

# **2013 DOE Bioenergy Technologies Office (BETO) Project Peer Review**

## **Pilot-Scale Demonstration of a Fully Integrated Process for Converting Woody Biomass into Clean Biomass Diesel Fuel**

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**Gasification Peer Review**

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# Project's Goal/Objective Statement

## Project Goal

- Integrate and demonstrate a hot gasification clean up process at the pilot scale for the production of FT diesel fuel from woody biomass

## Project Objectives

- A 300 hr steady state pilot scale operation of the syngas clean up system for Techno-economic analysis and commercial evaluation
- Validate syngas clean up technology for at least 500 hours of steady state operation, with at least 100 hours continuous operations

## Project goals/objectives support:

- BETO's and technology area's objective of enhancing gas clean up and production of transportation fuels from high impact biomass
- Industry's objective to lower cost of wood-to-fuels commercial processes to meet RFS2 milestones

# Quad Chart Overview

## Timeline

- Start: September 1, 2008
- End: December 31, 2014
- 25 % complete, project has undergone significant restructuring

## Budget

- Total project funding : \$3,141,751
- DOE share: \$1,997,793
  - Contractor share: \$1,143,958
- FY09 Funding: \$ 158,757 (\$153,339 DOE)
- FY10 Funding: \$ 71,121 (\$69,264 DOE)
- FY11 Funding: \$ 54,777 (\$49,010 DOE)
- FY12 Funding: \$1,619,793 (\$488,847 DOE)
- FY13 Funding Est.: \$682,424 DOE
- FY14 Funding Est.: \$441,393 DOE
- FY15 Funding Est.: \$113,486 DOE
- ARRA Funding: None

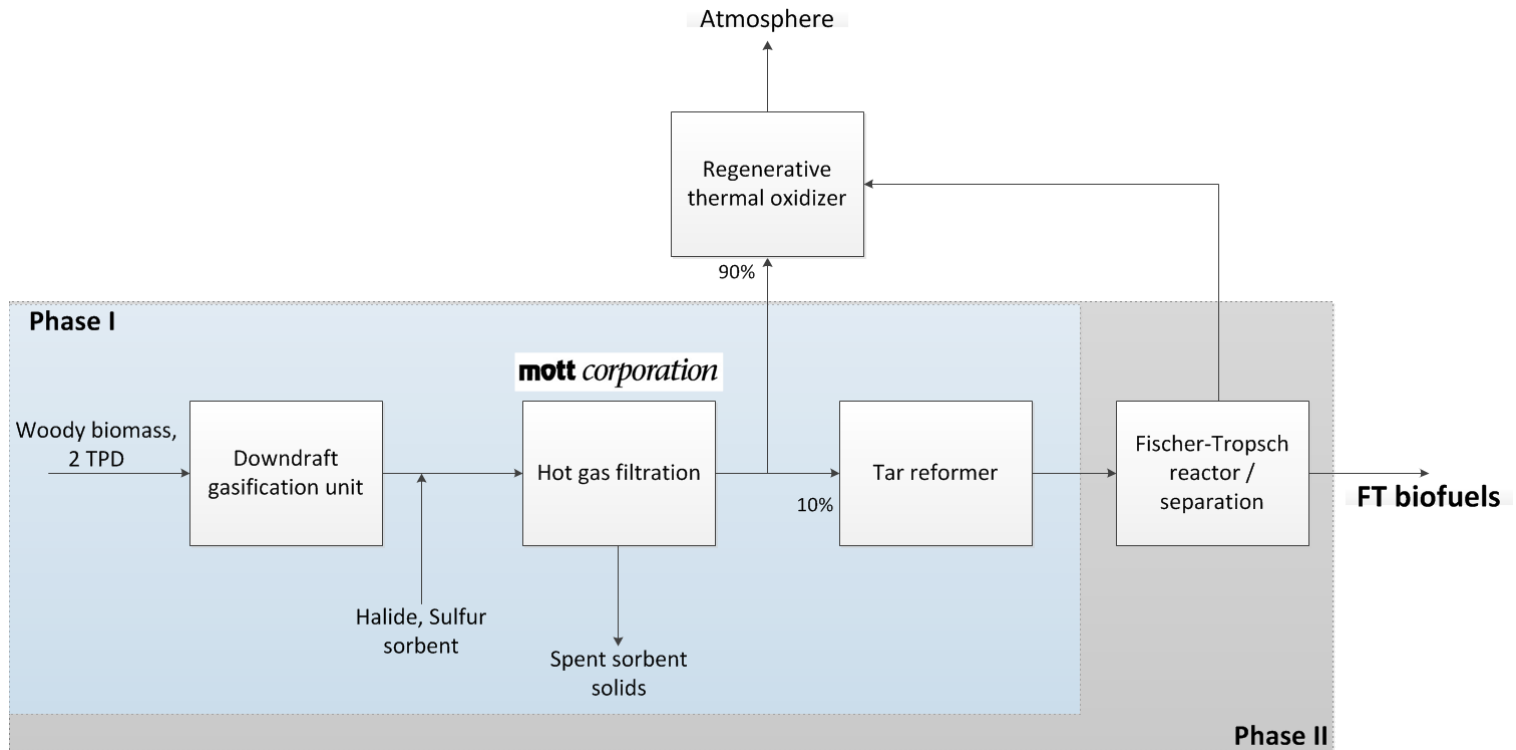
## Barriers

- Barriers addressed
  - Cost effective tar reforming and syngas cleanup
  - Pilot-scale demonstration of integrated gasification and gas cleanup
  - Pilot-scale demonstration of integrated biorefinery

## Partner

Mott Corporation

# Project Overview



## Unit Operation Being Improved

- Gas clean up
  - High temperature filtration
  - Sorbent removal of contaminants

## Barrier Addressed

- Integration challenges
- Filtration technologies and FT biomass catalyst longevity

# 1 – Approach

Activity / Milestones	Approach and Outputs
<p>Integrate and validate a syngas cleanup system with a biomass gasifier</p> <p><b>Milestone:</b> System shake down; 300 hours of operation</p>	<ul style="list-style-type: none"> <li>• Engineering design and specification of system; PI&amp;Ds, electrical drawings, plant outlay, HAZOP study, construction / instrumentation plans</li> <li>• Procurement of equipment instrumentation</li> <li>• System installation and instrumentation set up</li> <li>• System shake down</li> <li>• Operate integrated system, measure process performance; QA data</li> </ul>
<p>Integrate and test a gasifier/syngas cleanup system with a Fischer-Tropsch unit</p> <p><b>Milestone:</b> 500 hours of operation</p>	<ul style="list-style-type: none"> <li>• Connect gasifier/syngas clean up system               <ul style="list-style-type: none"> <li>▪ engineering design and construction</li> </ul> </li> <li>• HAZOP study to include FT unit</li> <li>• Experimental plan design and execution</li> </ul>
<p>Develop techno-economic modeling of process</p> <p><b>Milestone:</b> Functional model determines process feasibility</p>	<ul style="list-style-type: none"> <li>• Build upon gasifier’s Techno-economic modeling with hot gas clean up (hot filtration and tar reformer) data; add FT data when collected</li> </ul>
<p><b>Project management and reporting</b></p>	<ul style="list-style-type: none"> <li>• Project management, required quarterly and annual progress and financial reports, meetings, final report</li> </ul>

## 2 - Technical Accomplishments/ Progress/Results

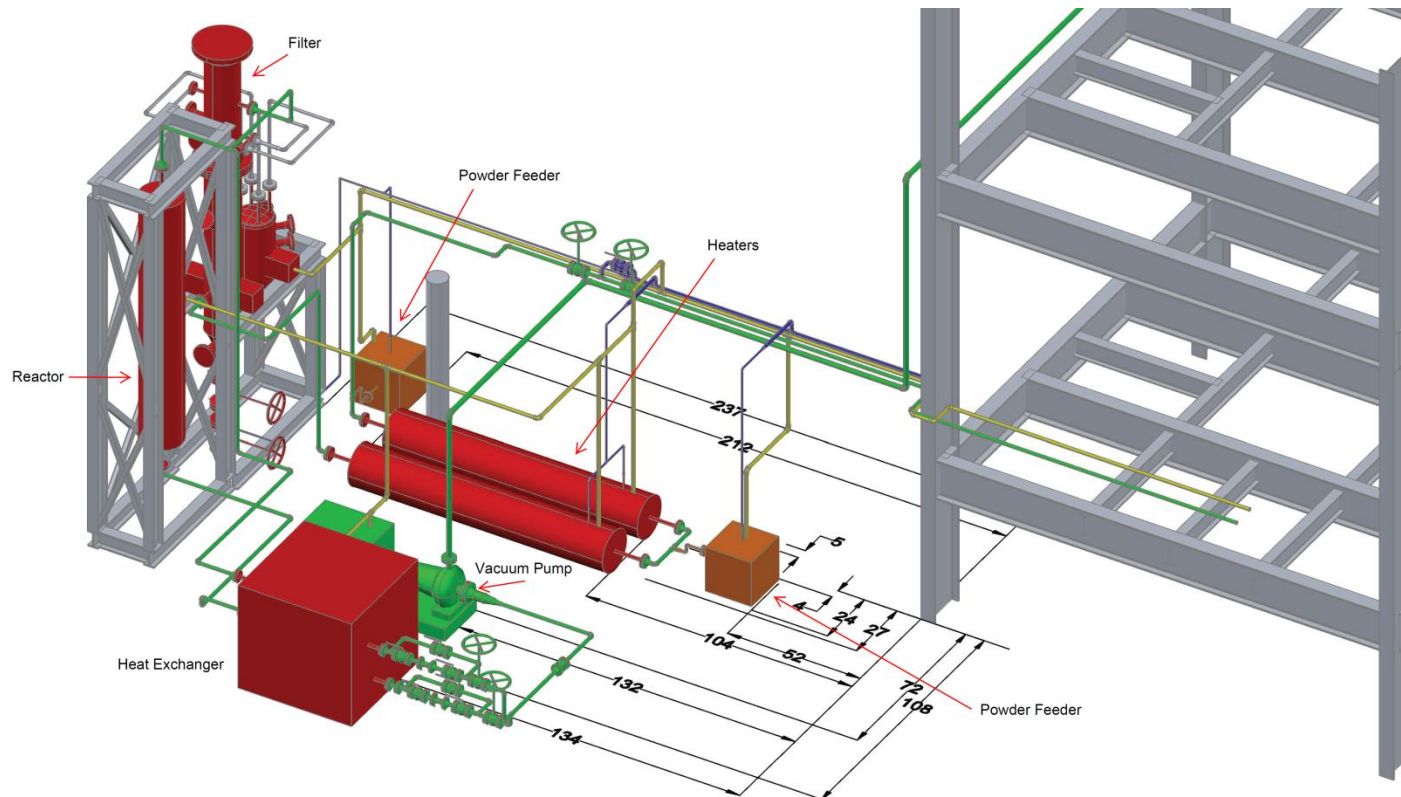
- Demonstrated steady state biomass gasification on woody biomass using the gasifier (pictured below)



## 2 - Technical Accomplishments/ Progress/Results (cont'd)

Integrated high temperature clean up:

- Engineering drawings (PI&Ds, 3D AutoCAD for facility layout), electrical drawings
- Equipment and instrument specifications for skid unit, pictured below



## 2 - Technical Accomplishments/ Progress/Results (cont'd)

- All major equipment, instruments, high T flanges / gaskets, etc. have been ordered
- Subcontracts and scope of works in place for construction work, fabrication, controls, electrical work





## 2 - Technical Accomplishments/ Progress/Results (cont'd)

- Disposable sorbent candidates selected and sources identified
- Commercial feeders were found in range of the desired flows

Impurities	Removal Reason	Sorbent Types and Expected Reductions		
		Dolomite	Kaolin Clay	Barium Carbonate
AsH <sub>3</sub>	C, F	>99%	---	---
Cl, F, HCl (Halides)	F	>50%	---	>90%
H <sub>2</sub> S & COS	C, F, P	>60%	---	---
Toxic Metals	C, F	---	>99%	---
Potassium	C, F, P	---	>99%	---

Reasons for reducing impurities

C = Catalyst (tar cracking) Protection

F = Filter Protection

P = Polishing Filter Protection

Tar reforming catalyst vendors have been identified – confidentiality agreements put in place & samples obtained

# 3 - Relevance

Project addresses several conversion goals, cross-cutting goals, and demonstration & deployment goals in Biomass Multi-Year Program Plan Conversion Goals:

- Development and deployment of integrated biorefineries:
  - Demonstration of technology at the pilot scale using scalable gasifier, high impact woody biomass, and industrially relevant FT reactor
- Conversion enabling technologies
  - Cost and energy efficient gas clean up
  - Testing the catalyst efficacy after clean up
- Integration and scale-up
  - Integration of gasification with gas clean up
  - Integration of gasification/clean up with Fischer-Tropsch

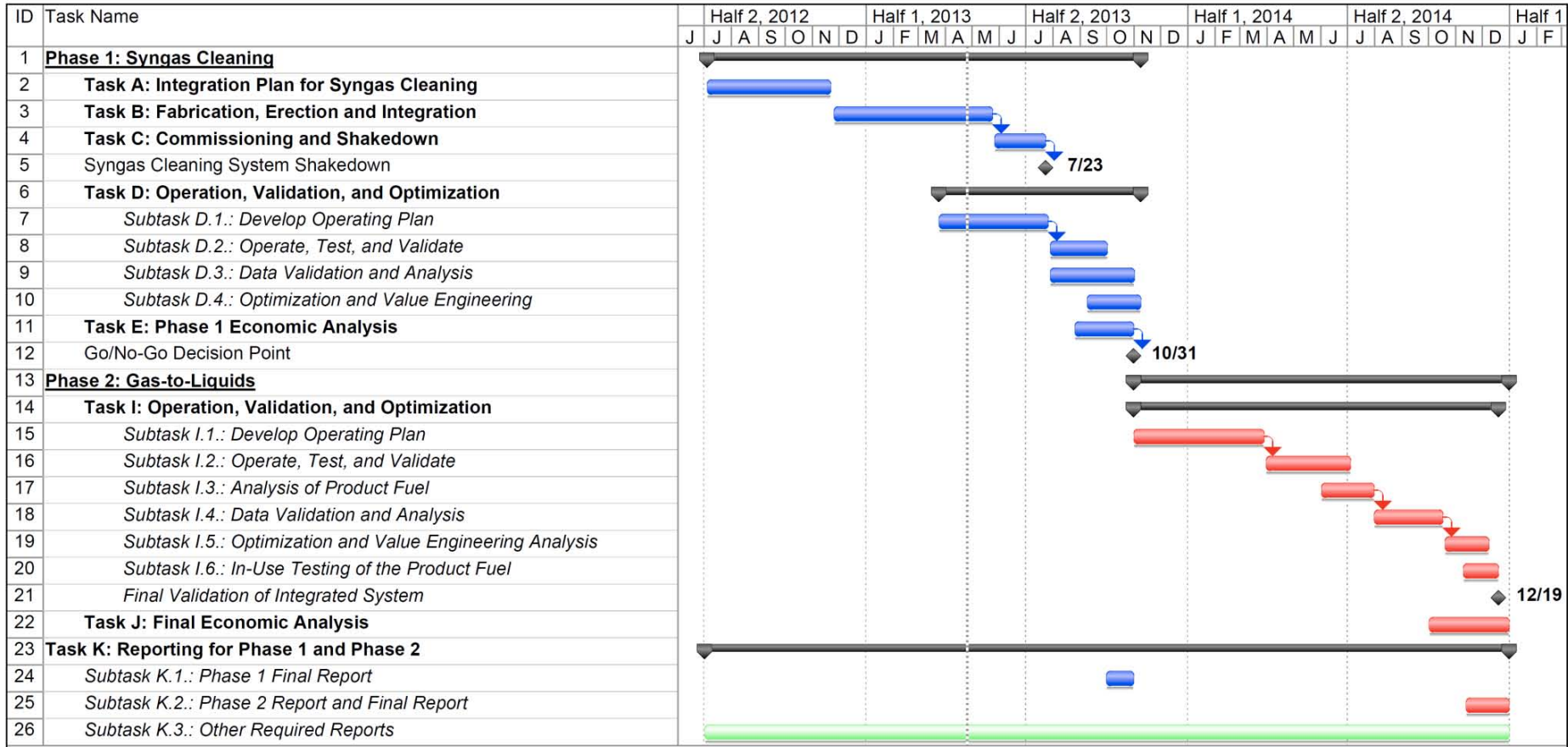
# 3 – Relevance (cont'd)

- Relevance to bio-energy industry
  - Cost effective tar reforming and syngas cleanup
  - Pilot scale and TEA scale data will generate basis for small commercial scale system
  - Interest of hot gas clean up by multiple gasification development companies
  - Adaptable to multiple gasification platforms test for other gasification platforms at the pilot scale
  - Enable industry to meet RFS2 goals and comply with EISA 2007
  - Potential for use with advanced TRI/EFT or Chevron selective FT catalyst from separate DOE-funded project to further advance the current state-of-the-art

# 4 - Critical Success Factors

- **Factors that will define technical and commercial viability**
  - Successful integration/operation of commercially demonstrated gasifier & FT line with new catalytic syngas cleaning system (500hrs); leading to intellectual property opportunities
  - Consistent reductions occur during operation in all FT and cracking catalyst poisons
  - Successful road test in diesel passenger vehicle
  - Economic viability estimated from final techno-economic analysis
- **Challenges to be overcome**
  - Catalytic syngas cleaning reactor size reduction
  - Maximize catalyst effectiveness on a wide range of tars & hydrocarbons
  - Maximize catalyst life using effective sorbents for tar reforming catalyst and FT contaminants

# 5. Future Work



# Summary

- Engineering, procurement, and preliminary experimental planning completed for pilot-scale woody biomass hot gas filtration and catalytic tar removal
- Construction and electrical engineering contracts are being finalized for DOE approval
- Construction for gas clean up integration with gasifier construction imminent, followed by shake down and commissioning
- Must overcome challenge of filter deactivation by removing halides and
- System has significant potential for advancing BETO's goal for system integration and clean up for gasification
- Techno-economic modeling in parallel to pilot operation data
- Goal of project to have 300 hours of operation with gas clean up system and 500 hours with the clean up/FT systems integrated
- Demonstrated success will lead to IP development, cross-platform testing and commercialization

# Additional Slides

# Responses to 2011 Reviewers' Comments

Comment: Tar reforming catalyst selection needed more discussion

Response: Catalyst selection and testing conditions used could potentially infringe on intellectual property

Comment: Goals are not quantitative in nature

Response: The go/no-go decisions and goals have a set amount of hours that are explicitly detailed. The upper and lower control limits to be considered at steady state will depend on operational data