2013 DOE Bioenergy Technologies Office (BETO) Project Peer Review

Catalytic Conversion to Liquid Hydrocarbons from Pyrolysis Oil and Syngas

May 20, 2013 Bio-Oil Technology Area Review

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On many slides, the slide notes section has important additional information

This presentation does not contain any proprietary, confidential, or otherwise restricted information

Goal/Objective Statement

- MSU pyrolysis/syngas program goals:
 - Develop hydrocarbon and biodiesel fuels from raw bio-oil produced from southern pine and agricultural products and residues; develop auger reactor designs that can provide test quantities of raw bio-oil; test designs at pilot plant scale
 - Develop technologies for biomass gasification and catalytic conversion of cleaned syngas to hydrocarbon biofuels. This is accomplished through the design and optimization of syngas-to-hydrocarbons pilot plant, including biomass gasification, syngas cleanup, syngas upgrading as well as new catalyst material development.
- The MSU pyrolysis/syngas program goals support the development of technologies for conversion of forest resources into cost-competitive liquid fuels, such as renewable gasoline, jet fuel and diesel. Technologies to be tested at laboratory (and pilot scale in FY14).

Project Quad Chart Overview

Timeline

•Project start date: June 1, 2006

•Project end date: June 30, 2014

•Percent complete:

SERC phase I: 100% SERC phase II: 100% SERC phase III: 90% SERC phase IV: 40%

Budget

Total project funding

DOE share: \$15,587,449Contractor share: \$4,414,254

- Funding received in FY 2011 (DOE & cost share): \$4.597.536
- Funding in FY 2012 (DOE & cost share): \$4,922,748
- ARRA Funding: \$0
- Years the project has been funded & average annual funding: 8 years, \$2,500,213 (DOE & cost share)

Barriers

- · Barriers addressed
- Pyrolysis
 - Tt-A Feeding dry biomass
 - TT-G Fuel synthesis and upgrading
- Syngas
 - Tt.-F. Syngas Cleanup and Conditioning
 - Tt-G. Fuels Catalyst Development

Partners & Roles

Pyrolysis

Piedmont Bio-Products: licensee

Syngas

- MS Choctaw Lignite LLC.
- Harrelson & Associates

Project Overview

Pyrolysis

Novel auger pyrolysis reactor

Bio-oil upgrading at mild conditions in the presence of pressurized hydrogen

Hydrocracking at severe conditions

Key unit operations:

- Bio-oil production
- 2) Hydrotreating

Technical barriers:

1)Tt-E Pyrolysis of biomass

Bio-oil upgrading at mild conditions in the presence of low hydrogen

Production of a high-ester boiler fuel with HHV >36

Hydrocarbon mixture with 0% water, acid value and oxygen content with HHV>44

Distillation of hydrocarbon mixture to gasoline, jet fuel and diesel equivalents

Project Overview

Syngas

Downdraft air-blown gasifier

Biomass derived syngas (bio-syngas) production



Bio-syngas cleanup and conditioning system

Key unit operations:

- Bio-syngas cleaning
- 2) Bio-syngas conversion

Technical barriers:

- 1) Tt.-F. Syngas Cleanup and Conditioning
- 2) Tt-G. Fuels Catalyst Development

Production of gasoline, jet fuel and/or diesel fuels

Cleaned bio-syngas catalytic conversion system

Distillation of hydrocarbon mixture to gasoline, jet fuel and diesel equivalents

1 - Approach

Pyrolysis

The approach is to produce high quality bio-oil with a novel design auger reactor and test design at pilot plant scale; the bio-oil is dexoxygenated in a first stage with pressurized hydrogen; this first stage can be utilized as a boiler fuel or hydrocracked to produce a hydrocarbon mixture comprised of (by simulated dist.) 55% gasoline, 30% jet fuel, 15% diesel. The research has also investigated hydrotreating with a low hydrogen gas which is estimated to conserve more than 60% of the hydrogen normally utilized during the deoxygenation stage.

1 - Approach

Syngas

The approach is to develop a pilot scale continuous process including catalyst preparation, gasification, syngas cleaning, and Fischer–Tropsch synthesis (FTS). Multifunctional catalysts are designed and tested for catalytic converting cleaned bio-syngas to biofuels. The activities, selectivity, stability, and life-time of the catalyst will be evaluated.

Pyrolysis and Syngas

This project has also utilized go/No-Go decision points numerous times as some projects were terminated for lack of results. We utilized technical metrics that ranged from indepth to cursory. This depended on the stage and perceived future success of the project.

Pyrolysis

 Design and fabrication of a 4-ton per day pyrolysis reactor (Pat. Pend.) with biomass processing equipment



Pyrolysis

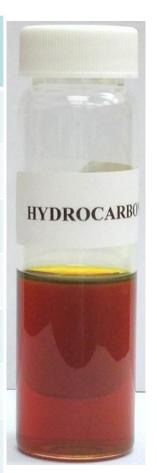
Partial deoxygenation via low hydrogen consumption

	Raw Bio-oil	Hydrogen	Low Hydrogen
Acid value	98.0	55.5	51.6
HHV, MJ/kg	16.1	34.7	36.5
Water, %	30.6	3.1	2.7
C,%	36.2	73.7	76.4
H,%	7.8	9.7	9.1
N,%	0.03	0	0
O,%	56.0	15.2	14.0

Pyrolysis

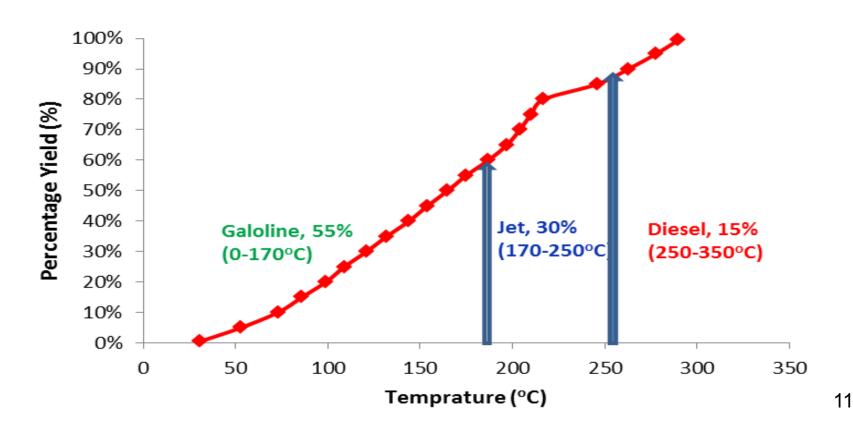
 Full deoxygenation to produce mixed hydrocarbons with zero oxygen, acid value and water.

	Raw Bio-oil	HC bio-oil (H ₂)	Diesel
Acid value	98.0	< 0.1	0
HHV, MJ/kg	16.1	43.0	45.8
Water, %	30.6	0.5	0
C,%	36.2	86.2	85.1
H,%	7.8	12.1	12.2
N,%	0.03	0.01	0
O,%	56.0	1.5	0



Pyrolysis

 Simulated distillation showing the petroleum equivalent components of the mixed hydrocarbons produced by full deoxygenation.



Pyrolysis

- Projects related to pilot plant production of bio-oil and fuels production:
 - Design and testing of a laboratory scale catalytic continuous packed bed and fluidized bed reactor for hydrotreating and hydrocracking
- Projects completed at this time:
 - Increase and utilization of anhydrosugars by spray method in the pyrolysis reactor. Project is complete, patent is pending.
 - Olefination/esterification of bio-oil to produce a high energy boiler fuel. Project complete and patent pending.
 - Produce hydroxymethyl furfural from maximized bio-oil anhydrosugars. Project complete.

Syngas

 Development of both lab scale and pilot scale biosyngas cleaning system to remove tar, oxygen, ammonia, and sulfur etc.



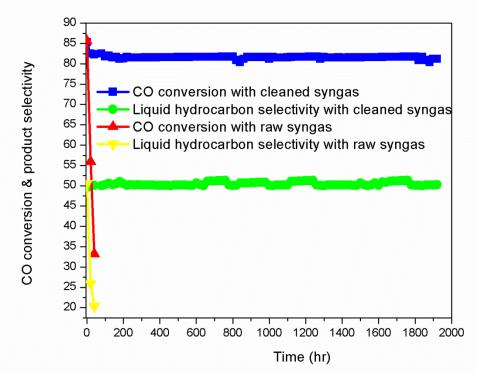


Impurities identified from bio-syngas before and after cleaning

Components	Tar	Oxygen	NH ₃	H ₂ S + COS
Before Cleaning	500-3000 ppm	0.1~2%	200-1000	200-400 ppm
After Cleaning	<1ppm	<0.1ppm	<1ppm	<1ppb

Syngas

 After bio-syngas cleaning, the selected catalyst showed better life time and stability.

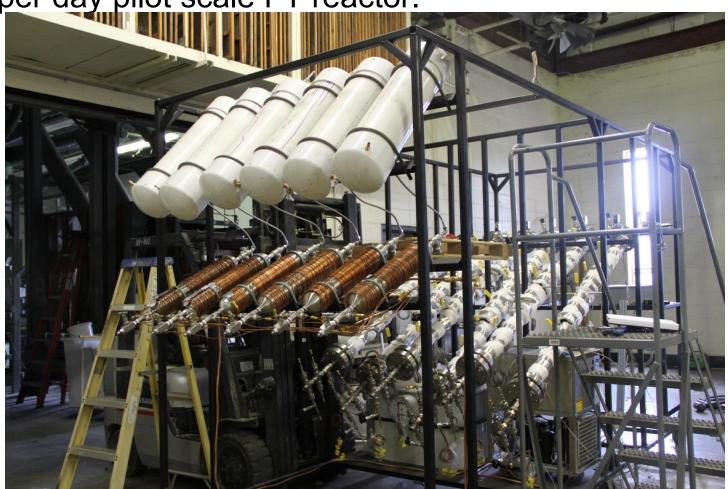


Time on stream of CO conversion, light hydrocarbon and liquid product selectivity on the catalyst at 260°C, 1000 psig, 3000 h⁻¹ with raw and cleaned bio-syngas.

Syngas

Design and fabrication of a 1-gallon liquid hydrocarbon

per day pilot scale FT reactor.



Syngas

 Development of a route to a Jet fuel sample with biosyngas catalytic conversion.

Properties	Syncrude	Distilled fuel	Jet Fuel A
Average Molecular	125.50	137.98	140.65
Weight			
Relative Density	0.804	0.810	0.815
Reid Vapor Pressure @	0.55	0.16	0.04
100°F(37.8 °C)			
Percent Carbon	86.58	86.61	86.95
Percent Hydrogen	13.29	13.36	13.05
Bromine Number (Calc)	26.16	6.12	3.18
Total Oxygen Content	0.12	0.025	0.0044
(mass %)			
Freeze point (°C)	-28.5	-37	-40



Syngas

 Development of a route to a wide-cut diesel sample with bio-syngas catalytic conversion.

Properties	Distilled fuel	No. 2 Diesel	
Specific gravity at 15 °C (Kg/m³)	840	845	
Flash point (°C)	95	75	
Average Molecular	183.6	184.5	
Weight			
Total Oxygen Content	0.015	-	
(mass %)			
Boiling point (°C)	177-355	188-345	



Syngas

- Projects related to pilot plant production of biofuels via syngas route:
 - Design and testing of bio-syngas purification system
 - Optimize the catalytic process conditions to account for the effects of impurities in the bio-syngas
 - Complete the process design and economic analysis
- Projects completed at this time:
 - Both pilot scale bio-syngas purification system and pilot scale catalytic conversion system were designed, fabricated and installed. Project complete.
 - Several multi-functional catalysts were screened and chosen for bio-syngas conversion into wide-cut diesel and jet fuel hydrocarbons in lab scale FT reactors. Project complete, 18 provisional patent filed.

3 - Relevance

- The novel auger pyrolysis technology and the capability to reduce hydrogen costs during hydrotreating contributed to the platform goal of increasing the cost competiveness of bio-oil fuels.
- The novel bio-syngas based catalytic conversion technology to produce wide-cut diesel and jet fuel range hydrocarbons contributed to the platform goal of increasing the cost competiveness of bio-fuels.
- The project is highly cognizant of the need to commercialize less costly pathways to biofuels from biopyrolysis oil and syngas.

4 - Critical Success Factors

- Technical: Production of fungible hydrocarbons equivalent to petroleum fuels;
- Market/business: Biofuels must be produced at a cost that is competitive
- Challenges to pyrolysis route: 1) Optimize the low hydrogen approach to boiler fuel and fungible hydrocarbons production; 2) Minimize catalyst costs and maximize yield of the low hydrogen approach to assure commercial success.
- Significant reduction of hydrogen cost for hydroprocessing will advance the technology of deoxgenation and greatly reduce the cost of production of fuels from bio-oil.
- Challenges to syngas route: 1) Improve the lifetime and stability of the catalysts from bio-syngas; 2) Demonstrate high conversion yields and high selectivity at pilot scale; and 3) Reduce costs through process integration.

5. Future Work

Pyrolysis

 MSU pyrolysis pilot plant will be completed; low hydrogen approach will be optimized and a low-cost catalyst will be developed.

Complete pilot plant	Quarter 1	Quarter 2	Quarter 3	Quarter 4
Optimize pyrolyzer bio-oil production	$\qquad \qquad \Rightarrow \qquad \qquad \\$			
Complete biomass processing system			>	
Produce bio- fuels in 4.5 gal stirred reactor			<u> </u>	
Testing and analysis of fuels for fungibility				<u> </u>

5. Future Work

Syngas

 MSU syngas pilot plant will be completed and tested; the economic analysis will be performed using the data from the pilot-scale process.

Complete pilot plant	Quarter 1	Quarter 2	Quarter 3	Quarter 4
Complete pilot plant via syngas route	$\qquad \qquad \Rightarrow \qquad \qquad \\$			
Test selected catalysts in the pilot bio-syngas cleaning reactor		>		
Test selected catalysts in the pilot FT reactor			\Longrightarrow	,
Perform the economic analysis				\Longrightarrow

Summary

- Relevance: Addresses barrier Tt-E to produce high quality bio-oil and produce biofuels at competitive cost. Addresses barrier Tt-F and Tt-G to produce biofuels from biosyngas.
- Approach: Laboratory scale and pilot scale production of bio-oil, syngas and biofuels.
- Technical accomplishments: Four projects completed; 4-ton per day pyrolysis reactor being optimized for bio-oil production; low hydrogen bio-oil successfully produces boiler fuel and hydrocarbons; both pilot scale bio-syngas purification system and pilot scale catalytic conversion system were installed. Several multifunctional catalysts were screened and chosen for bio-syngas conversion into biofuels.
- **Future work:** Completion of pilot plant; production of biofuels at pilot plant scale.
- Success factors and challenges: Bio-oil and biofuels produced at commercially viable cost.
- TT: Patents and numerous papers have presented this work to a wide audience.

Additional Slides

Responses to Previous Reviewers' Comments

- Reviewer: The scope and approach of the project is quite wide.
 Response: Researchers have responded by limiting their projects to only those relevant to the pilot plant activity of producing lower cost bio-oil and biofuels.
- <u>Reviewer:</u> Lack description of their technical approach.
 <u>Response:</u> The lack of description was related to our patenting program. DOE instructions are not to mention patentable technology approaches.
- Reviewer: MSU appears to be doing quality research but I would like to see better coordination with the TC platform.
 - Response: MSU is attempting to solve the barriers defined in TC platform Tt-E: Improvement in bio-oil quality and catalytic production of fuels from bio-oil. MSU has collaborated with PNNL in catalyst design and with INL in feedstock production.

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