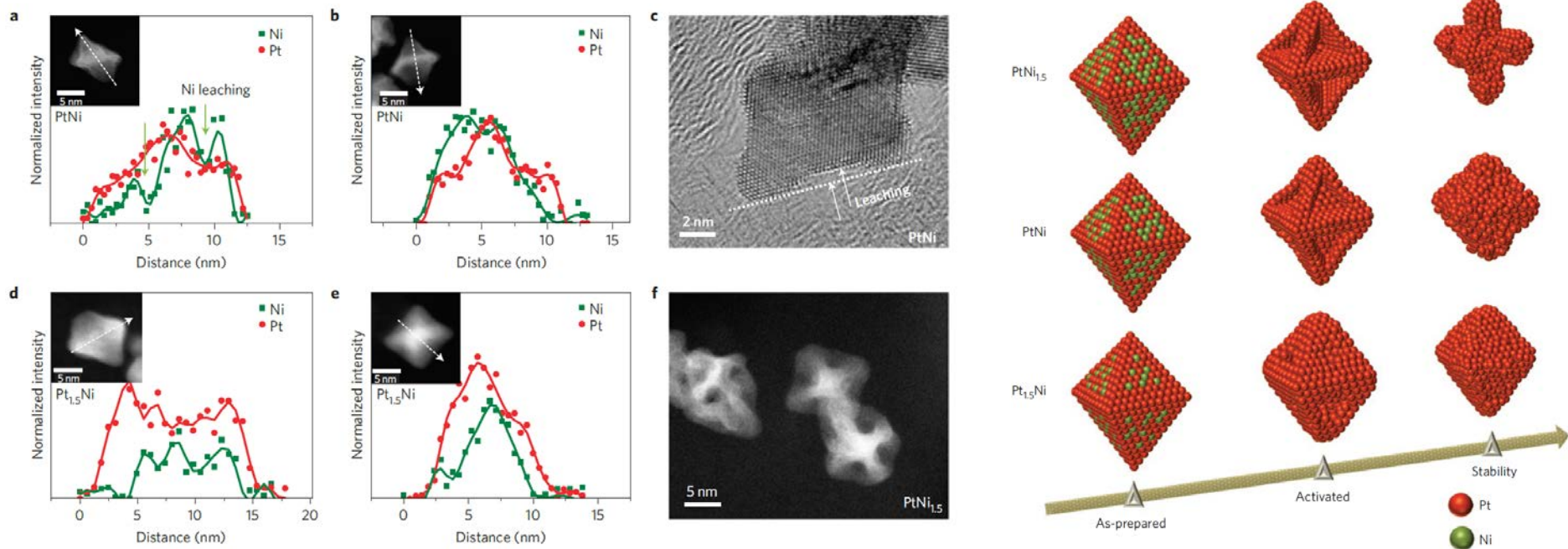


# Hierarchical PtCo Nanowires



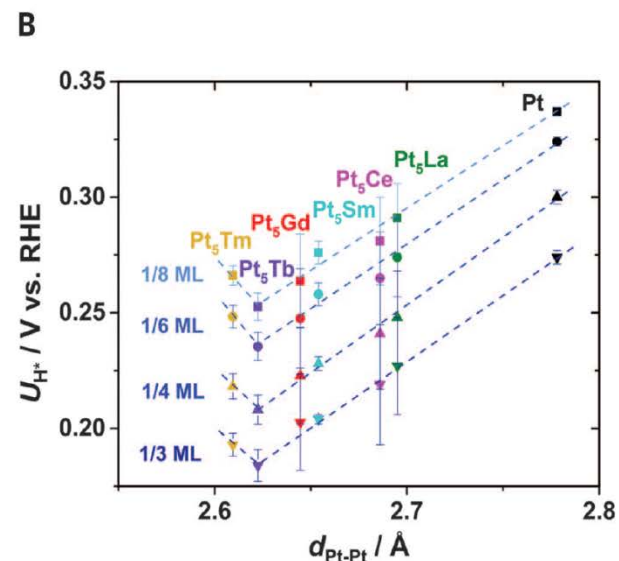
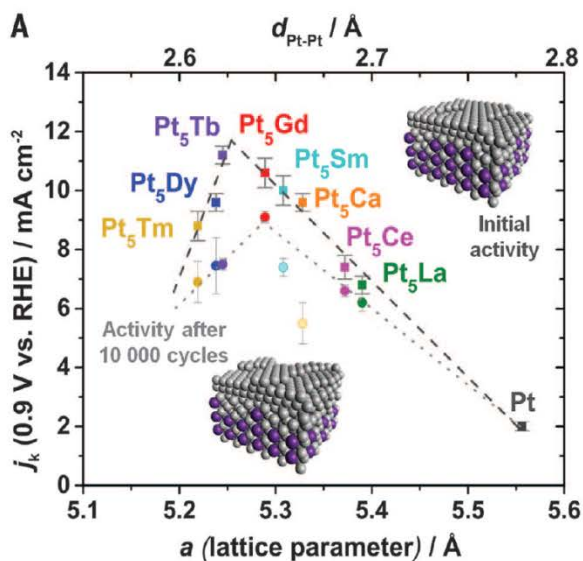
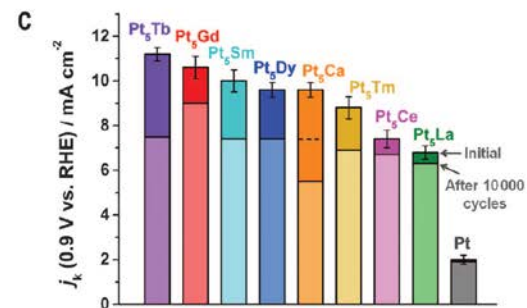
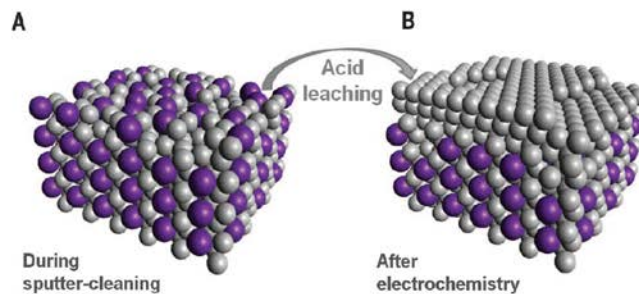
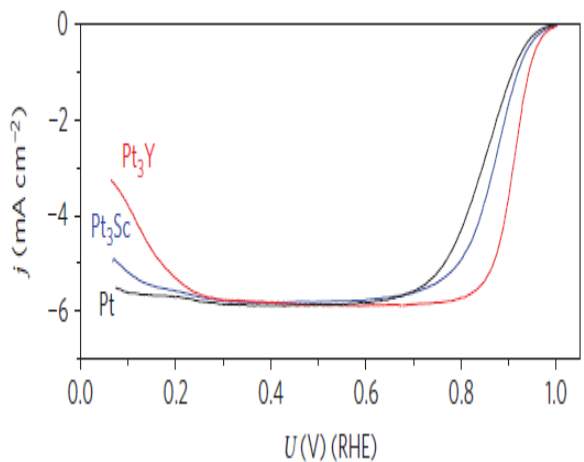
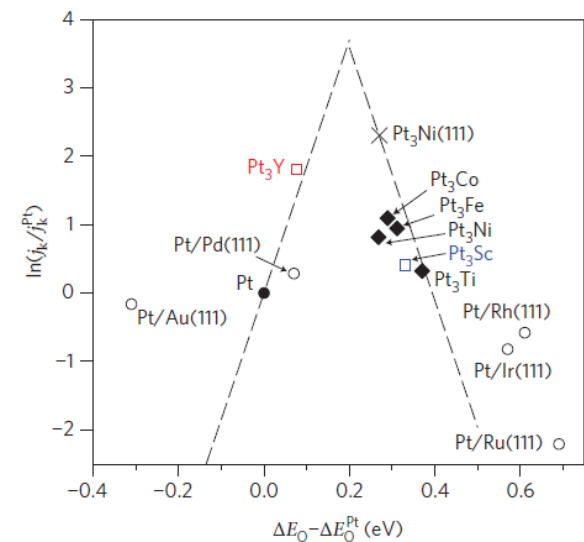
SA and MA over 30-fold vs. Pt/C

# Dealloying of PtNi octahedrons



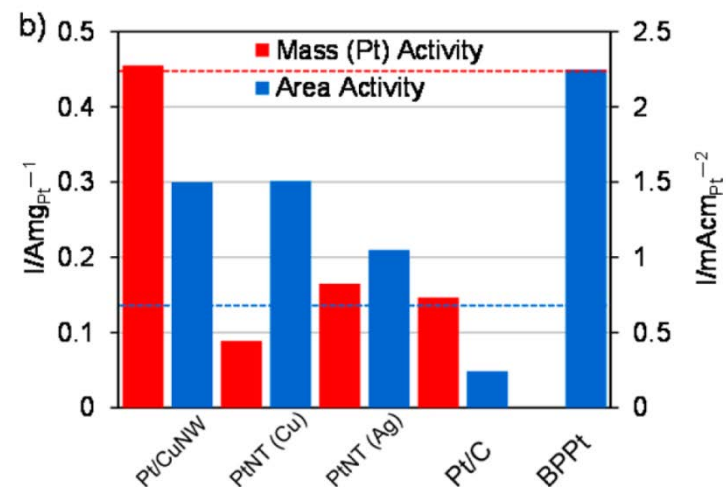
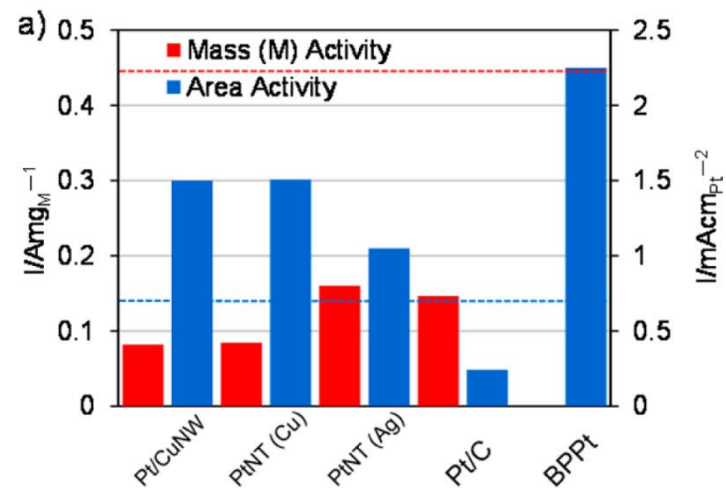
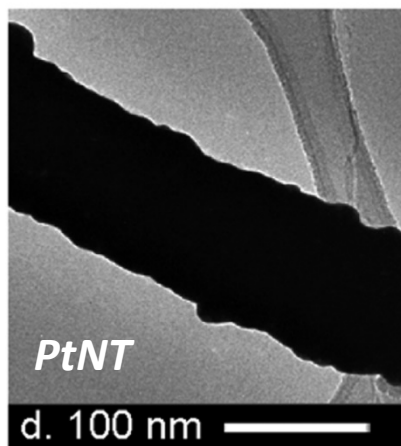
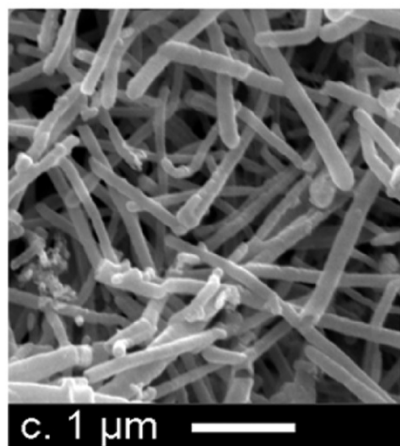
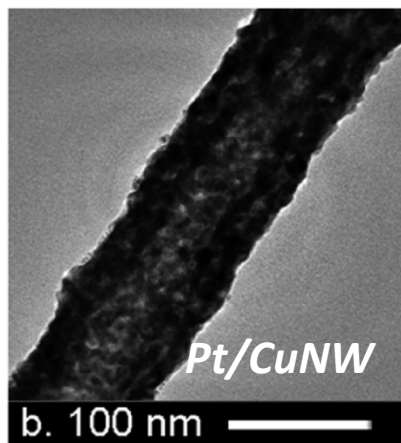
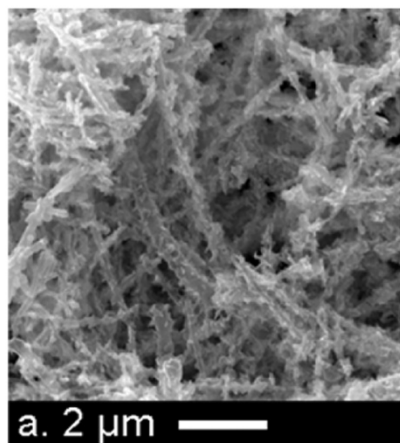
SA and MA over 10-fold vs. Pt/C

# Alloying Pt with Rare Earth Elements



**SA over 6-fold vs. Pt/C**

# Pt/CuNW and PtNT



SA and MA over 3-fold vs. Pt/C

# BNL: Electrocatalyst Development

## Approach

Increasing Pt monolayer activity and stability,  
and reducing the PGM content

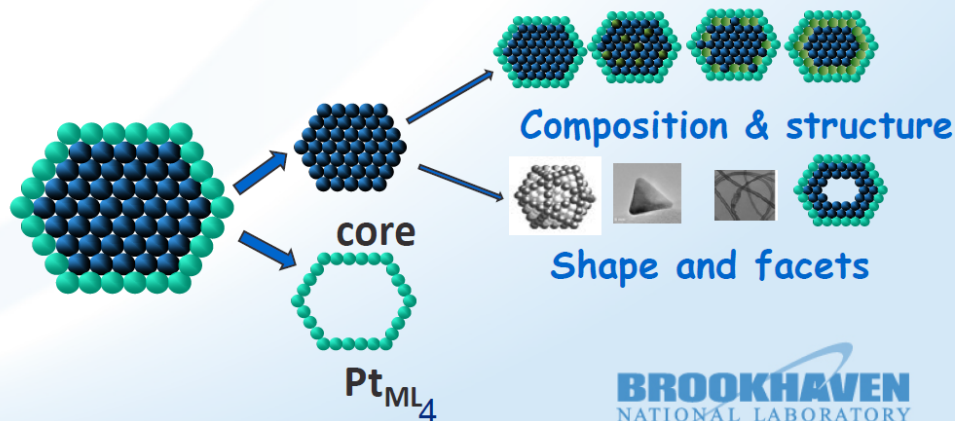
by

- Reducing oxygen binding energy
- Decreasing the number of low-coordination atoms
- Compressing the top layer of atoms
- Forming moderately compressed (111) facets
- Increasing stability of cores

accomplished via

- Surface contraction (induced by core, hollow core, subsurface ML, segregation),
- Improving Pt ML deposition process
- Designing the cores with specific structure, composition, shape and distribution
- Electrodeposition of cores and shells to maximize catalyst utilization
- Metal-, alloy- nanowires obtained in conventional syntheses
- Refractory metal alloys used as cores

tests, characterizations



\*J.X. Wang, H. Inada, L. Wu, Y. Zhu, Y. Choi, P. Liu,  
W.P. Zhou, R.R. Adzic, *J. Am. Chem. Soc.*, 131 (2009)  
17298, *JACS Select* #8

# Remaining Challenges and Barriers

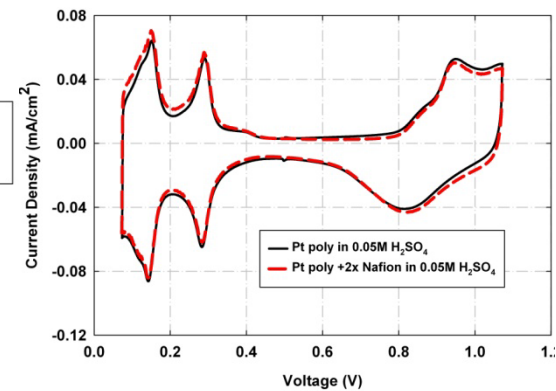
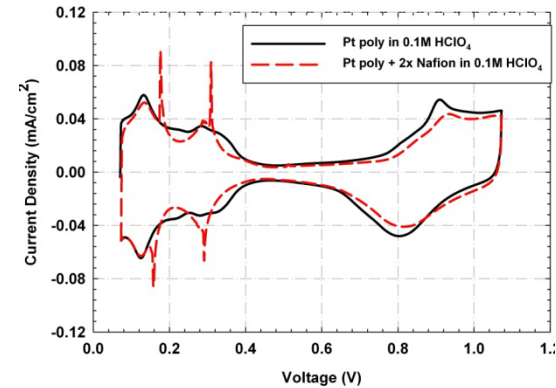
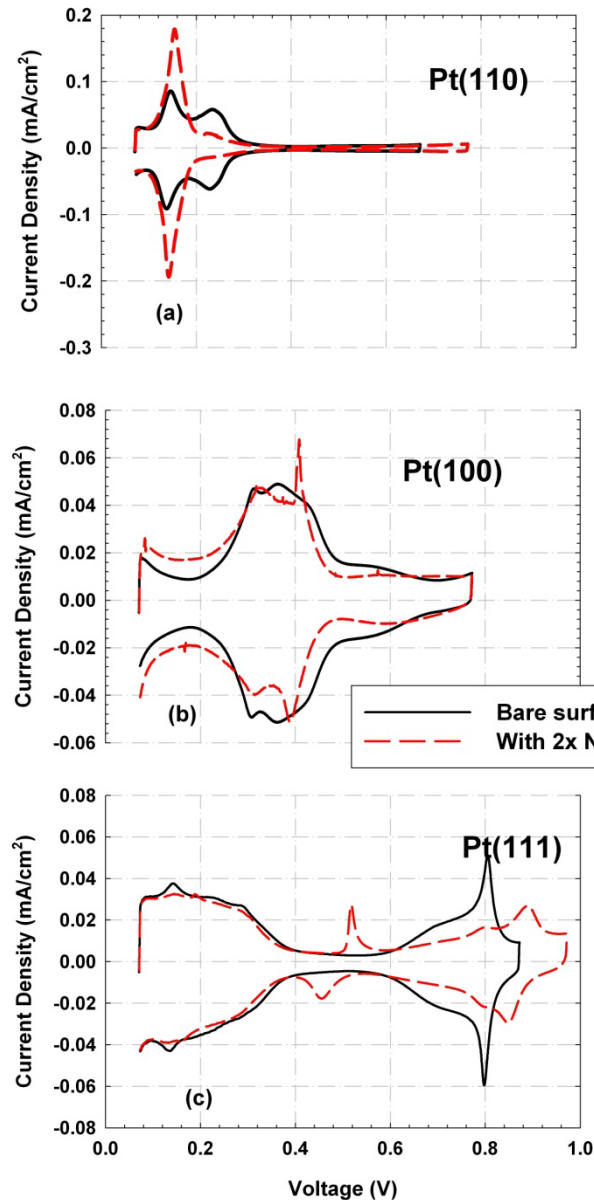
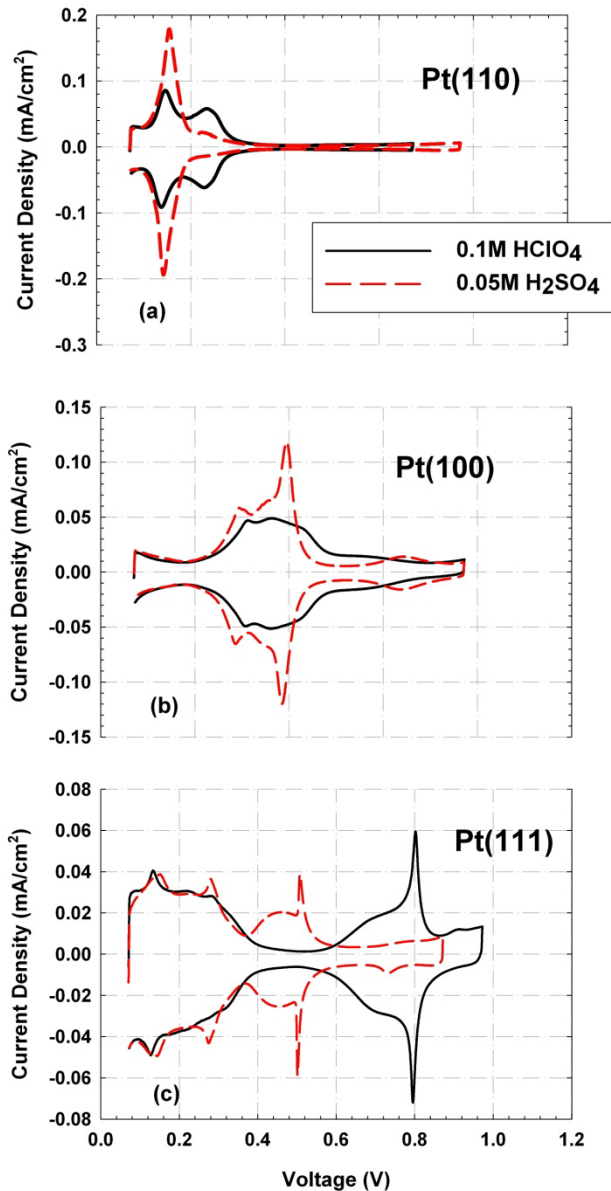
1) **Durability** of fuel cell stack (<40% activity loss)

2) **Cost** (total loading of PGM  $0.125 \text{ mg}_{\text{PGM}} / \text{cm}^2$ )

3) **Performance** (mass activity @ 0.9V  $0.44 \text{ A/mg}_{\text{Pt}}$ )

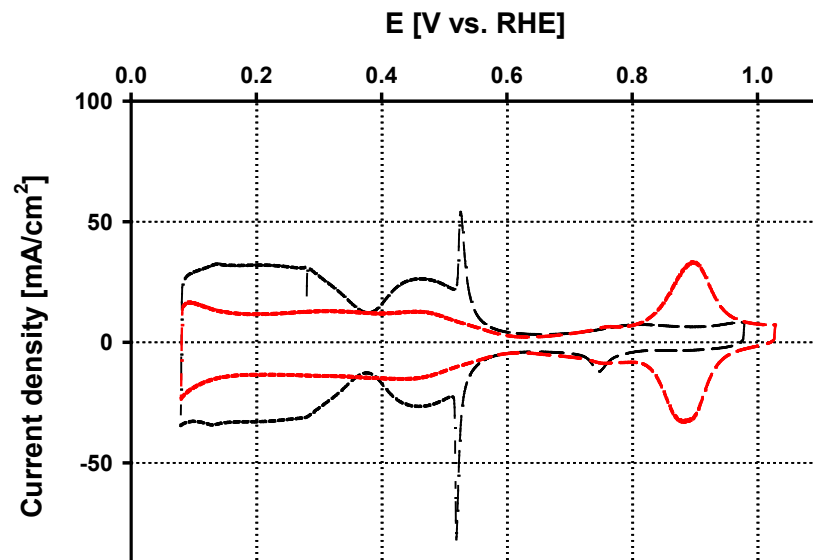
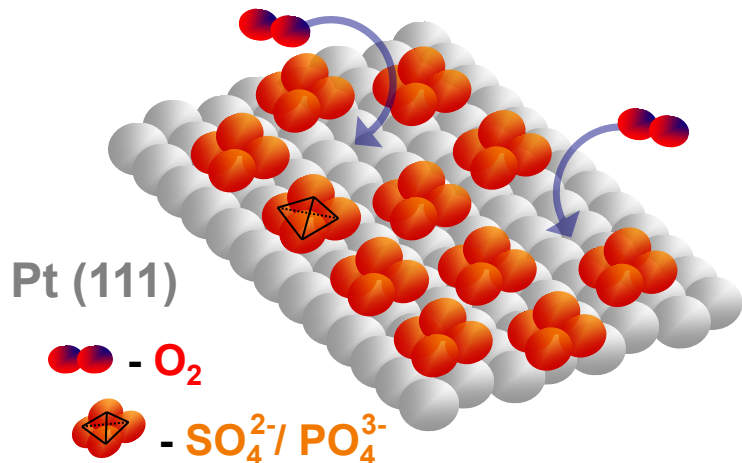
- **Differences** between RDE and MEA, surface chemistry, ionomer catalyst interactions
- **Temperature** effect on performance activity/durability
- **High current density** region needs improvements for MEA
- **Support** – catalyst interactions
- **Scale-up** process for the most advanced structures

# Pt(hkl) with Ionomer

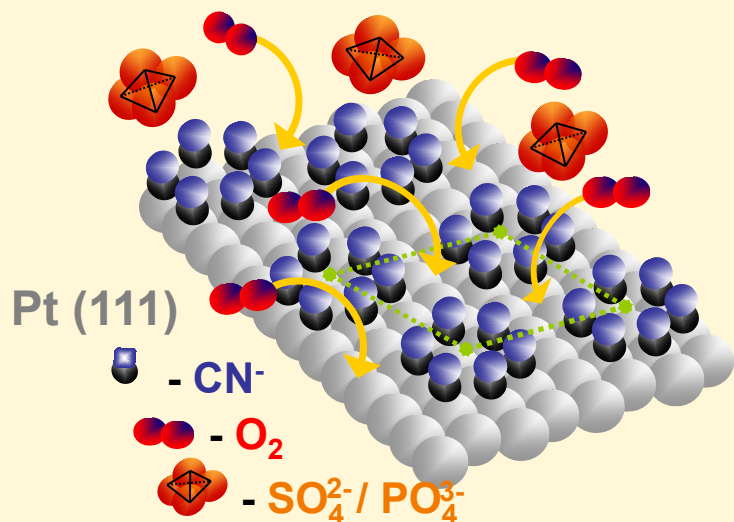


2x refers to the case of 10  $\mu$ l of solution (0.005% wt.) applied to the electrode. Thickness can then be calculated by using a dry density of 1.5 g/cm<sup>3</sup>

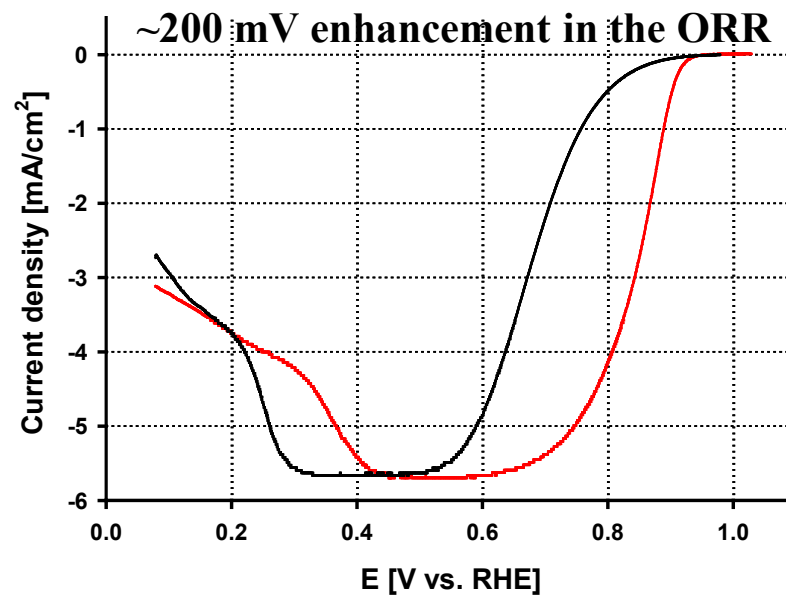
# Strongly Adsorbing Electrolytes: *Improving the ORR Rate*



Cyanide adlayer forms  $(2\sqrt{3} \times 2\sqrt{3})R30^\circ$  structure on Pt (111)  
 Itaya et al. J.Am.Chem.Soc. 118 (1996) 393

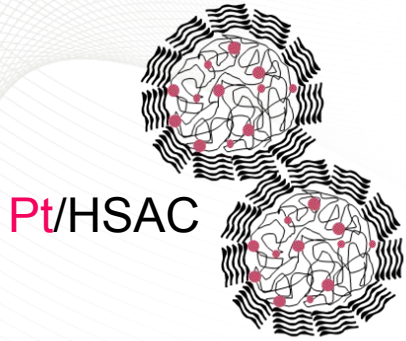


Cyanides prevent the adsorption of sulfates/phosphates

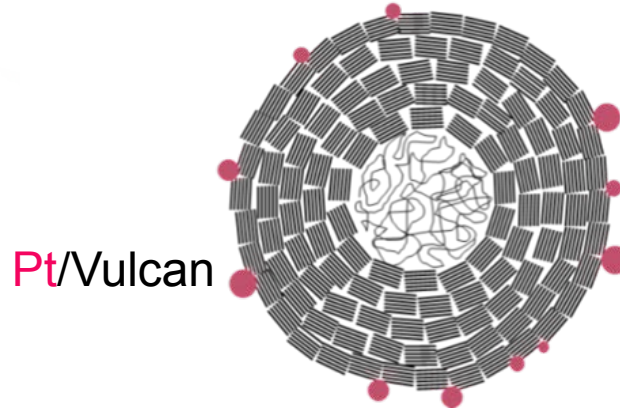




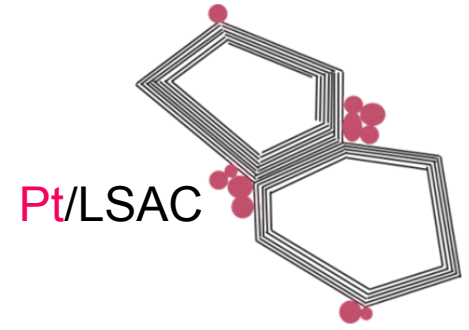
# Carbon Supports for Fuel Cell Catalysts



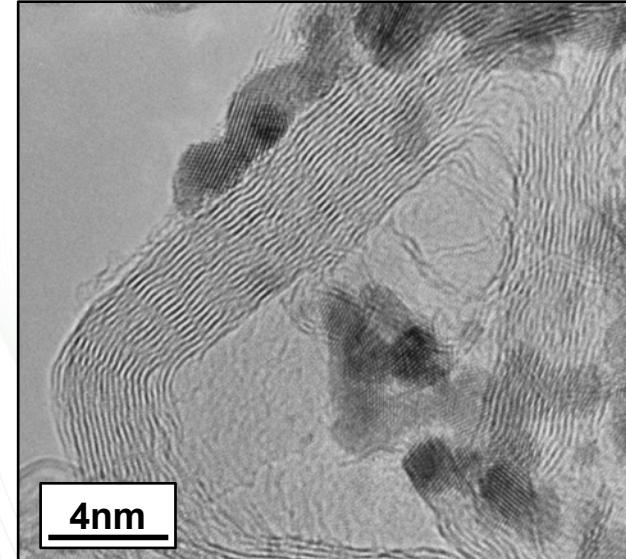
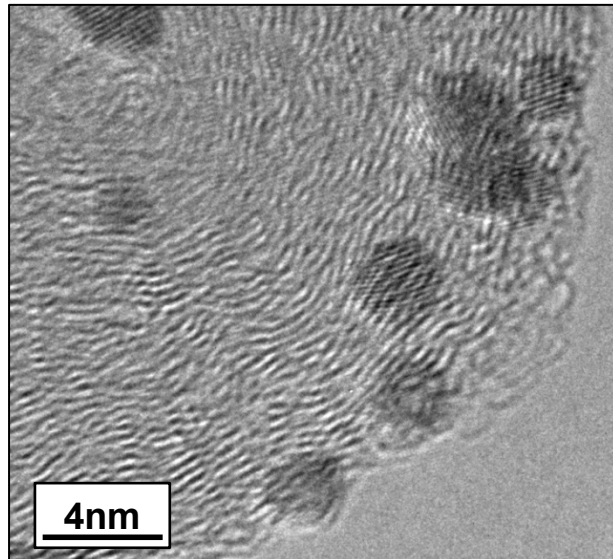
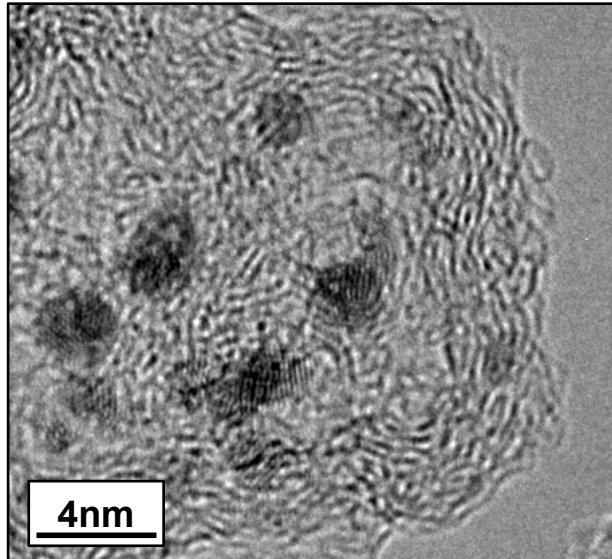
- highly disordered with meso-graphitic outer 'shell'
- Pt "inside" carbon particles



- concentric 'domain' structure ~4-5 nm graphite domain size
- Pt on surface of carbon particles

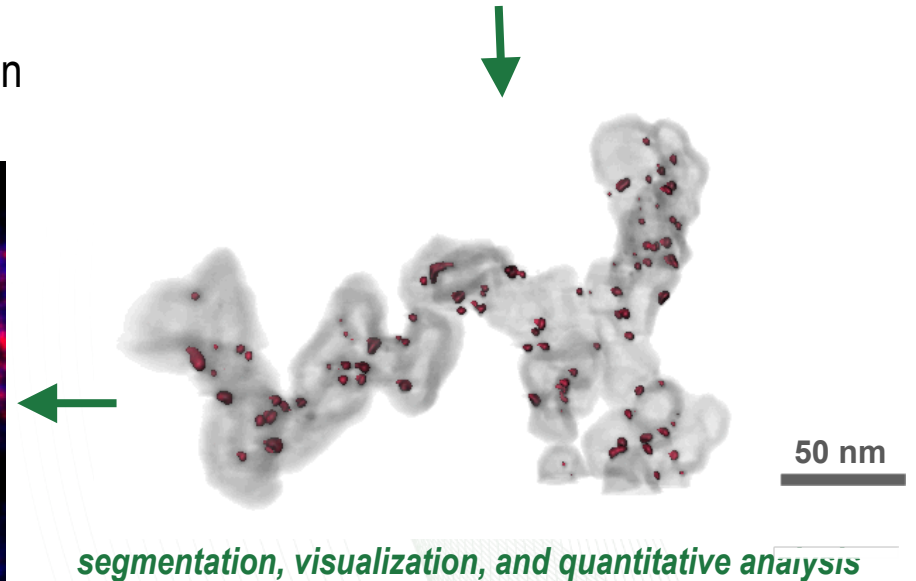
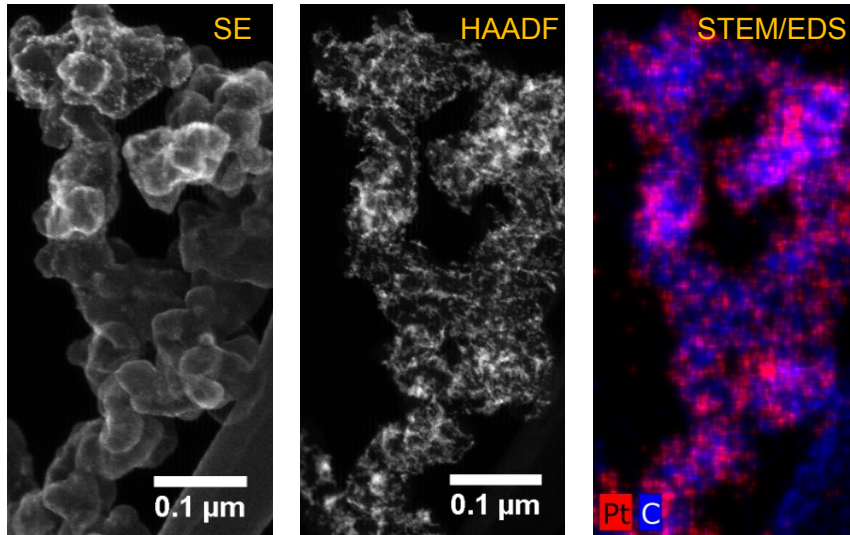
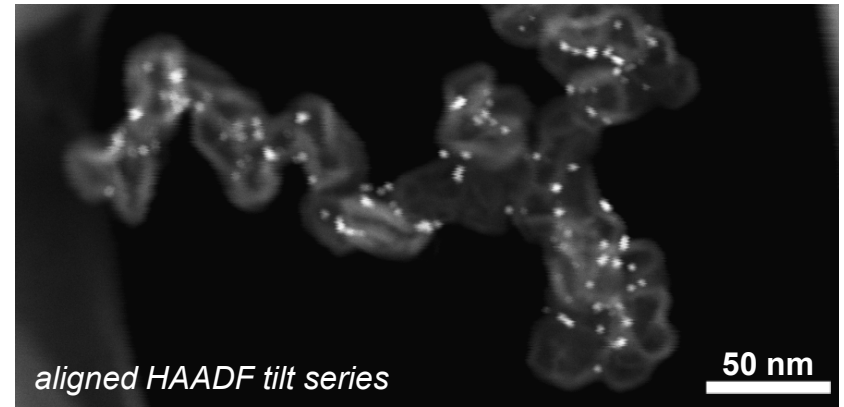


- highly ordered/faceted graphitic 'shell' with hollow core



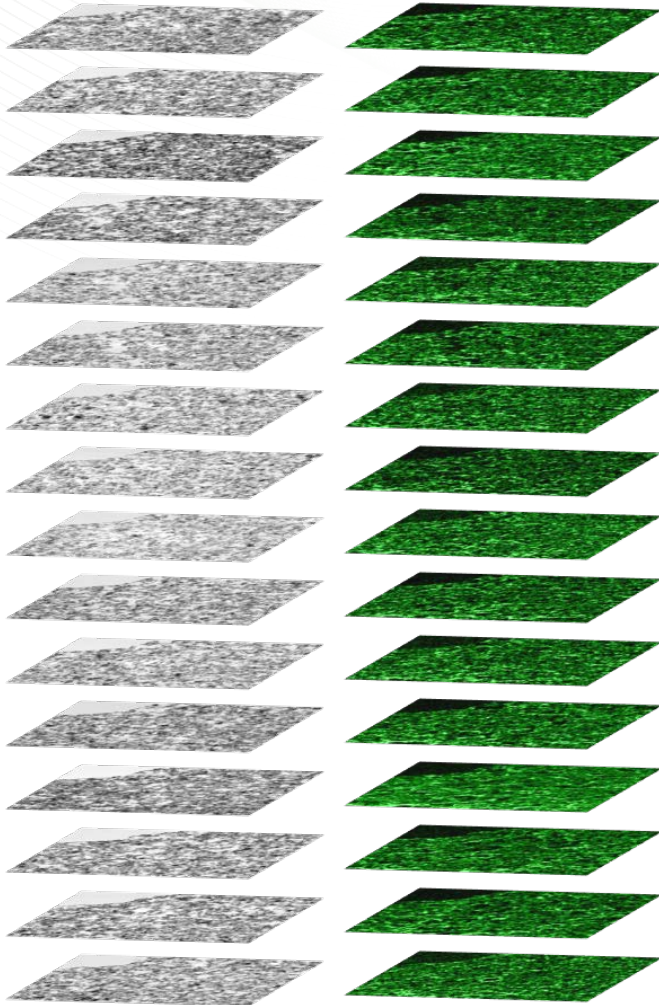
# Imaging Catalyst Distributions in 3D

- Quantify initial catalyst dispersions on different carbon supports → agglomeration
- Elucidate catalyst degradation mechanisms (Pt agglomeration, coarsening, dissolution) → AST for catalyst degradation  
30,000 cycles 0.6-1.0V
- Improve stability and durability of catalyst/support through structural optimization



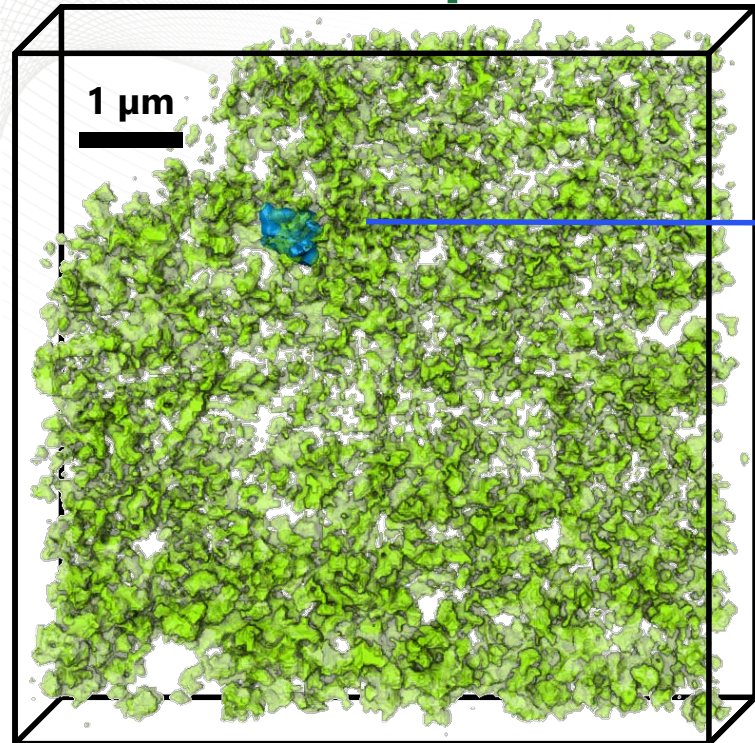
# Technical Accomplishments and Progress: Imaging Ionomer Dispersions in Catalyst Layers in 3D

17 MEA slices

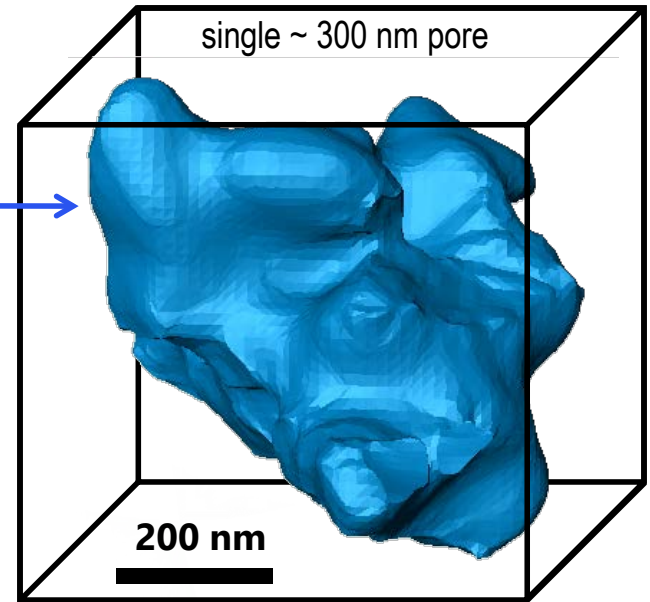


Individual F maps acquired from “slices” are stacked to create a **3D rendering/reconstruction** of the ionomer distribution within a given volume of the CL

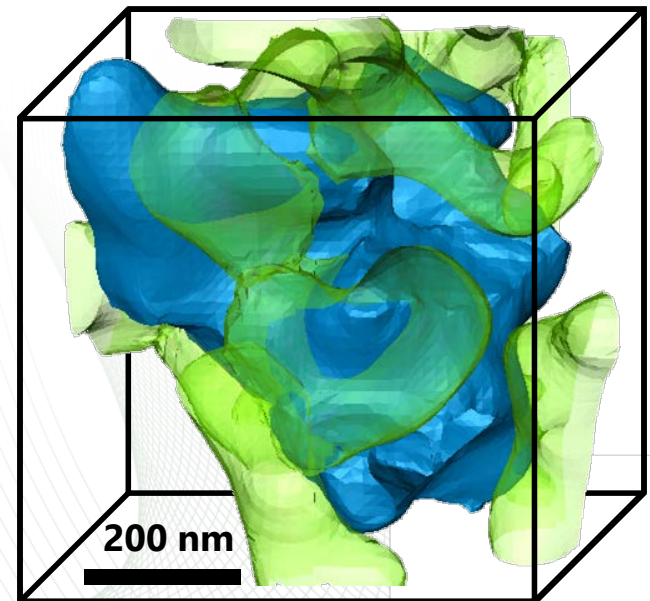
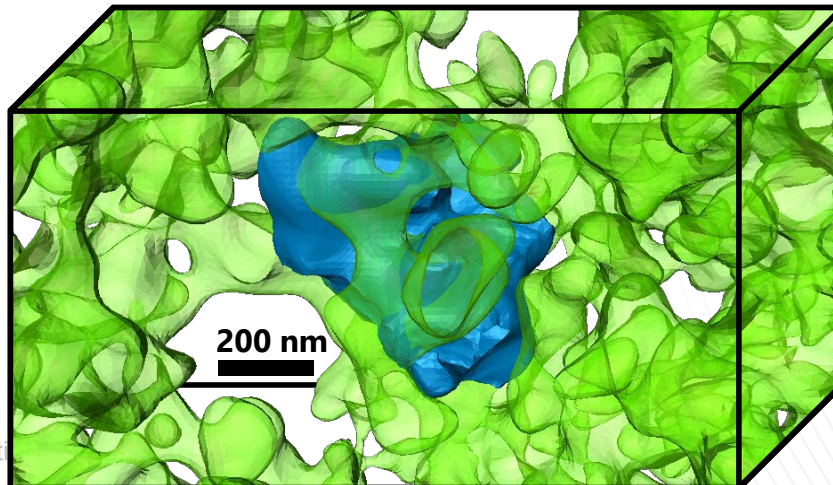
# Technical Accomplishments and Progress: Imaging Ionomer Dispersions in Catalyst Layers in 3D



To correlate ionomer with porosity (and simplify visualization), a single secondary pore is selected from CL volume using corresponding STEM images

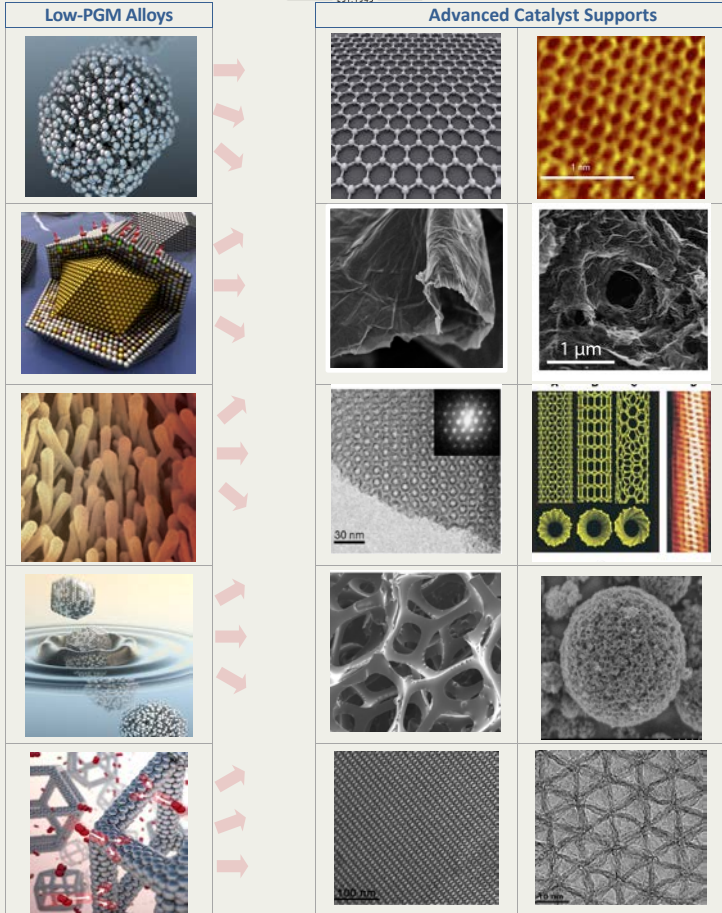


Same pore with ionomer

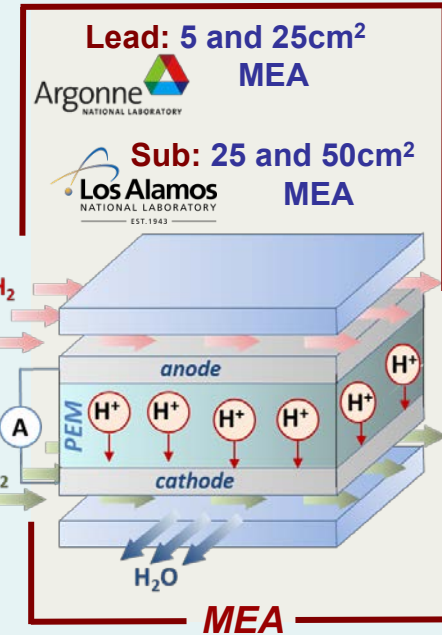
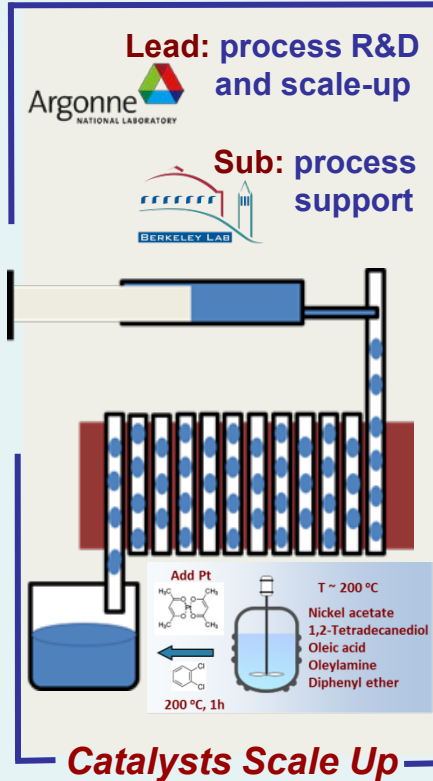


# Collaborations

**Argonne NATIONAL LABORATORY** **Lead: design, synthesis, evaluation**  
**BERKELEY LAB** **Sub: synthesis, scale-up support**  
**OAK RIDGE National Laboratory** **Sub: structural characterization**  
**Los Alamos NATIONAL LABORATORY** **Sub: catalyst supports**

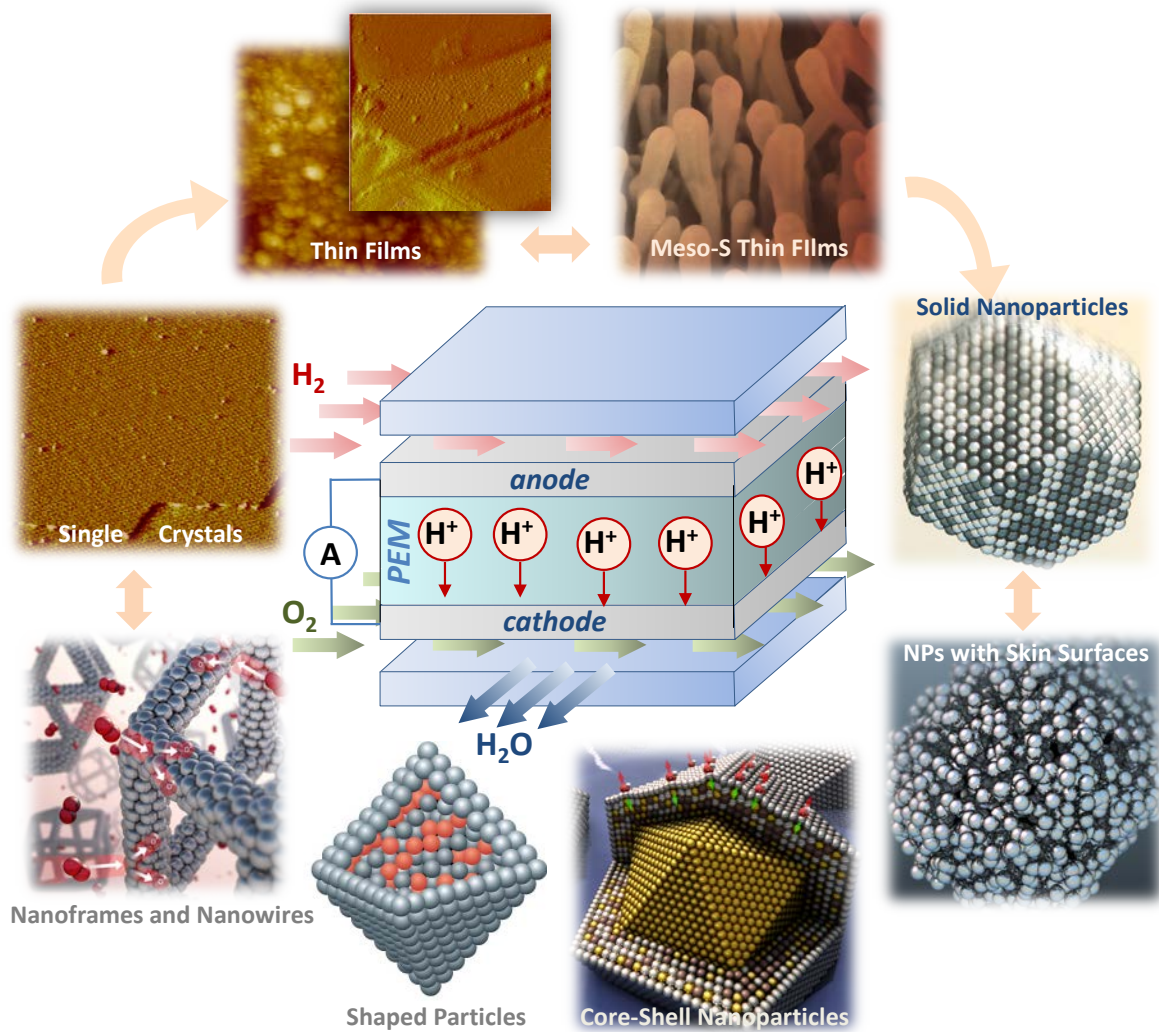


**Low-PGM Alloy Catalysts**



**OEMs**  
**T2M**

# APPROACH



RDE

MEA

Toyota - Mirai



**Principal Investigators:** Vojislav Stamenkovic  
Nenad Markovic

**Full time postdocs:** Dongguo Li (RDE, synthesis, thin films)  
Haifeng Lv (RDE, synthesis, MEA)  
Rongyue Wang (scale up syntehsis, RDE, MEA)

**Partial time postdocs:** Pietro Papa Lopes (RDE-ICP-MS)

**Partial time Staff:** Paul Paulikas (UHV, thin films)  
Dusan Strmcnik

**Grad student:** Nigel Becknell (synthesis, RDE, EXAFS)

**Collaborators:** Guofeng Wang, University of Pittsburgh  
Jeff Greeley, Purdue University  
Plamen Atanassov, University of New Mexico  
Debbie Myers, Argonne National Laboratory  
Rod Borup, Los Alamos National Laboratory  
Karren More, Oak Ridge National Laboratory  
Peidong Yang, University of California Berkeley

## Acknowledgments

Chao Wang, ANL (Johns Hopkins University)

Dennis van der Vliet, ANL (3M)

Ramachandran Subaraman, ANL (Bosch Research Center)

Yijin Kang, ANL (UESR)

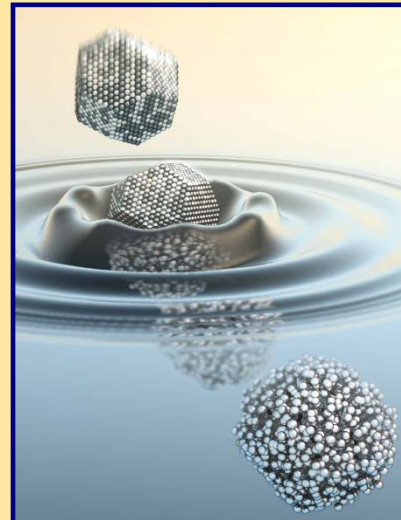
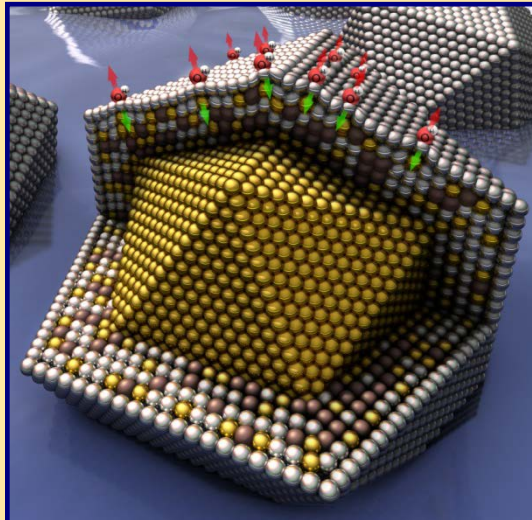
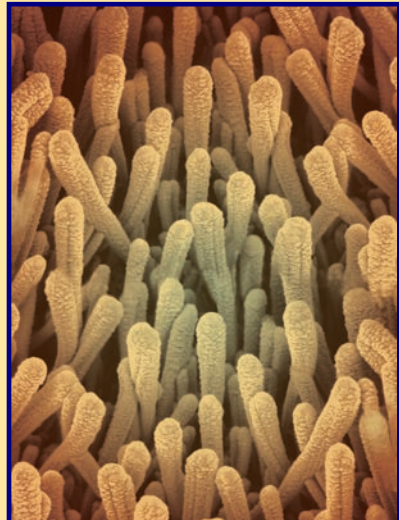
Nemanja Danilovic, ANL (ProtonOnSite)

This research was supported by the Office of Science, Basic Energy Sciences, Materials Sciences Division and the Office of Energy Efficiency and Renewable Energy of the U.S. Department of Energy



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of Energy

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managed by UChicago Argonne, LLC



# Thank you

**Dimitrios Papageorgopoulos**  
Program Manager – Fuel Cells  
DOE Fuel Cell Technologies Office

**Voya (Vojislav) Stamenkovic**  
Argonne National Laboratory

[hydrogenandfuelcells.energy.gov](https://hydrogenandfuelcells.energy.gov)