

Novel Approach for Biomass Synthesis Gas Cleaning for Liquid Fuel Applications

WBS 3.2.5.9



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Thermo-chemical Platform Review

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Project Overview

Timeline

- Start Date – 9/30/2008
- Completion Date – Dec 2012
- Construction – 100% complete
- Project – 100% complete

Budget

Total Project Funding

\$1,734,459 DOE

\$1,853,350 Contractor

Funding received in FY11

\$293,161

Funding for FY12

\$137,102.84

Barriers Addressed

1. Tt-C – Gasification of Wood, Biorefinery Residue Streams and Low Sugar Biomass
2. Tt-F – Syngas Cleanup & Conditioning
3. Tt-H – Validation of Syngas Quality

Partners

- Western Research Institute
- Ceramatec
- Idaho National Laboratory (sampling via FWP)

Goals and Objectives

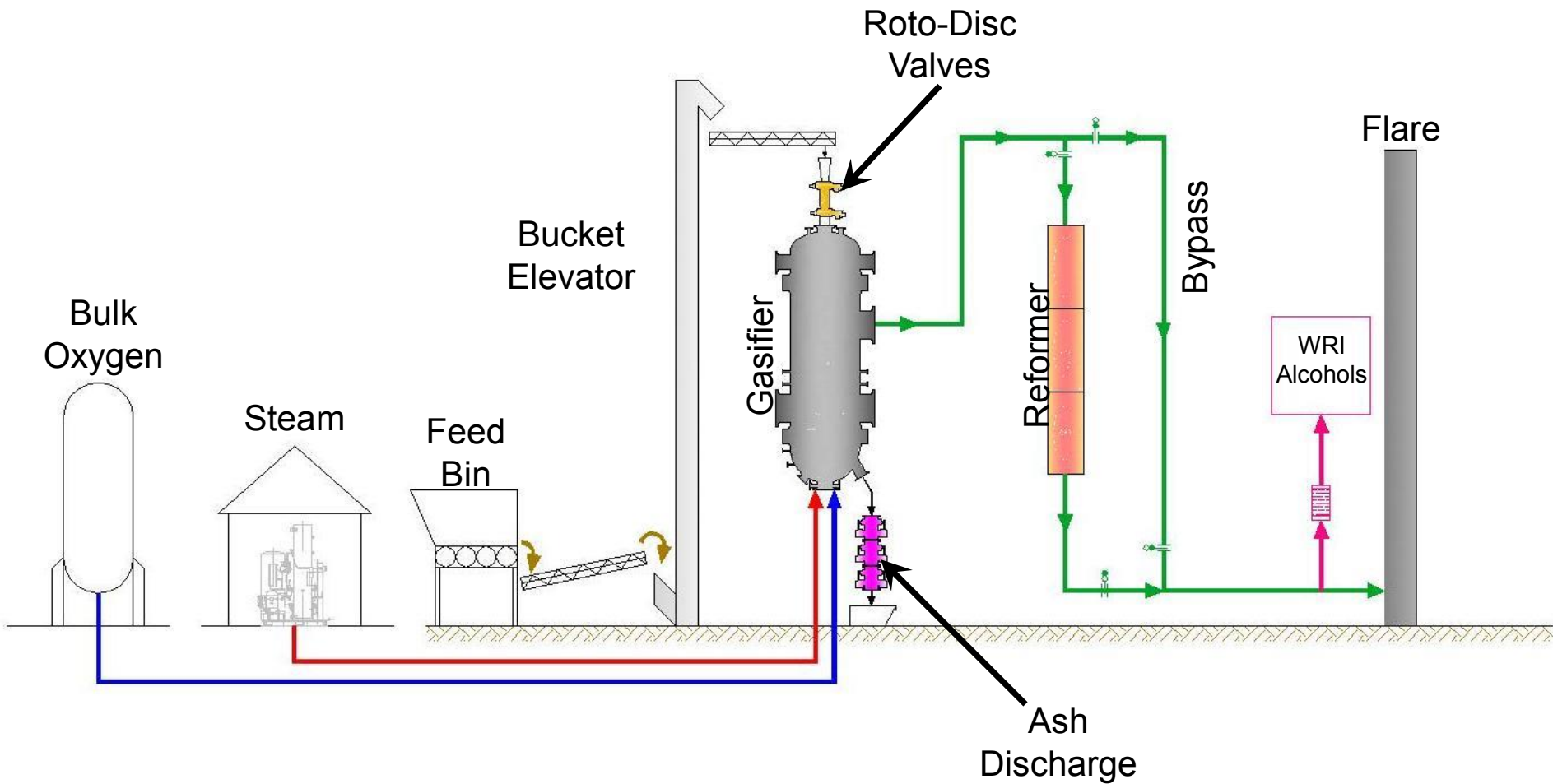
1. Demonstrate the ability of a cold plasma reformer to destroy tars and oils in syngas produced by biomass gasification.
 - Obtain operating data that documents destruction and provides a heat and mass balance. Use these to determine cost benefits relative to alternative processes.
 - Optimize the operation of the cold plasma reformer

Success will eliminate the need for catalyst reforming/ tar removal by water quench

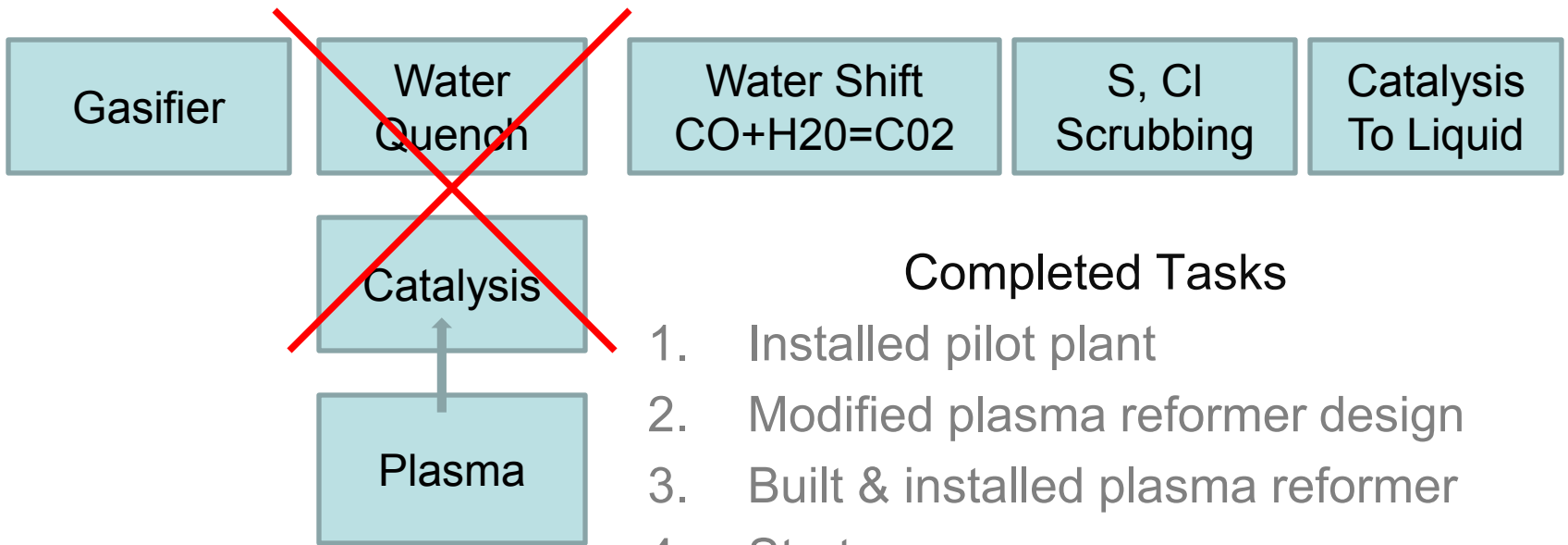
2. Use Syngas cleaned by the cold plasma reformer for liquid fuel production
 - Obtain operating data in an existing liquid fuel synthesis pilot plant
 - Identify commercial opportunities
 - Continue reformer data analysis to identify possible process improvements.

1 - Approach

Flowsheet



2 - Technical Accomplishments/Results



Water Shift
 $CO+H_2O=C0_2$

S, Cl
Scrubbing

Catalysis
To Liquid

Completed Tasks

1. Installed pilot plant
2. Modified plasma reformer design
3. Built & installed plasma reformer
4. Startup
5. Ran gasifier and obtained data
6. Submitted Report

2 – Technical Accomplishments (cont'd)

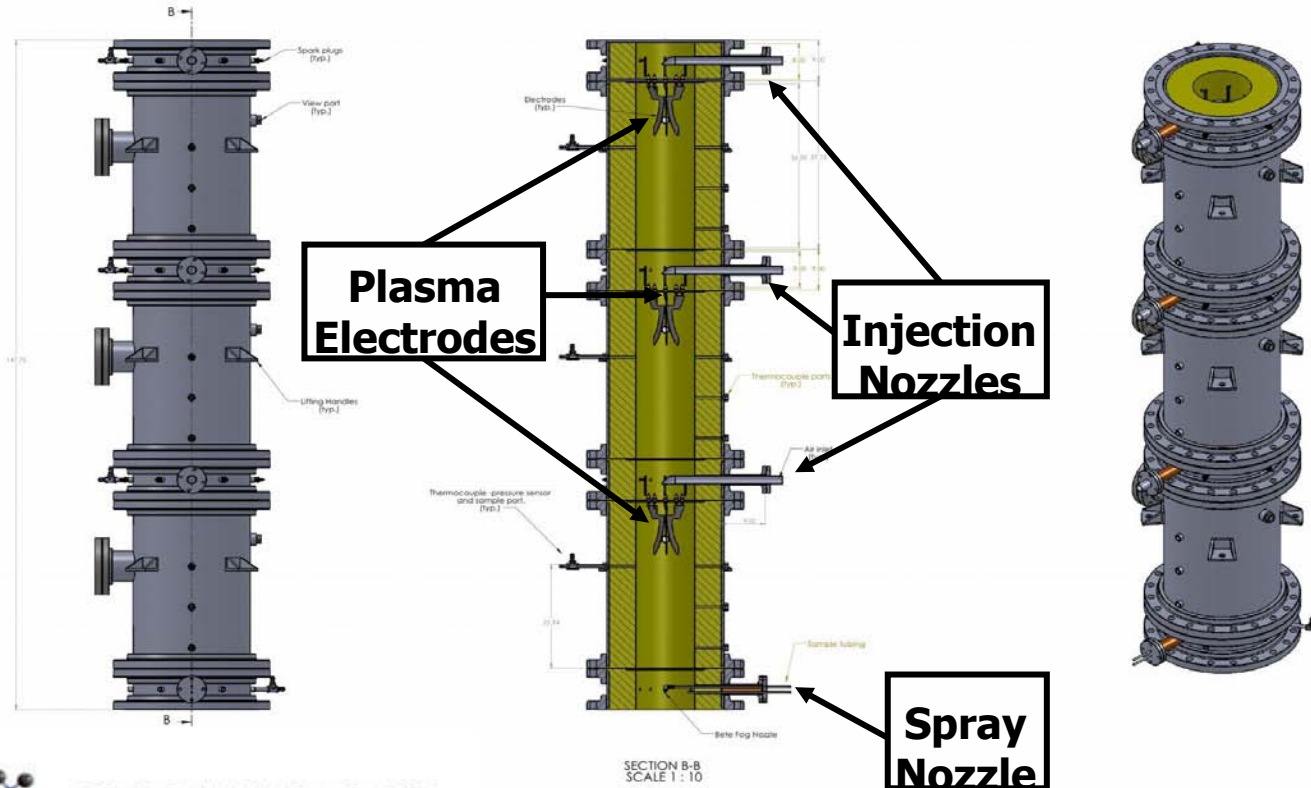
Completed Installation



2- Technical Accomplishments (cont'd)

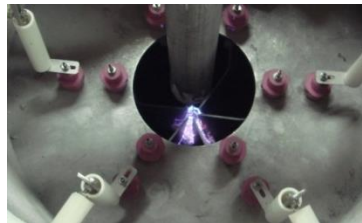
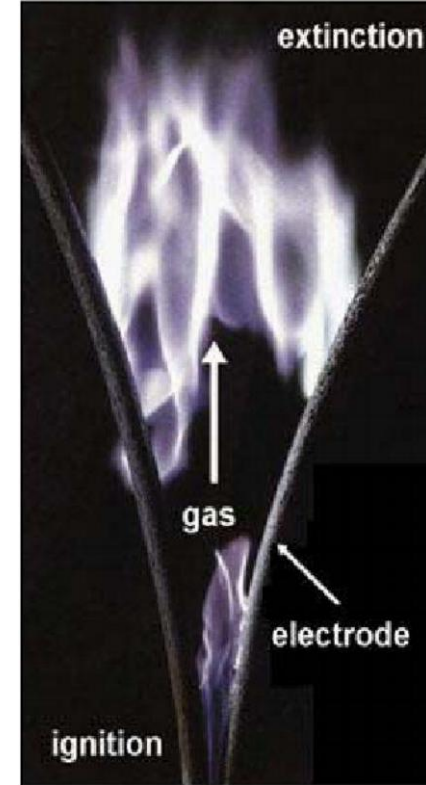
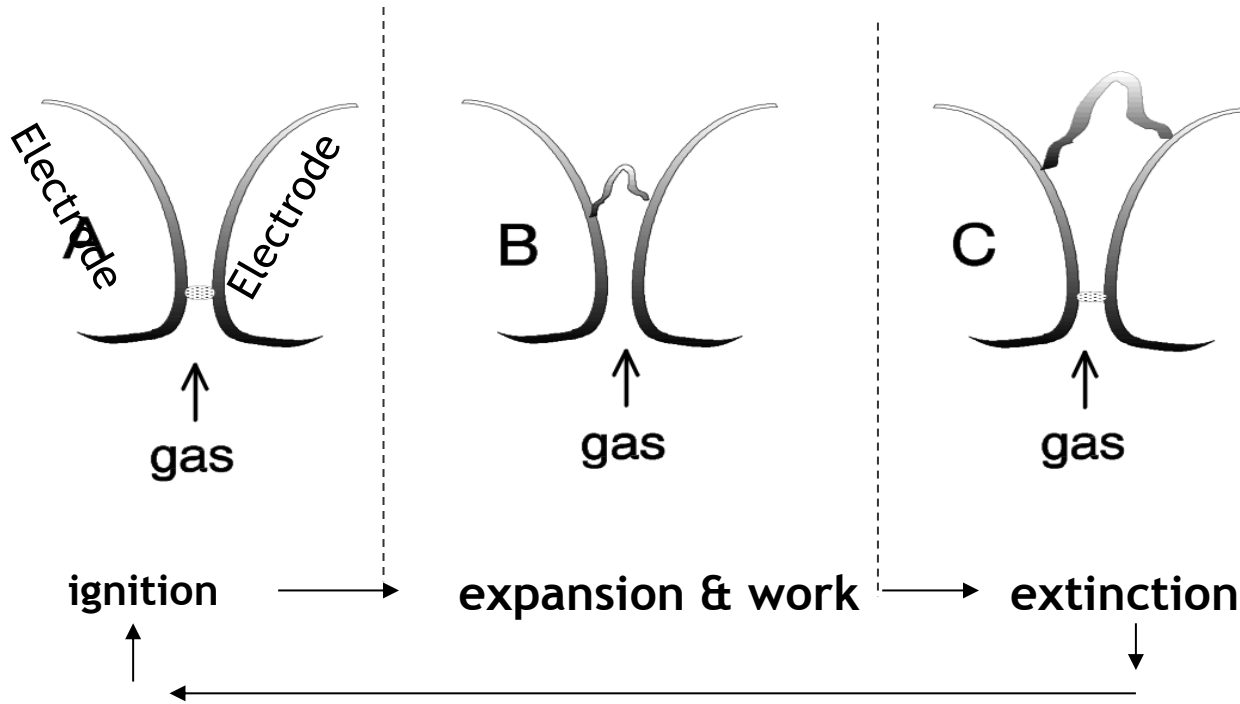
In-situ plasma reformer assembly

3-Stage plasma with quench stage



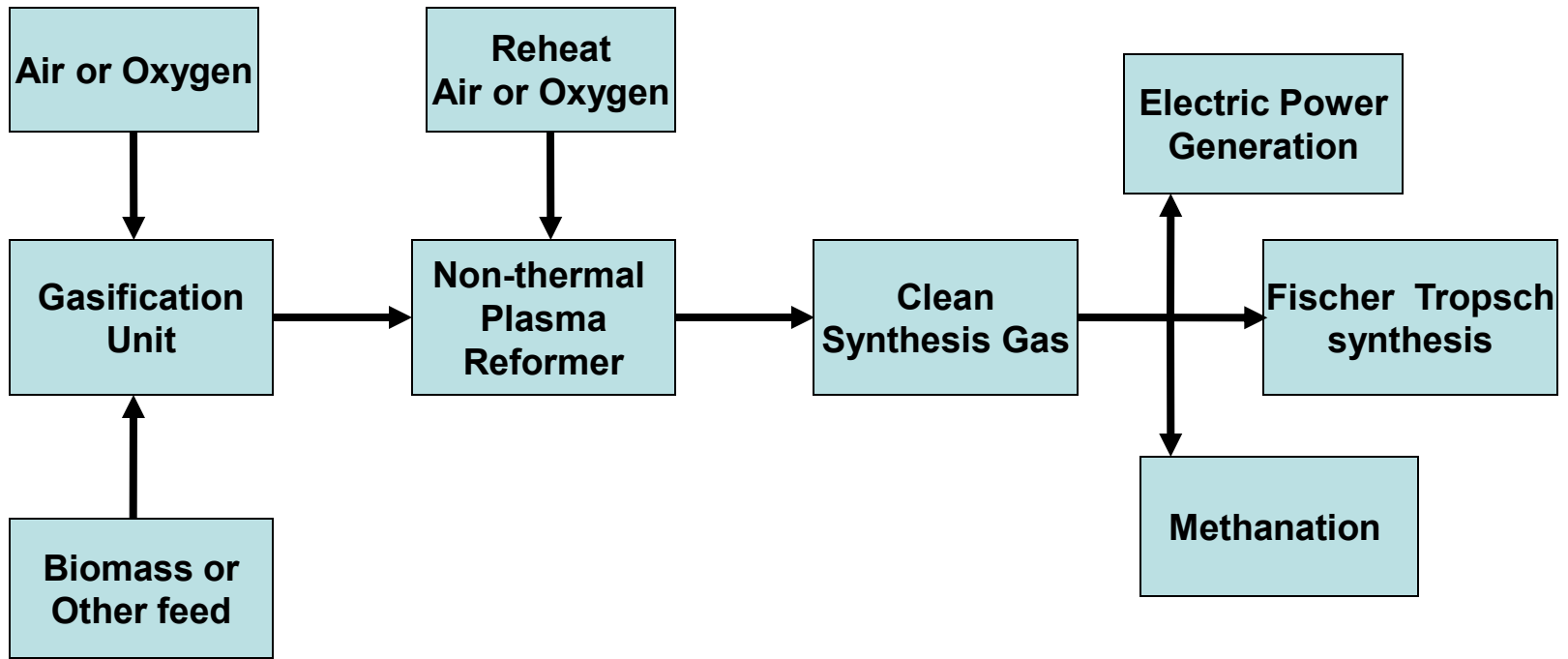
2 - Technical Accomplishments (cont'd)

Cold Plasma GlidArc Operation



2 - Technical Accomplishments (cont'd)

Directly reform tars & oils



2 - Technical Accomplishments (cont'd)

Laboratory scale plasma reformer

Simulated gasifier stream

- Bottled synthesis gas
- Toluene injection
- Steam, O₂ ,or air to obtain temperature
- GC analysis of toluene destruction and CGE



2 - Technical Accomplishments (cont'd)

Best combination

	Dry Gas	Air In	O ₂ In	H ₂ O In	Toluene In
Run	L/min	L/min	L/min	g/min	g/min
4	50	52	0	1.7	5.9

			Mole %	Output			
Run	H ₂	N ₂	CO	CO ₂	Toluene	CH ₄	H ₂ O
4	12	54	21	7	0	.3	6

	LHV Gas In	LHV Gas Out	Thermal Eff	Toluene
Run	kW	kW	Percent	% Destroyed
4	5.02	5.87	117	100

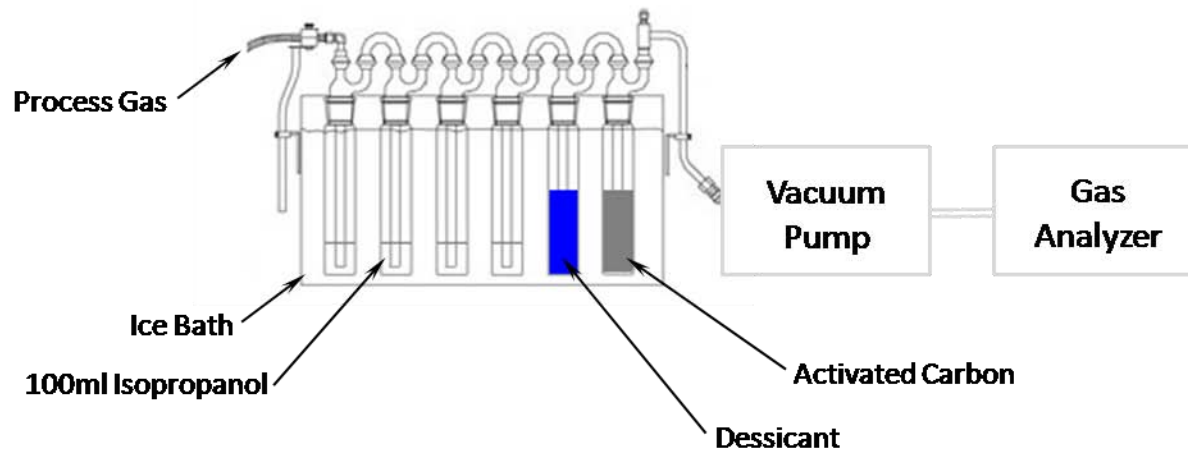
- **Run 4 had good destruction and good efficiency**

2 - Technical Accomplishments (cont'd)

- **Conversion of BTX and other hydrocarbons very good in laboratory**
 - **92% methane (near equilibrium limit)**
 - **96% ethane**
 - **100% (to detection limit) of other C2-C4**
 - **98% benzene**
 - **99% toluene**
 - **100% (to detection limit) of xylenes**

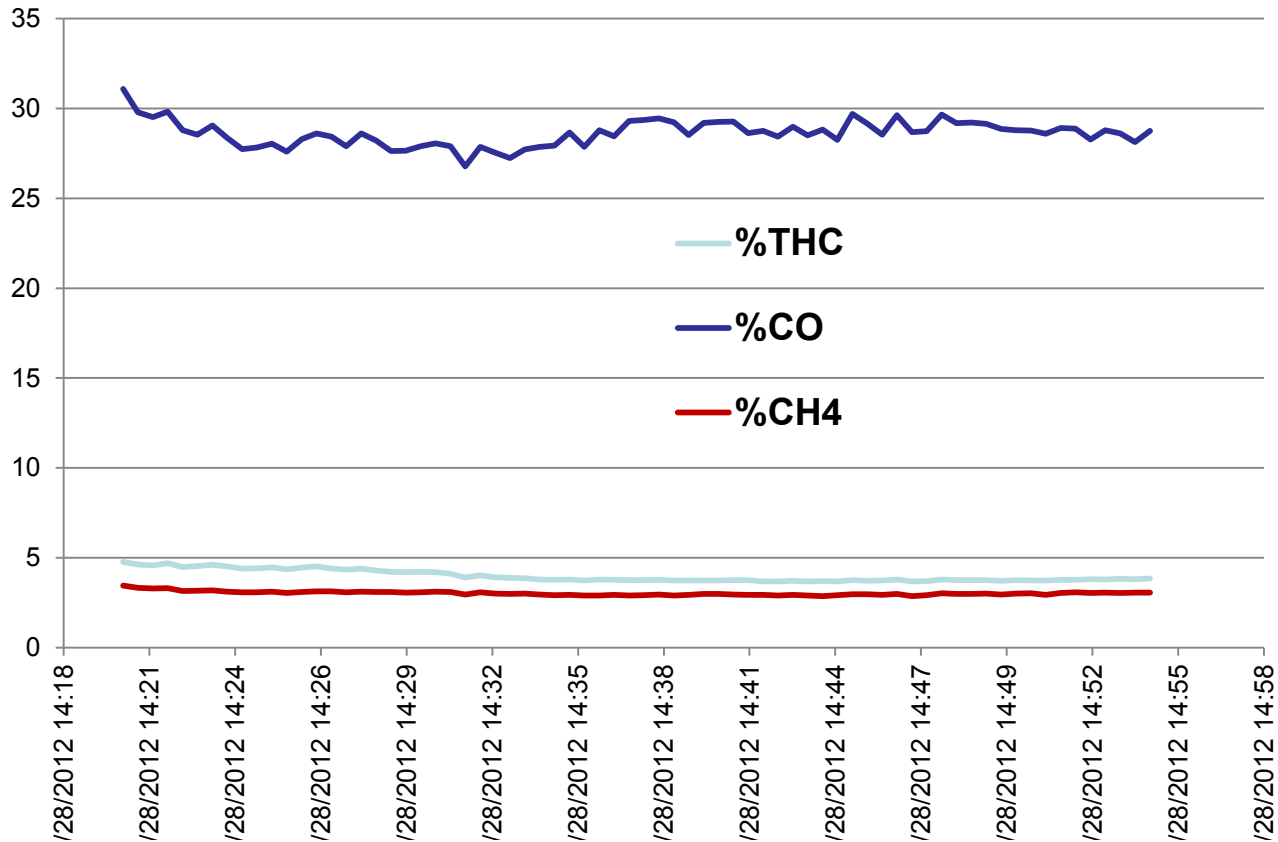
2 - Technical Accomplishments (cont'd)

- INL on-site testing of Emery Gasifier Reformer
 - Sample pre- and post-reformer
 - Collect impinger train samples and CEMS
 - Survey relative concentrations before and after reformer
- Test Equipment
 - Continuous Emissions Monitoring (CO, CH₄, THC)
 - IPA impinger train samples for semi-volatiles



2 -Technical Accomplishments (cont'd)

Pre-Reformer Measurement



- Gasifier generally operating at steady state
- THC represents sum of CH_4 and other hydrocarbons converted to CH_4
- Noncondensable THC gases range from 0.5-1.5% above CH_4 when converted to CH_4 -equivalent

2 – Technical Accomplishments (cont'd)

- Gas bag samples (foil bags) collected – results support CEMS results

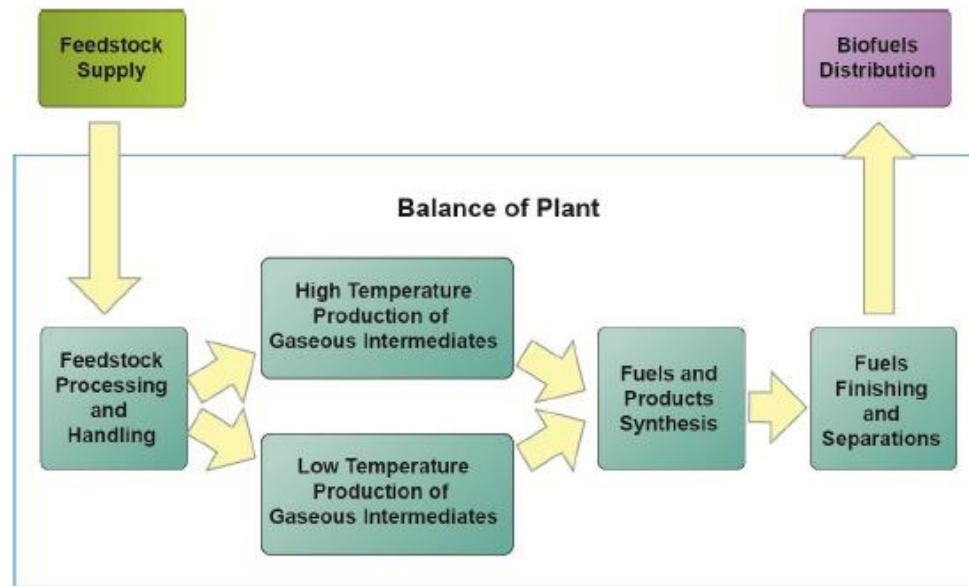
Corrected Samples:	H ₂	CO	CO ₂	Methane	Ethane	Ethene
Mean Pre-reformer	30.03	31.35	29.19	3.44	0.15	0.49
Corrected Post Reformer	28.80	35.57	26.24	3.69	0.13	0.65

- Liquid Impinger Samples
 - Polynuclear aromatic compounds are generally reduced
 - Styrene (intermediate product of naphthalene decomposition) appears to increase as naphthalene decreases

Compound:	Pre-Reformer	Post Reformer
Acetic Acid	34697	53924
Toluene	69729	48902
Styrene	9455	15910
Phenol	24289	23763
Benzene, 1-propynyl-...	53432	39708
Napthalene	130962	76698

3 - Relevance

- The expected output of the project will enable the large-scale production of cleaner syn-gas that is more compatible with down-stream processes for the production of energy or liquid fuels.



From MYPP 2012

3 – Relevance (cont'd)

- Program Mission:
 - *“Transform our renewable biomass resources into commercially viable, high-performance biofuels... through targeted research, development, demonstration, and deployment supported through public and private partnerships.*
 - *Enable sustainable, nationwide production of advanced biofuels*
- This project focuses on demonstration and deployment of a full-scale biomass conversion platform for production of a high quality gaseous intermediate.
- This addresses specific areas of the MYPP 2012:
 - Gt. C. High-Temperature Gas Production from Biomass
 - Gt. F. Gas Cleanup and Conditioning
 - Gt. H. Validation of Syngas Quality

4 - Critical Success Factors

- Critical success factors include the ability of this process to economically and efficiently eliminate unwanted heavier hydrocarbons from the syngas stream.
- Potential challenges:
 - Biomass feed specifications can affect overall quality of syngas
 - Process parameters must be explored to optimize production and process efficiency.
- This project is continuing to demonstrate viability in the production of biofuels, and continuing work will further demonstrate the importance of this technology for biofuels and bioenergy production.

5 - Future Work

- **No Future Work is Planned**

Summary

- Plasma Reformer:
 - Meets objectives of BETO per MYPP 2012
 - Technology demonstrated on full-size system
 - Work continues with other partners

(Not a template slide – for information purposes only)

- The following slides are to be included in your submission for Peer Evaluation purposes, but will **not** be part of your oral presentation
- You may refer to them during the Q&A period if they are helpful to you in explaining certain points

Project Delays

- Project was delayed twice due to weather and the need to make additional gasifier modifications.

TASK	PLANNED - LAST PEER REVIEW	TASK ACTUALLY INITIATED
Commissioning	May 2011	December 2011
Initial Runs	June 2011	August 2012
Reformer Runs	September 2011	November 2012

Contact Information

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C O M P A N Y

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